# BEFORE THE OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. 10869 and 10881 Exhibit No.

Yates Petroleum Corporatio Submitted by:

December 2, 1993 Hearing Date:\_

### **BEFORE THE**

### OIL CONSERVATION DIVISION

### NEW MEXICO DEPARTMENT OF ENERGY, MINERALS AND NATURAL RESOURCES

IN THE MATTER OF THE APPLICATION OF YATES PETROLEUM CORPORATION FOR AMENDMENT OF THE SPECIAL RULES AND REGULATIONS OF THE SOUTH DAGGER DRAW-UPPER PENNSYLVANIAN ASSOCIATED POOL (DIVISION ORDER NO. R-5353), EDDY COUNTY, NEW MEXICO. CA

CASE NO. 10869

### **AFFIDAVIT**

STATE OF NEW MEXICO ) ) ss. COUNTY OF SANTA FE )

William F. Carr, attorney in fact and authorized representative of Yates Petroleum Corporation, the Applicant herein, being first duly sworn, upon oath, states that in accordance with the notice provisions of Rule 1207 of the New Mexico Oil Conservation Division the Applicant has attempted to find the correct addresses of all interested persons entitled to receive notice of this application and that notice has been given at the addresses shown on Exhibit "A" attached hereto as provided in Rule 1207.

SUBSCRIBED AND SWORN to before me this If day of December, 1993.

otary Public

My Commission Expires:

14417 19,1995

# EXHIBIT A

Clifford Cone Post Office Box 1629 Lovington, NM 88260

Kenneth G. Cone Post Office Box 11310 Midland, TX 79702

D.C. Trust Marilyn Cone, Trustee Post Office Box 64244 Lubbock, TX 79464

Cathie Cone Auvenshine Post Office Box 658 Dripping Springs, TX 78620-0658

McKay Oil Corporation Post Office Box 2014 Roswell, NM 88201

Nearburg Producing Company 2200 North "A" Street, #8100 Midland, TX 79705-5421

Conoco Inc. 10 Desta Drive West Midland, TX 79705

Marathon Oil Company Post Office Box 552 Midland, TX 79702

Read & Stevens, Inc. Post Office Box 1518 Roswell, NM 88202-1518

# BEFORE THE OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. <u>10869 and 10881</u> Exhibit No. <u>1</u>

Submitted by: Yates Petroleum Corporation

Hearing Date: December 2, 1993

AFFIDAVIT, Page 2 Citation Oil & Gas Corporation 8223 Willow Place South, Suite 250 Houston, TX 77070-5623

Barbara Fasken 303 W. Wall Avenue, Suite 1900 Midland, TX 79701-5116

AFFIDAVIT, Page 3

# CAMPBELL, CARR, BERGE

# & SHERIDAN, P.A.

MICHAEL B. CAMPBELL WILLIAM F. CARR BRADFORD C. BERGE MARK F. SHERIDAN WILLIAM P. SLATTERY

PATRICIA A. MATTHEWS MICHAEL H. FELDEWERT DAVID B. LAWRENZ TANYA M. TRUJILLO

JACK M. CAMPBELL OF COUNSEL JEFFERSON PLACE SUITE I - IIO NORTH GUADALUPE POST OFFICE BOX 2208 SANTA FE, NEW MEXICO 87504-2208 TELEPHONE: (505) 988-4421 TELECOPIER: (505) 983-6043

October 28, 1993

# <u>CERTIFIED MAIL -</u> <u>RETURN RECEIPT REQUESTED</u>

Clifford Cone Post Office Box 1629 Lovington, NM 88260

> Re: Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

Dear Mr. Cone:

This letter is to advise you that Yates Petroleum Corporation has filed the enclosed application with the New Mexico Oil Conservation Division seeking amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool by deletion of Rule 5(b) thereby authorizing the simultaneous dedication of both gas wells and oil wells to the same spacing unit.

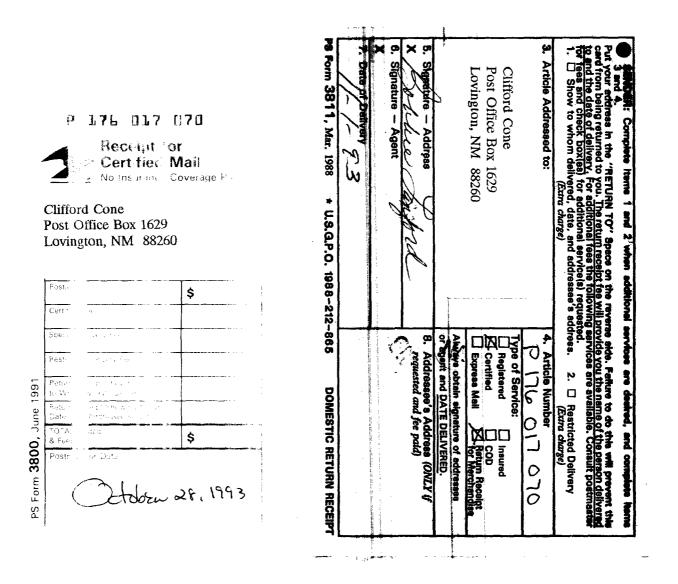
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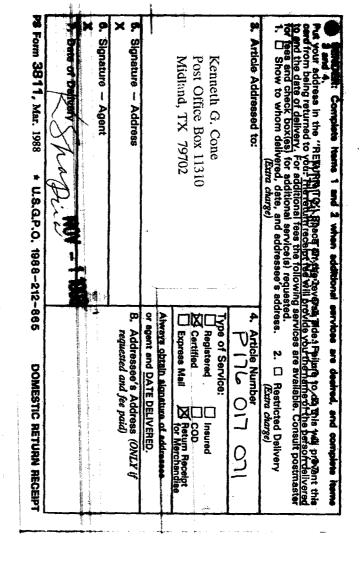
Parties appearing in cases have been requested by the Division (Memorandum 2-90) to file a Pre-hearing Statement substantially in the form prescribed by the Division. Pre-hearing statements should be filed by 4:00 o'clock p.m., on the Friday before a scheduled hearing.

Very truly yours,

lion

WILLIAM'F. CARR ATTORNEY FOR YATES PETROLEUM CORPORATION WFC:mlh Enclosure

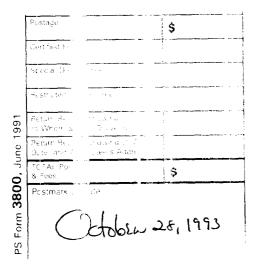




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Receip for Sertified Mail No insurance Coverage Provide

Kenneth G. Cone Post Office Box 11310 Midland, TX 79702



# CAMPBELL, CARR, BERGE & SHERIDAN, P.A.

LAWYERS

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October 28, 1993

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D.C. Trust Marilyn Cone, Trustee Post Office Box 64244 Lubbock, TX 79464

> Re: Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

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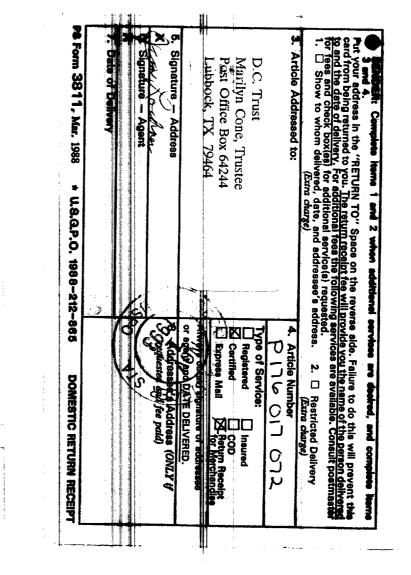
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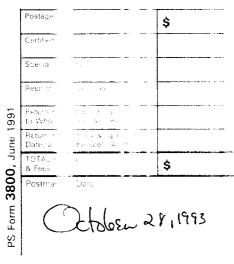
WILLIAM F. CARR ATTORNEY FOR YATES PETROLEUM CORPORATION WFC:mlh



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Receipt for Certifiext Mail No Insuring Proverage Struck

D.C. Trust Marilyn Cone, Trustee Post Office Box 64244 Lubbock, TX 79464



# CAMPBELL, CARR, BERGE & SHERIDAN, P.A.

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October 28, 1993

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Kenneth G. Cone Post Office Box 11310 Midland, TX 79702

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October 28, 1993

## <u>CERTIFIED MAIL -</u> <u>RETURN RECEIPT REQUESTED</u>

Cathie Cone Auvenshine Post Office Box 658 Dripping Springs, TX 78620-0658

> Re: Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

Dear Ms Cone:

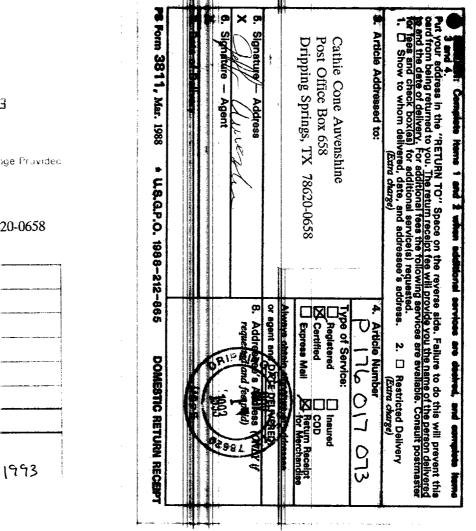
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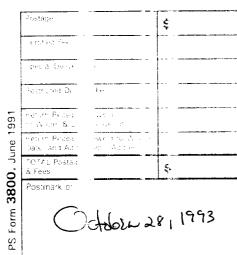
WILLIAM F. CARR 'ATTORNEY FOR YATES PETROLEUM CORPORATION WFC:mlh Enclosure



P 126 017 073

E Despt 10. rtified Mail insurance Coverage Provided

Cathie Cone Auvenshine Post Office Box 658 Dripping Springs, TX 78620-0658



## CAMPBELL, CARR, BERGE

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October 28, 1993

# <u>CERTIFIED MAIL -</u> <u>RETURN RECEIPT REQUESTED</u>

McKay Oil Corporation Post Office Box 2014 Roswell, NM 88201

> Re: Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

Gentlemen:

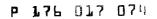
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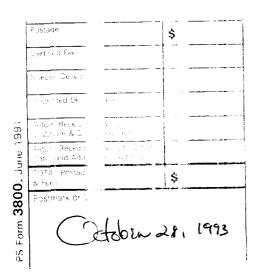


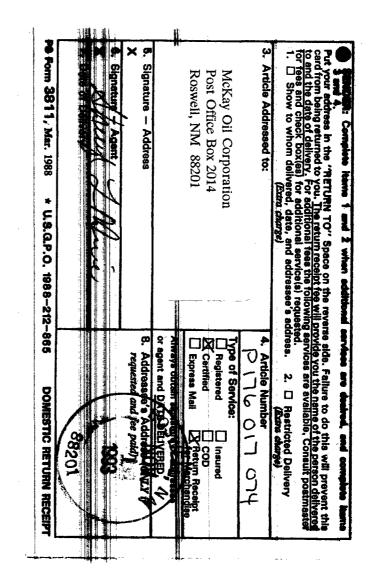


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McKay Oil Corporation Post Office Box 2014 Roswell, NM 88201





# CAMPBELL, CARR, BERGE

# **8** SHERIDAN, P.A.

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Nearburg Producing Company 2200 North "A" Street, #8100 Midland, TX 79705-5421

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Nearburg Producing Company 2200 North "A" Street, #8100 Midland, TX 79705-5421

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October 28, 1993

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Very truly yours,

WILLIAM F. CARR ATTORNEY FOR YATES PETROLEUM CORPORATION WFC:mlh Enclosure

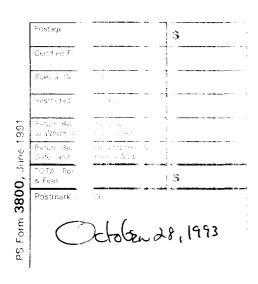
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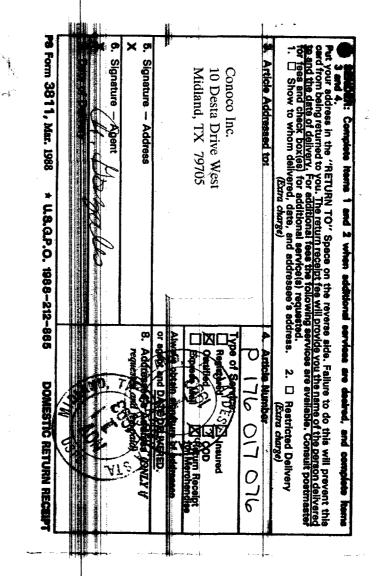


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Conoco Inc. 10 Desta Drive West Midland, TX 79705





# CAMPBELL, CARR, BERGE & SHERIDAN, P.A.

LAWYERS

MICHAEL B. CAMPBELL WILLIAM F. CARR BRADFORD C BERGE MARK F SHERIDAN WILLIAM P. SLATTERY

PATRICIA A. MATTHEWS MICHAEL H. FELDEWERT DAVID B. LAWRENZ TANYA M. TRUJILLO

JACK M. CAMPBELL OF COUNSEL JEFFERSON PLACE SUITE I - HO NORTH GUADALUPE POST OFFICE BOX 2208 SANTA FE, NEW MEXICO 87504-2208 TELEPHONE: (505) 988-4421 TELECOPIER: (505) 983-6043

October 28, 1993

### <u>CERTIFIED MAIL -</u> <u>RETURN RECEIPT REQUESTED</u>

Marathon Oil Company Post Office Box 552 Midland, TX 79702

> Re: Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

Gentlemen:

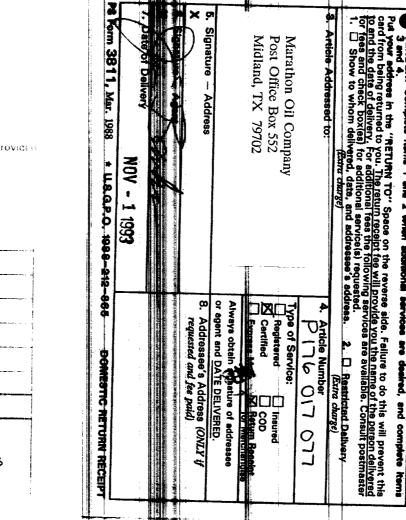
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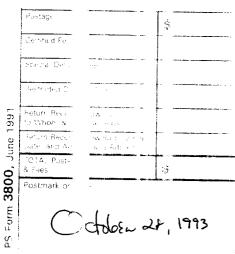
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> Insurance to - rage Provideo Marathon Oil Company

Post Office Box 552 Midland, TX 79702



# CAMPBELL, CARR, BERGE & SHERIDAN, P.A.

LAWYERS

MICHAEL B. CAMPBELL WILLIAM F. CARR BRADFORD C. BERGE MARK F. SHERIDAN W LLIAM P. SLATTERY

PATRICIA A. MATTHEWS MICHAEL H. FELDEWERT DAVID B. LAWRENZ TANYA M. TRUJILLO

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October 28, 1993

# <u>CERTIFIED MAIL -</u> <u>RETURN RECEIPT REQUESTED</u>

Read & Stevens, Inc. Post Office Box 1518 Roswell, NM 88202-1518

> Re: Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

Gentlemen:

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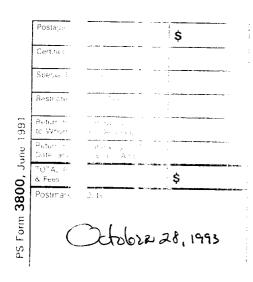
WILLIAM F. CARR ATTORNEY FOR YATES PETROLEUM CORPORATION WFC:mlh Enclosure

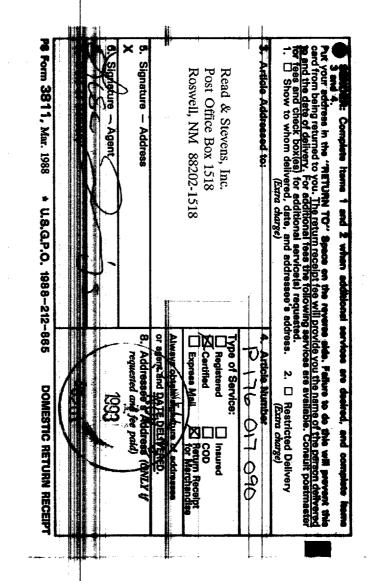
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Read & Stevens, Inc. Post Office Box 1518 Roswell, NM 88202-1518





### CAMPBELL, CARR, BERGE

# **8** SHERIDAN, P.A.

LAWYERS

MICHAEL B CAMPBELL WILLIAM F CARR BRADFORD C. BERGE MARK F. SHERIDAN WILLIAM P. SLATTERY

PATRICIA A. MATTHEWS MICHAEL H. FELDEWERT DAVID B. LAWRENZ TANYA M. TRUJILLO

> JACK M. CAMPBELL OF COUNSEL

JEFFERSON PLACE SUITE I - 110 NORTH GUADALUPE POST OFFICE BOX 2208 SANTA FE, NEW MEXICO 87504-2208 TELEPHONE: (505) 988-4421 TELECOPIER: (505) 983-6043

October 28, 1993

# <u>CERTIFIED MAIL -</u> <u>RETURN RECEIPT REQUESTED</u>

Citation Oil & Gas Corporation 8223 Willow Place South, Suite 250 Houston, TX 77070-5623

> Re: Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

Gentlemen:

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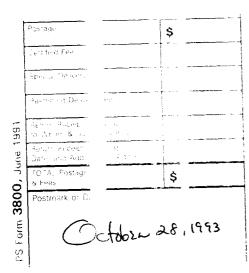
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Citation Oil & Gas Corporation 8223 Willow Place South, Suite 250 Houston, TX 77070-5623



-865 DOMESTIC RETURN RECEIPT	P8 Form 3811, Mar. 1988 + U.S.G.P.O. 1988-212-865
	7. Date of Delivery
	8. Signature Agent X X · Allred
8. Addressee's Address (ONLY if requested and fee paid)	5. Signature – Address X
Always obtain signature of addressee or agent and DATE DELIVERED.	
Centified Control Cont	8223 Willow Place South, Suite 250 Houston, TX 77070-5623
	Citation Oil & Gas Corporation
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# CAMPBELL, CARR, BERGE

# & SHERIDAN, P.A.

LAWYERS

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PATRICIA A. MATTHEWS MICHAEL H. FELDEWERT DAVID B LAWRENZ TANYA M TRUJILLO

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October 28, 1993

# <u>CERTIFIED MAIL -</u> <u>RETURN RECEIPT REQUESTED</u>

Barbara Fasken 303 W. Wall Avenue, Suite 1900 Midland, TX 79701-5116

> Re: Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

Dear Ms Fasken:

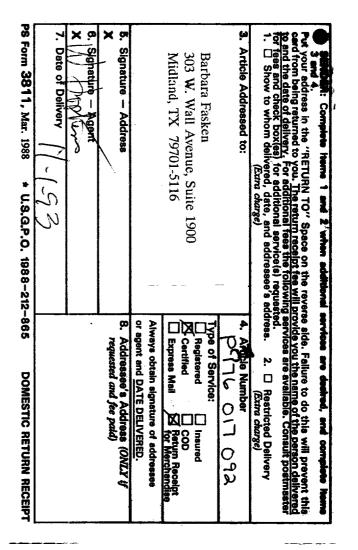
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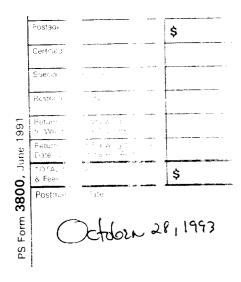
WILLIAM F. CARR ATTORNEY FOR YATES PETROLEUM CORPORATION WFC:mlh Enclosure



