												rm C-122 12-1-55
_		~ <b>4</b> •						ST FOR GAS				
	1 Gavilan											
Ini	tial		Annua	ıl		Spec	ial		_Date of	Test	tay 6, 1	1762
Com	pany pan	des	Petrol	erm. Co	rp.	Lease_	eari lla	Apache "	* LUS Well	l No	3	
Uni	ts	Sec	Twp	) <b>24</b>	Rg	е. <u>уч</u>	Purc	chaser				
Cas	ing 1/20 N	/t . <b>9.</b> 5	I.	D	<b>090</b> Se	t at_1	Pe	erf	3	То	1006	
Tub	ing 1-1/30 W	/t. 2.5	I.	D. <u>1.</u>	<b>610</b> Se	t at 40	<b>05</b> Pe	erf. y	73	То	4005	
Gas	Pay: From_	3966	_To_ <u></u>	026	_L_40	<b>05</b> x	G 0,70	GL_3	803	Bar.Pre	ss. 1	2
Pro	ducing Thru:	Ca	sing	·	Tu	bing	X	Type We	11	glo		
Date	e of Complet	ion:			Packe	r <b>iic</b>	Sir <b>De</b>	ngle-Brade Reservo	nhead-G. ir Temp.	G. or G	.O. Dua	1
	•	-					ED DATA					
m	k 3 m)			., , \	/		DD DAIA		m m			
Tes	ted Through								Type Tap	os		
			rlow Da oke)		Diff.	Temp.		Z Data Temp.	Casing I	Temp.	Du	ration
No.	(Line) Size	<b>PROPERTY</b>		psig		o <sub>F</sub> .		o <sub>F</sub> .	psig		٥	f Flow Hr.
SI	7 675		IZE	herR	h <sub>w</sub>	• 1	959 hare	F 4	959	F •		211 •
1. 2.	2 Indian	3/8	•	304			23)	60" (out.		60	7 %	ere
<del>2</del> • 3•		1		<del> </del>								
4. 5.					- F-						2.1	
<u> </u>		<u> </u>	+	· · · · · · · · · · · · · · · · · · ·				_ <del></del>	L		-	
	Coeffici	ent		Pr	essure	FLOW CAL Flow		Gravity	Compre	ss.	Rate of	Flow
No.	(24-Hou	r)	√ h <sub>w</sub> p	_	psia	Fac F	1	Factor F	Facto		Q-MCFP @ 15.02	
1.	(24-1100		V "WE	T	poid		-	Fg	Fpv			
2. 3. 4. 5.	12,3450				21.6	1,000		0,9298	1,0		253	
<u>ر</u> 4٠												
5.												!
					PR	ESSURE C	alcuiati	IONS				
as ]	Liquid Hydro	carbon	n Ratio	)					fic Gravi			
	ity of Liqui	-		ns _e=s)		deg.		Speci Pa	fic Gravi	ty Flow	ing flu	id
				_				<u></u>		· ·		
	$P_{\mathbf{W}}$	_2							_2 _2			_
No.	Pt (psia)	Pt	Fc		$(F_cQ)^2$	(F	္(၂) <sup>2</sup> -e-s)	P <b>w</b> 2	$P_c^2 - P_w^2$	Ca P	1. W	P <sub>w</sub> P <sub>c</sub>
<u>Ţ.</u>								20,329	424,323		<b>W</b>	
1. 2. 3. 4.												
<u>4.</u> 5.												
	olute Potent	ial:	2566			MCFPD;		.85				
COM	PANY	PAN	MELL	AITPE		on, Nev	10N				··	
AGE	NT and TITLE							(Frè	11 1	和心	<u> </u>	
	NESSEDPANY								_/K	-bLIY	101	

