STATE OF NEW MEXICO
ENERGY AND MINERALS DEPARTMENT

P. O. BOX 2088
SANTA FE, NEW MEXICO 87501

Form C-122
Revised 10-1-78

# MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELLS

RECEIVED
JAN 09 1985
OIL CON. DIV.
DIST. 3

| | | | | | |
|---|---|---|---|---|---|
| Type Test: [X] Initial [ ] Annual [ ] Special | | | | Test Date: 12-10-84 | |
| Company: Consolidated Oil & Gas | | | Connection: Gas Company of New Mexico | | Unit |
| Pool: Basin Dakota | | | Formation: Dakota | | |
| Completion Date: 11-12-84 | Total Depth: 8480 | | Plug Back TD: 8424 | Elevation: 7239' GR | Farm or Lease Name: Huron |
| Csg. Size: 5 1/2 / Wt.: 15.5 / d: 4.950 | Set At: 8469 | | Perforations: From 8190 To 8388 | | Well No.: 4 E |
| Tbg. Size: 1 1/2 / Wt.: 2.9 / d: 1.610 | Set At: 8321 | | Perforations: From To | | Unit: A / Sec.: 2 / Twp.: 26 / Rge.: 4 |
| Type Well – Single – Bradenhead – G.G. or G.O. Multiple: Dual gas | | | Packer Set At: 7850 | | County: Rio Arriba |
| Producing Thru: Tbg | Reservoir Temp. °F | Mean Annual Temp. °F | Baro. Press. – $P_a$ | | State: New Mexico |
| L | H | Gg: .650 | % $CO_2$ | % $N_2$ | % $H_2S$ | Prover: 6" pos. | Meter Run: choke nipple | Taps |

## FLOW DATA / TUBING DATA / CASING DATA

| NO. | Prover Line Size x Orifice Size | Press. p.s.i.g. | Diff. $h_w$ | Temp. °F | Tubing Press. p.s.i.g. | Tubing Temp. °F | Casing Press. p.s.i.g. | Casing Temp. °F | Duration of Flow |
|---|---|---|---|---|---|---|---|---|---|
| SI | 14 days | | | | 1520 | | Pkr. | | |
| 1. | 2" x 3/4" pos. choke | | | | 74 | 60 | Pkr. | | 3 hours |
| 2. | | | | | | | | | |
| 3. | | | | | | | | | |
| 4. | | | | | | | | | |
| 5. | | | | | | | | | |

## RATE OF FLOW CALCULATIONS

| NO. | Coefficient (24 Hour) | $\sqrt{h_w P_m}$ | Pressure $P_m$ | Flow Temp. Factor Ft. | Gravity Factor Fg | Super Compress. Factor, Fpv | Rate of Flow Q, Mcfd |
|---|---|---|---|---|---|---|---|
| 1 | 11.00 | | 86 | 1.000 | 1.240 | 1.000 | 1173 |
| 2. | | | | | | | |
| 3. | | | | | | | |
| 4. | | | | | | | |
| 5. | | | | | | | |

| NO. | $P_r$ | Temp. °R | $T_r$ | Z |
|---|---|---|---|---|
| 1 | | | | |
| 2. | | | | |
| 3. | | | | |
| 4. | | | | |
| 5. | | | | |

Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.
Specific Gravity Separator Gas _____ XXXXXXXXX
Specific Gravity Flowing Fluid XXXXX _____
Critical Pressure _____ P.S.I.A. _____ P.S.I.A.
Critical Temperature _____ R _____ R

$P_c$ 1532 $P_c^2$ 2347024

| NO | $P_t$ | $P_w$ | $P_w^2$ | $P_c^2 - P_w^2$ |
|---|---|---|---|---|
| 1 | | | 31299 | 2315725 |
| 2 | | | | |
| 3 | | | | |
| 4 | | | | |
| 5 | | | | |

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.0135$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.0100$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1185$

Absolute Open Flow 1185 Mcfd @ 15.025 | Angle of Slope θ 53.13° | Slope, n 0.75

Remarks: _____

Approved By Division | Conducted By: | Calculated By: | Checked By: