

APR 10 2015

Form 3160-5  
(August 2007)

UNITED STATES  
DEPARTMENT OF THE INTERIOR  
BUREAU OF LAND MANAGEMENT

NOV 06 2014

FORM APPROVED  
OMB No. 1004-0137  
Expires: July 31, 2010

**SUNDRY NOTICES AND REPORTS ON WELLS**  
*Do not use this form for proposals to drill or to re-enter an abandoned well. Use Form 3160-3 (APD) for such proposals.*

5. Lease, Serial No. **SF-078741**

6. If Indian, Allottee or Tribe Name

**SUBMIT IN TRIPLICATE - Other instructions on page 2.**

1. Type of Well  
 Oil Well  Gas Well  Other

7. If Unit of CA/Agreement, Name and/or No.  
**San Juan 30-6 Unit**

8. Well Name and No.  
**San Juan 30-6 Unit 11A**

2. Name of Operator  
**Burlington Resources Oil & Gas Company LP**

9. API Well No.  
**30-039-25898**

3a. Address  
**PO Box 4289, Farmington, NM 87499**

3b. Phone No. (include area code)  
**(505) 326-9700**

10. Field and Pool or Exploratory Area  
**Blanco MV/Basin DK**

4. Location of Well (Footage, Sec., T., R., M., or Survey Description)  
**Surface UNIT D (NWNW), 640' FNL & 510' FWL, Sec. 23, T30N, R6W**

11. Country or Parish, State  
**Rio Arriba, New Mexico**

**12. CHECK THE APPROPRIATE BOX(ES) TO INDICATE NATURE OF NOTICE, REPORT OR OTHER DATA**

TYPE OF SUBMISSION	TYPE OF ACTION			
<input checked="" type="checkbox"/> Notice of Intent	<input type="checkbox"/> Acidize	<input type="checkbox"/> Deepen	<input type="checkbox"/> Production (Start/Resume)	<input type="checkbox"/> Water Shut-Off
<input type="checkbox"/> Subsequent Report	<input type="checkbox"/> Alter Casing	<input type="checkbox"/> Fracture Treat	<input type="checkbox"/> Reclamation	<input type="checkbox"/> Well Integrity
<input type="checkbox"/> Final Abandonment Notice	<input type="checkbox"/> Casing Repair	<input type="checkbox"/> New Construction	<input type="checkbox"/> Recomplete	<input checked="" type="checkbox"/> Other <u>Remove tubing</u>
	<input type="checkbox"/> Change Plans	<input type="checkbox"/> Plug and Abandon	<input type="checkbox"/> Temporarily Abandon	<u>strings &amp; packer &amp;</u>
	<input type="checkbox"/> Convert to Injection	<input type="checkbox"/> Plug Back	<input type="checkbox"/> Water Disposal	<u>Commingle</u>

13. Describe Proposed or Completed Operation: Clearly state all pertinent details, including estimated starting date of any proposed work and approximate duration thereof. If the proposal is to deepen directionally or recomplete horizontally, give subsurface locations and measured and true vertical depths of all pertinent markers and zones. Attach the bond under which the work will be performed or provide the Bond No. on file with BLM/BIA. Required subsequent reports must be filed within 30 days following completion of the involved operations. If the operation results in a multiple completion or recompletion in a new interval, a Form 3160-4 must be filed once Testing has been completed. Final Abandonment Notices must be filed only after all requirements, including reclamation, have been completed and the operator has determined that the site is ready for final inspection.)

**Burlington Resources intends to remove the tubing strings and packer on the subject well and commingle production from the Blanco MV and the Basin DK per the attached procedure, & wellbore schematic. An H2S Contingency plan is attached. DHC application has been submitted and a copy has been sent to the BLM. The work will not be started until the DHC application has been approved.**

**Notify NMOCD 24 hrs prior to beginning operations**

**BLM'S APPROVAL OR ACCEPTANCE OF THIS ACTION DOES NOT RELIEVE THE LESSEE AND OPERATOR FROM OBTAINING ANY OTHER AUTHORIZATION REQUIRED FOR OPERATIONS ON FEDERAL AND INDIAN LANDS**

14. I hereby certify that the foregoing is true and correct. Name (Printed/Typed) **Kenny Davis** Title **Staff Regulatory Technician**  
Signature  Date **11/6/2014**

**THIS SPACE FOR FEDERAL OR STATE OFFICE USE**

Approved by **Troy Salyers** Title **PE** Date **12/8/2014**  
Office **FFO**

Title 18 U.S.C. Section 1001 and Title 43 U.S.C. Section 1212, make it a crime for any person knowingly and willfully to make to any department or agency of the United States any false, fictitious or fraudulent statements or representations as to any matter within its jurisdiction.

(Instruction on page 2)

FV

**ConocoPhillips**  
**SAN JUAN 30-6 UNIT 11A**  
**WO - Commingles**

Lat 36° 48' 12.456" N

Long 107° 26' 20.328" W

**PROCEDURE**

1. Hold pre-job safety meeting. Comply with all NMOCD, BLM, and COPC safety and environmental regulations. Test rig anchors prior to moving in rig.

