Form C-122

Size Size psig hw OF, psig OF,				MULTI-	-POINT BA	CK PRES	SSURE TES	ST FOR GA	S WELLS		Revised 12-1-55
Company PASILIE NEWINDER FIRST Lease Sea Juan 30-5 Well No. 23-7	Poo	1 Blanco		Fc	rmation_	Me	sa Verde	,	County_	Rio Arr	iba.
Company PASILIE NEWINDER FIRST Lease Sea Juan 30-5 Well No. 23-7	Ini	tial_	Anr	nual		Spec	ial		Date of	Test	8-8 -58
Casing											
Tubing 1-1/4" Wt. I.D. Set a	Uni	t H s	Sec	wp _ 300	Rge	. <u>5</u> v	Purc	haser	Not earne	eted	
Gas Pay: From To L xG GS GL Bar. Press. 12 Producing Thru: Casing XXX Tubing Type Well Single—Bradenhead-G. G. or G.O. Dual Reservoir Temp. OBSERVED DATA Tested Through (Choke) Hold Single—Bradenhead-G. G. or G.O. Dual Reservoir Temp. OBSERVED DATA Tested Through (Choke) Press. Diff. Temp. Press. Temp. Press. Temp. Ouration of Flow Size psig hw Op. psig Op. psig Op. psig Op. Hr. 1. 1100 1193 T. 1600 T.	Cas	ing 5-1" W	′t	I.D	Set	at 573	0¹ Pe	rf 56 7	8.	To	350'
Producing Thru: Casing Tubing Single-Bradenhead-G, G, or G,O, Dual	Tub	ing 1-1/4" W	't	I.D	Set	a 5670	Pe	erf		_To	
Date of Completion: Packer Reservoir Temp. Completion: Packer Completion:	Gas	Pay: From_	To_	·	L	x	G .650			Bar.Pr	ess. <u>12</u>
Date of Completion: Packer Reservoir Temp. Completion: Packer Completion:	Pro	ducing Thru:	Casing_	23X	Tub	i.ng	0.	Type W	ell	ngle	7 O D
Tested Through	Dat	e of Complet	ion:		Packer	···-	Sir	igie-Brad Reserv	ennead-G. oir Temp.	G. or	G.O. Dual
Flow Data						OBSERV	ED DATA				
Flow Data	Tes	ted Through	(44444)	(Choke)	(NAHA)	Shet :	in 7 days	5	Туре Тар	os	(* °)
No. (Line) (Orifice) Size psig hw OF, psig OF, psig OF, psig OF, Hr.					7:00				Casing I	Data	
SI	No.	(Line)	(Orifice)	.		_					of Flow
1. 2. 3. 4. 5. FLOW CALCULATIONS No. Coefficient Pressure Flow Temp. Gravity Compress. Rate of Flow Factor Factor	ST	Size	Size	psig	h _w		<u></u>	F.	+	F.	Hr.
FLOW CALCULATIONS FLOW CALCULATIONS Rate of Flow Temp. Gravity Compress. Rate of Flow Pactor Factor Facto	1.		3/4"	335		AT.				77	3 hours
PLOW CALCULATIONS No. Coefficient Pressure Flow Temp. Gravity Factor Fact	2•									†	
No. Coefficient Pressure Flow Temp. Gravity Compress. Rate of Flow Q-MCFPD Pactor Factor Factor	4. 5.							<u> </u>			
No. (24-Hour)	,										
PRESSURE CALCUVATIONS as Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity of Liquid Hydrocarbons deg. Specific Gravity Flowing Fluid Pc Pc 120 Pc 140.0 No. Pw Pt (psia) Pt FcQ (FcQ)2 (FcQ)2 Pw2 Pc-Pw Cal. Pw Fc 1. Pt (1-e-s) Pc 1. Pw Fc 1.	No.					Fac	tor	Factor	Facto	or	Q-MCFPD
PRESSURE CALCULATIONS as Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity Flowing Fluid c (1-e-3) Pc 122 Pc Pc 132.0 No. Pw Pt (psia) Pt FcQ (FcQ)2 (FcQ)2 Pw2 Pc-Pw Cal. Pw Fc 12.0 Absolute Potential: 633 MCFPD; n 75/1.053 ACGMPANY REMARKS	1.	(24-Hou	r) \sqrt{n}	w ^p f	psia	r'	t	rg	F pv		@ 15.025 psia