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Receipt to Certified Mail Do Insurce en versee Free

Barbara Fasken 303 W. Wall Avenue, Suite 1900 Midland, TX 79701-5116

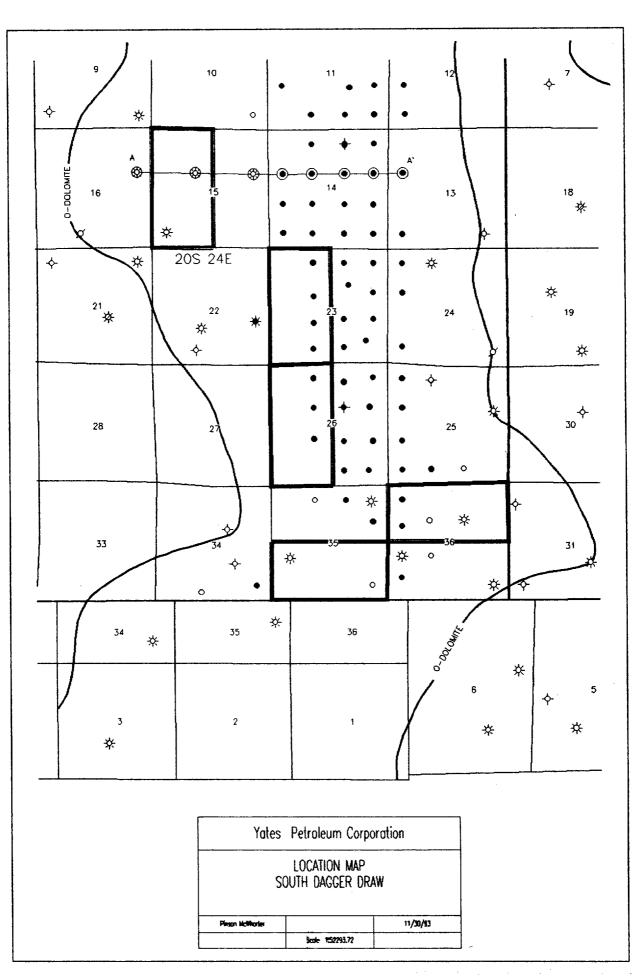


# BEFORE THE OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. <u>10869 and 10881</u> Exhibit No. <u>1</u>

Submitted by: Yates Petroleum Corporation

Hearing Date: December 2, 1993



# BEFORE THE OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. <u>10869 and 10881</u> Exhibit No. <u>2</u> Submitted by: <u>Yates Petroleum Corporation</u>

Hearing Date: December 2, 1993

Hearing Date: ecember 2, 1993 Submitted by: Yates Petroleum Corporation

Case Nos. 10869 and 10881 Exhibit No. ယ

# **BEFORE THE** IL CONSERVATION DIVISION Santa Fe, New Mexico

32 Hillview AHE Federal Com #3 33 Hillview AHE Federal Com #13	John AGU #1	30 Charolette McKay Federal Com #4	29 Saguaro AGS Federal Com #9	28 Hillview AHE Federal Com #2	27 Conoco AGK Federal #4	26 Hillview AHE Federal Com #10	25 Hillview AHE Federal Com #4	24 Saguaro AGS Federal Com #8	23 Conoco AGK Federal #2	22 Hillivew AHE Federal Com #16	21 Prickly Pear AIE Federal Com #1	20 Ceniza AGZ Com #3	19 Conoco AGK Federal #11	18 John AGU #3	17 John AGU #4	16 Sara AHA Com #5	15 Hillview AHE Federal #8	14 Conoco AGK Federal Com #10	13 Indian Hills State Com #4	12 Dahlia ALA Com #1	11 Sara AHA Com #4	10 Saguaro AGS Federal Com #1	9 John AGU #7	8 Hillview AHE Federal Com #5	7 Saguaro AGS Federal Com #5	6 Hillview AHE Federal Com #6	5 Conoco AGK Federal #9	4 Indian Hills State Com #3	3 Ceniza AGZ Com #2	2 Charolette McKay Federal Com #2	1 Saguaro AGS Federal Com #10	Well Name		
N 23-205-24E I 14-205-24E	C 14-20S-24E	E 25-20S-24E	C 23-20S-24E	G 23-20S-24E	A 26-20S-24E	H 23-20S-24E	J 23-20S-24E	0 14-20S-24E	G 26-20S-24E	M 14-20S-24E	P 23-20S-24E	E 13-20S-24E	J 26-20S-24E	G 14-20S-24E	H 14-20S-24E	N 11-20S-24E	P 14-20S-24E	J 11-20S-24E	E 36-20S-24E	L 25-20S-24E	0 11-20S-24E	L 11-20S-24E	E 14-20S-24E	A 23-20S-24E	F 23-20S-24E	B 23-20S-24E	P 26-20S-24E	D 36-20S-24E	M 12-20S-24E	D 25-20S-24E	C 26-20S-24E	Location		-
4364 1549	3730	3098	2148	1630	4261	1401	1694	2310	3228	539	3955	49	2697	668	1711	2253	747	920	2827	2167	922	1220	1359	1422	1603	607	4433	1884	125	2084	1848	Oil	July, 1993	
14516 5151	12460	10609	7728	5869	15767	5329	6571	9389	13733	2519	19130	251	14633	3646	10086	14404	5060	6479	20682	16590	7638	10663	12465	13582	15971	6054	47141	21725	1733	37778	37347	Gas	993	
4255 1476	3534	1540	2025	1407	3746	953	1630	2428	3196	490	3599	76	2457	637	1524	2103	725	854	3021	1982	912	1150	1186	1117	1589	555	4475	755	107	2668	894	<u>O</u> I	August, 1993	PRODUCTION
15205 5015	11767	6226	8266	5559	15277	4944	5621	9063	10720	2227	19673	958	15163	3367	8758	14845	4764	7054	22706	15529	7451	10504	17996	14477	15631	6482	49358	15562	1308	37818	31732	Gas	1993	CTION
3881 1210	2944	687	1824	1190	3319	735	1242	2112	2875	473	3043	57	2292	593	1312	1931	500	804	3175	1790	816	1063	1069	266	1599	486	3956	1865	117	2701	1570	oï	September, 1993	
14823 4395	10499	9310	7302	5454	14286	4306	9023	9470	8581	1892	18307	886	14560	3024	7938	13612	4162	6104	25132	13554	6525	8818	14643	11048	15081	5958	46002	29732	1144	36145	27559	Gas	er, 1993	
3,326 3,325	3,340	3,424	3,598	3,601	3,700	3,804	3,879	4,065	4,254	4,673	4,837	5,122	5,426	5,458	5,895	6,393	6,774	7,042	7,316	7,656	8,284	8,740	9,172	9,551	9,963	9,974	10,634	11,531	13,864	18,128	20,209	Scf/Bbl	Jul-93	GA
3,573 3,398	3,330	4,043	4,082	3,951	4,078	5,188	3,448	3,733	3,354	4,545	5,466	12,605	6,171	5,286	5,747	7,059	6,571	8,260	7,516	7,835	8,170	9,134	15,174	12,961	9,837	11,679	11,030	20,612	12,224	14,175	35,494	Scf/Bbl	Aug-93	GAS-OIL RATIO
3,819 3,632	3,566	13,552	4,003	4,583	4,304	5,859	7,265	4,484	2,985	4,000	6,016	15,544	6,353	5,099	6,050	7,049	8,324	7,592	7,916	7,572	7,996	8,295	13,698	11,137	9,432	12,259	11,628	15,942	9,778	13,382	17,554	Scf/Bbl	Sep-93	0

South Dagger Draw

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Oil Well GOR

GOR-2.XLS/pbs

Page 1

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GOR-2.XLS/pbs

22 of 56 wells > 4500:1 (39%)

7 of 56 wells ≥ 10,000:1 (12.5%)

39 John AGU #5 37 36 John AGU #2 35 Senita AIP Federal Com #1 34 40 Ceniza AGZ Com #4 38 Staghorn AJG Federal Com #1 26 55 54 23 52 51 Hillview AHE Federal Com #17 20 49 48 47 46 **4**5 44 Hillview AHE Federal Com #12 43 Saguaro AGS Federal Com #4 Sara AHA Com #1 Staghorn AJG Federal Com #2 Conoco AGK Federal #15 Conoco AGK Federal #8 John AGU #6 Conoco AGK Federal #5 Saguaro AGS Federal Com #12 Senita AIP Federal Com #2 Mayer 24 #2 Mayer 24 #1 Sara AHA Com #6 Palo Verde AJV Federal #1 Conoco AGK Federal #3 Conoco AGK Federal Com #6 Hillview AHE Federal Com #7 Well Name **Oil Well Totals** 14-20S-24E 14-20S-24E 13-20S-24E 23-20S-24E 25-20S-24E 14-20S-24E 24-20S-24E 24-20S-24E 11-20S-24E 25-20S-24E 23-20S-24E 24-20S-24E 26-20S-24E 26-20S-24E 26-20S-24E 26-20S-24E 14-20S-24E 26-20S-24E 14-20S-24E 12-20S-24E 14-20S-24E 11-20S-24E 14-20S-24E Location 132428 11886 0ii 3395 6871 1633 1780 1964 2916 2778 6567 1499 1847 1489 1928 July, 1993 5177 7614 2925 2235 1230 457 **781** 581347 16158 28434 Gas 13994 11336 3850 8163 5506 333( 7687 4534 5342 8197 1335 8308 1443 5989 6329 2117 1685 4884 118341 August, 1993 <u>0</u> 10375 1431 2439 3305 5147 1706 1805 1959 1211 3458 6428 7043 2816 1644 2586 1775 1327 1789 326 705 0 560786 17670 26857 Gas 12523 10091 3346 3749 5891 5048 7585 4512 1670 1613 1132 5215 7645 7750 5614 4816 6249 746 80 104510 September, 1993 <u>o</u> 6074 4523 8223 1466 1924 1088 1485 1032 3572 5343 2387 1530 2987 1242 1275 2206 1445 1720 628 138 534471 16984 11817 22734 Gas 9524 3575 4418 2913 7288 2800 4533 6277 1637 1364 5822 7272 4275 4503 5436 815 320 688 Scf/Bbl 4,390 2,358 2,811 Jul-93 1,577 1,838 2,221 2,352 2,547 2,720 2,991 3,158 3,243 3,283 1,726 1,882 2,264 2,392 3,280 1,370 1,709 947 Scf/Bbl Aug-93 4,739 2,433 2,645 3,134 3,493 1,332 1,704 1,606 1,570 2,509 1,793 2,035 2,295 2,620 2,589 2,889 2,997 2,288 3,163 3,629 852 Scf/Bbl Sep-93 5,114 1,630 2,614 2,878 3,092 3,780 6,442 2,958 4,139 3,661 1,298 2,796 2,440 2,765 2,196 2,845 1,322 1,783 1,851 1,904 952

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South Dagger Draw

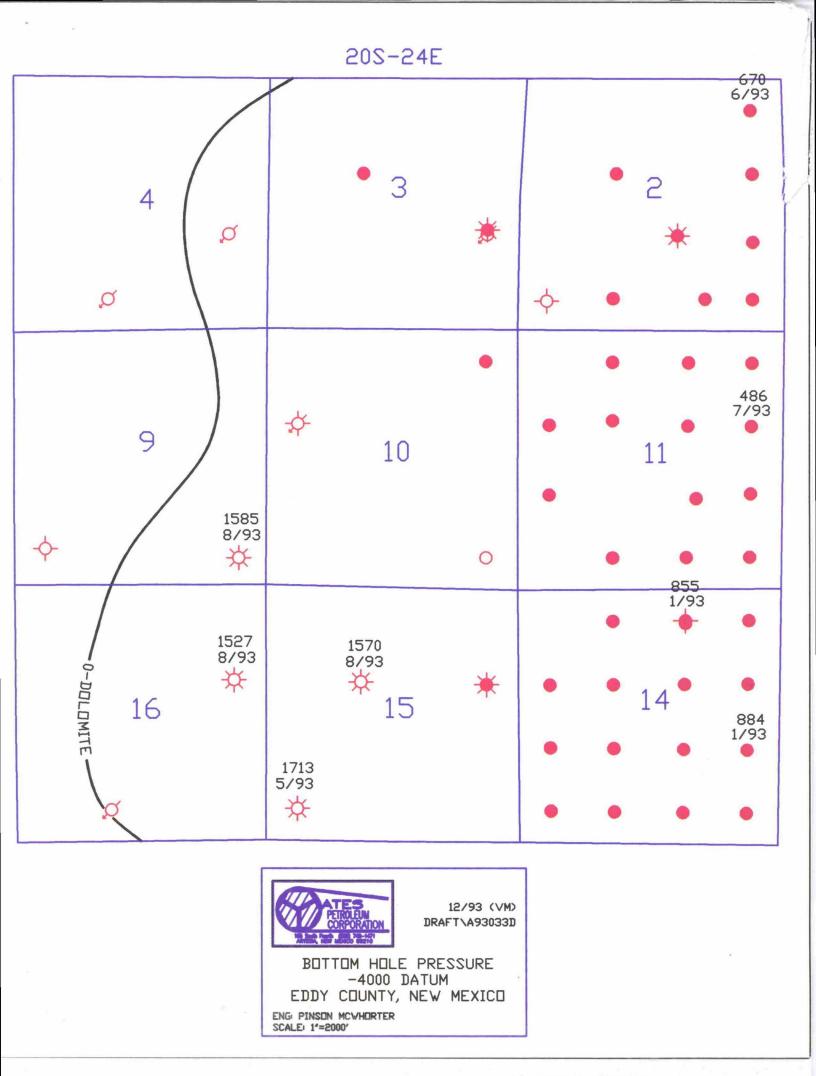
**Oil Well GOR** 

PRODUCTION

**GAS-OIL RATIO** 

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# BEFORE THE OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. 10869 and 10881 Exhibit No. 4

Submitted by: Yates Petroleum Corporation

Hearing Date: December 2, 1993

# BEFORE THE OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. <u>10869 and 10881</u> Exhibit No. <u>5</u>

Submitted by: Yates Petroleum Corporation

Hearing Date: December 2, 1993



SCIENTIFIC SOFTWARE-INTERCOMP

Advanced Technology for the Petroleum Industry

# RESERVOIR SIMULATION STUDY 3-D SECTOR AREA CANYON RESERVOIR DAGGER DRAW FIELD, NEW MEXICO

FINAL REPORT

**NOVEMBER 1993** 

PERFORMED FOR: YATES PETROLEUM CORPORATION

PERFORMED BY: SCIENTIFIC SOFTWARE-INTERCOMP, INC.

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- Table 3Reservoir Fluid Properties
- Table 4
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- Table 5
   Prediction Simulations Reservoir Performance Summary

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- Figure 15 Prediction Case 1 Model Production Water

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### SUMMARY

SSI was authorized by Yates to perform a reservoir simulation study on the Canyon reservoir, Dagger Draw field in New Mexico. The objective of the study was to determine the effect of gas cap depletion on down dip oil production.

SSI constructed a representative 3-D simulation model containing one row of wells (east-west) extending from the gas cap through the oil and water column. The simulation model was calibrated by performing history match simulation runs. After the simulation model was properly calibrated for the history period (January 1990 through October 1992), three 26-year prediction runs were made to investigate the effect of gas cap depletion on oil production down dip.

The following table summarizes the 26 year oil recoveries obtained from each prediction case:

	CASE 1	<u>CASE 2</u>	CASE 3
End of Case	December, 2018	December, 2018	December, 2018
Oil, MSTB	682	684	682
Gas, BSCF	19.5	9.7	21.5

**Case 1 - Continued Depletion** 

Case 2 - Continued Depletion without Gas Cap Depletion

Case 3 - Continued depletion with Gas Cap Infills

Operational changes in the management of the gas cap have little effect on oil recoveries in the oil leg down dip. This is consistent with the geological evaluation that indicated a tortuous lateral connection (with some sedimentary barriers) between the gas cap and the oil leg.

The simulations in this study were performed using SSI's SimBest II simulator. The simulator was run in single porosity, three phase (black oil) mode. The simulation and post-processor modules

of WorkBench were used in construction of the initial reservoir model, in making modifications to the model during history matching, and in the display of the results (tables, plots, and maps) of all simulations.

The 3-D sector reservoir simulation model consisted of 552 grid cells  $(23 \times 3 \times 8)$ . The model contained eight layers corresponding to the correlation units derived from geologic evaluation. The initial reservoir rock properties (net thickness, porosity, permeability, relative permeability, and capillary pressure) and fluid properties of the simulation model were derived from the results of geological, petrophysical, and engineering analyses.

The initial simulation model was calibrated through a history matching procedure. Well oil rates were specified in the model, and pressures, gas rates, and water rates were calculated by the simulation model. In order to account for high volumes of water production in the up dip portion of the reservoir, a modeling scheme was required to create high initial water saturations up dip without adversely affecting oil and gas production in the mid dip and down dip portions of the reservoir.

The resulting model utilized isolated model layers with high capillary pressures in Layers 5 and 6. This resulted in high water saturation values up dip for Layers 5 and 6. Layer 4 contained most of the hydrocarbon volumes. The initial input porosity and permeability values were modified accordingly to obtain history matches on pressure, gas production and water production. This calibrated model was then used for the prediction simulations.

The discussion section contains more detailed descriptions of the simulation model and the simulation runs.

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### DISCUSSION

### **RESERVOIR SIMULATION**

The following sections of this report describe the construction of the initial reservoir simulation model and the calibration of the reservoir characterization within the model during history matching. The history period was defined as January, 1990 to the end of October, 1992.

The simulations in this study were performed using SimBest II (version 3.1 15), SSI's three-dimensional, multi-phase, dual porosity reservoir simulator. The simulator was run in single-porosity, three-phase (black oil) mode. The simulation and post-processor modules of WorkBench were used in construction of the initial reservoir model, in making modifications to the model during history matching, and in the display of the results (tables, plots, and maps) of all simulations.

The methods and results of the simulation phases of this study are discussed in the following sections of this report and illustrated in the accompanying tables, figures, and appendices. In addition, listings of the final input and output data for all simulations have been provided to Yates in tape format.

### **Model** Construction

The initial reservoir rock and fluid properties of the simulation model were derived from the results of the geological, petrophysical, and engineering analyses. The 3-D sector model covers an area 13,800 by 1,800 feet (2.6 by 0.3 miles). The grid is shown in Figures 1 and 2. The model contains one row of wells (east-west) extending from the gas cap (wells AIG 1, SAG 2, and SARA 2) through the oil column and into the water column (wells JOHN 5, JOHN 3, JOHN 4, and CEN 3). The grid contains 23 cells in the x-direction (east-west) and 3 cells in the y-direction (north-south). The model contains eight layers. This results in a total of 552 cells, but not all of these cells are active. The areal dimensions of each cell are 600 by 600 feet. Square cells were used to minimize the numerical dispersion effects of rectangular cells.

The structural depths of each of the layers at each grid location were determined from the structure and gross thickness maps constructed during the initial geological analyses.

The characteristics of the reservoir rock are defined in the simulator on a cell-by-cell basis. The reservoir characteristics include the following:

- net reservoir thickness
- effective porosity
- effective permeability (in the x, y and z directions)
- relative permeability
- capillary pressure

All the properties listed above are representative of the net reservoir. For example, the values of effective porosity are average values for the net reservoir rock and do not include porosities which are below the cutoffs.