2. MIRU work over rig. Check casing, tubing, and bradenhead pressures and record them in Wellview. If there is pressure on the BH, contact Wells Engineer.

**Note: Well is a dual Mesa Verde and Dakota well with a 5-1/2" Baker Model "D" packer @ 6200'.**

3. Remove existing piping on casing valve. RU blow lines from casing valves and begin blowing down casing pressure. Kill both Mesa Verde and Dakota sides with 2% KCl as necessary. **Attempt to pump down short string - Possible trapped pressure below shallow fish @ 29' in short string.** Ensure well is dead or on vacuum. Pick up handling tools for 1-1/2" IJ tubing.

4. ND wellhead and NU BOPE with 1-1/2" offset pipe rams and offset spool. Install 1-1/2" H-prep subs on both strings (short string: 1-1/2" IJ, long string 1-1/2" EUE). Pressure and function test BOP to 250 psi low and 1000 psi over SICP high to a maximum of 2000 psi held and charted for 10 minutes as per COP Well Control Manual. Record pressure test in Wellview. PU and remove tubing hanger on short string (Mesa Verde).

5. TOOH and LD short string of 1-1/2" IJ tubing (per pertinent data sheet). **Possible trapped pressure below shallow fish @ 29' in short string. Make note of corrosion, scale, or paraffin and save a sample to give to the engineer for further analysis.**

6. Ensure well is dead and will stay dead during ram change. Change pipe rams and handling tools to 1-1/2" EUE, non-offset and remove offset spool. Function test pipe rams. Unseat seal sleeve from Baker Model "D" packer with straight pick up. PU and remove long string (Dakota) tubing hanger. If possible, pick up and land new 2-3/8" tubing hanger with cross-overs and pressure test pipe rams. **Note: Schematic shows fish in wellbore above packer but records do not mention any un-recovered fish left in the hole besides the fish in the Mesa Verde tubing at 29'. Wireline on 4/13/2014 tagged fill at 6142'.**

7. TOOH and LD long string of 1-1/2" EUE tubing (per pertinent data sheet). Make note of corrosion, scale, or paraffin and save a sample to give to the engineer for further analysis.

8. If tubing head needs to be replaced set an RBP at ~1000'. Test RBP. Replace the tubing head. If RBP is set, leave until BOP is set up in next step.

9. Ensure barriers are holding. Change pipe rams and handling tools to accommodate 2-3/8" tubing and NU annular. Function test and pressure test BOP to 250 psi for the low pressure test 1000 psi over SICP high to a maximum of 2000 psi held and charted for 10 minutes as per COP Well Control Manual. Retrieve RBP if it was set.

10. **Note: 5-1/2" liner top at 3395'. TIH with packer plucker, drill collars, and 2-3/8" tubing and retrieve 5-1/2" Baker Model "D" Packer @ 6200'. TOOH and LD packer and plucker.**

11. PU 4-3/4" string mill and bit and CO to PBTD @ 7840' using the air package. TOOH. LD mill and bit. If fill could not be CO to PBTD, call Wells Engineer to inform how much fill was left and confirm/adjust landing depth.

12. TIH with tubing using Tubing Drift Procedure (detail below).

		<u>Tubing and BHA Description</u>	
<b>Tubing Wt/Grade:</b>	4.7#, J-55	1	2-3/8" Expendable Check
<b>Tubing Drift ID:</b>	1.901"	1	2-3/8" (1.78" ID) F-Nipple
		1	2-3/8" Tubing Joint
<b>Land Tubing At:</b>	7810'	1	2-3/8" Pup Joint (2' or 4')
<b>KB:</b>	12'	+/- 245	2-3/8" Tubing Joints
		As Needed	2-3/8" Pup Joints to space
		1	2-3/8" Tubing Joint

13. Ensure barriers are holding. ND BOPE, NU Wellhead. Pressure test tubing slowly with an air package as follows: pump 3 bbls pad, drop steel ball, pressure tubing up to 500 psi, and bypass air. Monitor pressure for 15 mins., then complete the operation by pumping off the expendable check. Note in Wellview the pressure in which the check pumped off. Purge air as necessary. Notify the MSO that the well is ready to be turned over to Production Operations. RDMO.

## Tubing Drift Check

### PROCEDURE

1. Set flow control in tubing. With air, on location, use expendable check. With no air on location, use wire line plug.
2. RU drill tool to a minimum 70' line. Drift tool will have an OD of at least the API drift specification of 1.901" for the 2 3/8", 4.7# tubing, and will be at least 15" long. The tool will not weigh more than 10# and will have an ID bore the length of the tool, so fluids may be pumped through the tool if it becomes stuck.
3. Drop the tool into the tubing string and retrieve it after every 2 joints of tubing run in hole. If any resistance to the tool movement is noticed, going in or out, that joint will be replaced.

NOTE: All equipment must be kept clean and free of debris. The drift tool will be measured with calipers before each job, to ensure the OD is the correct size for the tubing being checked. The maximum allowable wear of the tool is 0.003".

