

AP - 37

**STAGE 2  
REPORT  
(Event 4)**

**Date**  
**6-6-13**

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**MOBILE DUAL PHASE EXTRACTION REPORT  
LOVINGTON DEEP 6 PIPELINE RELEASE**

**LEA COUNTY, NEW MEXICO**

**SRS # 2002-10312**

**NMOCD# AP-037**

RECEIVED OCD

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**PREPARED FOR:**

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**JUNE 6, 2013**



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## **I. MDPE SUMMARY REPORT AND WASTE DISPOSITION**

### **A. MDPE Results**

The following report summarizes data collected during the scheduled 24-hour High Vacuum Multi-Phase Extraction (MDPE) event conducted on February 27-28, 2013, at the Lovington Deep 6 Pipeline release site, located in Lea County, New Mexico. The objective of the MDPE treatment was to remove both vapor and liquid phase separated hydrocarbons (PSH) from onsite groundwater wells. Talon/LPE utilized an MDPE unit which consisted of an SVE extraction pump capable of generating vacuum up to 25" hg. Off gas vapors extracted from the extraction wells were destroyed using a propane-fired 1000-SCFM thermal oxidizer capable of processing 172.96 lbs/hr of gasoline.

A total of 9.5 hours (0.40 days) of PSH recovery was performed due to freezing of propane tank and inability of vendor to refill. MW2, MW13, MW-14, MW15, MW16 & MW17 for 9.5 hours.

Prior to and immediately following the event, the groundwater wells were gauged for groundwater elevation and PSH. Depth to groundwater ranges were measured in feet below the top of casing. Refer to Attachment 1 for a summary of data collected during the MDPE event.

The volume of PSH removed during the MDPE event is shown to reflect the portions of PSH in the liquid phase and as off-gas vapor. Air removal rates were calculated from velocity measurements recorded at the influent manifold prior to entry into the MDPE unit. PSH recovery and air flow data has been detailed and is contained in Table 1. One influent air sample was collected over the course of the event. This sample was submitted for laboratory testing in order to compare the predicted vapor concentrations (based on field-screening or calculated based on fuel consumption) to the actual vapor concentrations. The influent sample was tested for Total-Gas Analysis (Hydrocarbon Composition) by GPA 2261-C6+. Laboratory analytical results can be found in Attachment 2.

Based on a combination of field vapor screening and collected laboratory samples, a combined estimated total of **285.44 equivalent gallons of hydrocarbons (Total)** were removed during the event. The combined volume of hydrocarbons were comprised of approximately **280 gallons of PSH (liquid phase)** and approximately **5.44 gallons as off-gas vapor**. The calculations used to estimate the off-gas vapor mass recovered reflect the mass of total hydrocarbons recovered and does not necessarily equate to an equal mass of the product released. The mass recovery calculations may be affected by variations in the specific gravity of hydrocarbon released, age of release, activity of aerobic and/or anaerobic processes, and site specific geochemical factors.

The cumulative air flow measurements for the MDPE event were calculated using a combination of field data measurements and Preso® B+ manufacturer provided formulas. **Air flow rates extracted from the recovery wells averaged 119.22 SCFM** during the event.

A portion of the extracted air flow rates measured is attributable to compressed air, which was “injected” into the extraction wells. This “injected” air is introduced into the extraction wells for the purpose of enhancing liquid recovery rates.

**B. Air Quality**

One influent air sample was collected during the event. The sample was submitted for laboratory testing in order to compare the predicted vapor concentrations (based on field-screening or calculated based on fuel consumption) to the actual vapor concentrations. The maximum influent concentration was recorded as 7,440 ppmv for Hydrocarbon Composition. Laboratory analytical results can be found in Attachment 2.

**C. Waste Management and Disposition**

A cumulative total of 1,679 gallons of fluid were generated during this event. The fluids were temporarily transferred to an on-site storage tank prior to being transferred to an authorized disposal facility. A copy of the waste ticket can be found in Attachment 4.