Net thickness maps were input in digital form to the initial reservoir simulation model. Net thickness values are used in the model primarily in the calculation of volumetrics and conductivity. Any changes to the volumetrics ( $\phi$ h) or conductivity (kh) during history matching may imply change to the net thickness, porosity, or permeability. Changes to conductivity due to stratigraphic or structural barriers were implemented in the model as modifications to transmissibility between cells since these barriers do not require changes to the reservoir rock permeability.

Effective porosity maps were digitized and input into the initial reservoir simulation model. These values were entered on a cell-by- cell basis and are representative of the net reservoir, not the gross reservoir. These initial porosity values were used in the initial estimation of horizontal permeabilities. The primary effect of porosity in the simulation model is on the calculation of volumetrics. Porosities were modified heavily during the history matching phase.

The effective horizontal permeabilities used in the initial reservoir description of the simulation model were calculated on a cell-by-cell basis from the porosity-permeability relationships derived from cross plots of porosity and permeability. Plots of air permeability vs. core porosity were made

for each simulation model layer (Appendix I). Core data were not available for Layer 1. Based on these plots, the following equations were derived and used to transform average porosity for each simulation cell in each layer to horizontal permeability:

LAYER	HORIZONTAL PERMEABILITY EFFECTIVE POROSITY RELATIONSHIP
1	Log K = 22.9885 * (φ) - 1.0555
2	Log K = 22.9885 * (φ) - 1.0555
3	Log K = 60.6061 * (φ) - 2.1079
4	Log K = 45.4545 * (φ) - 1.5017
5	Log K = 23.2558 * (\$) - 1.1367
6	Log K = 16.6436 * (¢) - 0.9393
7	$Log K = 20 * (\phi) - 0.8$
8	Log K = 26.3158 * (\$) - 0.8697

Three permeability arrays were input to the reservoir simulation model. These correspond to permeabilities in the x, y, and z direction. There were no data to suggest that x and y permeabilities should differ. As far as the z direction permeability, vertical transmissibility between layers was reduced to zero to reflect the presence of permeability reductions and sealing barriers within the model layers.

The laboratory core analysis performed by Scal, Inc. (Appendix II) was the basis for the relative permeability used in the simulation model. The Scal relative permeability analysis was performed on extracted cores. Since the core samples were not preserved, the Scal analysis was used only as a starting point to determine saturation and relative permeability endpoints.

Through cross-sectional model simulation, pseudo relative permeability curves were developed in order to match oil and water rates in the reservoir. In particular, the water relative permeability at residual oil saturation was increased to .5947. This change was necessary for the model to calculate and match the high volumes of water produced throughout the reservoir especially in the up dip

areas within the gas cap. Also the oil relative permeability at critical gas saturation was increased to .7174 in order to match oil production rates in the mid dip areas of the reservoir.

Segregated flow was assumed, and straight-line relative permeabilities were used as depicted in Figure 3. Table 1 summarizes the relative permeability endpoints that were used for the water-oil and gas-oil relative permeability data in the simulation model.

High capillary pressure was used in Layers 5 and 6 to create a large water-oil transition zone in those layers in order to allow up dip water production in the simulation model. Figure 4 illustrates and Table 2 summarizes the capillary pressures which were used in the simulation model.

Only one set of fluid properties was required by the simulation model to characterize the fluids in this reservoir. These properties were derived from available fluid data and correlations. The saturated oil properties (gas-oil ratio, formation volume factor, compressibility, and viscosity) and the gas properties (formation volume factor and viscosity) were assigned to the model based on saturation pressure. Undersaturated oil properties were calculated by the model from the saturation pressure, the reservoir pressure, the compressibility, and the modified undersaturated viscosity slope. Table 3 and Figures 5 through 9 summarize the PVT data input.

Yates provided SSI with a Core Labs' reservoir fluid analysis report. This report is included in Appendix III. The analysis was performed in April 1990. At that time the reservoir pressure had dropped below 2000 psia, and the saturation pressure that was reported in the analysis was 2003 psig.

The original pressure of the reservoir is believed to be 3000 psig. The saturation pressure is also believed to be equal to the original reservoir pressure. Therefore, SSI used correlations provided within WorkBench to create PVT "data" giving a saturation pressure of 3015 psia and oil API gravity of 42.7, etc.

For wells located within the gas cap (wells Algerita 1, Saguaro 2, and Sara 2), gas production rates were specified in the simulation model. For all other wells in the model, oil production rates were

specified. The production data were derived from the monthly production reports provided by Yates. The production data were specified in the model on a quarterly basis.

Wells were completed in model layers according to perforation depths supplied by Yates. Since fracture treatments were performed on all wells, these initial well completions were not considered completely reliable. In order to account for hydraulic fracture production near the wellbore, well completions were altered as needed during the history match.

### **History Matching Procedure**

Most of the initial reservoir description was based, by necessity, on measurements made at the points in the reservoir which were penetrated by wells. Most of these measurements do not reveal information about the reservoir characteristics between and beyond wells. Due to the small percentage of the reservoir that is directly sampled, and the range of accuracy of some of the measurements themselves, even a carefully derived initial reservoir description may not represent the actual reservoir with complete accuracy.

The objective of the history matching phase of this study was to adjust the reservoir description to a more accurate representation of the field. Mathematical reservoir simulators have proven to be reliable in reproducing the physical processes taking place in petroleum reservoirs. The quality of the results derived from a simulator depends primarily on the quality of the final reservoir description. The quality of this final description depends partially on the quality and quantity of the basic data used to derive the initial description.

The quality of the simulation results also depends on the quality and quantity of the measurements of historical reservoir behavior and quality of the match of these measurements by the simulator. The quality of measurements of historical behavior is average for this reservoir. Oil, gas, and water volumes seem to be measured very well. However, pressure data are limited. Only a handful of wells within the study area have pressure data. Those wells that have pressure data have only one pressure point in time. In addition, there are no pressure data for isolated layers or zones. The length of the history period for most wells is two or three years, which is a fairly short period for a history match. These facts, combined with the moderate quantity and quality of the data used to determine the initial reservoir description, indicate that the final reservoir description derived from a satisfactory history match can be used with moderate confidence to predict future reservoir behavior. The limitations imposed by the short history period for most wells and the quality of the initial reservoir description should be remembered when interpreting the results of the prediction cases.

It is through the iterative process of "matching" the measured reservoir behavior that the initial reservoir description is adjusted to its final form. Adjustments in this study were made only to reservoir characteristics which were not known with accuracy. Changes to these characteristics were maintained within a reasonable range for the particular parameter.

The history match parameters for this study were:

- reservoir pressure
- gas production
- water production

The oil production rates were specified by well on a quarterly basis in the simulator. The three parameters listed above were calculated by the simulator for each well and compared to the values measured in the field. For wells within the gas cap, gas production was specified, and reservoir pressure and water production were calculated by the simulator for each well and compared to field measured data. The following section of this report discusses the procedures followed to match each of the parameters listed above.

### **Reservoir Pressure Match**

As mentioned previously, there was not an abundance of pressure data available for the sector area. However, the data that were available indicated that reservoir pressure had dropped quickly from an initial value of 3000 psig to around 1000 psig in three years of sustained field production.

Areal averages of pressure were made from existing pressure data so that well pressures could be matched to some "ball park" number depending upon the well's location within the sector area. In general pressures taken in the fall of 1992 were around 1800 psig for the up dip region of the gas cap, 1200 psig for the mid dip region and 800 to 1000 psig for the down dip region.

Since so few wells had pressure data and only a few had two pressure points, less emphasis was placed on pressure matching. The goal was to obtain pressures which were reasonable for each well, given its location within the reservoir.

Early simulation runs were made with all three phases (oil, gas, and water rates) specified. This was done to insure proper voidage in the early stages of history matching. With the proper voidage rate specified for each well, calculated pressures were compared to actual pressures and "ball park" estimates for each well. Most wells required porosity adjustments to all completed layers to correct the pressure level. Some wells required permeability adjustments to all completed layers to correct the shape of the pressure curve.

These porosity and permeability adjustments were first made on an areal basis and then on a well-by-well basis. Modifications were made equally to all completed layers since historical pressure data for isolated layers were not available.

### Saturation Match (Gas and Water Production)

Better data were available for historical gas and water production. In the saturation match simulation runs, only oil rate was specified, and the simulation calculated pressures, gas rates, and water rates were compared to observed data. However for the gas cap wells, gas rate was specified, and the simulation calculated pressures and water rates were compared to observed data.

The biggest problem to overcome in history matching this reservoir was modeling water production up dip in the gas cap without affecting gas and oil production in the mid dip and down dip regions. The simulation model consisted of isolated layers with no vertical transmissibility between layers. Layers 5 and 6 were assigned a very high capillary pressure to create a large water-oil transition zone resulting in high initial water saturations up dip in these layers.

With this model, most of the hydrocarbon production was obtained from Layer 4. By modifying permeabilities for Layers 4, 5 and 6, the correct mix of oil and water could be achieved in all wells up dip or down dip.

Similarly, additional gas production could be obtained by modifying permeabilities in Layers 2 and 3. In addition, well completions were altered if the existing completions could not allow for the proper production. This was within reason since all wells were fractured upon completion, and arguments could be made for communication with non completed layers close to the wellbore.

Table 4 summarizes the initial volumes in place by layer and for the entire simulation model. Note that Layer 4 has the highest oil and gas volumes in place, while Layers 5 and 6 contain very high volumes of initial water in place.

Figure 10 illustrates the quality of the history match with respect to model oil, gas, and water cumulative production data. The observed data is plotted as circles and the simulation calculated results are plotted as lines. If oil rates had been specified for all wells, the calculated oil production would match exactly with the observed oil production data. As can be seen in Fiugre 10, this is not the case because gas production was specified in the simulation for the three gas cap wells (Algerita 1, Saguaro 2, and Sara 2). However, the figure does illustrate that a satisfactory match was obtained for oil, gas, and water production.

Plots of individual well history matches are given for each well in the study area in Appendix IV. Aactual observed data is plotted as circles and the calculated simulation results are plotted as lines. A review of each individual well plot reveals that most wells were matched very well.

The plots contained in Appendix IV illustrate the quality of the history match more clearly. For the gas cap wells (Algerita 1, Saguaro 2, and Sara 2) gas production was specified, and the quality of the match is measured by inspecting the oil and water production curves and the pressure plots.

The plots for these three gas cap wells show very good matches for water production and pressure. These three wells have associated condensate production that was not matched, as seen on the oil production plot. However, this associated condensate production is a negligible amount (less than 10 MSTB of cumulative oil production per well).

For the remaining wells, oil rate was specified in the simulation, and the history match quality is measured by inspecting the gas and water production curves and the pressure plots. As the remaining plots in Appendix IV illustrate, satisfactory history matches were obtrained on all remaining wells (John 5, John 3, John 4, and Ceniza 3).

### Predictions

### Well Productivity Calibration

Prior to simulation of the prediction cases, a productivity match was performed for each well. During history match runs, all wells have a specified oil rate or gas rate and are constrained by that rate. However, during the prediction runs, the wells must be pressure constrained since rates are being predicted.

All wells within the study area are produced with beam pumping units. Yates provided SSI with fluid level data for the wells, and these data were converted to bottomhole pressure (BHP) data.

For the productivity match, all wells were assigned their respective BHP's. In addition, each well was assigned an oil rate far above the rate it is capable of producing. This forces the well to be pressure constrained in the simulator. The productivity match run duration was short, about five days. Through an iterative process, well indices (WI's) were altered for each well until the calculated rate for each well (under bottomhole pressure constraint) matched the observed oil rate at the end of history.

### **Prediction Case Descriptions**

All prediction cases were simulated for a total of 26 years beginning in November 1992 and continuing through December 2018. No economic limit was input for any of the runs.

The completion intervals for new wells were determined from neighboring wells. Similarly the PI or WI values assigned to the new wells were average values for the given location of each new well.

Since current water cuts are above 90 percent for most wells in the study area, oil producing wells were assigned a maximum water cut limit of 99 percent. Oil wells were also assigned a maximum GOR limit of 100,000 SCF/STB. In the event that these limits are reached for a given well, the simulator shuts-in layers one by one to improve the water cut and/or GOR until there is only one layer completed. When only one layer remains completed and a limit is exceeded, the well is shut-in.

The following paragraphs briefly describe the characteristics of each prediction case. Unless otherwise specified, the general guidelines just discussed are applicable to each case.

### **Prediction Case 1 (Continued Depletion - Base Case)**

This case continued the existing depletion of the reservoir with the existing wells.

### **Prediction Case 2 (Continued Depletion without Gas Cap Depletion)**

In order to determine the effect of gas cap production on field oil production, all gas cap wells were shut-in while the rest of the wells were allowed to deplete. The wells that were shut-in during this run were: Algerita 1, Saguaro 2, and Sara 2.

### Prediction Case 3 (Continued Depletion with Gas Cap Infills)

Two additional gas cap wells were drilled in order to deplete the gas cap at an increased rate. One well was placed between Sara 2 and Saguaro 2 in grid cell x = 8, y = 2. The other well was placed between Saguaro 2 and Algerita 1 in grid cell x = 4, y = 2 (see Figure 11).

### **Prediction Case Results**

Prediction case results can be evaluated on several levels. The most common types of evaluations are based on:

- cumulative oil recovery
- rate of oil recovery
- recovery efficiency
- economics

Although a great deal of importance is frequently given to the final oil recovery the items shown above should all be taken into consideration. The results of economic analyses should normally control the development of a reservoir, rather than simply trying to maximize ultimate oil recovery. The optimum development scheme is frequently different for each of the criteria listed above. In some situations, outside factors may take precedence over the need for economic efficiency. An example is the case where contractual obligations require production at a certain rate over a given period of time. Yates should include any such external factors in their final evaluation of the results of this study. A comparison of case results, according to the categories above, is discussed in the following sections of this report.

### **Case Comparisons**

Table 5 shows a comparison of the cumulative recoveries at the end of each of the prediction cases. Note that the recoveries in Table 5 and those discussed in the text that follows are 26-year recoveries. Note that there is little difference in oil recovery with and without gas cap depletion (Cases 1 and 2). Also note that accelerated depletion of the gas cap with two additional gas cap wells (Case 3) does not affect ultimate oil recoveries. The case comparison plot in Figure 12 illustrates that gas cap management does not affect oil production down dip. Although cumulative gas production varies for each of the three prediction cases, the ultimate oil recovery is the same. Since the oil recoveries for all three prediction cases are very similar (Table 5), plots of model oil, gas, and water production have been provided only for prediction Case 1 (continued depletion) (Figures 13 through 15). Plots of individual well production for Case 1 are given in Appendix V. Also, plots of individual well production for Case 3 (Gas Cap Infills) are included in Appendix VI including production plots for the two infill gas cap wells (NEW 1 and NEW 2).

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- Table 5
   Prediction Simulations Reservoir Performance Summary

## Table 1Relative Permeability EndpointsCanyon Reservoir - Dagger Draw Field

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Permeability
Relative
Water-Oil

Gas-Oil Relative Permeability

Simulation	.5476	.0490
<u>Model</u>	.0000	.7174
Scal	.5969	.0490
Sample 4w	.1305	.4160
Scal	.6437	.1240
Sample 3	.2076	.1230
	Slr Sgc	krgro krogc
Simulation	.2 <b>456</b>	1.0000
<u>Model</u>	.3019	.5947
Scal	.2 <b>456</b>	1.0000
Sample 4w	.3019	.1330
Scal <u>Sample 3</u>	.3103	1.0000 .1886
	Swc Sorw	krocw krwro

# Table 2Water-Oil and Gas-Oil Contacts &Water-Oil Capillary Pressure EndpointsCanyon Reservoir - Dagger Draw Field

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Model Pcow at Swc (psia)	<b>3</b> 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5
Model WOC (subsea feet)	4053 4092 4123 4179 4228 4366 4403
Model GOC (subsea feet)	3832 4030 3997 3959 4020 4125 4125
Model <u>Layer</u>	- 1 m 4 v v 7 <b>m</b>

## Table 3Reservoir Fluid PropertiesCanyon Reservoir - Dagger Draw Field

RESERVOIR GAS PROPERTIES RESERVOIR OIL PROPERTIES						
Pressure	FVF	Viscosity	Pressure	Rso	FVF	Viscosity
<u>psia</u>	rb/mscf	CD	<u>psia</u>	scf/stb	rb/stb	cp
14.6	205.83	0.012	14.6	9.79	1.026	1.285
<b>9</b> 9.7	29.86	0.012	99.7	36.12	1.034	1.197
214.6	13.62	0.012	214.6	65.03	1.044	1.133
<b>41</b> 4.6	6.83	0.012	414.6	112.25	1.061	1.027
614.7	4.47	0.012	614.7	159.12	1.080	0.933
814.7	3.27	0.013	814.7	206.81	1.100	0.873
1014.7	2.55	0.013	1014.7	255.78	1.122	0.818
1214.7	2.07	0.014	1214.7	306.26	1.145	0.765
1414.7	1.73	0.015	1414.7	358.41	1.170	0.715
1614.7	1.49	0.016	1614.7	412.35	1.197	0.668
1814.7	1.30	0.017	1814.7	468.15	1.225	0.624
2017.7	1.16	0.018	2017.7	526.79	1.255	0.583
2114.6	1.10	0.018	2114.6	555.54	1.270	0.565
2214.6	1.05	0.019	2214.6	585.69	1.286	0.547
2314.6	1.00	0.019	2314.6	616.35	1.302	0.530
2514.6	0.92	0.020	2514.6	679.29	1.335	0.498
2714.6	0.86	0.022	2714.6	744.43	1.371	0.468
<b>2914</b> .6	0.81	0.023	2914.6	811.82	1.407	0.441
*3014.6	0.79	0.023	*3014.6	846.38	1.426	0.428
3514.6	0.70	0.026	3514.6	1028.25	1.526	0.369
4014.6	0.65	0.029	4014.6	1226.04	1.635	0.320
4514.6	0.61	0.031	4514.6	1441.02	1.753	0.277
<b>5014</b> .6	0.58	0.034	5014.6	1674.56	1.881	0.238
5514.6	0.55	0.036	5514.6	1928.22	2.017	0.203
<b>6014.</b> 6	0.53	0.038	6014.6	2203.74	2.164	0.171

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\* Values extrapolated beyond Bubble Point for simulation purposes

Table 4Simulation Model - Initial in Place Volumes and PressuresCanyon Reservoir - Dagger Draw Field

Total	6.122	40.276	30.442	25.256	3016
Layer 8	0.137	0.703	0.116	0.000	3074
Layer 7	0.224	0.510	0.190	0.000	3064
Layer 6	0.000	8.261	1.325	1.325	3001
Layer 5	0.372	20.347	3.593	3.278	3017
Layer 4	4.788	8.442	21.621	17.565	3017
Layer 3	0.257	0.775	1.580	1.362	3011
Layer 2	0.019	0.539	1.139	1.123	3002
Layer 1	0.325	0.698	0.878	0.603	3033
	Oil (MMSTB)	Water (MMSTB)	Gas (BSCF)	Free Gas (BSCF)	Average Pressure

### TABLE 5

### PREDICTION SIMULATIONS - RESERVOIR PERFORMANCE SUMMARY CANYON RESERVOIR, DAGGER DRAW FIELD, NEW MEXICO

	CASE 1	CASE 2	CASE 3
End of Case	December, 2018	December, 2018	December, 2018
Oil, MSTB	682	684	682
Gas, BSCF	19.5	9.7	21.5
Water, MSTB	7435	4890	8398