Current Schematic

ConocoPhillips

Well Name: SANDAN OPER UNIT 111

API/USVI 3003925898	Surface Leg # Location 023-030N-006W-D	Field Name SANDAN OPER UNIT 111	USE Well No.	State Province NEW MEXICO	Well Configuration Type
Ground Elevation (ft) 6,438.00	Original MDRTY Elevation (ft) 6,450.00	Original Distance (ft) 12.00	IS-Casing Top Distance (ft) 12.00	IS-Casing Bottom Distance (ft) 6,450.00	IS-Tubing String Distance (ft) 6,450.00

Original Hole, 10/6/2014 4:53:01 PM

Vertical schematic (actual)		MD (ftKB)	Formation Tops
Tubing; 1 1/2 In; 12.0 ftKB; 45.6 ftKB		12.1	
Fish; 29.0-34.0; On 7/26/2014, wireline tagged junk in the tubing 1' below ground level. Attempts to retrieve it failed. The junk had been beat down to 29' prior to becoming completely stuck.		34.1	
Tubing Sub; 1 1/2 In; 45.6 ftKB; 65.6 ftKB	1; Surface; 9 5/8 In; 0.000 In; 12.0 ftKB; 244.5 ftKB SINGLE; 12.0-245.0; 8/13/1998; Cemented w/ 200 sx Class B cement. Circulated 17.5 sx cement to surface.	65.6 244.4	
Tubing; 1.90 In; 2.76 lb/ft; J-55; 12.0 ftKB; 5,908.9 ftKB	STAGE 2 OF 2; 12.0-2,803.0; 8/17/1998; Cement 2nd stage w/ 300 sx Class B cement. Circulated 23 bbls cement to surface.	2,544.9	OJO ALAMO KIRTLAND
Tubing; 1 1/2 In; 65.6 ftKB; 6,195.9 ftKB	2; Intermediate; 7 In; 6,456 In; 12.0 ftKB; 3,552.5 ftKB	2,803.1	PICTURED CLIFF
Cut and recovered 5-1/2" casing @ 3395'	STAGE 1 OF 2; 2,803.0-3,560.0; 8/17/1998; Cemented 1st stage w/ 170 sx Class B 50/50 cement. Circulate 1 bbl cement to dv tool	3,395.0	
Profile Nipple; 1.90 In; 5,908.9 ftKB; 5,909.7 ftKB	PERF - LEWIS; 4,120.0-4,844.0; 12/4/1998	3,509.5	GLIFFHOUSE
Tubing; 1.90 In; 2.75 lb/ft; J-55; 5,909.7 ftKB; 5,942.1 ftKB	PERF - CLIFF HOUSE / MENELEE UPPER; 4,990.0-5,424.0; 12/3/1998	4,990.2	MENELEE
Mule Shoe Guide; 1.90 In; 5,942.1 ftKB; 5,942.4 ftKB	PERF - POINT LOOKOUT / MENELEE LOWER; 5,493.0-5,948.0; 12/3/1998	5,423.9	POINT-LOOKOUT
Seal Assembly; 1 1/2 In; 6,195.9 ftKB; 6,196.9 ftKB		5,909.8	
Fish; 6,194.0-6,200.0; There are wireline tools stuck in the Mesaverde side of wellbore		5,942.0	
Packer; 6,200.0-6,202.0		5,956.0	MANOOS
Tubing; 1 1/2 In; 6,196.9 ftKB; 7,762.0 ftKB		6,195.9	
Seal Nipple; 1 1/2 In; 7,762.0 ftKB; 7,763.0 ftKB		6,200.1	
Tail Joint; 1 1/2 In; 7,763.0 ftKB; 7,798.0 ftKB		6,819.9	GALLUP GREENHORN GRANERGS
PBTD; 7,840.0	PERF - DAKOTA; 7,874.0-7,804.0; 12/3/1998	7,801.0	DAKOTA
	3; Liner; 5 1/2 In; 4,950 In; 3,395.0 ftKB; 7,879.6 ftKB	7,726.0	
	SINGLE STAGE; 3,670.0-7,884.0; 8/21/1998; Cement w/ 250 sx Class H 50/50 poz cement. TOC @ 3670' (CBL 8/98)	7,763.1	
		7,804.1	
		7,877.6	
		7,879.6	

**ConocoPhillips  
P&A Rig  
H<sub>2</sub>S Contingency Plan**

**SAN JUAN 30-6 UNIT 11A**

640' FNL & 510' FWL, Spot D, Section 23, T30N, R06W  
Lat 36° 48' 12.456" N Long 107° 26' 20.328" W

Prepared by	Jake Morrissette
Area Engineer	Diana Guo
Rig Supervisor	Joe McElreath
COPC Rig Superintendent	Stan Terwilliger
COPC Expense Rig Manager	Mark Chambers

## Table of Contents

Introduction	3
Scope of Work	
Radii of Exposure Map	
General Emergency Action	4
Communication Directory	5 - 6
List of Public Areas	7
Responsibilities	8 - 10
Igniting the Well	11
Precautionary Measures	12
Special Safety Training	13
Equipment and Material Specifications	13
H2S Contingency Equipment Checklist	14
Effects of H2S and Other Gases on Workover Operations	15 - 16
H2S Effects	17
Sulfide Testing Procedure	18
Definitions	19
References	20

## Introduction

ConocoPhillips is planning a to commingle the Mesa Verde and Dakota of the SAN JUAN 30-6 UNIT 11A.

Hydrogen sulfide ( $H_2S$ ) may be present in the gas formation. Hydrogen sulfide ( $H_2S$ ) is a flammable and highly toxic gas, which in relatively small concentrations, can have adverse effects on people and equipment (refer to the section - Effects of  $H_2S$ ).

Precautionary measures concerning  $H_2S$  in this plan have been formulated based on the following assumptions:

ConocoPhillips is expecting the possibility of  $H_2S$  from this location, although gas samples previously analyzed or taken from this well location indicate a concentration of less than 100ppm, levels of >100 ppm can be expected from this particular well based on BLM recommendation for this well site. This contingency plan will be provided should  $H_2S$  levels arise during workover operations.

Based on Radius of Exposure (ROE) equations provided in the Department of Interior, Bureau of Land Management, Part II, 43 CFR Part 3160, Onshore Order No. 6, Hydrogen Sulfide Operations, the 100 ppm  $H_2S$  ROE for a hypothetical well is 1.1 feet and the 500 ppm  $H_2S$  ROE is 0.5 feet. These ROE are based upon 10 ppm  $H_2S$  gas at a rate of 0.1 MMSCFD which includes a safety margin.

No residences, schools, business or parks where the public could reasonably be expected to frequent fall within either the 100 ppm ROE or the 500 ppm ROE. The only roads in the ROE are dirt well servicing roads. The SAN JUAN 30-6 UNIT 11A is located 300 yards away from a lease road

This plan has been designated as a guide for well requirements and special considerations to provide for safe and efficient servicing operations in the presence of hydrogen sulfide.



500 ppm ROE  
100 ppm ROE

Red Circle  
Blue Circle

0.5'  
1.1'

## General Emergency Action

In the event an emergency situation occurs, the following action shall be initiated:

1. If the H2S alarm sounds, stop the workover activities immediately.
2. Evacuate quickly to the pre-designated "Safe Briefing Area".
3. Those who must enter the hazard area must wear self-contained breathing apparatus and use other appropriate safety equipment. Secure rig and close well in, if necessary, using self-contained breathing apparatus and other appropriate safety equipment. (Use the "buddy system" at all times.)
4. Account for all personnel and take appropriate action as necessary for personnel safety.
5. Raise appropriate color warning flag to describe the type of emergency.

The Rig Supervisor will assess the situation and assign duties to various persons to bring the situation under control. The Rig Supervisor will advise the ConocoPhillips Rig Superintendent as soon as the emergency will permit. In the event of a well kick, procedures outlined in the Operations Plan will be followed. Stations to be manned and duties to be performed will be discussed in the safety meeting and captured in the JSA prior to commencing rig operations.

Notification of local law enforcement agencies, residents and emergency vehicles as per the following Communications Directory, will be assigned by the ConocoPhillips Rig Superintendent.

Any press inquiries are to be referred to the ConocoPhillips Expense Rig Manager (Mark Chambers).

## Contact Information

ALL AREA CODES ON THIS PAGE ARE 505 UNLESS OTHERWISE INDICATED

### Expense Rig Department

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<u>Name</u>	<u>Office</u>	<u>Home</u>	<u>Cell</u>
<b>Expense Rig Manager</b>			
Mark Chambers	326-9570	432-2447	215-2354
<b>Expense Rig Superintendents</b>			
Kelly Kolb	326-9582	327-2177	320-4785
Stanley Terwilliger	599-4066	793-4993	320-5921
Lyle Ehrlich	599-4002	327-7459	320-2613
<b>Production Engineering</b>			
Rob Stanfield	324-5168		320-2862
Chris Pierson	326-9776		860-2533
Dusty Mars	324-6147		215-1854
<b>Wells Engineering</b>			
Jake Morrisette	326-9872		215-7063

### Health, Safety & Environmental Department

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<u>Name</u>	<u>Office</u>	<u>Home</u>	<u>Cell</u>
<b>HSE Manager</b>			
Sharon Zubrod	326-9793	436-2288	330-5395
<b>HSE Representatives</b>			
Shannon Donnelly	324-6181	(907)-394-0520	215-82985
Bryan Salazar	599-3413		320-7365
<b>Contract Safety</b>			
Steve Martinez (DMX Safety Alliance)	325-7233		320-0544
Ginger Lockeby (Advanced Safety)	324-0575		320-6250

### Well Control Resources

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<u>Name</u>	<u>Office</u>	
Cudd Well Control Co.	(713)-849-2769	24 hr Contact