**II. SYSTEM OPERATION DATA AND MASS RECOVERY CALCULATIONS**

**Formulae:**

$$\text{Concentration (C\_mg/l)} = \frac{\text{C\_ppmv} \times \text{Mol. wt. in mg(estimated)} \times 1000 \times 0.000001}{0.0821 \times \text{Temp (K)}}$$

$$\text{Recovery Rate (lbs/hr)} = \frac{(\text{C\_mg/l}) \times 2.2 \times (\text{Flowrate}) \times 60 \times 28.32}{1,000,000}$$

$$\text{Recovery (lbs)} = (\text{lbs/hr}) \times (\text{hrs})$$

$$\text{Correction Factor (CF)} = \frac{\text{PID Reading(ppm)}}{\text{PID Reading at Time of Laboratory Analysis}}$$

$$\frac{8.34 \text{ lbs}}{\text{gallon water}} \times 0.82 \text{ average specific gravity of light crude (estimated)} = \frac{6.84 \text{ lbs light crude}}{\text{gallon}}$$

**Table 1**  
**System Operation Data and Mass Recovery Calculations**

Time	Period (hours)	Influent Temp. (°F)	Vacuum (In. hg)	Vacuum (In. h2O)	Differential pressure (In. h2O)	Flow (SCFM)	FID Readings (ppm)	Lab Result (ppmv)	Assigned Lab Result (ppmv)	Correction Factor (CF)	Adjusted Lab Result (ppmv)	Adjusted Lab Result (mg/L)	Recovery (lbs/hr)	Recovery in Period (lbs)	Total Recovery (lbs)
15:30	0.5	62	19	258.57	56	159.41	35789	-	7440.00	0.72	5325	6.40	3.82	1.91	1.91
16:00	0.5	62	19	258.57	55.1	158.12	50000	7440.00	7440.00	1.00	7440	8.95	5.29	2.64	4.55
17:00	1	62	18	244.96	31.8	125.49	36705	-	7440.00	0.73	5462	6.57	3.08	3.06	7.63
18:00	1	60	17	231.35	19.8	103.27	50000	-	7440.00	1.00	7440	8.98	3.47	3.47	11.10
19:00	1	56	16.5	224.55	19.3	104.31	50000	-	7440.00	1.00	7440	9.05	3.53	3.53	14.63
20:00	1	52	15.5	210.94	19.9	110.21	49766	-	7440.00	1.00	7405	9.08	3.74	3.74	18.37
21:00	1	50	15.5	210.94	19.8	110.15	50000	-	7440.00	1.00	7440	9.16	3.77	3.77	22.14
22:00	1	50	15.5	210.94	18.9	107.62	50000	-	7440.00	1.00	7440	9.16	3.68	3.68	25.83
23:00	1	50	15.5	210.94	19.3	108.75	50000	-	7440.00	1.00	7440	9.16	3.72	3.72	29.55
0:00	1	50	15	204.14	19.9	112.32	50000	-	7440.00	1.00	7440	9.16	3.85	3.85	33.40
1:00	1	50	15	204.14	19.7	111.78	50000	-	7440.00	1.00	7440	9.16	3.83	3.83	37.22

Event stopped short @ 01:45 due to freezing of propane and inability for vendor to refill tank.

Averages: 54.91 16.50 224.55 27.23 119.22 47478.18

Total 37.22

PSH Mass Recovered in Vapor Phase = 5.44 gallons

FID maximum Concentration = 50,000 PPM

Ex: Conversion from ppmv to mg/L (Influent 1)

Measured Conc.	Molecular Wt.	Pressure	Gas Constant	Temp.	Temp.	Conc.
(ppmv)	(Grams)	(atm)	(atm.liter/K.mole)	(F)	(K)	(C_mg/l)
5325	26.6008	1	0.0821	62	289.666667	5.40454711

Inputs are the green values.

Calculated values are yellow.

Constants are purple values.

Outputs are the blue values.

Liquid-phase Hydrocarbon Recovery

$V = r^2 \cdot h = \text{volume}$

Gallons removed determined at time of pick up

PSH Volume in Gallons=

280

PSH Mass in Pounds=

1915.2

SG = 0.82

### Total Hydrocarbon Recovery

PSH Mass Recovered in Vapor Phase =

37.22 lbs

PSH Mass Recovered in Liquid Phase =

5.44 gallons

1915.20 lbs

280.00 gallons

**TOTAL = 1952.42 lbs**

**285.44 gallons**

#### % Vol. (Wt. %) Hydrocarbon to ppmv - Influent 1

Compound	Molecular Weight (g/mol)	Wt. %	=	ppmv
Methane (CH4)	16.04	0		0.00
Ethane (C2H6)	30.07	0		0.00
Propane (C3H8)	44.10	0		0.00
iso-Butane (C4H10)	58.12	0.006		60.00
n-Butane (C4H10)	58.12	0.018		160.00
iso-Pentane (C5H12)	72.15	0.048		480.00
n-Pentane (C5H12)	72.15	0.091		910.00
Hexane+ (C6H14)	87.40	0.583		5830.00
<b>Total</b>				<b>7440.00</b>

\*Hexane+ is treated as 60% hexanes, 30% heptanes, and 10% octanes, as such its  
(0.6\*93.1867)+(0.3\*100.2019)+(0.1\*114.2285) = 97.3966

