## NEW MEXICO OIL CONSERVATION COMMISSION

											Form C-122
Poo	ol <b>Undesi</b> gi	nated						ST FOR GAS	J WILLIO		Revised 12-1-55
											Juan
											-29-57
Com	pany Magnol	La Peti	roleum	Compan	<b>y</b> ]	Lease At	-NuseBal	1	We	ll No.1	···
Uni	t <u>K</u>	Sec22	Tw:	25	Rge	. 11W	Pur	chaser	No con	nection	
Cas	ing 5 1/2" V	/t. <u>11:#</u>	I.	D. <u>5.01</u>	<b>2*</b> Set	at5	6 <b>0001</b> Pe	erf. 1.89	21	To	9311
Tub	ing 2 3/8" V	it. <b>4.7</b>	<u> </u>	D. <b>1.99</b>	<b>5</b> Set	at_ <b>h</b>	<b>869</b> Pe	erf	•	То	
Gas	Pay: From_	4,892	To 4	931'	_L		cG <b>0,68(1</b>	st.) GL_		Bar.Pre	SS• 12 pais
	ducing Thru:										
Dat	e of Complet	ion:	7-1	5 <b>-57</b>	Packer	· non	Sir •	ngle-Brade Reserve	enhead-G. oir Temp.	G. or G	.O. Dual
	-						ED DATA	· · · · · · · · · · · · · · · · · · ·			
Test	ted Through	( <del></del>	/· 	holeo \	( <del>25</del>	OBBINE	DD DRIN				
					ACCUSATE OF THE PARTY OF THE PA				Type Tar		
	(ZEEFER)		low Da		Diff.	Temp		Data Temp.	Casing I		Duration
No.	`(Line)´	(Det				_		1		1	of Flow
	2 tre	XEX	XXX	psig	h <sub>w</sub>	°F.	<del></del>	°F.	psig	<sup>o</sup> F∙	Hr.
SI	2#	0.25	O.B.	1.243		<b>5</b>	1,335		1,335		3
2.	2# 2# 2#	0.37		1.075	*	73	1,243		1,276		3 hrough min.
<u>3.                                     </u>		0.50	0	750	•	13	750	1 5 -	1,1kg		2 4/2 1884
4. 5.	2*	0.75	0	394		84	391	8	891	ļ	3 kms.
<u> </u>	<del></del>	L			<u>-</u>	***************************************	<u> </u>	1	<u> </u>	<u> </u>	L.
<del></del>	Coeffici	ont					CULATION		10		Rate of Flow
No.	ODELLICI	enc		_   ' ' '	essure		Temp.	Gravity Factor	Compre		Q-MCFPD
	(24-Hou	r)	$\sqrt{h_{\mathbf{w}}}$ p	f	osia		't	$F_{g}$	Fpv	1	@ 15.025 psia
1.	1.3309		-	1	255	-987	77	.9393	7.11	8	1,779
2. 3.	3.0300			1	087	98		9393	1.15		3-67
20	5.4 <b>315</b> 12.3650		-		762 h03	971		-9393	1.08	<del></del> (	4,110
4. 5.					1113	-977		-9393	1.0	1	4,76k
	Liquid Hydro ity of Liqui		ocarbo	ns -e <sup>-s</sup> )	PRE			Speci Speci		ty Flow	rator Gas ing Fluid 0.68
No.	$P_{\mathbf{W}}$	$P_{\mathbf{t}}^2$	Fc	a	$(F_cQ)^2$	(F	(cQ) <sup>2</sup> (-e-s)	P <sub>w</sub> 2	P <sub>c</sub> -P <sub>w</sub> <sup>2</sup>	Ca	1. Pw
	1288		<del></del>			(1				P	l. Pw Pc
1. 2.	1161							1658.9	155.5 466.5		
3.	973				•			\$16.7	867.7		
4. 5.	833				<del></del>			693.9	1,120.5	<del></del>	
Abso COMP ADDF AGEN	PANY MAGNOL RESS P. O. NT and TITLE NESSED	IA PET Box 2h	RCLEUM OS Ho	COMPAI	w.Mrie		nl.9		R	CEN	

