NEW MEXICO OIL CONSERVATION COMMISSION

Form C-122 Revised 9-1-65 c/SF File

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

RECEIVED

JAN 20 '88

O. C. D.
ARTESIA, OFFICE

Type Test: [X] Initial [ ] Annual [ ] Special		Test Date: 1-7-88	
Company: Maralo, Inc. ✓	Connection: None		
Pool: ~~Baldridge~~ MOSLEY Canyon STRAWN	Formation: Strawn		Unit
Completion Date: 1-1-88	Total Depth: 10,826'	Plug Back TD: 10,265'	Elevation: 3910 GR
Farm or Lease Name: State H.K. Com	Well No.: 1		

Csg. Size	Wt.	d	Set At	Perforations: From	To
5 ½"	17#	4.892	10826	9438	9445

Tbg. Size	Wt.	d	Set At	Perforations: From	To
2 3/8"	4.7	1.995	9403	Open	Ended

Unit	Sec.	Twp.	Rge.
L	6	24S	25E

Type Well – Single – Bradenhead – G.G. or G.O. Multiple	Packer Set At	County
Single	9403'	Eddy

Producing Thru	Reservoir Temp. °F	Mean Annual Temp. °F	Baro. Press. – P_a	State
Tubing	154° @ 9432'	60°	13.2	N.M.

L	H	Gg	% CO_2	% N_2	% H_2S	Prover	Meter Run	Taps
*9442	9442	.646	.42	.538	0		4.026	Flange

FLOW DATA / TUBING DATA / CASING DATA

NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	Tubing Press. p.s.i.g.	Tubing Temp. °F	Casing Press. p.s.i.g.	Casing Temp. °F	Duration of Flow
SI							2345		PKR	CHOKE	48 Hrs.
1.					5.00	57°	2227			5/64	1 Hr.
2.	4"	X	1.000	600	10.00	60	2066			7/64	1 Hr.
3.	4"	X	1.000	610	20.00	57	1875			9/64	1 Hr.
4.	4"	X	1.000	610	22.00	58	1680			12/64	1 Hr.
5.	4"	X	1.000	615	52.00	62	1320			16/64	1 Hr.

RATE OF FLOW CALCULATIONS

NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	4.753	55.37	613.2	1.003	1.244	1.073	352
2.	4.753	78.94	623.2	1.000	1.244	1.075	502
3.	4.753	111.64	623.2	1.003	1.244	1.075	712
4.	4.753	117.09	623.2	1.002	1.244	1.075	746
5.	4.753	180.74	628.2	.9981	1.244	1.064	1135

NO.	P_r	Temp. °R	T_r	Z
1.	.91	517	1.38	.869
2.	.93	520	1.39	.866
3.	.93	517	1.38	.866
4.	.93	518	1.39	.866
5.	.93	522	1.40	.883

Gas Liquid Hydrocarbon Ratio 22.3 Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons 61.8 ° 60° Deg.
Specific Gravity Separator Gas .646 XXXXXXXXXX
Specific Gravity Flowing Fluid XXXXX
Critical Pressure 673 P.S.I.A. ____ P.S.I.A.
Critical Temperature 372 R ____ R

P_c 2358.2 P_c^2 5561.1

	NO	P_t^2	P_w	P_w^2	$P_c^2 - P_w^2$
**	1	2982.2	2306.1	5318.1	243.0
**	2	2787.2	2153.1	4635.8	925.3
**	3	2544.2	1965.4	3862.8	1698.3
**	4	2272.2	1758.2	3091.3	2469.8
**	5	1834.2	1429.3	2042.9	3518.2

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.581$

(2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.319$

$AOF = Q\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.497$

Post ID-2
2-5-88
Comp. & Strawn

Absolute Open Flow 1,497 Mcfd @ 15.025 Angle of Slope θ 59 Slope, n .604

Remarks: * BHP Instrument set @ 9442'- Well Made 6.45 Bbls. 61.8 @ 60° condensate during test. Also produced 3.27 Bbls. H20.
Shut-In BHP = 3117.2 (Psia)
** Flowing BHP.

Approved By Commission:	Conducted By:	Calculated By:	Checked By:
	R.W.	J.B.M.	J.B.M.