**Case 1 - Continued Depletion** 

Case 2 - Continued Depletion without Gas Cap Depletion

Case 3 - Continued Depletion with Gas Cap Infills

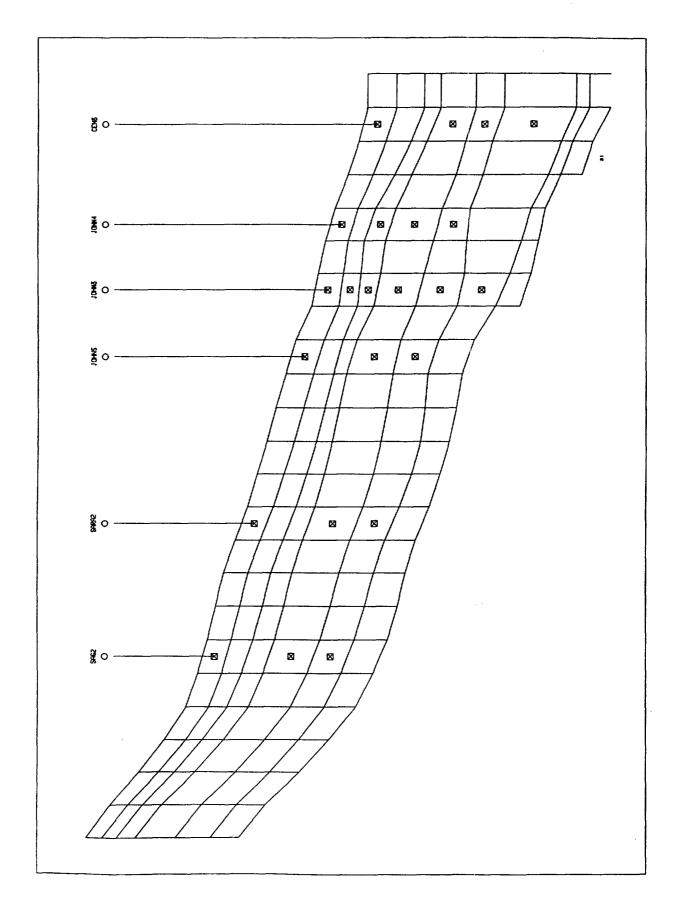


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		12			1	<u>0</u>				24	
Ю		O Erv			CENS	*	O HILL7	MAYR2 O	MRYRI O		PRLV1
SARA3 O		SARA1 O	SARA6	JOHN2	JOHN4	entring G	О	H1LL5	О	HILL12 O	PRIC1
SAG13 O	SAGE	11 Conib	SARR4		JOHNS O	she	SAGB	HILLS	HILL2	A HILL4 O	. –
O CON	CON7		SARAS	INHO O	J DHNS	SENI 5	O SEN2	ShG O	Shes.		ELLL3
	CON12	SAGI				sa\$12 " O "					
00011	-				SARA2 O					CHRLI	
	:	0			Sa62				c	CARLZ CARLZ O	
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Figure 2 Sector Model Grid - Cross Section (J = 2) Canyon Reservoir - Dagger Draw Field



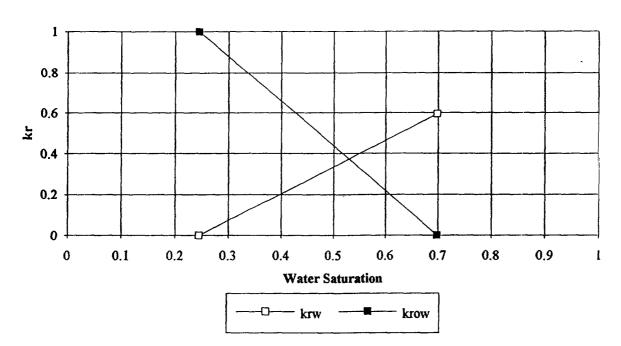
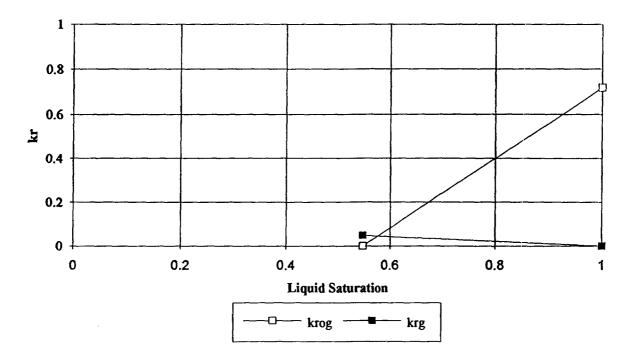


Figure 3 Water - Oil Relative Permeability - Simulation

Gas - Liquid Relative Permeability - Simulation



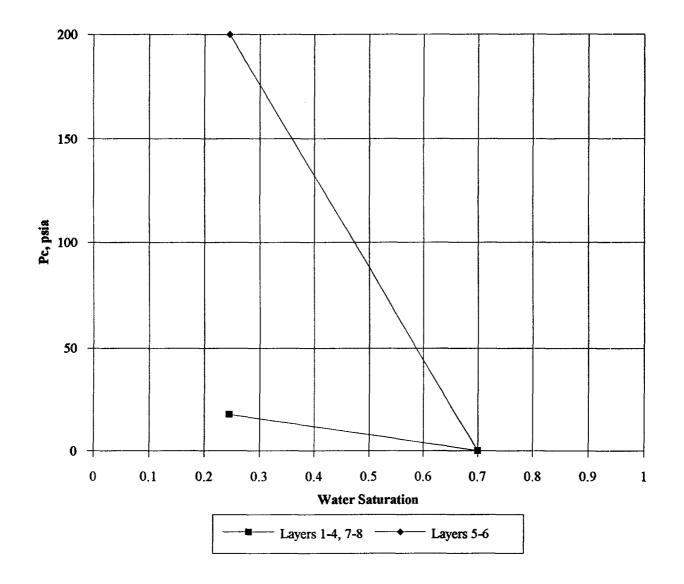


Figure 4 Water - Oil Capillary Pressure - Simulation

Figure 5 Oil Formation Volume Factor vs Pressure - Simulation Canyon Reservoir - Dagger Draw Field

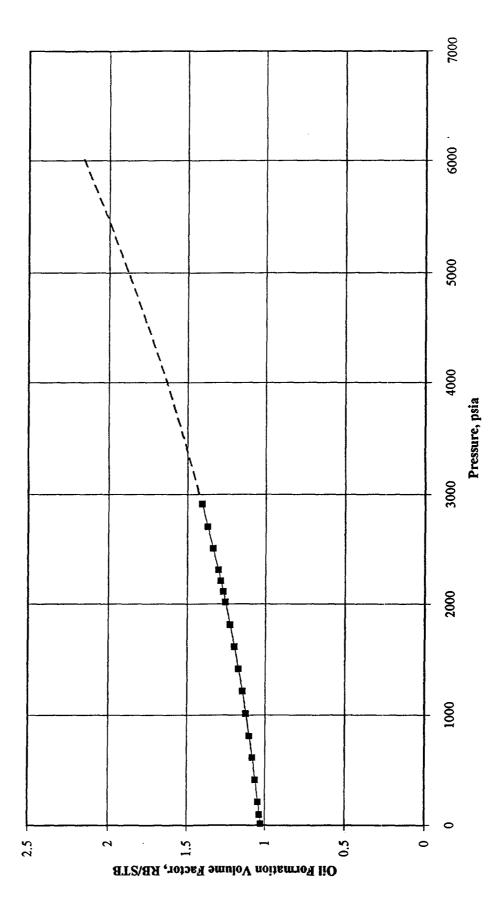


Figure 6 Solution Gas Oil Ratio vs Pressure - Simulation Canyon Reservoir - Dagger Draw Field

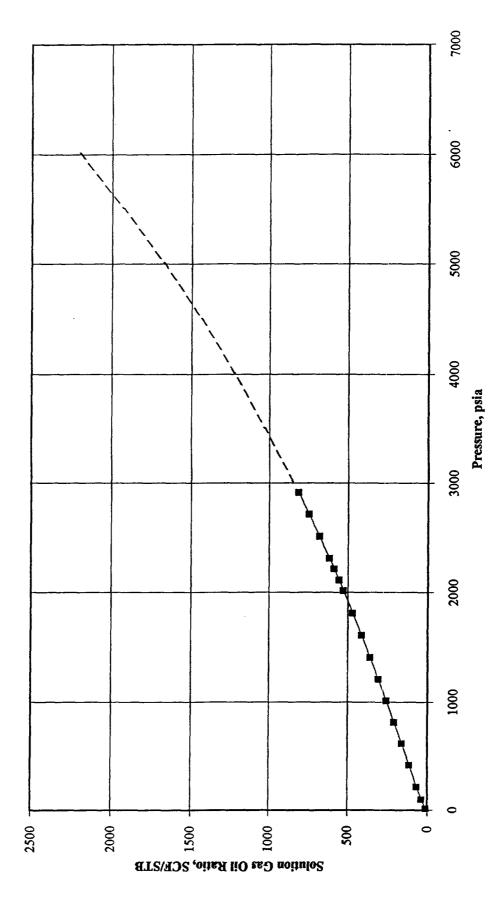


Figure 7 Oil Viscosity vs Pressure - Simulation Canyon Reservoir - Dagger Draw Field

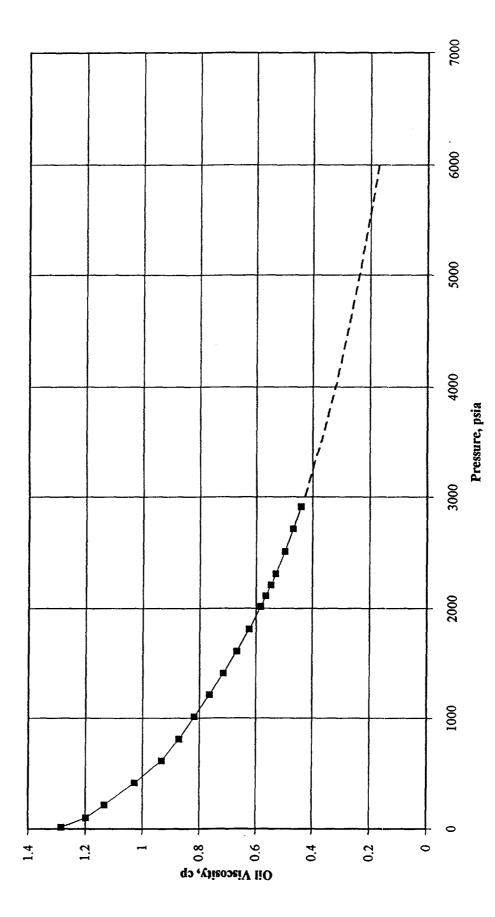
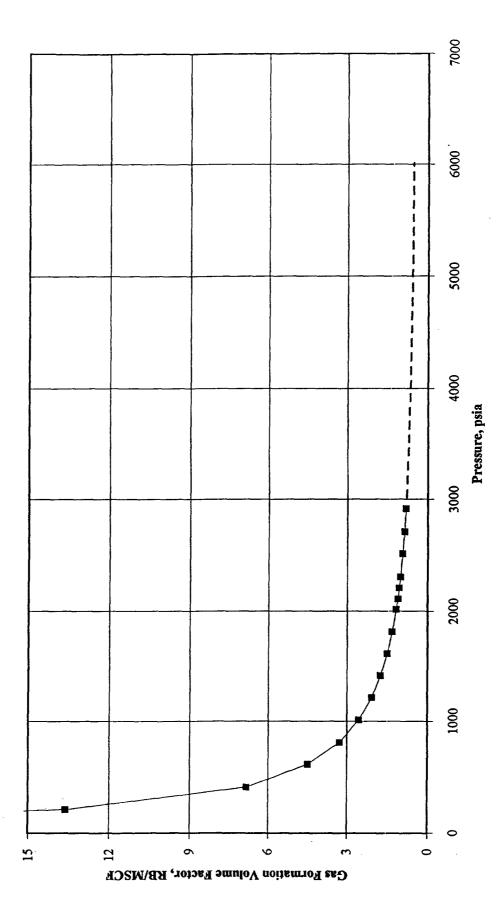


Figure 8 Gas Formation Volume Factor vs Pressure - Simulation Canyon Reservoir - Dagger Draw Field



Gas Viscosity vs Pressure - Simulation Canyon Reservoir - Dagger Draw Field

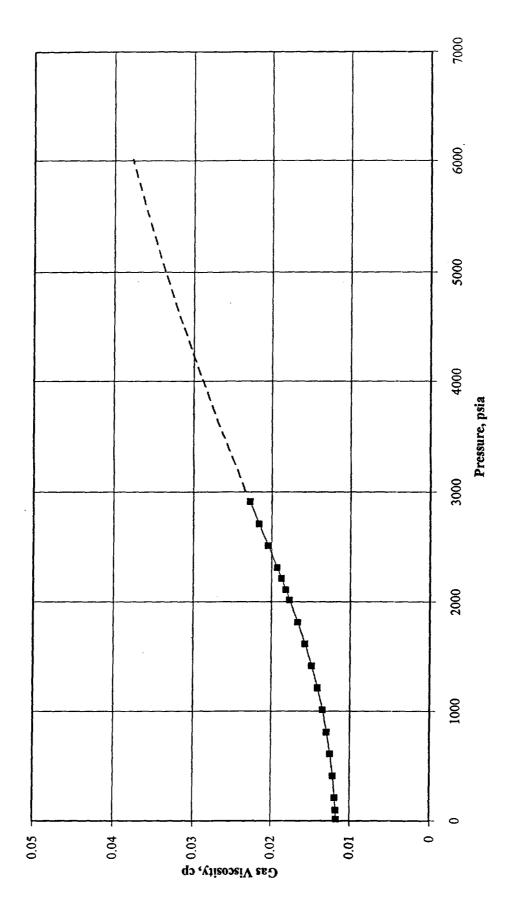


Figure 9

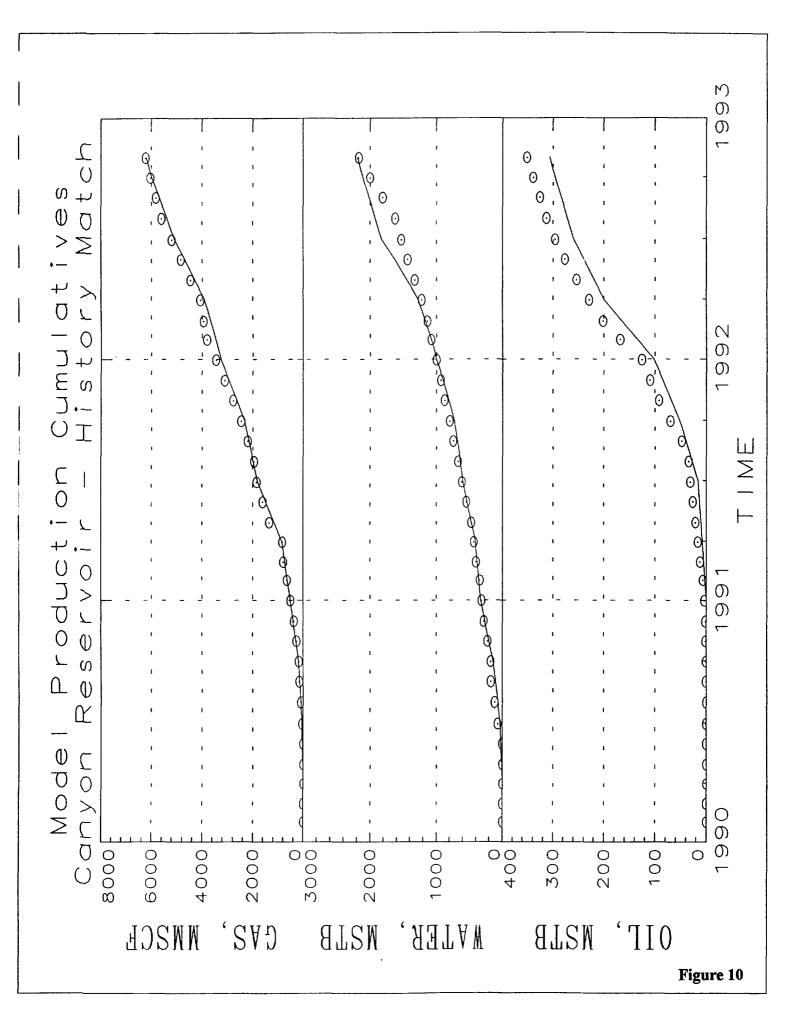
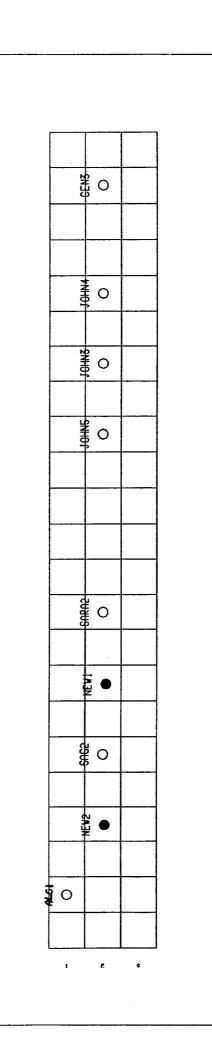
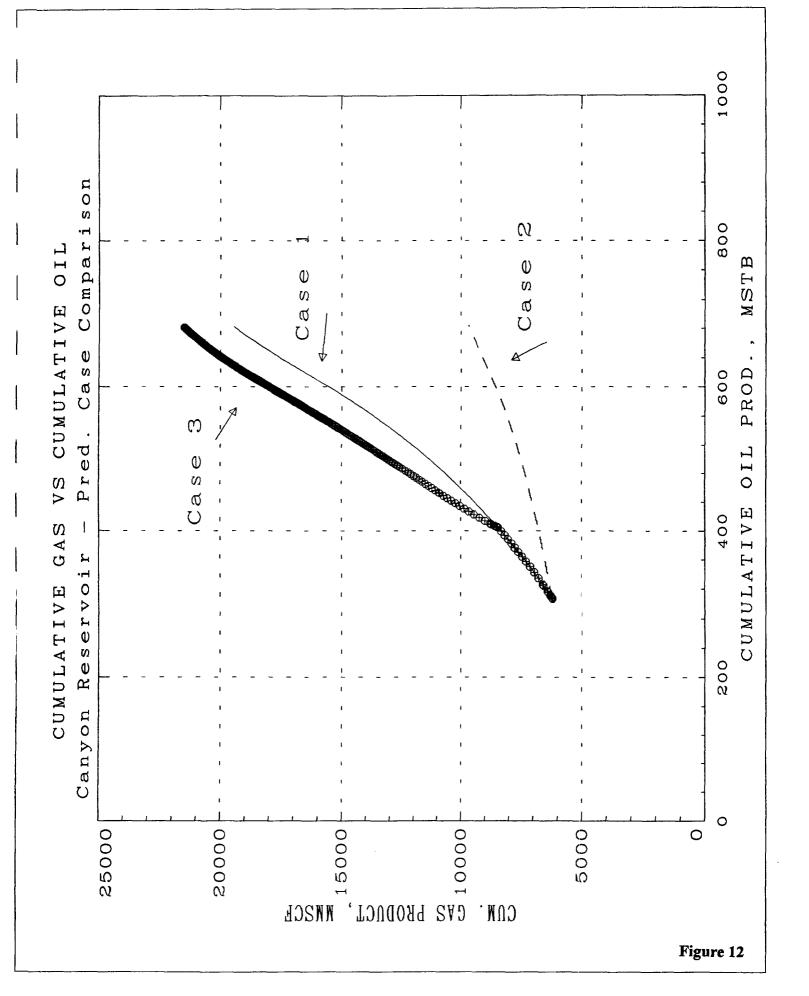
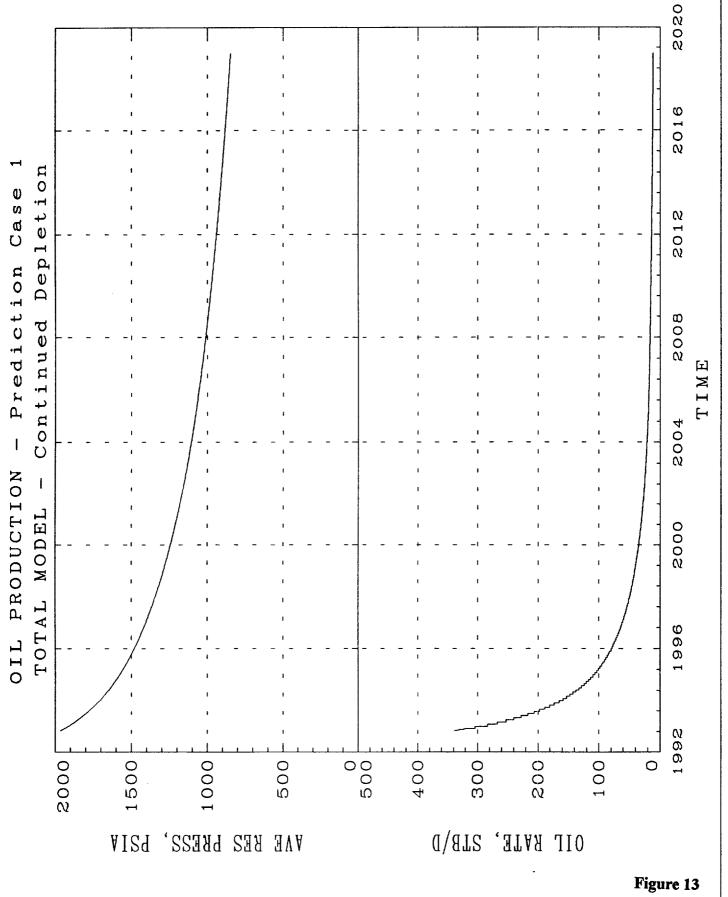
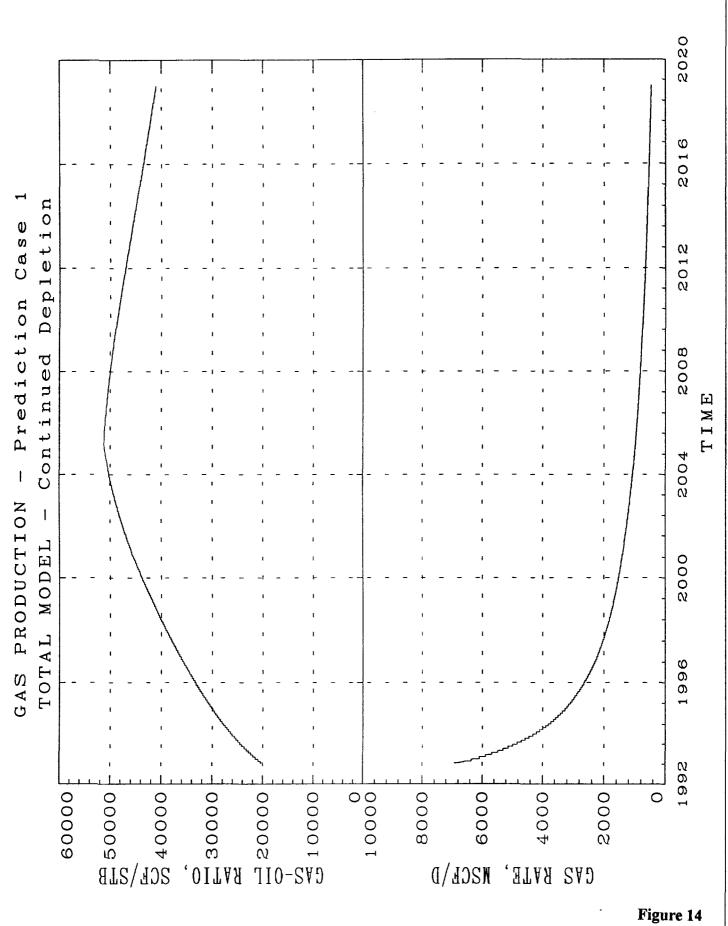