PRESSURE CALCUTATIONS as Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity of Liquid Hydrocarbons deg. Specific Gravity Flowing Fluid Pc 1.25	2.										
PRESSURE CALCULATIONS as Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity Flowing Fluid Pc Pc Pc Pc	4.										
As Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity Flowing Fluid Pc (1-e-s) Pc 1.25 P	لت				PRE:	SSURE C	A CCULATT	ONS			·
ravity of Liquid Hydrocarbons c (1-e-s) No. Pw Pt (psia) Pt Fc (FcQ) (FcQ) Pv Pv Pc Pv Pc Pv Pv Pc Pt (psia) Absolute Potential: 4.633 COMPANY AGENT and TITLE COMPANY REMARKS REMARKS REMARKS	as I	Liquid Hydro	carbon Rat	io					ific Gravi	itv Sena	arator Gas
No. Pw Pt (psia) Pt FcQ (FcQ)2 (FcQ)2 Pw2 Pc-Pw Cal. Pw Pc Cal. Pw	rav	ity of Liqui	d Hydrocar	bons		deg.		Spec	ific Gravi	ity Flor	wing Fluid
1. 172.2 12.3. 1.13 2. 2. 3. 4. 5.	c		-	.(= 0 <u>Z_</u>			•	•		C _	
1. 172.2 12.3. 1.13 2. 2. 3. 4. 5.	No	$P_{\mathbf{w}}$	_{P2}	FQ	(F ₋ Q) ²	(F	(-Q) ²	115 P 2	P2-P2	Cá	al. P.
Absolute Pouential: 1,653 MCFPD; n_15/1.0959 COMPANY AGENT and TITLE 1.653 MCFPD; n_15/1.0959 WITNESSED COMPANY REMARKS		Pt (psia)	- t	- c ·	1- G-2	(i					Pw Pc
Absolute Potential: 1,653 MCFPD; n .75/1.0959 COMPANY AGENT and TITLE C. 1. May 1. Ma	2.										
Absolute Potential: 4,653 MCFPD; n .75/1.0959 COMPANY AGENT and TITLE C. 1.0959 WITNESSED COMPANY REMARKS	4.									 	
AGENT and TITLE		olute Porent	ial: 4,653	3		MCFPD:	n •75/	1.0959		L	
AGENT and TITLE C. R. Macher - Well 2000 Englaces WITNESSED COMPANY REMARKS	COME	PANY MATTIE	t broaker	Paris . Takab					POFINI	m	
	AGE	NT and TITLE	C. H. M.	gas - V	il fest	Region	nr .		KITTIA	.oc0	
						рги	ARKS		AUG 15		
						TETAL		1	OIL CON	r. 3	<i>f</i>

INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

NOMENCLATURE

- Q \equiv Actual rate of flow at end of flow period at W. H. working pressure (P_W). MCF/da. @ 15.025 psia and 60° F.
- P_c = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater. psia
- Pw Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- Pt Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- Pf Meter pressure, psia.

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- hw Differential meter pressure, inches water.
- $F_g = Gravity$ correction factor.
- F_t Flowing temperature correction factor.
- Fpv Supercompressability factor.
- n I Slope of back pressure curve.

Note: If $P_{\mathbf{W}}$ cannot be taken because of manner of completion or condition of well, then $P_{\mathbf{W}}$ must be calculated by adding the pressure drop due to friction within the flow string to $P_{\mathbf{+}}$.

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