#### Molecular Weight Calculations

component	Molecular Weight (g/mol)	mol%
Nitrogen (N2)	28.016	97.0480
Methane (CH4)	16.0425	0.0000
Carbon Dioxide (CO2)	44.011	2.7070
Ethane (C2H6)	30.089	0.0000
Propane (C3H8)	44.0958	0.0000
iso-Butane (C4H10)	58.1222	0.0030
n-Butane (C4H10)	58.1222	0.0080
iso-Pentane (C5H12)	72.1488	0.0190
n-Pentane (C5H12)	72.1488	0.0360
Hexane+	97.3966	0.1790
<b>Total</b>		<b>100</b>
<b>Calculated MW</b>		<b>28.6006</b>

Calculated MW=  $\frac{\text{sum (individual component MW x their reported mol\%)}}{100}$

ppmv= % Vol x 10,000

*Lovington Deep 6 – 700376.051.05 - SRS# 2002-10312 – Event 4 – 24 Hour*

**ATTACHMENT 1**  
MDPE Field Logs



Start Date: 28-Feb-13

MDPE FIELD DATA - 24hr 1107 Event#1

TIME	SAMPLE TAKEN	Well Flow			FID Composite (PPM)	Propane Tank (%-size) 75	EXHAUST TEMP F	Well Data				
		Inflent temp. (°f)	Diff. Pressure (INH2O) 2" Preso	Vac (In.Hg)				COMMENTS:				
								MW2	MW13	MW14	MW16	MW17
								VAC (INH2O)				
15:30		62	56.6	19	35789	32	1406	5.9	24.8	21.5	17.8	10.8
16:00	*	62	55.1	19	>50k	70	1408	5.8	23.9	22	11.9	9.1
17:00		62	31.8	18	36705	69	1407	5	22.4	15.8	9.3	8.1
18:00		60	19.8	17	>50k	64	1410	2.7	19.6	12.9	8.8	6.5
19:00		56	19.3	16.5	>50k	59	1410	3.1	20.1	13.3	9.1	6.5
20:00		52	19.9	15.5	49766	55	1408	3.2	20.4	13	9	5.6
21:00		50	19.8	15.5	>50k	50	1410	3.3	19.9	12.8	8.7	6.3
22:00		50	18.9	15.5	>50k	45	1410	2.8	20.4	13.2	8.4	6.2
23:00		50	19.3	15.5	>50k	41	1407	2.4	20.1	13.8	7.3	6.3
0:00		50	19.9	15	>50k	36	1415	3.2	19.8	12.9	7.9	6.2
1:00		50	19.7	15	>50k	33	1409	2.9	19.9	13.6	7.1	6.1

Soil Vacuum Influence

Observation Well	MW15
Extraction Well (EW)	MW2
Time:	In.H2O
16:00	0.05

*Lovington Deep 6 – 700376.051.05 - SRS# 2002-10312 – Event 4 – 24 Hour*

**ATTACHMENT 2**  
Laboratory Analytical Results



INDUSTRIAL LABORATORY  
 2120 M. EMERSON BLVD  
 HOUSTON, TEXAS 77058  
 PHONE: 281-261-3347

## Certificate of Analysis

Number: 1030-2013030100-001A

Simon I. Walshe, CAPM  
 Talon/LPE  
 921 N. Bivins St.  
 Amarillo Texas 79107

March 06, 2013

Sample ID:		Sampled By:	BH
Station Name :	Influent #1	Sample Of:	Gas Spot
Station Number :		Sample Date:	02/28/2013 10:00
Station Location :	Hobbs, NM.	Sample Conditions:	N.G. Pres. , N.G. Temp.
Sample Point:		PO / Ref. No:	

### ANALYTICAL DATA

Components	Mol %	Wt %	GPM at 14.650 psia	Method	Lab Tech.	Date Analyzed
				GPA-2261 M	DK	3/5/2013 4:16:22 AM
Nitrogen	97.048	95.089				
Carbon Dioxide	2.707	4.167				
Iso Butane	0.003	0.006	0.001			
n-Butane	0.008	0.016	0.003			
Iso Pentane	0.019	0.048	0.007			
n-Pentane	0.036	0.091	0.013			
Hexanes Plus	0.179	0.583	0.078			
	<u>100.000</u>	<u>100.000</u>	<u>0.102</u>			
	<b>C2 +</b>	<b>C3 +</b>	<b>iC5 +</b>			
GPM TOTAL :	0.102	0.102	0.098			
Relative Density	Real Gas			0.9871		
Calculated Molecular Weight				28.59		
Compressibility Factor				0.9996		
<b>GPA 2172-09 Calculation :</b>						
<b>Calculated Gross BTU per ft<sup>3</sup> @14.650 psia &amp; 60°F</b>						
Real Gas:	Dry BTU:		12			
	Water Sat. Gas_Base BTU:		11			
Comments :	H2O Mol% - 1.75_Wt% - 1.11					