Figure 11 Sector Model Grid - Plan View Prediction Case 3 Canyon Reservoir - Dagger Draw Field







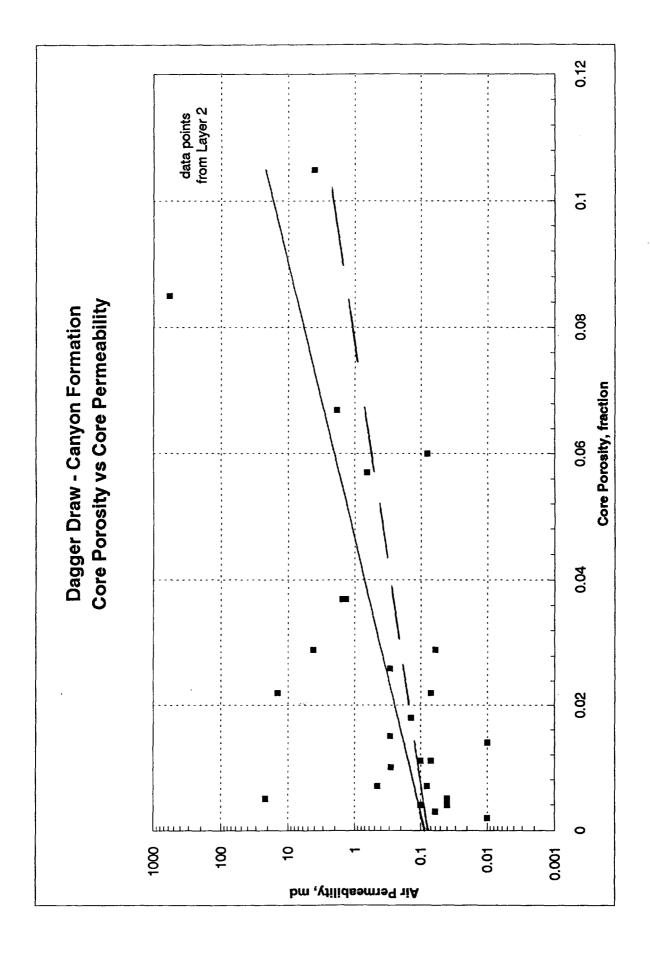


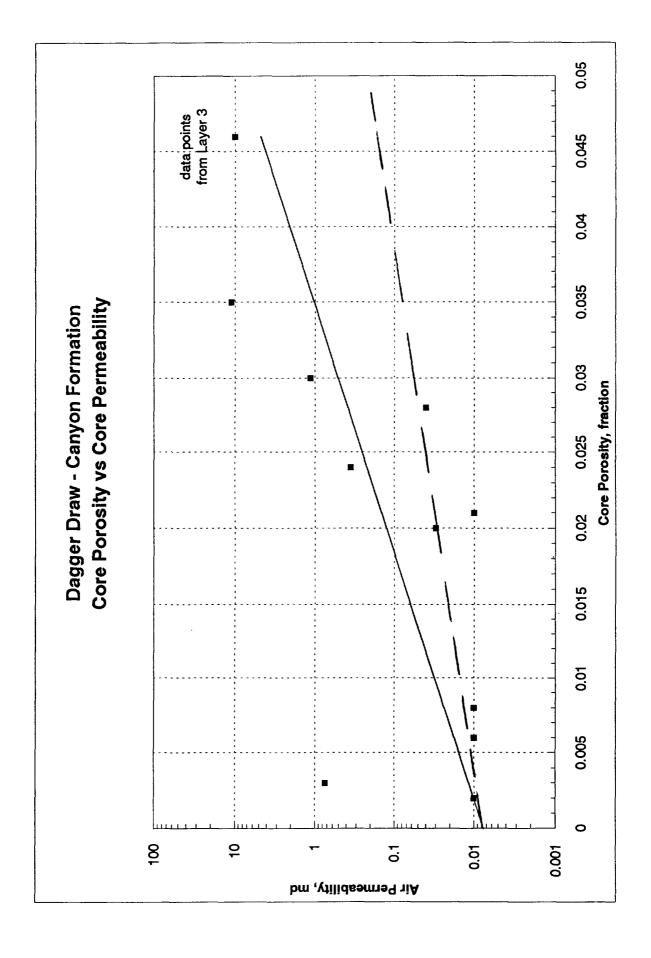
2020 2016 Depletion Case 2012 Prediction 2008 Continued TIME 2004 1 **PRODUCTION** MODEL 2000 TOTAL WATER 1996 1992 5000. ω. <u>ເ</u> 2000 1000 ю . 0 4000 3000 4 WATER CUT, FRACTION WATER RATE, STB/D