## Contact Information

ALL AREA CODES ON THIS PAGE ARE 505 UNLESS OTHERWISE INDICATED

### Agencies

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#### Name

#### **State Police/Sheriff/City Police**

New Mexico State Police		325-7547	
San Juan County Sheriff's Department	911	334-6622	
San Juan County Police Department	911	334-6622	
Ambulance	911	334-6622	
Fire Department	911	334-6622	
Air Care 1	911	599-6046	1-800-452-9990

#### **Bureau of Land Management**

Farmington Office		599-8900	
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#### **New Mexico Oil Conservation Division**

Aztec Office		334-6178	
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#### **Hospitals**

San Juan Regional Medical Center		325-5011	
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## List of Public Areas

No residences, schools, business, parks or other areas where the public could reasonably be expected to frequent were found to be within the 100 ppm ROE or 500ppm ROE. Included is an aerial map indicating the physical location of the Radius of Exposure. All land within the 100 ppm radius of exposure from the wellhead is still on the wellpad.



500 ppm ROE  
100 ppm ROE

Red Circle  
Blue Circle

0.5'  
1.1'

## Responsibilities

### All Personnel

All Personnel on the ConocoPhillips location shall be familiarized with the procedures outlined in this directive.

All personnel will attend to their personal safety first.

Report to the "Safe Briefing Area" and follow the instructions of the rig supervisor.

### Rig Supervisor

Ensure that a Safety Contractor representative and Toolpusher are on site.

It is the responsibility of the Rig Supervisor to see that all personnel on the ConocoPhillips location observe these safety and emergency procedures.

The Rig Supervisor will advise the ConocoPhillips Rig Superintendent whenever the procedures as specified herein are complied with or cannot be followed. A checklist (attached) will be utilized. One (1) completed copy of the checklist will be forwarded to the ConocoPhillips Rig Superintendent and one copy to ConocoPhillips HSE Department.

The Rig Supervisor shall keep the number of personnel on location to a minimum during hazardous operations.

The Rig Supervisor shall be trained in the use of all safety equipment and completely briefed on safety and emergency procedures. This shall include full knowledge of the requirements in this contingency plan.

It is the responsibility of the Rig Supervisor to see that all Contractors have been adequately trained in the handling of emergency situations. He should satisfy himself that this is the case. He should notify the ConocoPhillips Rig Superintendent if the Contractor fails to fulfill this responsibility.

If an unexpected emergency occurs, or the H2S alarm sounds, the Rig Supervisor (or Toolpusher) will assess the situation and will advise all personnel what conditions exist. Action to be taken under each of three possible conditions is as follows:

#### **CONDITION I - POTENTIAL DANGER TO LIFE**

(such as hazardous amount of toxic gasses detected at surface)

Order nonessential personnel out of the potential danger area and display the YELLOW CONDITION I warning sign and flag.

Order all essential personnel to check their safety equipment to see that it is working properly and in the proper location (see supervisor's checklist). Persons without respiratory protection cannot work in the hazard area.

Notify Rig Superintendent of condition and action taken.

Increase gas monitoring activities and continue operations as appropriate.

**CONDITION II - MODERATE DANGER TO LIFE**  
(such as circulating out a potentially toxic gas kick)  
**IN ADDITION TO CONDITION I REQUIREMENTS**

Display only the ORANGE CONDITION II warning sign and flag.

Direct corrective action to control flow of gas.

Set up roadblocks and restrict personnel movements to a minimum.

**CONDITION III - EXTREME DANGER TO LIFE**  
(when it appears that well control will be lost)  
**IN ADDITION TO CONDITION I and II REQUIREMENTS**

Display only the RED CONDITION III warning sign and flag.

Contact and request local police to evacuate people and to control traffic within the danger zone. Should the condition be immediately dangerous to the public, take necessary life saving action until local police arrive.

Ignite the well if necessary. (See the following section - Igniting the Well.)

Contract Rig Supervisor (Toolpusher)

A Toolpusher will be on-site at all times when a contingency plan is in place.

In the absence or incapacitation of the Rig Supervisor, the Toolpusher will assume all responsibilities designated herein to the Rig Supervisor.

Assist the Rig Supervisor and Safety Representative in training crews for handling emergency situations.

Will be trained for all well control or emergency situations as contained herein and how to properly use all safety equipment.

HSE Department

Shall provide safety and environmental information and guidance when required.

Shall review and approve any changes in safety or environmental procedures.

Shall assist as appropriate with operating and maintenance procedures for the safety equipment called for in this plan.

Shall assist with arranging initial training on safety procedures and equipment. Shall provide assistance as needed for follow up training.

Rig Contractor

Shall have personnel properly trained in First Aid/CPR and H2S Awareness.

Shall keep personnel trained in use of safety equipment and safety procedures.

Visitors, Service Personnel (Vendors) and Others

Only personnel authorized by the Rig Supervisor shall be permitted to enter area when an emergency condition exists.

Shall be permitted to enter area under an emergency condition only if needed and then only after being properly instructed in use of safety equipment and have necessary equipment issued or available.

Vendors must have all of their personnel trained in H2S procedures who will be on location during any work which could result in an H2S release through rig release.

