3- NMOCC

1- L.G. Truby 1- El Paso (Galloway) 1- W.R. Johnston 1- File

## NEW MEXICO OIL CONSERVATION COMMISSION

Form C-122

Revised 12-1-55

MULTI-POINT BACK PRESSURE TEST FOR GAS WELLS

Coefficient	Pool	Blan	<b>c</b> o	I	ormation	<u> Xe</u>	a Verde	)	County	Rio	Arriba
	[nit	ialXX	An:	nual		Spec	cial	<del></del>	Date of	Test	4-17-57
Sing 5	Comp	any <b>Pacifi</b>	e Northw	est Pi	peline	Lease	28-5		Wel	1 No	11-33
Ding 2   Wt.   I.D.   Set at 5785   Perf.   To	Jnit	KS	Sec. <u>33</u>	Iwp. 28	N Rg	e. <u>5</u> W	Purc	haserU	Inconnect	ed	
Second   Packer   Single   S	asi	ng_5}	/t	_I.D	Se	t at _58	<b>346</b> Pe	rf <b>520</b>	2	To <b>5</b>	828
Tubing	'ubi	ng <b>2</b> W	/t	I.D	Se	t at	<b>785</b> Pe	rf		То	
Tubing	as	Pay: From_	<b>5202</b> To	5828	L		G .650	_GL_		Bar.Pre	ess. 12
Completion:										_	
Companies	ate	of Complet	ion:		Packe	r	Sin	gle-Brade Reserve	enhead-G. oir Temp.	G. or (	G.O. Dual
Sted Through   Recent   Choke   Choke   Recent   Sted Through   Recent   Choke   Press   Diff   Temp   Press   Temp   Press   Temp   Of Flow   Choke   Choke   Press   Diff   Temp   Press   Temp   Press   Temp   Of Flow   Chine   Cirifice   Size   psig   hw   OF   psig   OF   psig   OF   Hr.		•						<b></b>			
Prove   Prove   Prove   Press   Diff   Temp   Press   P	est	ed Through	(Brewner)	(Choke)	( <b>E</b> ATES )			LVS.	Twne Tan	e	
Prover   (Choke   Press.   Diff.   Temp.   Press.   Temp.   Press.   Temp.   Of Flow   Size   Size   psig   hw   Of.   psig   Of.   psig   Of.   psig   Of.   psig   Of.   Psig   Of.   Psig   Of.									·		
Cline   Corifice   Size   psig   hw   OF.   psig   OF.   psig   OF.   hr.	Т	(Prover)	(Choke)	Press	. Diff.	Temp.			Press.	Temp.	Duration
Coefficient	۰.				<u> </u>	ο <sub>υ</sub>	nete	O <sub>E</sub>		1	of Flow
Second   S	1	5126	5126	psig	W <sup>11</sup>	F •		<u> </u>	<del></del>		nr.
PLOW CALCULATIONS	;+		3/4	356	+	67	356	67		<del> </del>	3
Pressure   Flow Calculations   Gravity   Compress.   Rate of Flow   Compress   Flow Temp.   Factor											
Pressure   Flow Temp.   Gravity   Compress.   Rate of Flow	4				-					ļ	
FLOW CALCULATIONS  Coefficient  Coefficient  Coefficient  Coefficient  Pressure  Flow Temp. Factor F	+			+	+					<del>                                     </del>	<del>                                     </del>
PRESSURE CALCULATIONS  Liquid Hydrocarbon Ratio of bl. Specific Gravity Separator Gas Specific Gravity Flowing Fluid Pc Pc Pc Pc Cal. Pc	· ·	Coefficient Pressure Flow Temp. Gr Factor F					Gravity Factor	Factor Factor Q-MCFPD			
PRESSURE CALCULATIONS  Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity Flowing Fluid Pc	+			WPf							<del>-</del>
PRESSURE CALCUIATIONS  Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas	+	14.1007	<u> </u>		311		733	,3000		-	2410
PRESSURE CALCULATIONS  Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity Flowing Fluid Pc Pc Pc Callers Pc Calle	$\prod$										
