Form C-122

1-WD 1-D

1-D 1-F

## MULTI-POINT BACK PRESSURE TEST FOR GAS WELLS

Revised 12-1-55

Southwe Se Se Wt 3/8 Wt From Thru: Completi	. 17# I	30N D. 4.8 .D. 1.9	Rge Rge Set  L 666  Tub:	at 675 at 669 95 x	Purch 4 KB Per 5 Per 6 .67	ndage naser	Well Page N	latural To 66 To 66 Bar.Pre	Gas Company	
Southwe Se Se Wt 3/8 Wt From Thru: Completi	et Product c. 12 Tw . 17# I . 4.70 I 6513 To Casing on: 2/24	30N D. 4.8 .D. 1.9	Rge Rge Set  L 666  Tub:	at 675 at 669 95 x	Purch 4 KB Per 5 Per 6 .67	ndage naser	Well Page N	latural To 66 To 66 Bar.Pre	Gas Company 603	
3/8 Wt From_ g Thru: Completi	. 17# ] . 4.70 ] 6513 To Casing on: 2/24	6603	92 Set  95 Set  L 66	at 669 95 x	<b>4 KB</b> Per Per G .67	cf. 65	4486	To 66 Bar.Pre	603 695	
3/8 Wt From_ g Thru: Completi	. 17# ] . 4.70 ] 6513 To Casing on: 2/24	6603	92 Set  95 Set  L 66	at 669 95 x	<b>4 KB</b> Per Per G .67	cf. 65	4486	To 66 Bar.Pre	603 695	
3/8 Wt From_ g Thru: Completi	. 4.70 I	6603	P5 Set  L 66	at 669	Per G67	cf	4486	To 60	695	
From	6513 To	6603	L <b>66</b>	95 x	G67		4486	Bar.Pre		
Completi	on: <u>2/24</u>	/61	Tub: Packer	ing	X	Them a 1st -				
Completi	on: <u>2/24</u>	/61	Packer			Trabe we	11 315	igle-Gar	<u> </u>	
nrough					Sing	gle-Brade Reservo	nhead-G.   ir Temp	G. or G	i.O. Dual	
	(FLANSEL) (				ED DATA					
		Choke)					Туре Тар	s_		
	Flow D			<del></del> 1	Tubing	Data	Casing D	ata		
	(Choke)		Diff.	Temp.	Press.		Press.		Duration of Flow	
Size	Size	psig	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	°F.	psig	°F.	psig	°F∙	Hr.	
	3/4"		299	90 08	2380 301	80	2380 848		7-Day 3-Hr.	
								<b></b>		
		<b>. </b>						<u></u>		
efficie	nt	Pr		Flow '	Temp.	Gravity	Compre		Rate of Flow	
(24-Hour) 7/h,		psia							Q-MCFPD @ 15.025 psia	
3650			309			.9463		530	3,642	
-			PRE	SSURE C	ALCU ATIO	ONS				
l Hydroc	arbon Rati	Lo	(	cf/bbl.		Speci	fic Gravi	ty Sepa	rator Gas	
Liquid	Hydrocart	ons					fic Gravi <b>2392</b>	ty Flow	ving Fluid	
	\			<del></del>		P <sub>w</sub>	860	P_2	739.6	
	<sub>D</sub> 2	20	(E 0)2	(12	0)2	<u> п</u> 2	<sub>p2 p2</sub>		) P	
(psia)	Pt F	c <sup>w</sup>	(F <sub>C</sub> (Q)	(1	c <sup>Q</sup> ) -e <sup>-S</sup> )	••		P	P <sub>w</sub> P <sub>c</sub>	
						739.6	4982.0		.359	
				<del></del>				<del> </del>	_	
	pefficie (24-Hour 3650	3/4"  Defficient (24-Hour) √ h <sub>w</sub> 3690  Hydrocarbon Rati Liquid Hydrocarb	3/4"  Defficient  (24-Hour)  1 Hydrocarbon Ratio  1 Liquid Hydrocarbons  (1-e-5)	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	SO   2380   301	SO   2380   301   301   301	SO   2380   2380   2380   301   30   348   301   30   348   301   30   348   301   30   301   30   301   30   301   30   30	SO   2380   2380   2380   3/4"   299   80   301   80   848   301   801	

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## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- Q I Actual rate of flow at end of flow period at W. H. working pressure ( $P_{\rm W}$ ). MCF/da. @ 15.025 psia and 600 F.
- $P_c$ = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater. psia
- $P_{\mathbf{w}}^{\mathsf{T}}$  Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- Pt Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- $P_{f}$  Meter pressure, psia.
- $h_{\mbox{\scriptsize W}}\mbox{\footnotesize -}$  Differential meter pressure, inches water.
- $F_g$ : Gravity correction factor.
- FtT Flowing temperature correction factor.
- $F_{DV}^{-1}$  Supercompressability factor.
- n I Slope of back pressure curve.

Note: If  $P_{\mathbf{W}}$  cannot be taken because of manner of completion or condition of well, then  $P_{\mathbf{W}}$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_{\mathbf{t}}$ .