*Simon I. Walshe*

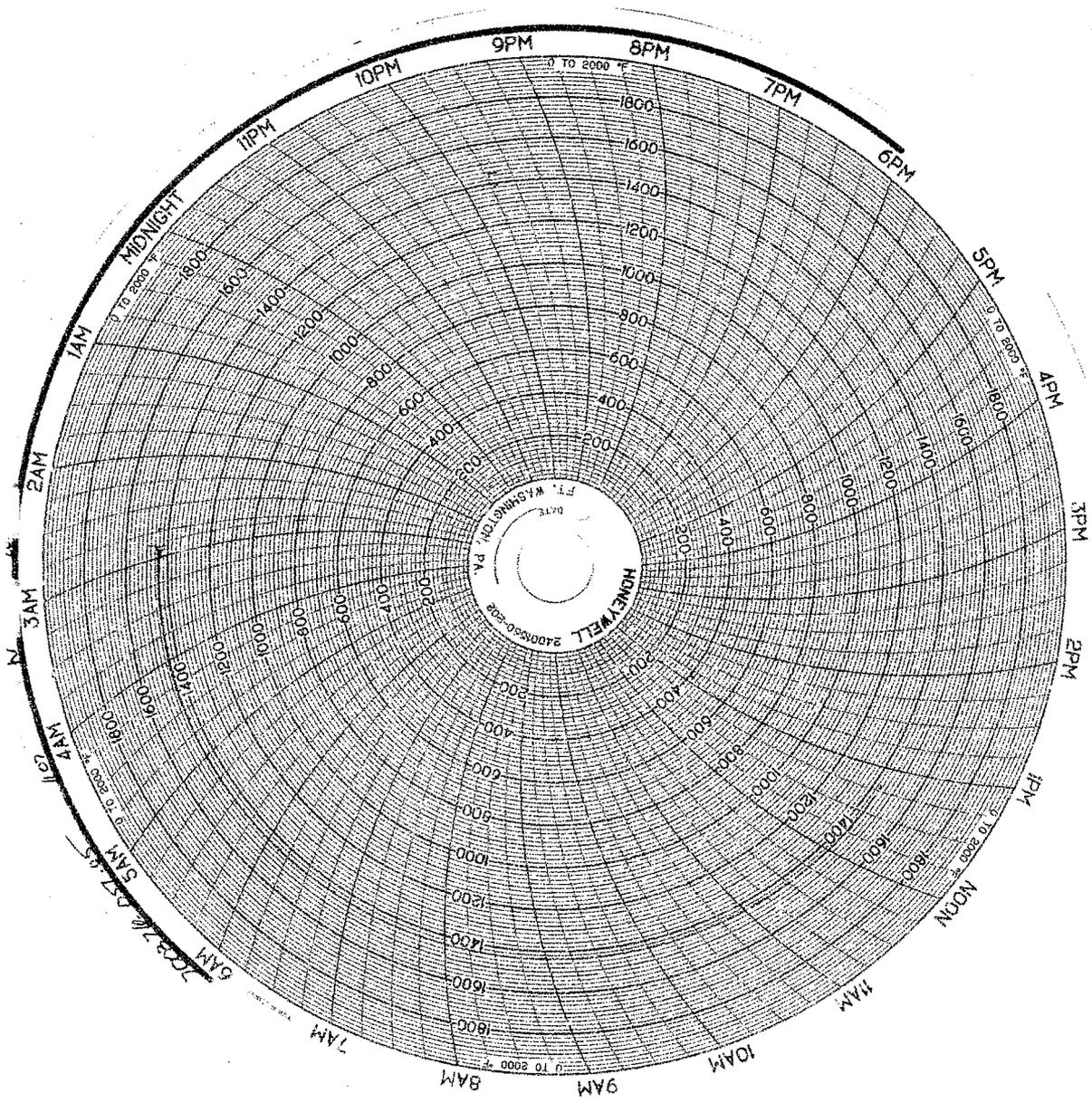
Hydrocarbon Laboratory Manager

**Quality Assurance:**

The above analyses are performed in accordance with ASTM, UOP or GPA guidelines for quality assurance, unless otherwise stated



**ATTACHMENT 3**  
Oxidizer Charts



**ATTACHMENT 4**  
Waste Ticket