## Igniting the Well

### Responsibility

The decision to ignite the well is the responsibility of the ConocoPhillips Rig Superintendent. However, the decision should be made only as a last resort and in a situation where it is clear that:

Human life or property is endangered.

There is no hope of controlling the blowout under the prevailing conditions at the well.

In all cases, an attempt should be made to notify the Rig Superintendent of the plans to ignite the well, if time permits. However, the Rig Superintendent and Rig Supervisor must not delay a decision if human life is threatened.

**If the well is ignited, the burning H<sub>2</sub>S will be converted to sulfur dioxide (SO<sub>2</sub>), which is also highly toxic. Do not assume that the area is safe after the well is ignited. Follow through with all plans to evacuate endangered persons.**

### Means of Ignition

In preparation for igniting the well, keep unnecessary persons in the "Safe Briefing Area". A two person team is required for the actual ignition. Both team members will wear self-contained breathing units and will have 200 feet retrieval ropes attached to safety harnesses. One team member is responsible for checking the atmosphere for explosive gasses with the quad gas monitor. The other member is responsible for igniting the well. Persons remaining in the "Safe Briefing Area" will closely watch the ignition team; and should either man be overcome, they will immediately pull him to safety by the retrieval ropes and apply revival measures.

The primary method for igniting the well will be with a 25 mm meteorotype flare gun. (The location of the flare gun (if available) will be discussed during and noted in the JSA.) These guns have a range of approximately 500 feet. If this method fails or well conditions are such that a safer or better method is apparent, then an alternate method should be used.

Always ignite the well from upwind and do not approach the well any closer than warranted.

Select a location to fire the flare gun that provides maximum protection to the ignition team (behind equipment) while keeping in visible sight by personnel in the "Safe Briefing Area".

Choose a location that has good accessibility and from which retreat can easily be made.

**Before firing the flare gun or igniting flammable material, check the atmosphere at your location for combustible gasses with explosimeter.**

## Precautionary Measures

Two areas shall be designated as safe briefing areas, each located, as a minimum: 150 feet from the wellhead and vent discharge area; spaced 160 degrees apart on an arc, with the wellhead as the center point; and as best suited for topographical considerations and prevailing winds. Six NIOSH approved Positive Pressure SCBAs shall be located as follows: one in the Rig Supervisor's vehicle, one in the Tool Pusher's trailer, and two at each of the "Safe Briefing Areas". Packs should be readily accessible and properly protected from exposure to the elements.

Emergency equipment shall be on location as described in the H2S Contingency Equipment Checklist.

A copy of all emergency telephone numbers shall be posted on the rig equipment trailer, at the "Safe Briefing Areas" and in the Rig Supervisor's vehicle.

Wind direction indicators shall be located where at least one can be viewed from any position on the location.

An automatic hydrogen sulfide (H<sub>2</sub>S) monitor shall be provided, with detectors placed at the flow line and rig floor. Either of these detectors shall be capable of sensing a minimum of 5 ppm H<sub>2</sub>S in air and shall be able to independently activate visual and audio alarms. Both the visual alarm and the audible alarm will be activated at 10 ppm. The audible alarm must be capable of alerting people at any point on the location.

A sign that reads, "Caution - Poisonous Gas May be Present", will be posted at the last intersection leading to location.

If conditions warrant, two (2) explosion-proof, 24 inch or larger, electric fans will be located: (a) one on the rig floor to blow fumes downwind; (b) the second under the rig floor to clear gas from the substructure.

The well-site shall be equipped with commercial communications. The equipment should be located for safe access and should not be an ignition source.

The Rig Supervisor's vehicle should always be parked a safe distance (at least 100 feet) from the rig, and in an upwind direction when feasible.

For all well kicks, the Operations Plan will be followed. All rig personnel shall be trained, and drills shall be conducted to insure proper well control procedures.

The checklist of all emergency equipment (see Rig Supervisor's checklist) shall be completed prior to starting work as identified in the Introduction. The Rig Supervisor shall inspect the equipment with assistance, as needed, from ConocoPhillips HSE personnel as to working condition, proper placement, etc. The inspection will be noted on the checklist. A copy of the checklist will be placed in the Rig Supervisor's files and one copy each will be provided to the Rig Superintendent and HSE Department.

A Safety Contractor will be on-site monitoring head count, enforcing that all personnel on location will have no facial hair in face piece seal area, keeping only essential personnel on location, and all personnel on location are trained to work in an H<sub>2</sub>S environment. They will also be the designated rescue agent for injured.

## Special Safety Training

The minimum training for personnel working in affected areas shall include the following elements:

Hazards, characteristics and symptoms of hydrogen sulfide (H<sub>2</sub>S), sulfur dioxide (SO<sub>2</sub>), carbon monoxide (CO), methane gas, and other hazardous substances as may be appropriate. Effects of these substances are discussed in a section that follows.

Effect on metal components of the system.

Safety precautions to include possible sources at the site.

Operation of safety equipment and life support means and systems.

Corrective action and shutdown procedures.

Detection and measurements of H<sub>2</sub>S, CO and combustible gas.

