NEW MEXICO OIL CONSERVATION COMMSSION

# MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122
Revised 9-1-65

OCT 27 1969
OIL CON. COM.
DIST. 3

| | | | | | |
|---|---|---|---|---|---|
| Type Test: [X] Initial [ ] Annual [ ] Special | | | | Test Date: 10-9-69 | |
| Company: PAN AMERICAN PETROLEUM CORP. | | | Connection: None | | |
| Pool: Basin | | | Formation: Dakota | | Unit |
| Completion Date: 10-1-69 | Total Depth: 7219 | | Plug Back TD: 7184 | Elevation: / RDB GL 6671/6686 | Farm or Lease Name: Jicarilla Gas Com 35-C |
| Csg. Size: 4.500 / Wt.: 10.5 / d: 4.052 / Set At: 7219 | | | Perforations: From 6986 To 7125 | | Well No.: 1 |
| Tbg. Size: 2.375 / Wt.: 4.7 / d: 1.995 / Set At: 7022 | | | Perforations: From Open End To | | Unit: M / Sec.: 2 / Twp.: 24 / Rge.: 5 |
| Type Well – Single – Bradenhead – G.G. or G.O. Multiple: Single | | | Packer Set At: None | | County: Rio Arriba |
| Producing Thru: Tubing | Reservoir Temp. °F: 90° @ TD | Mean Annual Temp. °F: Est. 60° | Baro. Press. – $P_a$: 12 PSIA Est. | | State: New Mexico |
| L: 7056 | H: 7056 | Gg: .700 | % $CO_2$ | % $N_2$ | % $H_2S$ / Prover / Meter Run / Taps |

| FLOW DATA | | | | | TUBING DATA | | CASING DATA | | |
|---|---|---|---|---|---|---|---|---|---|
| NO. | XXXX Line Size | X XXXXX Size | Press. p.s.i.g. | Diff. $h_w$ | Temp. °F | Press. p.s.i.g. | Temp. °F | Press. p.s.i.g. | Temp. °F | Duration of Flow |
| SI | 2-Inch | Choke | | | | 2117 | | 2113 | | |
| 1. | 7 Days | .750 | 190 | | | 190 | 60° est. | 667 | | 3 Hrs. |
| 2. | | | | | | | | | | |
| 3. | | | | | | | | | | |
| 4. | | | | | | | | | | |
| 5. | | | | | | | | | | |

## RATE OF FLOW CALCULATIONS

| NO. | Coefficient (24 Hour) | $\sqrt{h_w P_m}$ | Pressure $P_m$ | Flow Temp. Factor Ft. | Gravity Factor Fg | Super Compress. Factor, Fpv | Rate of Flow Q, Mcfd |
|---|---|---|---|---|---|---|---|
| 1 | 12.3650 | | 202 | 1.000 | .9258 | 1.023 | 2366 |
| 2. | | | | | | | |
| 3. | | | | | | | |
| 4. | | | | | | | |
| 5. | | | | | | | |

| NO. | $P_t$ | Temp. °R | $T_r$ | Z |
|---|---|---|---|---|
| 1 | | | | |
| 2. | | | | |
| 3. | | | | |
| 4. | | | | |
| 5. | | | | |

Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.
Specific Gravity Separator Gas _____ XXXXXXXXX
Specific Gravity Flowing Fluid XXXXX _____
Critical Pressure _____ P.S.I.A. _____ P.S.I.A.
Critical Temperature _____ R _____ R

$P_c$ 2129 $P_c^2$ 4,532,641

| NO | $P_t^2$ | $P_w$ | $P_w^2$ | $P_c^2 - P_w^2$ |
|---|---|---|---|---|
| 1 | | 679 | 461,041 | 4,071,600 |
| 2 | | | | |
| 3 | | | | |
| 4 | | | | |
| 5 | | | | |

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.1132$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.0837$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 2564$

Absolute Open Flow 2564 Mcfd @ 15.025 | Angle of Slope θ _____ | Slope, n .75

Remarks: _____

| Approved By Commission: | Conducted By: | Calculated By: | Checked By: |
|---|---|---|---|
| | B. D. Dukes | | J. J. Layton |