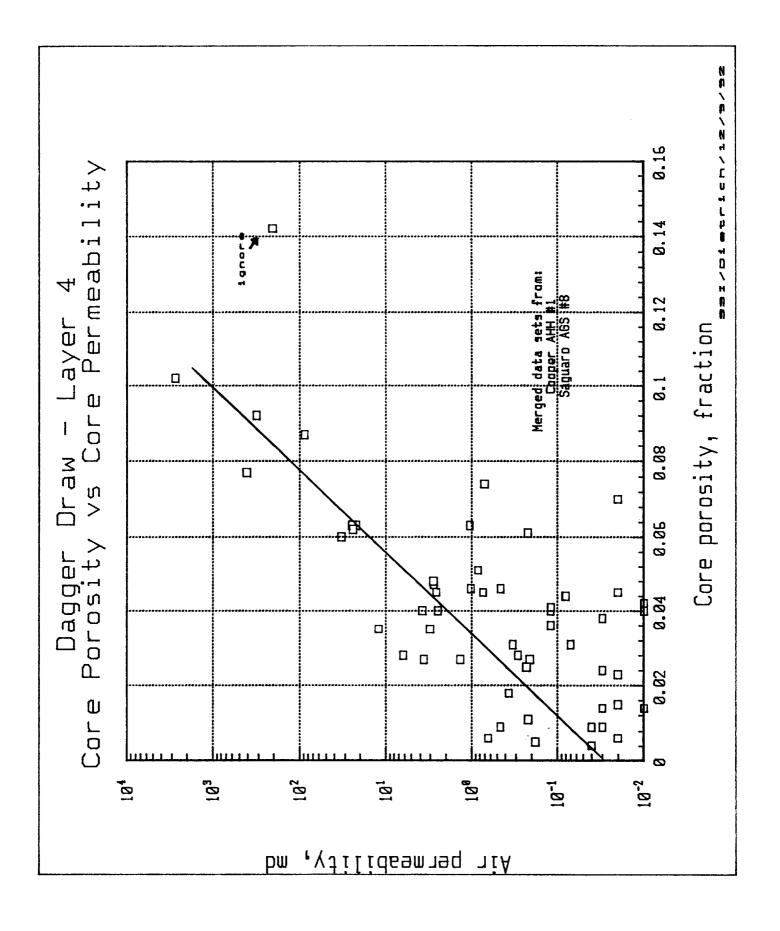
Figure 15

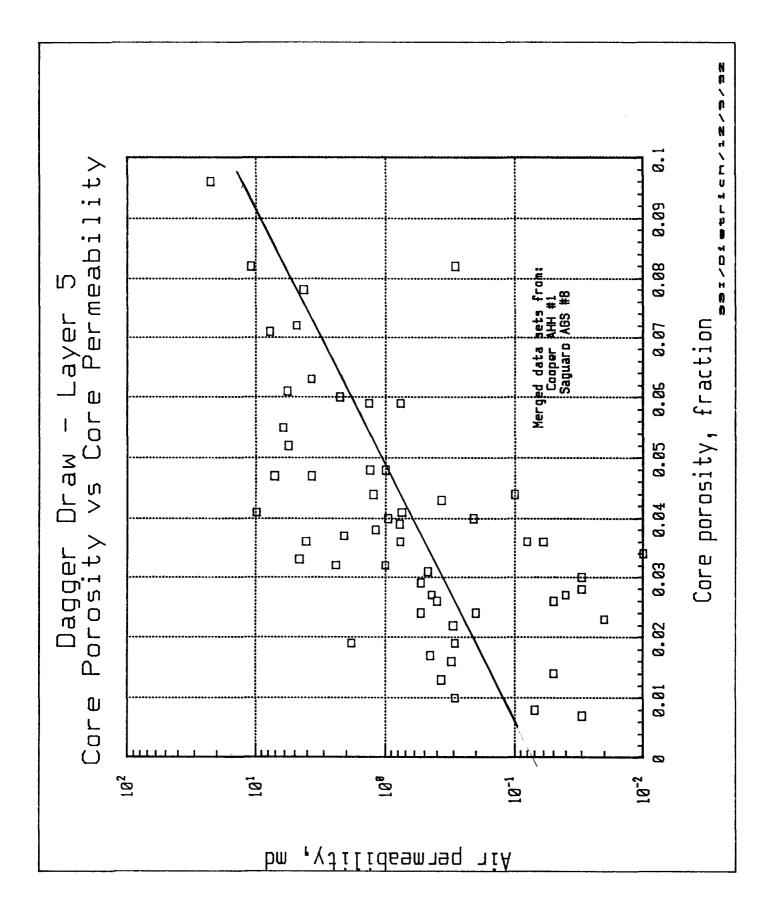
**APPENDIX I** 

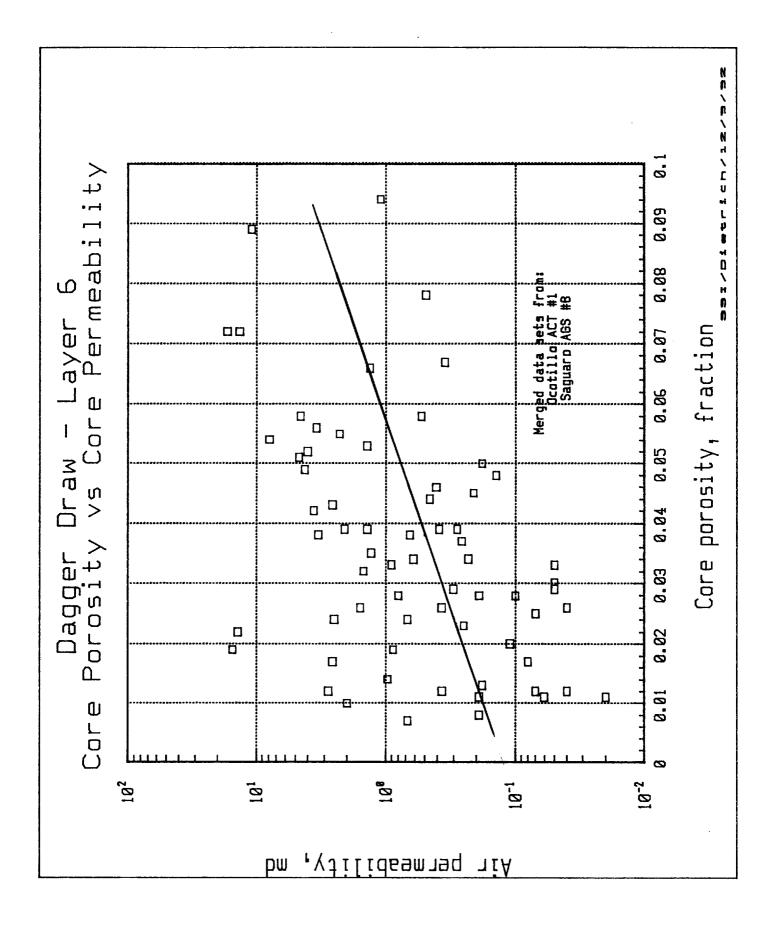
**CORE ANALYSIS PLOTS** 

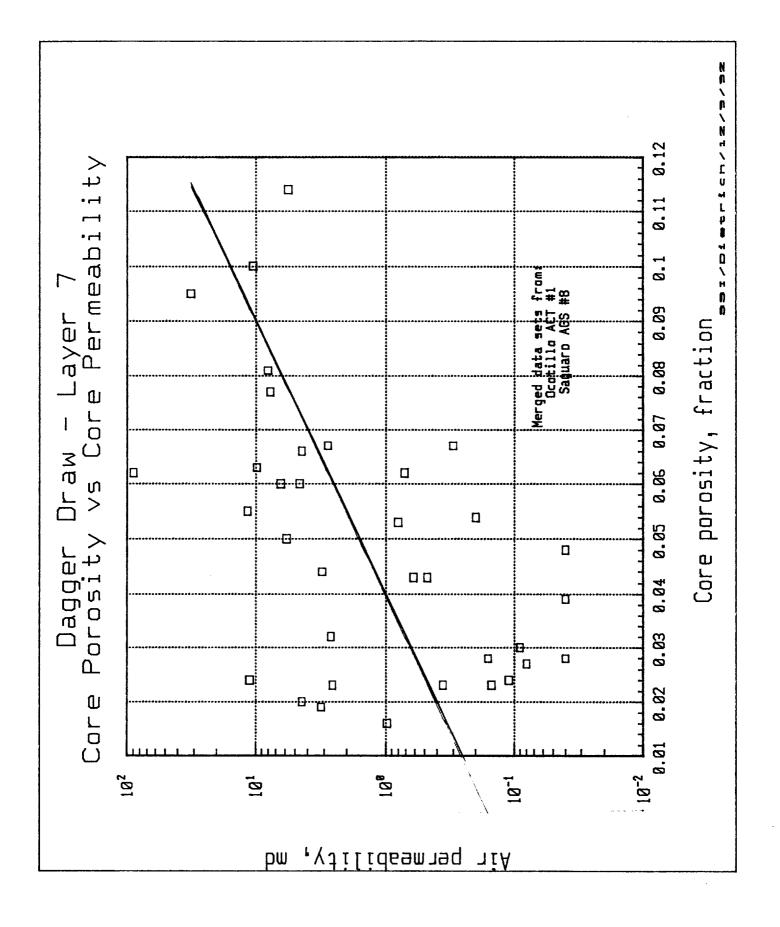


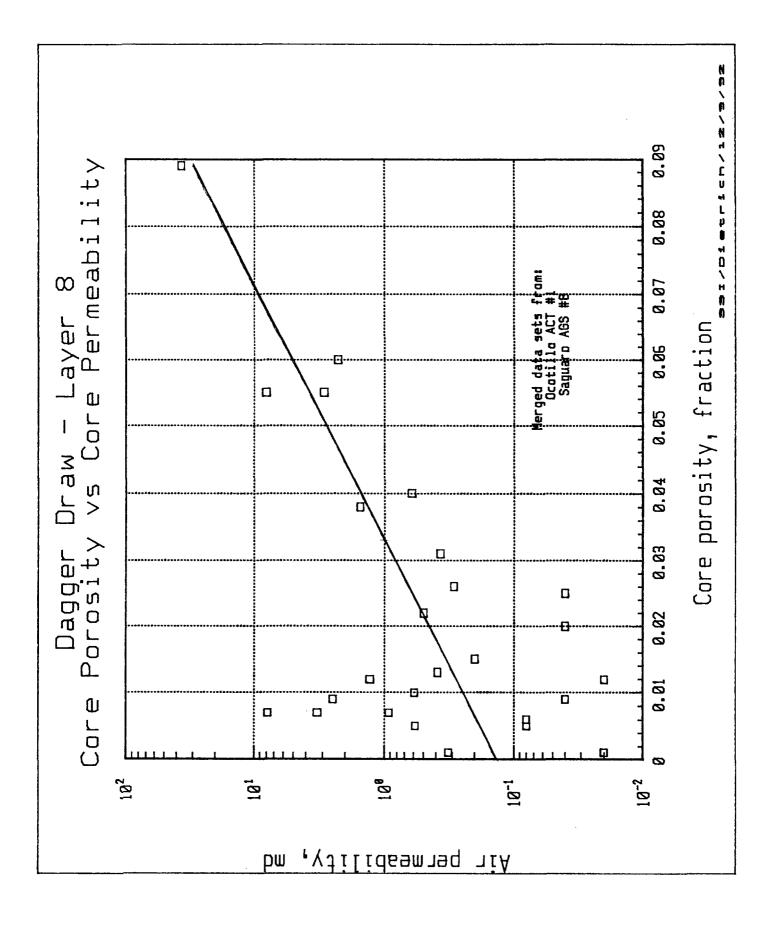


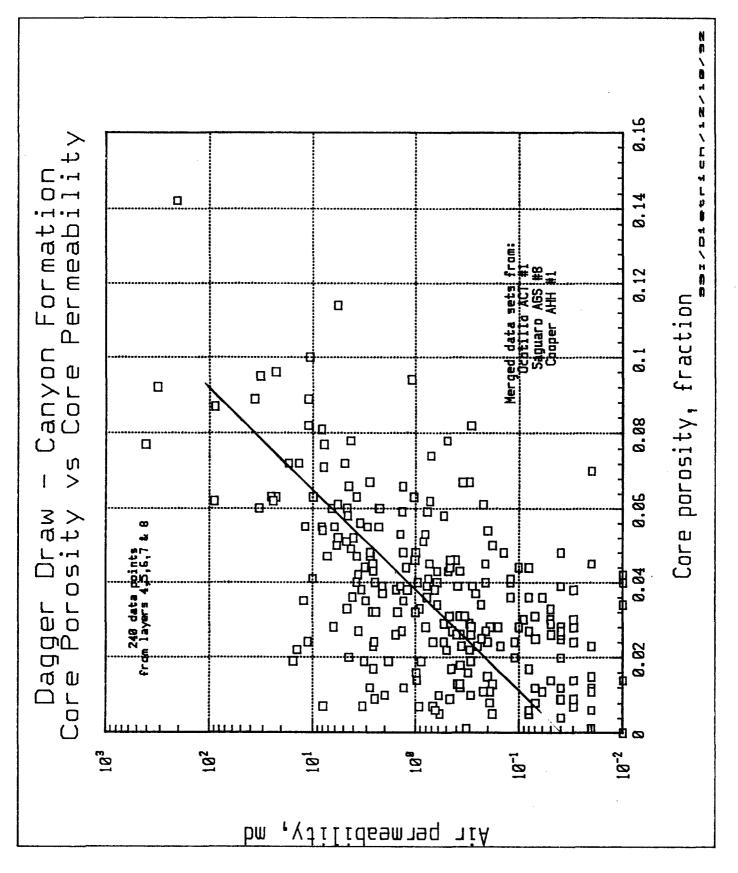












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#### **APPENDIX II**

## SCAL, INC.

### **RELATIVE PERMEABILITY LAB ANALYSIS**



# **Gas-Oil Relative Permeability**

# Dagger Draw Federal No. 12 Eddy County, New Mexico

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P.O. BOX 9730 • MIDLAND, TX 79708-2730 • (915) 561-5406 • FAX (915) 561-5339

# Unsteady-State Gas-Oil Relative Permeability

Company :	Conoco	Inc.		
Field : Well Name :		Draw Draw Fede ounty, New		
Sample : Depth :	3 7658' 11	1-	Porosity : Permeability :	9.82 % 507 mD
Temperature : Oil Viscosity : Gas Viscosity :	22.00 22.40 0.018	deg. C cP cP	Keo & Siw: Keg & Sro: Siw Sro	72.9 mD 9.04 mD 31.03 % 33.34 %

. . .

#### TEST RESULTS

No. -	Sg %	• Krg -	• Kro -	Krg/Kro -
1	20.76	0.034	0.123	0.280
2	23.51	0.061	0.064	0.959
3	25.17	0.097	0.046	2.106
4	26.41	0.104	0.033	3.170
5	26.84	0.108	0.031	3.521
6	27.54	0.110	0.027	4.124
7	28.23	0.115	0.024	4.781
8	29.43	0.117	0.020	5.698
9	30.62	0.120	0.016	7.675
10	35.63	0.124	0.000	

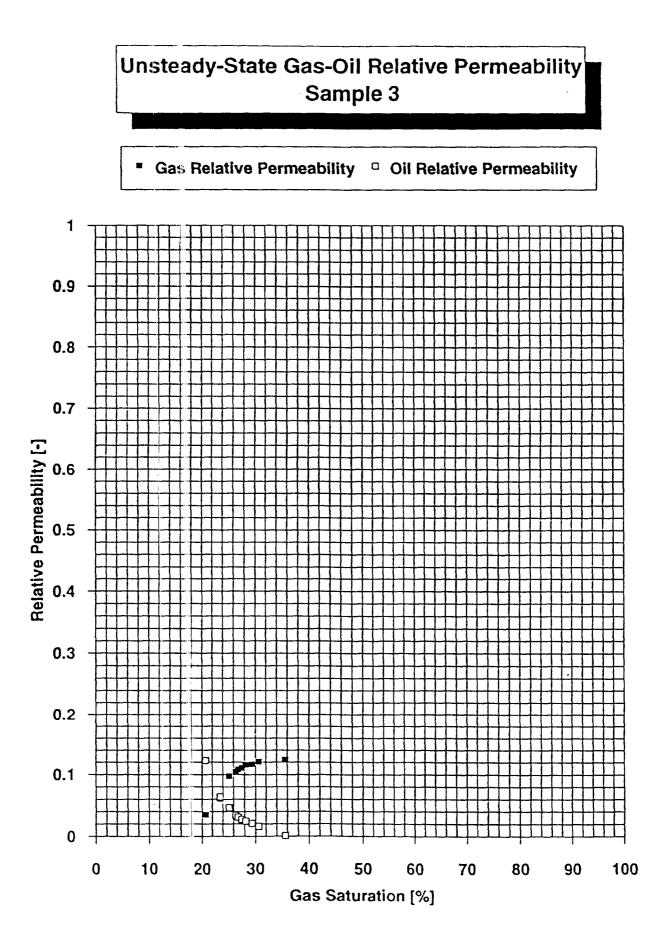
\* Relative to Keo @ Swi

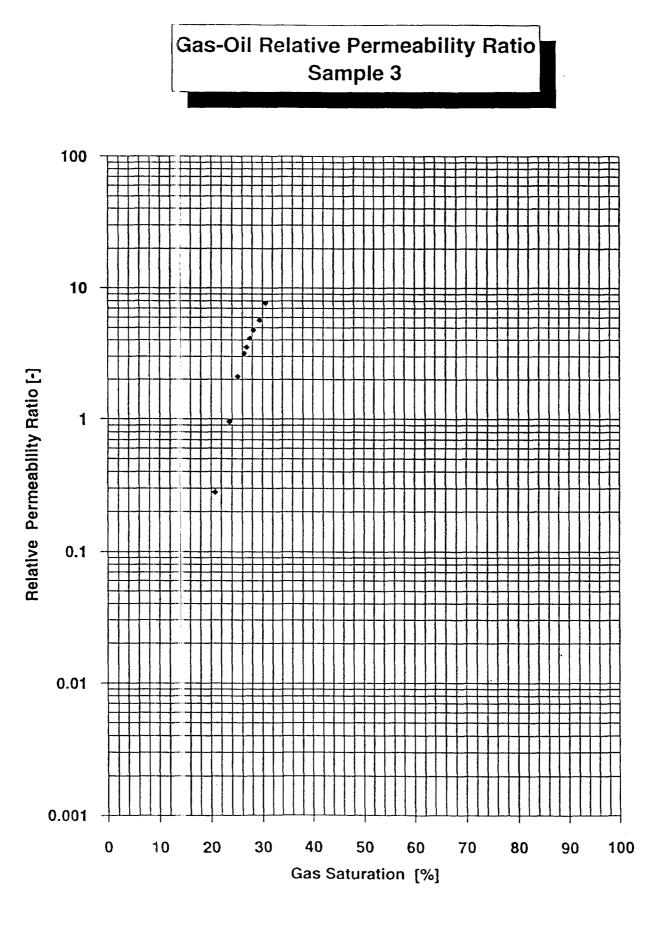
Notations:

**6**...

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Кео	Effective Oil Premeability
Keg	Effective Gas Permeability
Sro	<b>Residual Oil Saturation</b>
Siw	Irreducible Water Saturation





# Unsteady-State Gas-Oil Relative Permeability

Company :	Conoco	Inc.		
Field : Well Name :		Draw Draw Fede ounty, New		
Sample : Depth :	4W 7806' 6 <b>'</b>		Porosity : Permeability :	10.27 % 29.8 mD
Temperature : Oil Viscosity : Gas Viscosity :	22.00 22.40 0.018	deg. C cP cP	Keo @ Siw : Keg @ Sro : Siw Sro	11.7 mD 0.57 mD 24.56 % 35.13 %

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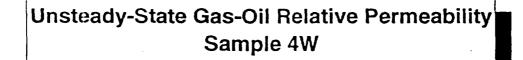
#### **TEST RESULTS**

No. -	Sg %	* Krg -	* Kro -	Krg/Kro -
1	13.05	0.018	0.416	0.043
2	14.90	0.027	0.254	0.106
3	17.34	0.029	0.126	0.229
4	22.50	0.029	0.037	0.796
5	29.23	0.038	0.022	1.708
6	30.11	0.040	0.020	1.961
7	31.88	0.042	0.016	2.650
8	32.49	0.044	0.015	2.964
9	33.12	0.046	0.014	3.327
10	<b>3</b> 3.88	0.047	0.012	3.838
11	40.31	0.049	0.000	

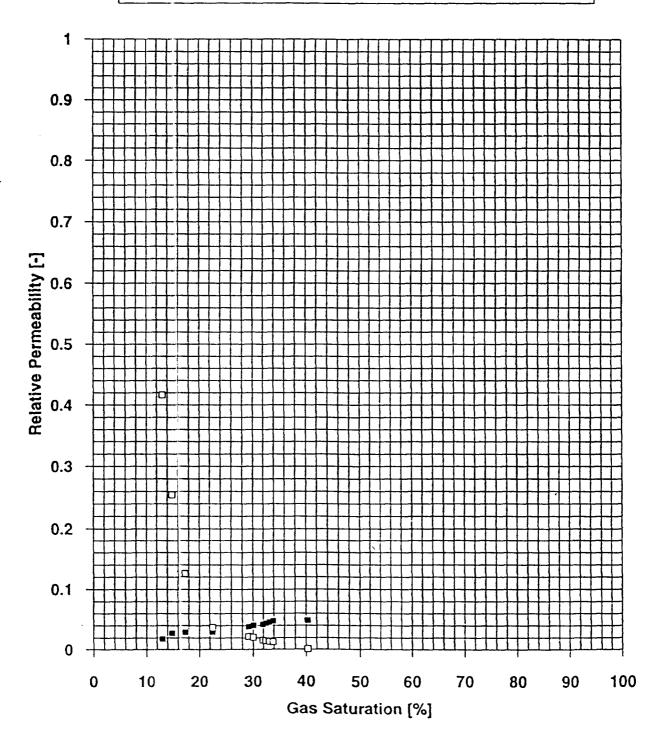
\* Relative to Keo @ Swi

#### Notations:

Кео	Effective Oil Premeability
Keg	Effective Gas Permeability
Sro	Residual Oil Saturation
Siw	Irreducible Water Saturation



Gas Relative Permeability O Oil Relative Permeability



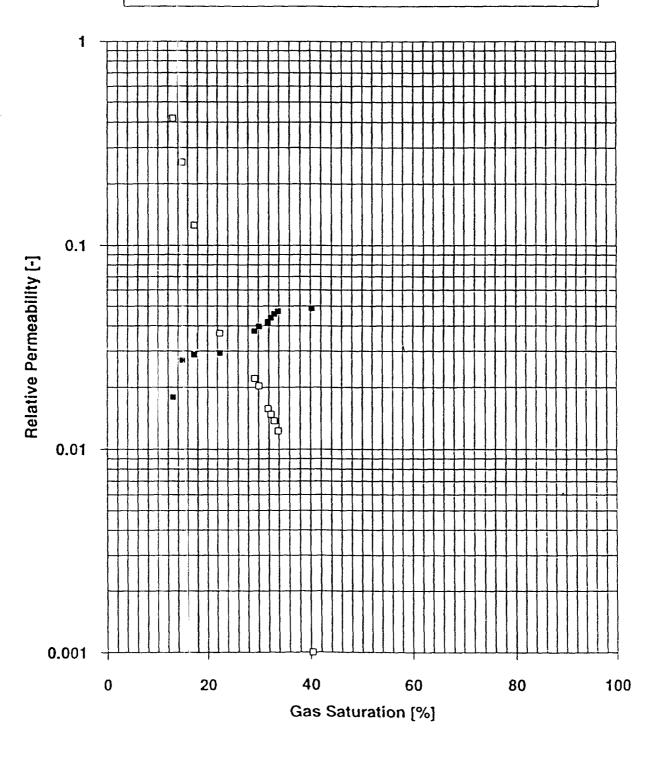
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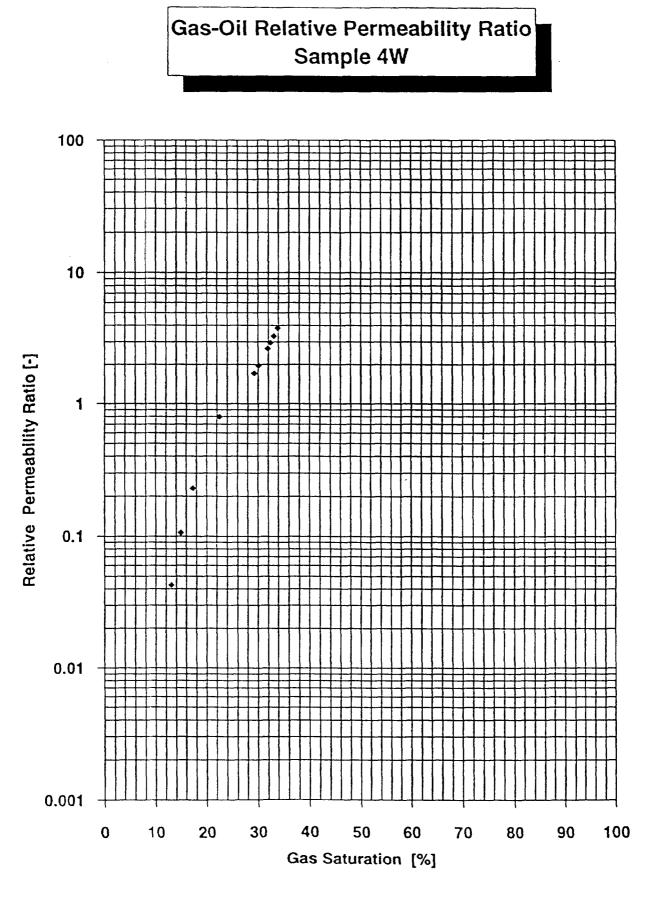
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Gas Relative Permeability Oil Relative Permeability



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# Water-Oil Relative Permeability

# Dagger Draw Federal No. 12 Eddy County, New Mexico

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### Unsteady-State Water-Oil Relative Permeability

Company :	Conoco Inc.		
Field :	Dagger Draw		
Location :	Dagger Draw Federa	1#12	
Well Name :	Eddy County, New Mexico		
Sample :	3	Porosity :	9.82 %
Depth :	7658' 11"	Permeability:	<b>507 m</b> D
Temperature :	22 deg. C	Keo @ Siw:	72.9 mD
Oil Viscosity :	22.4 cP	Kew @ Sro :	13.8 mD
Brine Viscosity :	1.03 cP		

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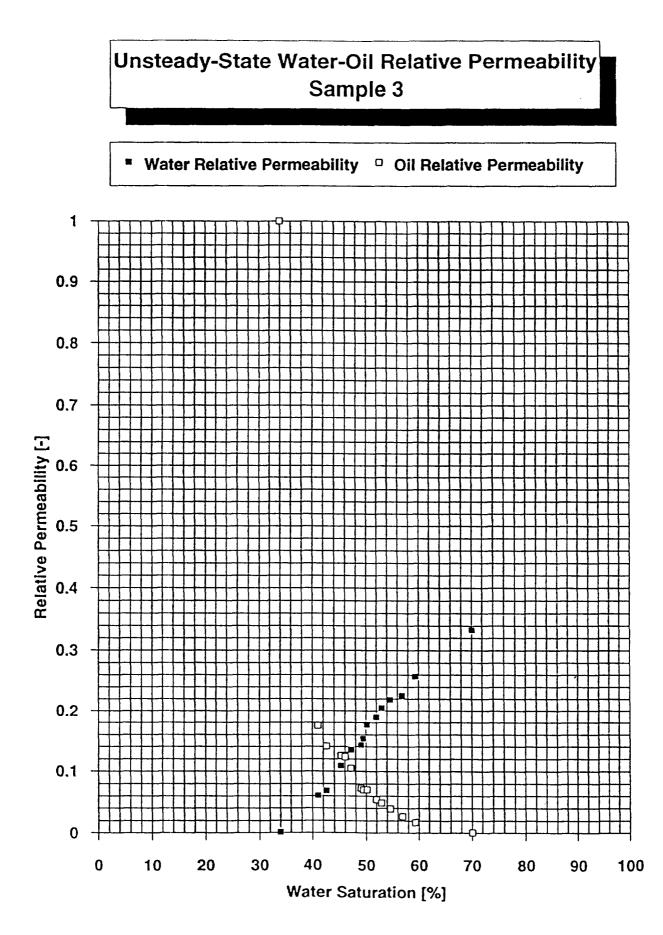
TEST RESULTS :

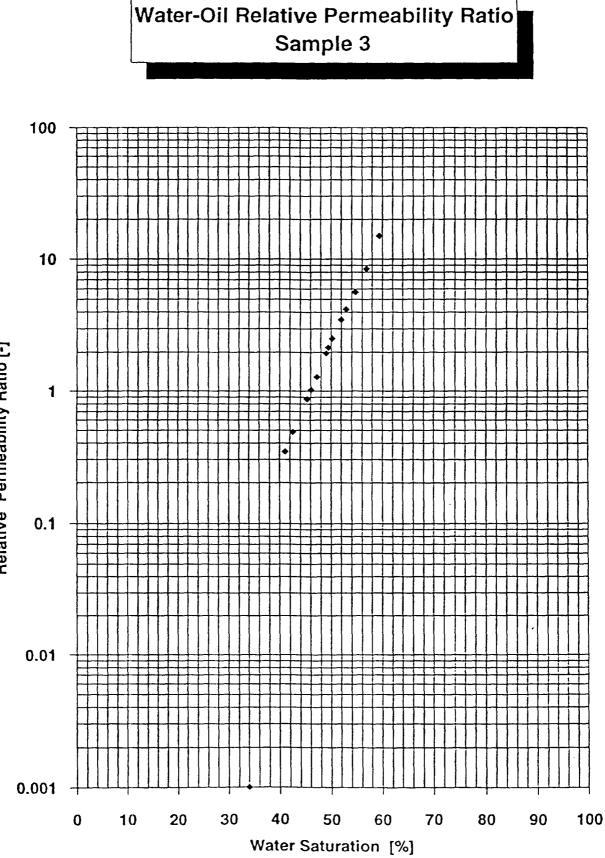
No.	Sw	* Krw	* Kro	Krw/Kro
-	%	_	-	-
1	31.03	0.0000	1.0000	0.000
2	34.22	0.0697	0.6272	0.111
3	41.89	0.0996	0.2391	0.417
4	43.80	0.1049	0.1625	0.646
5	45.33	0.1112	0.1182	0.940
6	48.33	0.1387	0.0708	1.958
7	52.78	0.1426	0.0215	6.625
8	54.12	0.1637	0.0176	9.292
9	55.89	0.1742	0.0084	20.792
10	60.08	0.1886	0.0000	

\* Relative to Keo @ Siw

Notal	tions:
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Кео	Effective Oil Permeability
Kew	Effective Water Permeability
Sro	Residual Oil Saturation
Siw	Irreducible Water Saturation





Relative Permeability Ratio [-]

## **Unsteady-State Water-Oil Relative Permeability**

Company : C

Conoco Inc.