### **THE RIG SUPERVISOR ON LOCATION SHALL BE RESPONSIBLE FOR THE OVERALL ON-SITE OPERATION, INCLUDING THE SAFETY AND TRAINING PROGRAM.**

All personnel, contracted or employed on an unscheduled basis, shall be trained as a minimum in the severity of H<sub>2</sub>S and other toxic gasses, safety precautions, evacuation procedures, and as appropriate, the use of respiratory protection equipment. This training shall be completed prior to entering the H<sub>2</sub>S location. Visitors shall also be instructed regarding these matters.

To promote efficient safety procedures, an on-site toxic gas safety program, which includes a drill and training session, shall be established for all crews. Records of attendance shall be maintained on the workover rig.

## Equipment and Material Specifications

Wellhead and blowout equipment is to conform as per Operations Plan.

BOP equipment will be tested to pressure rating prior to starting any work, with all testing witnessed and recorded by the Rig Supervisor.

The BOP will be operationally tested on every trip. BOP drills will be held prior to operation with the potential to release H<sub>2</sub>S, these will be recorded on the Rig Supervisor's report.

Downhole equipment planned for this well will be listed in the Operations' Plan. Ensure that any equipment has been designed in accordance with ConocoPhillips' requirements for sour service.

## H2S Contingency Equipment Checklist

- |       |       |  |
|-------|-------|--|
| _____ | (All) | Personnel training with attendance records on site.  |
| _____ | (2)   | Cleared land areas for use as "Safe Briefing Areas", 150' from wellhead, and 160° apart  |
| _____ | (1)   | Warning sign with current well condition indicator, located at last intersection to location so vehicles may have turn-around area.  |
| _____ | (3)   | Wind direction indicators, located to provide visibility from any place on location.   |
| _____ | (3)   | No Smoking signs on drive posts.   |
| _____ | (3)   | Safe Briefing Area signs on drive posts.   |
| _____ | (2)   | Fans - electric motor driven and explosion proof; one located on rig floor, and one located in substructure (if conditions warrant).   |
| _____ | (1)   | H2S monitor (continuous) located on rig floor with detectors (sensitivity of 5 ppm in air) located at the flow line, mud pits discharge, and on the rig floor.   |
| _____ | (1)   | Alarm system capable of individual activation by any detector with maximum settings as follows: visual and audible alarms at 10 ppm (audible must be capable of alerting personnel at any point on location).                      |
| _____ | (5)   | Niosh Approved Positive Pressure SCBAs - 30 min. self-contained breathing apparatus: one in the supervisor's office, and two at each of the "Safe Briefing Areas". Easily accessible, and protected from exposure to the elements. |
| _____ | (3)   | Condition warning flags (1 each yellow, orange, and red).  |
| _____ | (1)   | Trailer - full enclosure, at location entrance (based on prevailing winds), containing everything below  |
| _____ | (1)   | Length of Stain Polymetric Tube Type Detectors with lower range tubes for CO2, H2S, and SO2  |
| _____ | (1)   | MSHA Explosimeter (or equivalent).   |
| _____ | (1)   | Flare gun - 25mm meteor type with flares.  |
| _____ | (2)   | Derrick safety belts with 10' tail ropes.  |
| _____ | (2)   | 200' retrieval ropes.  |
| _____ | (3)   | Hearing protectors - muff type.  |
| _____ | (1)   | First aid kit - 25 unit.   |
| _____ | (3)   | Flashlights w/batteries (explosion-proof & watertight).  |
| _____ | (1)   | Disinfectant, cleaner, and towels for breathing apparatus  |
| _____ | (1)   | Inspection records for breathing apparatus and air supply.   |
| _____ | (1)   | Fire extinguisher (rated 60:BC).   |
| _____ | (4)   | Emergency telephone numbers in plastic weatherproof holders located at: rig equipment trailer; Rig Supervisor's vehicle; in both Safe Briefing Areas   |

## Effects of H2S and Other Gases on Workover Operations

### Hydrogen Sulfide - H<sub>2</sub>S

Hydrogen sulfide is a colorless, flammable, extremely poisonous gas. It is 1.2 times as heavy as air and will accumulate in low areas. It forms an explosive mixture with air between 4.3 and 46.0 percent by volume. It can be detected by smell at a concentration in air of only 0.02 ppm. Exposure to 10 ppm can be tolerated up to 8 hours without respiratory equipment. Respiratory equipment is required to protect workers should conditions exceed the foregoing allowable exposure limit. Concentrations in excess of 20 ppm have an effect on the olfactory nerve which deadens the sense of smell. Unconsciousness can occur without warning within seconds of inhalation at concentrations above 500 ppm.

Concentration Percentage %	Parts Per Million ppm	Physical Effect
0.001	10	Obvious and unpleasant odor. Current ACGIH TLV allowed for 8 hour exposure.
0.01	100	Kills smell in 3 to 15 minutes, may sting eyes & throat.
0.02	200	Kills smell shortly, stings eyes & throat.
0.05	500	Dizziness, breathing ceases in a few minutes. Needs prompt artificial respiration.
0.07	700	Unconscious quickly; death will result if not rescued promptly.
0.1	1000	Unconscious at once; followed by death within minutes.