		Flo	v Data			Tubing	Data	Casing I	)ata	T
۰.	(Line)	(Choke			Temp.	Press.	1	Press.	Temp.	of Flo
	Size	Size	psi	g h <sub>w</sub>	°F.	psig	o <sub>F</sub> ,	psig	°F∙	Hr.
I •	7 days					959		777		
•		3//-	304	<del></del>		23)	60" (oak.	743	60	) hours
╌┼				<del></del>		<del> </del>	<del> </del>		+	<del> </del>
+							†	ļ	+	<del> </del>
. †				ATTACK PARTIES						ad.
					mr. 64.7 . 64.7	OUT AMTON	re.			171
Т	Coeffici	ent.	- 1	Pressure		CULATION Temp.	Gravity	Compre	988	Rate of Flow
,	00011101			licoourc		tor	Factor	Facto		Q-MCFPD
	(24-Hou	r)  ¬/	h <sub>w</sub> p <sub>f</sub>	psia		t	$\mathbf{F}_{\mathbf{g}}$	Fpv	-	@ 15.025 psi
+		- Y	- T			<del></del>		- P*		
	12,3650			216	1,000		0.9298	1,0	5	2537
1										
$\perp$										
	iquid Hydro	carbon K			-0/12		0	64 - 0		<b>-</b>
	ty of Liquid	d Hydroca		Σ	cf/bbl.deg.		Speci Speci <sup>P</sup> c—	fic Gravi	ity Sep ity Flo P <sup>2</sup>	arator Gas wing Fluid
	$P_{\mathbf{W}}$	d Hydroca	rbons		deg.		Speci	fic Gravi	ity Flo	wing Fluid
-		d Hydroca	arbons(1-e <sup>-s</sup>		deg.	- -e-s)	Speci P <sub>c</sub> P <sub>w</sub> 2	P <sub>c</sub> -P <sub>w</sub> <sup>2</sup>	ity Flo	wing Fluid
Ī	$P_{\mathbf{W}}$	d Hydroca	arbons(1-e <sup>-s</sup>		deg.	- -e-s)	Speci P <sub>c</sub>	fic Gravi	ity Flo	wing Fluid
Ī	$P_{\mathbf{W}}$	d Hydroca	arbons(1-e <sup>-s</sup>		deg.	- -e-s)	Speci P <sub>c</sub> P <sub>w</sub> 2	P <sub>c</sub> -P <sub>w</sub> <sup>2</sup>	ity Flo	wing Fluid
 T	$P_{\mathbf{W}}$	d Hydroca	arbons(1-e <sup>-s</sup>		deg.	- -e-s)	Speci P <sub>c</sub> P <sub>w</sub> 2	P <sub>c</sub> -P <sub>w</sub> <sup>2</sup>	ity Flo	wing Fluid
so	Pw Pt (psia)	P <sub>t</sub> <sup>2</sup>	F <sub>c</sub> Q	(F <sub>c</sub> Q) <sup>2</sup>	(F (1	cQ) <sup>2</sup> -e-s)	Speci P <sub>c</sub> P <sub>w</sub> 2	P <sub>c</sub> -P <sub>w</sub> <sup>2</sup>	ity Flo	wing Fluid
so MP	Pw Pt (psia) lute Potent	Pt Pt PAR A	F <sub>c</sub> Q	(F <sub>c</sub> Q) <sup>2</sup>	deg. (F (1	n 0.	Speci Pc— Pw2	P <sub>c</sub> -P <sub>w</sub> <sup>2</sup>	ity Flo	wing Fluid
so MP DR	Pw Pt (psia)  lute Potent ANY ESS	PAN AR	F <sub>c</sub> Q	(F <sub>c</sub> Q) <sup>2</sup>	deg. (F (1	100 Nextce	P <sub>c</sub>	P <sub>c</sub> -P <sub>w</sub>	ity Flo	wing Fluid
so MP DR	Pw Pt (psia) lute Potent	PAN AR	F <sub>c</sub> Q	(F <sub>c</sub> Q) <sup>2</sup>	deg.  (F (1)  MCFPD;	100 Nextce	Speci Pc— Pw2	P <sub>c</sub> -P <sub>w</sub>	ity Flo	wing Fluid
so MP DR EN	Pw Pt (psia)  lute Potent: ANY ESS T and TITLE	PAN AR	F <sub>c</sub> Q	(F <sub>c</sub> Q) <sup>2</sup>	deg.  (F (1)  MCFPD;	100 Nextce	P <sub>c</sub>	P <sub>c</sub> -P <sub>w</sub>	ity Flo	al. Pw Pc

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- Q = Actual rate of flow at end of flow period at W. H. working pressure ( $P_{\rm W}$ ). MCF/da. @ 15.025 psia and 600 F.
- $P_c$ = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater.
- Pw Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- Pt Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- Pf Meter pressure, psia.
- hw Differential meter pressure, inches water.
- $F_g = Gravity$  correction factor.
- $F_t$ : Flowing temperature correction factor.
- $F_{pv}$  Supercompressability factor.
- n \_ Slope of back pressure curve.

Note: If  $P_{\rm W}$  cannot be taken because of manner of completion or condition of well, then  $P_{\rm W}$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_{\rm t}$ .