Field :Dagger DrawLocation :Dagger Draw Federal # 12Well Name :Eddy County, New Mexico

Sample : Depth :	4W 7806' 6"	Porosity : Permeability :	10.27 % 29.8 mD
Temperature :	22 deg. C	Keo @ Siw:	11.7 mD
Oil Viscosity :	22.4 cP	Kew @ Sro:	1.556 mD
Brine Viscosity :	1.03 cP		

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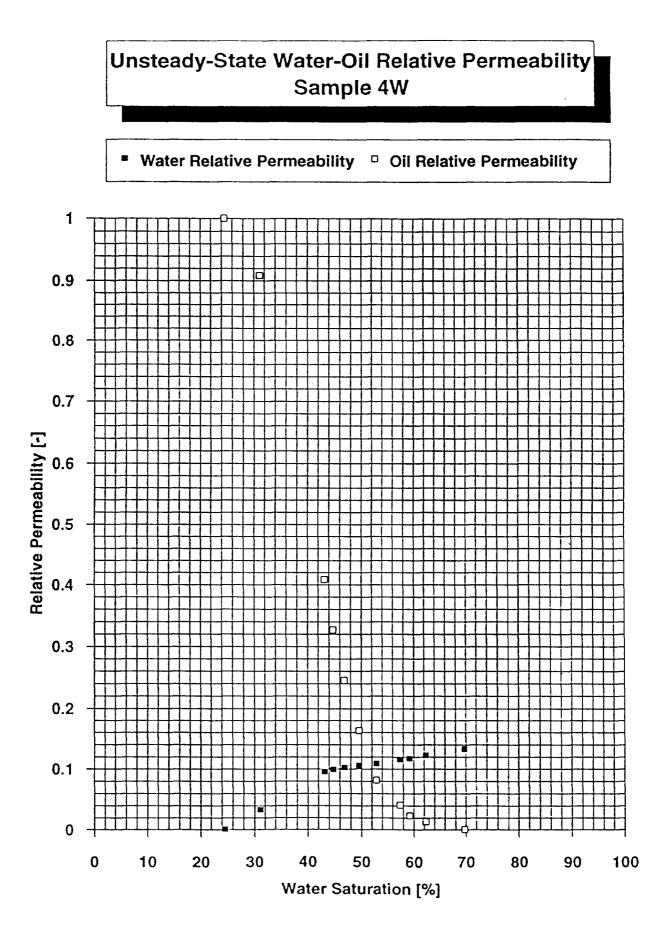
**TEST RESULTS :** 

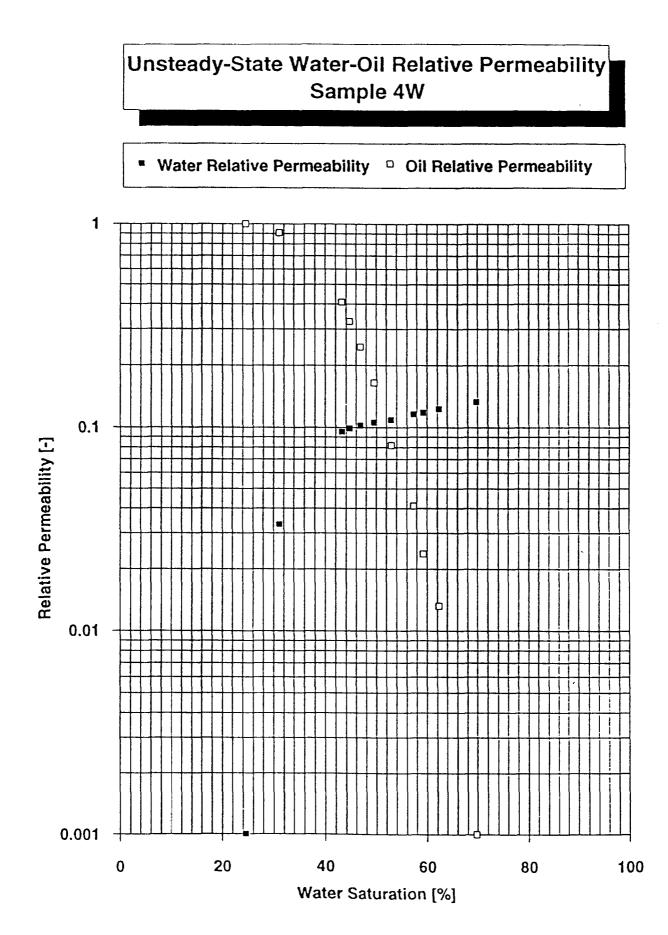
No.	Sw	* Krw	* Kro	Krw/Kro
-	%	_	-	-
1	24.56	0.0000	1.0000	0.000
2	31.12	0.0331	0.9084	0.036
3	43.21	0.0953	0.4085	0.233
4	44.75	0.0987	0.3268	0.302
5	46.88	0.1021	0.2451	0.417
6	49.60	0.1055	0.1634	0.646
7	52.91	0.1089	0.0817	1.333
8	57.39	0.1157	0.0411	2.815
9	59.24	0.1177	0.0237	4.958
10	62.37	0.1227	0.0132	9.292
11	69.81	0.1330	0.0000	

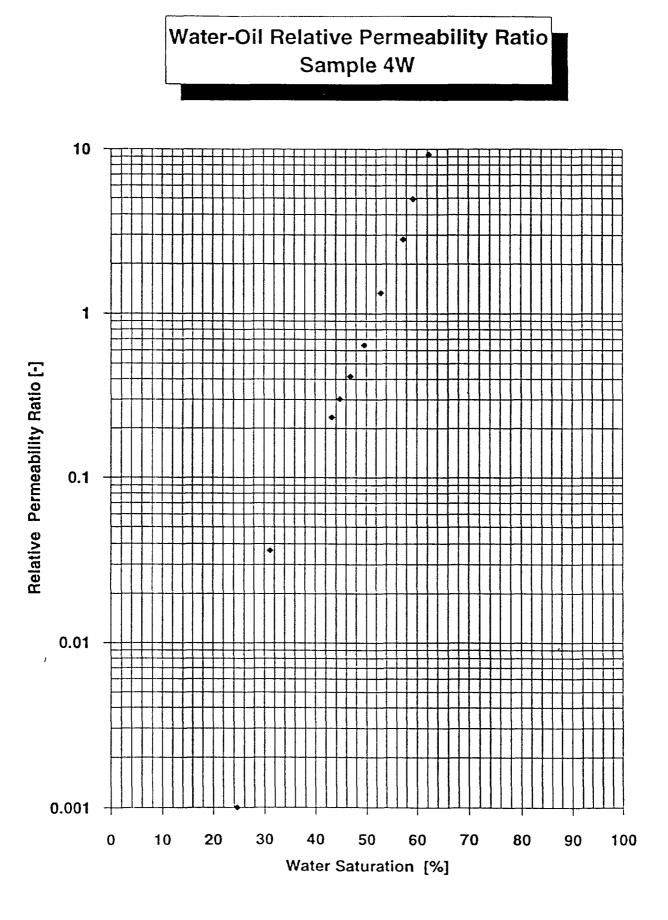
\* Relative to Keo @ Siw

Notations:

Keo	Effective Oil Permeability
Kew	Effective Water Permeability
Sro	<b>Residual Oil Saturation</b>
Siw	Irreducible Water Saturation







**APPENDIX III** 

# CORE LABS RESERVOIR DATA FLUID ANALYSIS

## RESERVOIR FLUID ANALYSIS

#### FOR

YATES PETROLEUM CORPORATION State CO #2 Dagger Draw North Field Eddy County, New Mexico

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April 3, 1990

YATES PETROLEUM CORPORATION 105 South 4th Street Artesia, New Mexico 88210

Attention: Mr. Pinson McWhorter

Subject: Reservoir Fluid Study State CO #2 Dagger Draw North Field Eddy County, New Mexico File: RFLM 90017

Gentlemen:

Duplicate separator liquid and gas samples were collected from the subject well and were submitted to our Midland laboratory on December 1, 1989 for use in a reservoir fluid study. Presented in the following report are the results of this study as requested by Yates Petroleum Corporation.

The subject well is currently producing a gas/oil ratio greater than what is expected for this reservoir. This indicates that there is free-gas production associated with the solution gas. Therefore, it was decided to recombine the separator products to create a reservoir fluid that has a bubble point of 2000 psig at 130°F. This fluid was used for the remainder of the study.

The hydrocarbon composition of the reservoir fluid was determined by spike-flash/chromatographic technique. The results in terms of both mol percent and weight percent are presented on page four.

A small quantity of the reservoir fluid was charged to a high pressure windowed cell and thermally expanded to the reservoir temperature of 130°F. During a constant composition expansion at this temperature, the fluid was found to have a bubble point pressure of 2003 psig. The results of the pressure-volume measurements at reservoir temperature may be found on page seven. YATES PETORLEUM COMPANY Page 2

When subjected to differential pressure depletion at the reservoir temperature. The fluid evolved a total of 485 cubic feet of gas at 15.025 psia and 60°F. per barrel of residual oil at 60°F. The resulting relative oil volume factor was 1.247 barrels of saturated fluid per barrel of residual oil. The oil density and the properties of the evolved gases were measured at each point during the differential pressure depletion and these data are included in the summary of the differential depletion data on page eight.

The viscosity of the reservoir fluid was measured over a wide range of pressures at 130°F. in a rolling ball viscosimeter. The viscosity of the fluid was found to vary from a minimum of 0.77 centipoise at the saturation pressure to a maximum of 1.92 centipoise at atmospheric pressure. The results of the viscosity measurements are tabulated on page fifteen.

One multi-stage separator test was performed to measure gas-oil ratio, stock tank oil gravity, and formation volume factor. The results of the separator test can be found on page eleven.

For your convenience, differential data has been adjusted to separator conditions. The results can be found on page twelve.

Thank you for the opportunity to be of service to Yates Petroleum Corporation. If you have any question or if we may be of further assistance in any way, please feel free to call upon us.

Very truly yours,

CORE LABORATORIES, a division of WESTERN ATLAS INTERNATIONAL, INC.

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Richard Hulme Supervisor Reservoir Fluid Lab

#### File RFLM 90017

YATES PETROLEUM CORPORATION Date Sampled: December 1, 1989 State CO #2 Eddy County, New Mexico Dagger Draw North Field

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Date Sampled: December 1, 1989

#### FORMATION CHARACTERISTICS

Formation Name Date First Well Completed Original Reservoir Pressure Original Produced Gas/Liquid Ratio Production Rate Separator Pressure and Temperature Liquid Gravity at 60°F. Datum

Canyon N/A 3010 psig @ 7572 ft. N/A SCF/Bbl N/A Bbls/Day N/A psig N/A°F. N/A °API N/A ft. Subsea

#### WELL CHARACTERISTICS

Elevation Total Depth Producing Interval Tubing Size and Depth Open Flow Potential Last Reservoir Pressure Date Reservoir Temperature Status of Well Pressure Gauge

**REMARKS:** 

3618 ft. KB, 3605 ft. GL 9427 ft. TD 8800 ft. PBTD 7751-7843 ft. 2 7/8 In. to 7699 ft. 409 BOPD,817 MCFD,979 BWPD 2000 psig @ N/A ft. N/A 130°F. @ 7565 ft. N/A

#### SAMPLING CONDITIONS

N/A

Flowing Tubing Pressure 331 psig Flowing Bottom Hole Pressure 931 psig Primary Separator Pressure 67 psig Primary Separator Temperature 100°F. Secondary Separator Pressure 29 psig Secondary Separator Temperature 108°F. Field Stock Tank Liquid Gravity 44.5°API @ 60°F. Primary Separator Gas Production Rate 709.711 MSCF/Day Pressure Base 15.025 psia Temperature Base 60°F. Compressibility Factor (Fpv) 1.000 Gas Gravity (Laboratory) Gas Gravity Factor (Fg) 0.737 1.000 Stock Tank Liquid Production Rate @ 60°F. 735.55 Bbls/Day Primary Separator Gas/Stock Tank Liquid Ratio 965 SCF/Bbl Tefteller Inc. Sampled by

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#### SUMMARY OF RESERVOIR FLUID PVT DATA

<u>Volumetric Data</u> Bubble point pressure (Pb) at 130°F. = 2003 psig

Thermal expansion of reservoir fluid at  $5000 \text{ psig} = \underline{V \text{ at } 130^{\circ}\text{F.}} = 1.03111$  $V \text{ at } 67^{\circ}\text{F.}$ 

Compressibility of reservoir fluid at 130°F. from 3000 psig to 2500 psig =  $9.45 \times 10^{-6} \text{ V/V/psi}$ from 2500 psig to 2003 psig =  $10.06 \times 10^{-6} \text{ V/V/psi}$ 

#### Differential Vaporization Data

Solution gas/oil ratio at 2003 psig and 130°F. = 485 standard cubic feet of gas at 15.025 psia and 60°F. per barrel of residual oil at 60°F.

Relative oil volume at 2003 psig and  $130^{\circ}F. = 1.247$  barrels of oil per barrel of residual oil at  $60^{\circ}F.$ 

Density of reservoir fluid at 2003 psig and 130°F. = 0.7177 gm/cc

<u>Viscosity Data</u> Viscosity of reservoir fluid at 2003 psig and 130°F. = 0.77 centipoise

Separator Test Data

Separator ConditionsBo(1)Rs(2)Tank Oil Gravity67 psig and 100°F.67API at 60°F.67to29 psig and 110°F.100°F.4300 psig and 68°F.1.23343042.7

- (1) Formation volume factor, barrels of oil at 2003 psig and 130°F. per barrel of stock tank oil at 60°F.
- (2) Total solution gas/oil ratio at 2003 psig and 130°F., total standard cubic feet of gas at 15.025 psia and 60°F. per barrel of stock tank oil at 60°F.



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## SUMMARY OF QUALITY CONTROL DATA OF SEPARATOR LIQUID SAMPLES

Cylinder <u>Number</u>	Sampling <u>Conditions</u> Pressure, <u>PSIG</u>	Temperature, °F.	Laboratory <u>Bubble point</u> Pressure, <u>PSIG</u>	Temperature, •F.
1*	28	108	20	68
2	28	108	18	68

\* Selected for use in study.

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### HYDROCARBON ANALYSIS OF RESERVOIR FLUID SAMPLE

<u>Component</u>	Mol <u>Percent</u>	Weight <u>Percent</u>	Density	<u>API</u>	Mol <u>Weight</u>
Hydrogen Sulfide	0.00	0.00			
Carbon Dioxide	0.34	0.14			
Nitrogen	0.18	0.05			
Methane	37.33	5.56			
Ethane	4.96	1.38			
Propane	3.43	1.40			
<b>iso-</b> Butane	1.03	0.56			
n-Butane	2.36	1.27			
iso-Pentane	1.27	0.85			
n-Pentane	1.43	0.96			
Hexanes	1.33	1.04			
Heptanes plus	46.34	86.79	0.8240	40.1	202.
	100.00	100.00			

#### Sample Molecular Weight = 107.8



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#### HYDROCARBON ANALYSIS OF SEPARATOR GAS SAMPLE

<u>Component</u>	Mol <u>Percent</u>	GPM
Hydrogen Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane iso-Butane n-Butane iso-Pentane n-Pentane Hexanes Heptanes Octanes Nonanes Decanes Undecanes Dodecanes	$\begin{array}{c} 0.00\\ 1.24\\ 0.74\\ 0.39\\ 80.17\\ 8.43\\ 4.38\\ 0.94\\ 1.77\\ 0.56\\ 0.53\\ 0.42\\ 0.29\\ 0.12\\ 0.29\\ 0.12\\ 0.01\\ 0.00\\ 0.01\\ 0.00\\ 0.01\\ 0.00\\ 0.01\\ 0.00\\ 0.01\\ 0.00\\ 0.01\\ 0.00\\ 0.01\\ 0.00\\ 0.01\\ 0.00\\ 0.00\\ 0.00\\ 0.01\\ 0.00$	2.242 1.200 0.306 0.555 0.204 0.191 0.162 0.121 0.054 0.005 0.000 0.006 0.000
	100.00	5.046

Calculated Gas Gravity = 0.737

Calculated Gross Heating Value = 1248 BTU per cubic foot of dry gas at 15.025 and 60°F.

Collected at 67 psig and 99°F.

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#### VOLUMETRIC DATA OF RESERVOIR FLUID SAMPLE

Saturation pressure (bubble point pressure) = 2003 PSIG 130°F. Specific volume at saturation pressure = 0.02223 ft <sup>3</sup>/lb @ 130°F. Thermal expansion @ 5000 PSIG = 1.03111 V @ 130°F./V @ 67°F. Compressibility @ 130°F.:

> From 5000 PSIG to 4000 PSIG =  $7.65 \times 10^{-6} \text{ V/V/PSI}$ From 4000 PSIG to 3000 PSIG =  $9.29 \times 10^{-6} \text{ V/V/PSI}$ From 3000 PSIG to 2500 PSIG =  $9.45 \times 10^{-6} \text{ V/V/PSI}$ From 2500 PSIG to 2003 PSIG =  $10.06 \times 10^{-6} \text{ V/V/PSI}$

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·····	<u>onstant Composi</u>		<u> </u>
Pressure	Relative	Y	Density
PSIG	<u>Volume(1)</u>	Function(2)	_Gm/cc
5000	0.9736		0.7372
4500	0.9771		0.734
4000	0.9811		0.731
3500	0.9856		0.7282
3000	0.9903		0.724
2500	0.9950		0.721:
2400	0.9961		0.720
2300	0.9972		0.719
2200	0.9981		0.719
2100	0.9992		0.718
2003 Pb	1.0000		0.717
1971	1.0029		
1948	1.0050		
1925	1.0070		
1900	1.0091		
1858	1.0205		
1760	1.0448	3.057	
1600	1.0855	2.918	
1422	1.1462	2.766	
1249	1.2286	2.609	
1088	1.3355	2.473	
955	1.4590	2.354	
869	1.5631	2.278	
765	1.7274	2.182	
683	1.8929	2.118	
533	2.3541	1.981	
410	3.0023	1.872	
300	4.0356	1.781	

PRESSURE-VOLUME RELATIONS OF RESERVOIR FLUID AT 130°F.