### Sulfur Dioxide - SO<sub>2</sub>

Sulfur dioxide is a colorless, nonflammable, intensely irritating gas and 2.2 times heavier than air. It is a by-product of combustion of hydrogen sulfide and is highly toxic. Exposure to 2 ppm can be tolerated for a maximum of 8 hrs. Respiratory equipment will be available and should be used by personnel measuring SO<sub>2</sub> concentration downwind from a flare.

### Methane - CH<sub>4</sub>

Methane is the major component of natural gas and is colorless, odorless and extremely flammable. The chief danger from methane is explosion. Mixture of CO<sub>2</sub>, H<sub>2</sub>S and CH<sub>4</sub> will burn if the total H<sub>2</sub>S and CH<sub>4</sub> content, in any ratio, is above 25 percent. Also the presence of methane causes an oxygen deficient environment and requires adequate ventilation for breathing.

### Carbon Monoxide - CO

Carbon monoxide is a colorless, odorless toxic gas. Its toxicity results from preferential reaction with the hemoglobin in the blood; however, it has no unique toxic action on any of the bodily

tissues. CO displaces oxygen from hemoglobin and reduces the oxygen carrying capability of the blood.

The primary danger from CO is that it binds with hemoglobin within the blood, thereby preventing oxygen / blood transfer. Respiratory equipment should be considered for atmospheres containing greater than 25 ppm. Exposure to 25 ppm is allowed up to 8 hours; however, at higher levels it will tend to cause headaches, dizziness and nausea. Concentrations above 1200 ppm are considered immediately dangerous to life and health.

In addition to the toxic effects of CO, carbon monoxide burns readily in air. The flammability limits of CO in air change with pressure. At atmospheric pressure, however, the lower limit is ± 12.5% and upper limit is ± 74%.

Properties of Various Gases

Common Name	Chemical Formula	Specific Gravity	Time Weighted Average*	IDLH**	Lethal Conc.***	LFL	UFL
		Air = 1	ppm	ppm	ppm	%	%
Hydrogen Sulfide	H <sub>2</sub> S	1.18	10	100	600	4.3	46
Sulfur Dioxide	SO <sub>2</sub>	2.21	2	---	1000	---	---
Methane	CH <sub>4</sub>	0.55	---	---	---	5.3	14
Carbon Monoxide	CO	0.97	25	1200	---	12.5	74

- \* Time Weighted Average (TWA) - Employee's average exposure in any eight-hour work, of a 40-hour work week that shall not be exceeded
- \*\* Hazardous Concentration that may cause death
- \*\*\* Lethal Concentration that will cause death with short term exposure

## H2S Effects

### Effects of H2S In Fluids

When H2S is entrained in a fluid, it will disassociate to some degree depending on the pH of the system.

Undissociated hydrogen sulfide is the molecule that attacks steel surfaces and causes corrosion and embrittlement. At a low pH, nearly all of the H2S in a system is in this molecular state. With increasing pH, H2S disassociation increases so that above pH 10, effectively all of the H2S is disassociated into bisulfide and sulfide ions. These ions are relatively harmless in the mud as long as the high pH is maintained. If pH is lowered, the reaction will be reversed and hydrogen sulfide gas will be evolved.

In addition to sulfide ions, disassociation of H2S in drilling mud produces hydrogen ions, which will react with hydroxyl ions in a high pH mud to form water. With sufficient H2S contamination, excess lime, if any, can be depleted and pH will begin to drop. A sufficient decrease in pH will, as previously stated, evolve H2S gas.

It is therefore desirable to know whether H2S has been encountered at the least possible time. This can be accomplished by testing the mud or other working fluids for sulfide ions daily, as described in the sulfide testing procedures that follow (API RP 13B).

### Corrosion Effects of H2S on Steel

The three forms of hydrogen sulfide corrosion of steel are as follows:

- general or weight loss
- localized or pitting
- sulfide stress cracking

In both general and localized corrosion, hydrogen sulfide reacts with the steel to produce iron sulfide. General corrosion is characterized by the formation of an iron sulfide film on the surface of the steel. After long periods of exposure, weight loss can lead to a significant reduction in strength. Localized corrosion is much more serious and predominantly occurs in the pH range below six. Chloride or similar ions must be present for pitting to occur. Iron chloride accumulates at the metal to iron sulfide film interface and promotes a localized attack. Pitting corrosion has not presented a significant problem in drilling operations.

Of foremost concern is sulfide stress cracking or hydrogen embrittlement where failure may take place without warning or significant metal loss. This problem is related to strength of the steel, hydrogen sulfide concentration, pH, exposure time, and temperature and stress level of the steel. Hydrogen sulfide absorbed on the metal surface promotes the entry of atomic hydrogen into the metal. The atomic hydrogen that enters the steel matrix diffuses to positions of high stress where it can induce hydrogen embrittlement. Thus, brittle failure can occur at stress levels significantly less than normal yield stress. A high total dissolved sulfide concentration can be tolerated if the pH is high enough (9.5 or greater).