PRESSURE CALCULATIONS  Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity Flowing Fluid Pc Pc Pc Callers Pc Calle						<del></del>		· <u></u>			<del></del>
Pt (psia)  Pt FcQ (FcQ)2 (FcQ)2 Pw2 Pc-Pw Cal. Pw Pc  Pt (psia)  Pt FcQ (FcQ)2 (FcQ)2 Pw2 Pc-Pw Cal. Pw Pc  Pt (psia)  Pt FcQ (FcQ)2 (FcQ)2 Pw2 Pc-Pw Cal. Pw Pc  Pt (psia)  Pt FcQ (FcQ)2 (FcQ)2 Pw2 Pc-Pw Cal. Pw Pc  Pt (psia)  Pt FcQ (FcQ)2 Pw2 Pc-Pw Cal. Pw Pc  Pt (psia)  Pt FcQ (FcQ)2 (FcQ)2 Pw2 Pc-Pw Cal. Pw Pc  Pt (psia)  Pt FcQ (FcQ)2 Pw2 Pc-Pw Cal. Pw Pc  Pt (psia)  Pt FcQ (FcQ)2 Pw2 Pc-Pw Cal. Pw Pc  Pt (psia)  Pt FcQ (FcQ)2 Pw2 Pc-Pw Cal. Pw Pc  Pt (psia)  Pt FcQ (psia)  Pt	vi	ty of Liqui	d Hydrocar	bons		cf/bbl.		Speci Speci	fic Gravi	ty Flow	
solute Potential: 11,024 MCFPD; n .75/ 2.0887  MPANY Reaffic Northwest Pipeline Corp.  DRESS 405 West Breedway, Farmington, New Mexico  ENT and TITLE C. R. Wagner, Well Test Engineer	•		Pt <sup>2</sup>	F <sub>c</sub> Q		(F	(cQ) <sup>2</sup> -e-s)	<b>983</b> P <sub>w</sub> 2	$P_c^2 - P_w^2$	Ca F	Pw Pc
solute Potential: 11,024 MCFPD; n .75/ 2.0887  MPANY Pacific Northwest Pipeline Corp.  DRESS 405: West Breedway, Farmington, New Mexico  ENT and TITLE C. R. Wagner, Well Test Engineer			<del>``</del>		72			779.7	468.0	<del> </del>	2.67
solute Potential: 11,024 MCFPD; n .75/ 2.0887  MPANY Pacific Northwest Pipeline Corp.  DRESS 405: West Breedway, Farmington, New Mexico  ENT and TITLE C. R. Wagner, Well Test Engineer	. Т			77 3	<del>)</del>	+		<del></del>		+	THE STATE OF THE S
MCFPD; n ./5/ 2.000/ MPANY Pacific Northwest Pipeline Corp.  DRESS 405: Vest Breedway Farmington, New Mexico  ENT and TITLE C.R. Hagner, Voll Test Engineer											<b>XLLIVE</b>
MCFPD; n ./5/ 2.000/ MPANY Pacific Northwest Pipeline Corp.  DRESS 405: Vest Breedway Farmington, New Mexico  ENT and TITLE C.R. Hagner, Voll Test Engineer										11	
ENT and TITLE C.R. Wagner, Well Test Engineer	MP.	ANY Pro	ifie Nor	thwest	Pipel	ne Cor	ρ		0887	-	OIL CON. COM
	EN'	r and TITLE	C.R.	Vacuus	Vol	Test	Enginee	r			

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- Q I Actual rate of flow at end of flow period at W. H. working pressure  $(P_w)$ . MCF/da. @ 15.025 psia and 60° F.
- $P_c$  72 hour wellhead shut-in casing (or tubing) pressure whichever is greater. psia
- PwT Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- $P_t$  Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- Pf Meter pressure, psia.
- hw Differential meter pressure, inches water.
- FgI Gravity correction factor.
- Ft Flowing temperature correction factor.
- $F_{pv}$  Supercompressability factor.
- n I Slope of back pressure curve.

Note: If  $P_{\rm W}$  cannot be taken because of manner of completion or condition of well, then  $P_{\rm W}$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_{\rm t.}$ .

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