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Tested Through (Choke) (Choke)					Type Taps							
Flow Data						Tubing Data   Casing Data						
	(PRINCE)	(Chok		. Diff.	Temp.	Press.		Casing Press.	Temp.	Duration		
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SI 1: 2: 3:						1.335	_	1,335		7		
1.	2*	0.250	1.24		73	1.243	73	1,276		2 has 5 sta		
2.	2#	0_375			78	1.075	78			9 3/0		
<u>3.</u>	2"	0.500			83	750	83	1,149 961		S she made		
<u>4.</u> 5.	2**	0.750	391	<u> </u>	84		8	897		3 100		
<u> </u>		L					<u> </u>			3 - 300		
					T.OW CAT	CULATION	S					
	Coeffici	ent	P	ressure	Flow		Gravity	Compre	ess.	Rate of Flow		
No.	,		I		Fac		Factor	Facto	or	Q-MCFPD		
	(24-Hou	r)   <sub>7</sub>	/ hwpf	psia	F.	t	${ t F_g}$	Fpv	ŀ	@ 15.025 psia		
1.	1.3309	•	_	1.255	-987	9	<del></del>	<del></del>		• • • • • • • • • • • • • • • • • • • •		
1. 2. 3.	3,0300		-	1.087	983		.9393 .9393	1.1		1,779		
3。	5.4315		•	762	.978		9393	1.00		1 110		
<u>4.</u> 5.	12.3650		-	103	.977		.9393	1.0		4,112 4,764		
5.							V/3/3	250	-	43104		
Grav	Liquid Hydro ity of Liquid				cf/bbl. deg.		Speci	fic Gravi	ity Sepa ity Flow _Pc	rator Gas ing Fluid 0.68		
No.	$P_{\mathbf{W}}$	P <sub>t</sub> <sup>2</sup>	P.O.	$(F_cQ)^2$	(F	0)2	D 2	P <sub>c</sub> -P <sub>w</sub> <sup>2</sup>	T			
MO.	psia)	<sup>r</sup> t	F <sub>c</sub> Q	(r <sub>c</sub> w)		cQ) <sup>2</sup> -e <sup>-s</sup> )	$P_w^2$	rc-rw	Ca P	$\frac{1}{w}$ $\frac{P_w}{P_c}$		
I.	1288		<del>                                     </del>		<del></del>		1658.0	155.5	+	<u>w</u>		
2.	1161						1315 0	166.5				
3.	973			*			616.3	867.7				
4.	833			. <del></del>			693.9	1.120.5	 <del></del> -			
5.		<del></del>										
Abso	olute Potent	ial:	5,990		_MCFPD;	n			4514			
A DDI	PANY MAGNOL	Dam Cho	CLEUM COMP	ANT			<del> </del>		TIME			
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	COMPANY						AUG 12 1857					
	REMARKS											
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	DIST. 3											
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## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- Q  $\equiv$  Actual rate of flow at end of flow period at W. H. working pressure (P<sub>w</sub>). MCF/da. @ 15.025 psia and 60° F.
- $P_c$ = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater. psia
- Pw Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- $P_{t}^{-}$  Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- Pf Meter pressure, psia.
- $h_{\mbox{W}}\mbox{\fontfame}$  Differential meter pressure, inches water.
- $F_g = Gravity$  correction factor.
- $F_t$  Flowing temperature correction factor.
- $F_{pv}$  Supercompressability factor.
- n I Slope of back pressure curve.
- Note: If  $P_{\mathbf{W}}$  cannot be taken because of manner of completion or condition of well, then  $P_{\mathbf{W}}$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_{\mathbf{t}}$ .

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