# (1) Relative Volume: V/Vsat is barrels at indicated pressure barrel at saturation pressure.

(Pabs) (V/Vsat-1)

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Mastern Atlas International	

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130°F
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VAPORIZATION
DIFFERENTIAL

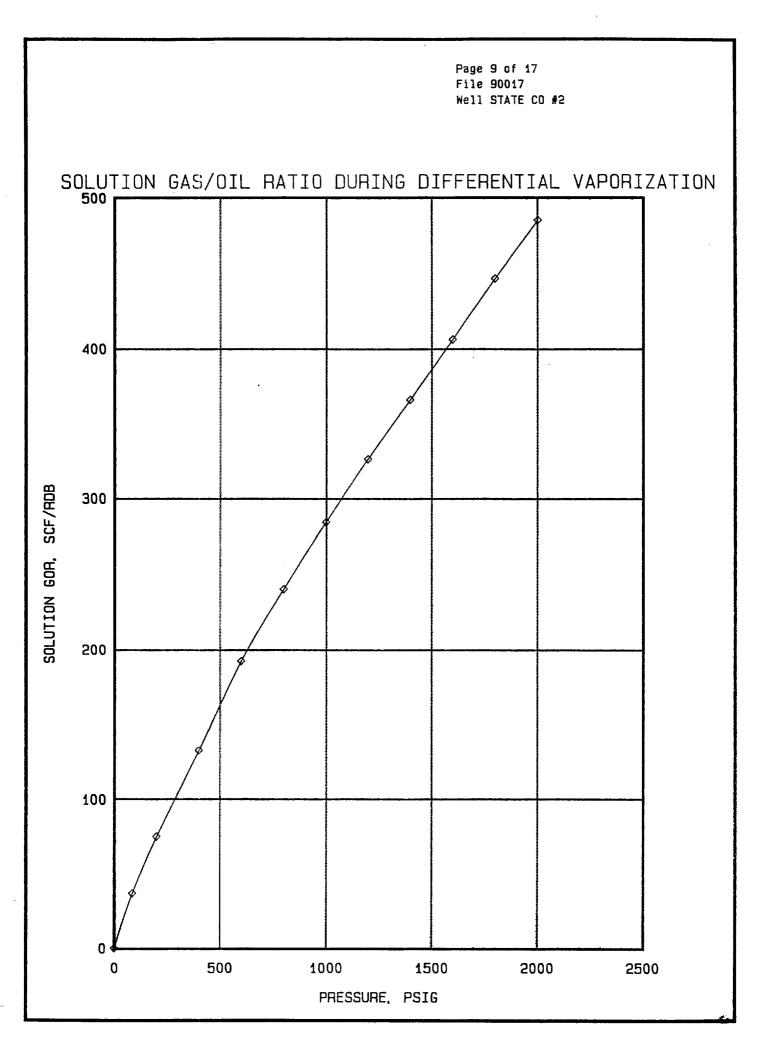
Incremental Gas Gravíty	0.651 0.651 0.655 0.655 0.667 0.681 0.768 0.768 1.614	
Gas Formation Volume Factor(4)	0.00790 0.00899 0.01040 0.01231 0.01500 0.02570 0.03894 0.07707 0.16826	
Deviation Factor, Z	0.841 0.852 0.863 0.877 0.863 0.877 0.863 0.877 0.927 0.927 0.927 0.927 0.987	
oil Density, Gm/CC	0.7177 0.7218 0.7269 0.7382 0.7382 0.7577 0.7577 0.7577 0.7743 0.7743 0.7798	
Relative Total Volume(3)	1.247 1.288 1.344 1.530 1.530 1.974 2.463 3.545 6.699 14.482	
Relative oil Volume, Bod(2)	1.247 1.233 1.217 1.217 1.182 1.182 1.182 1.182 1.035 1.035 1.035	
Solution Gas/Oil Ratio,Rsd(1)	485 4466 3266 3266 11922 3356 11922 1322 1322 1322 1322 1322 1322 132	
Pressure, psig	2003 1800 1600 1400 800 85 85 0 0 85 0 0	

at 60°F = 1.000

Gravity of Residual Oil = 42.5°API @ 60°F.

Oubic feet of gas at 15.025 psia and 60°F. per barrel of residual oil at 60°F. Barrels of oil at indicated pressure and temperature per barrel of residual oil at 60°F. Barrels of oil plus liberated gas at indicated pressure and temperature per barrel of residual oil at 60°F. £00£

Cubic feet of gas at indicated pressure and temperature per cubic foot at 15.025 psia and 60°F.



Page 10 of 17 File 90017 Well STATE CO #2 RELATIVE OIL VOLUME DURING DIFFERENTIAL VAPORIZATION 1.25 1.20 RELATIVE OIL VOLUME, V/Vr 1.15 1.10 1.05 1.00 500 1000 1500 2000 2500 0 PRESSURE, PSIG

Western Atlas International 

CORE LABORATURIES

File RFIM 90017 Page 11 of 17 State  $\infty$  #2

SEPARATOR TEST OF RESERVOIR FIUID SAMPLE

Specific Gravity of Flashed Gas	0.724	0.868*	1.148	
Separator Volume Factor (4)	1.048	1.054	1.004	
Formation Volume Factor, Bofb(3)			1.233	
Stock Tank Gravity, API @ 60°F			42.7	
Gas/Oil Ratio (2)	404	e	23	11
Gas/Oil Ratio (1)	386	m	23	Rsfb
Separator Temperature, °F	100	011	68	
Separator Pressure, PSI Gauge	67 to	to 3	0	

\* Theoretical value

- Gas/Oil Ratio in cubic feet of gas @ 60°F. and 15.025 PSI absolute per barrel of oil @ indicated pressure and temperature. <del>3</del>
- <u>ര</u>.ഇ
- Gas/Oil Ratio in cubic feet of gas @ 60°F. and 15.025 PSI absolute per barrel of stock tank oil @ 60°F. Formation Volume Factor is barrels of saturated oil @ 2003 PSI gauge and 130°F. per barrel of stock tank oil @ 60°F.
- Separator Volume Factor is barrels of oil @ indicated pressure and temperature per barrel of stock tank oil @ 60°F. (4)



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#### DIFFERENTIAL VAPORIZATION DATA ADJUSTED TO SEPARATOR CONDITIONS\*

Pressure, psig	Solution Gas/Oil Ratio, Rs(1)	Formation Volume Factor, Bo(2)	Gas Formation Volume Factor, Bg(3)	Oil Density, gm/cc	Oil/Gas Viscosity Ratio
<b>500</b> 0	430	1.200		0.7372	
4500	430	1.205		0.7345	
4000	430	1.210		0.7315	
3500	430	1.215		0.7282	
<b>300</b> 0	430	1.221		0.7247	
<b>250</b> 0	430	1.227		0.7213	
<b>230</b> 0	430	1.223		0.7197	
<b>220</b> 0	430	1.231		0.7191	
<b>210</b> 0	430	1.232		0.7183	
2003 Pb	<b>4</b> 30	1.233		0.7177	
<b>180</b> 0	391	1.219	0.00790	0.7218	49.7
<b>160</b> 0	352	1.203	0.00899	0.7269	54.5
<b>140</b> 0	312	1.187	0.01040	0.7323	60.5
<b>120</b> 0	273	1.169	0.01231	0.7382	66.7
1000	231	1.150	0.01500	0.7442	73.5
800	188	1.131	0.01901	0.7507	81.7
<b>60</b> 0	140	1.109	0.02570	0.7577	91.3
<b>40</b> 0	81	1.085	0.03894	0.7656	103.3
<b>20</b> 0	25	1.059	0.07707	0.7743	126.7
85	0	1.044	0.16826	0.7798	150.0
0	0	1.023			223.3

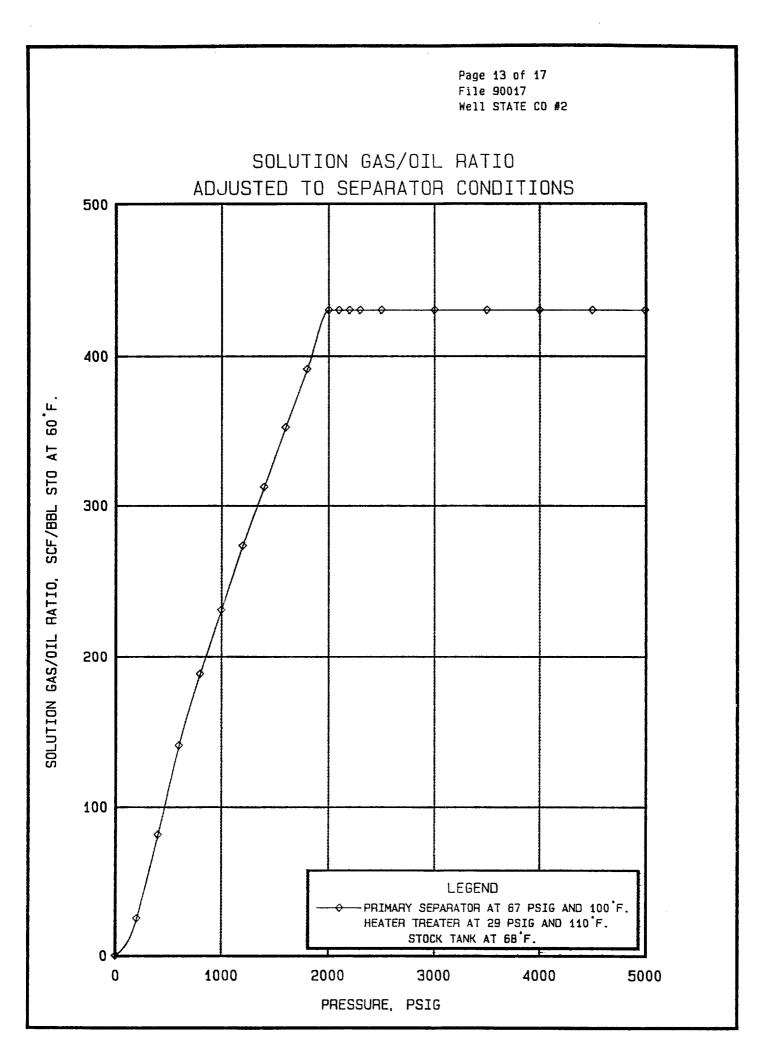
 $@ 60^{\circ}F. = 1.000$ 

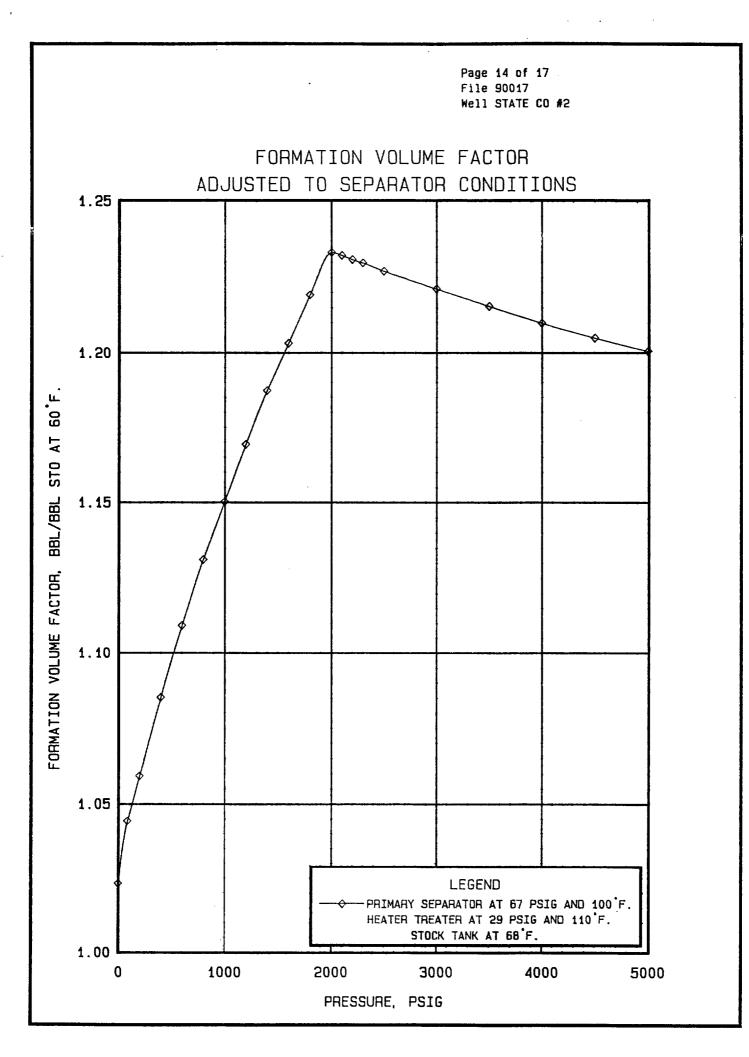
Gravity of Stock Tank Oil = 42.7°API @ 60°F.

\*Separator Conditions: Separator at 67 psig and  $100^{\circ}F.$ , Heater Treater at 29 psig and  $110^{\circ}F.$ , stock tank at  $68^{\circ}F.$ 

- (1) Cubic feet of gas at 15.025 psia and 60°F. per barrel of stock tank oil at  $60^{\circ}$ F.
- (2) Barrels of oil at indicated pressure and 130°F. per barrel of stock tank oil at 60°F.
- (3) Cubic feet of gas at indicated pressure and  $130^{\circ}F$ . per cubic foot at 15.025 psia and  $60^{\circ}F$ .

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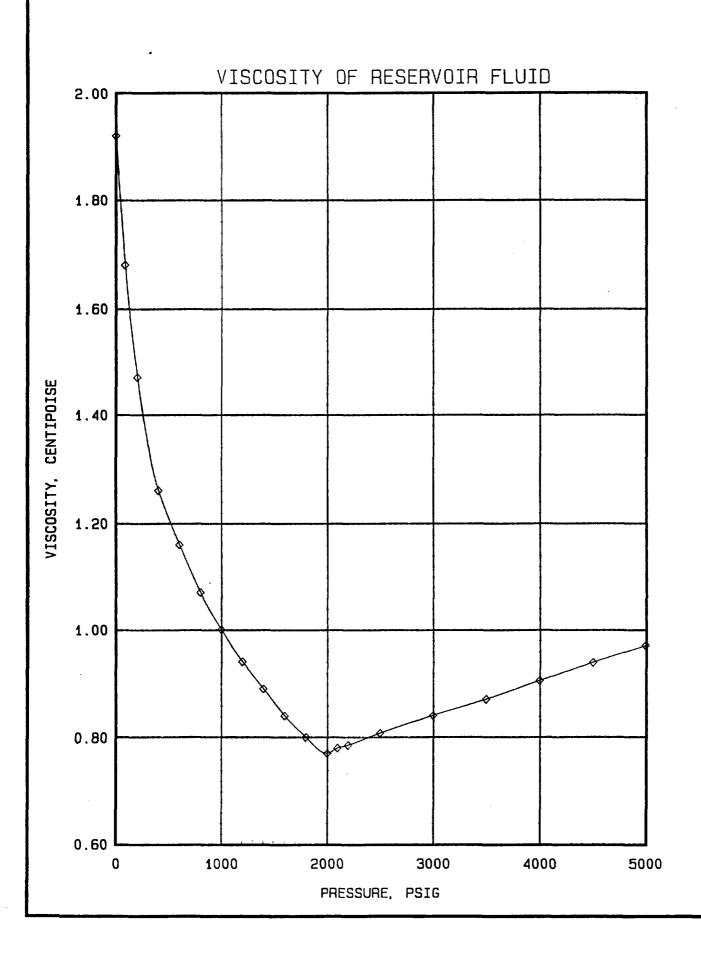
Page 15 of 17 File RFLM 90017 State CO #2

#### VISCOSITY DATA AT 130°F

Pressure psig	, Oil Viscosity Centipoise	Calculated Gas Viscosity, <u>Centipoise</u>	Oil/Gas Viscosity <u>Ratio</u>
<b>50</b> 00	0.97		
4500	0.94		
4000	0.90		
3500	0.87		
3000	0.84		
2500	0.80		
2200	0.78		
2100	0.78		
2003 P	b 0.77		
1800	0.80	0.0161	49.7
1600	0.84	0.0154	54.5
1400	0.89	0.0147	60.5
1200	0.94	0.0141	66.7
1000	1.00	0.0136	73.5
800	1.07	0.0131	81.7
600	1.16	0.0127	91.3
400	1.26	0.0122	103.3
200	1.47	0.0116	126.7
85	1.68	0.0112	150.0
0	1.92	0.0086	223.3

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#### NOMENCLATURE AND EQUATIONS TO ADJUST DIFFERENTIAL VAPORIZATION DATA TO SURFACE CONDITIONS

- Pb = Bubble point pressure
- Bo = Oil formation volume factor
- Bofb = Formation volume factor from field conditions (or optimum) separator flash test.
- Bob = Relative oil volume from differential vaporization test.
- Bodb = Value of Bod at the bubble point pressure.
- R.V. = Relative volume from pressure-volume relations test.

For Bo above the bubble point pressure:

 $Bo = R.V. \times Bofb$ 

For Bo below the bubble point pressure:

Bo = (Bod) (Bofb/Bodb)

- Rs = Gas in solution, standard cubic feet per barrel of stock tank oil.
- Rsfb = Sum of separator gas and the stock tank gas from field conditions (or optimum) separator flash test, standard cubic feet per barrel of stock tank oil.
- Rsd = The gas in solution from the differential vaporization test.
- Rsdb = The value of Rsd at the bubble point pressure.

Rs - Rsfb - [(Rsdb - Rsd)(Bofb/Bodbl)]

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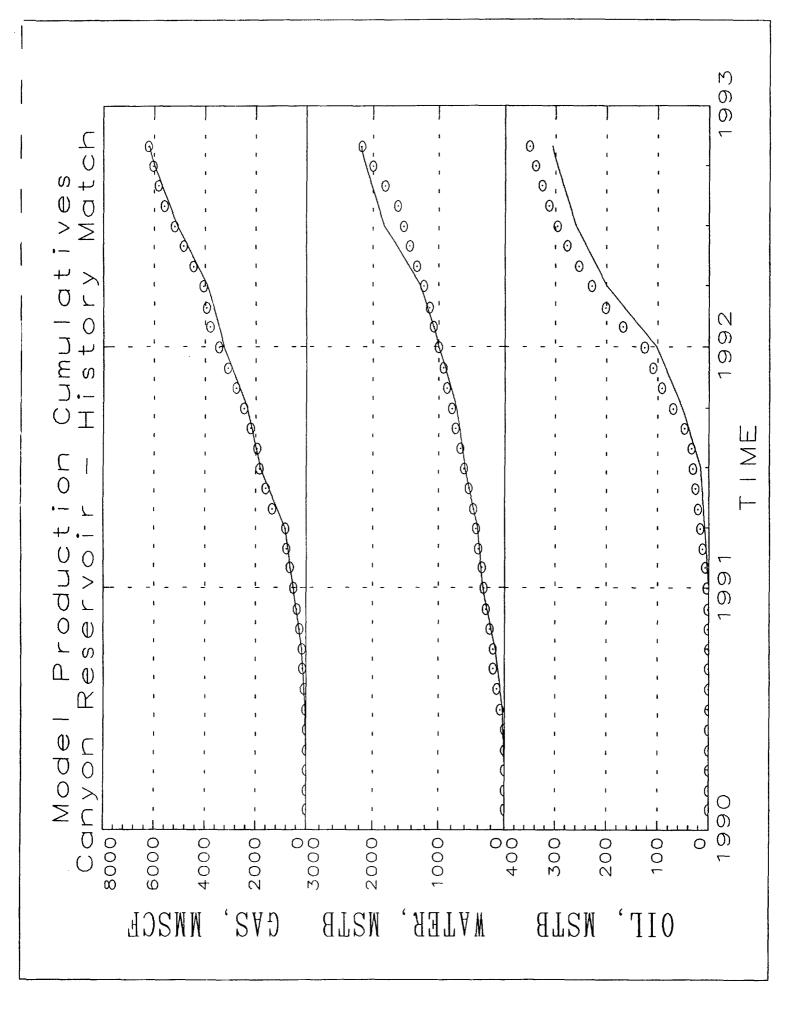
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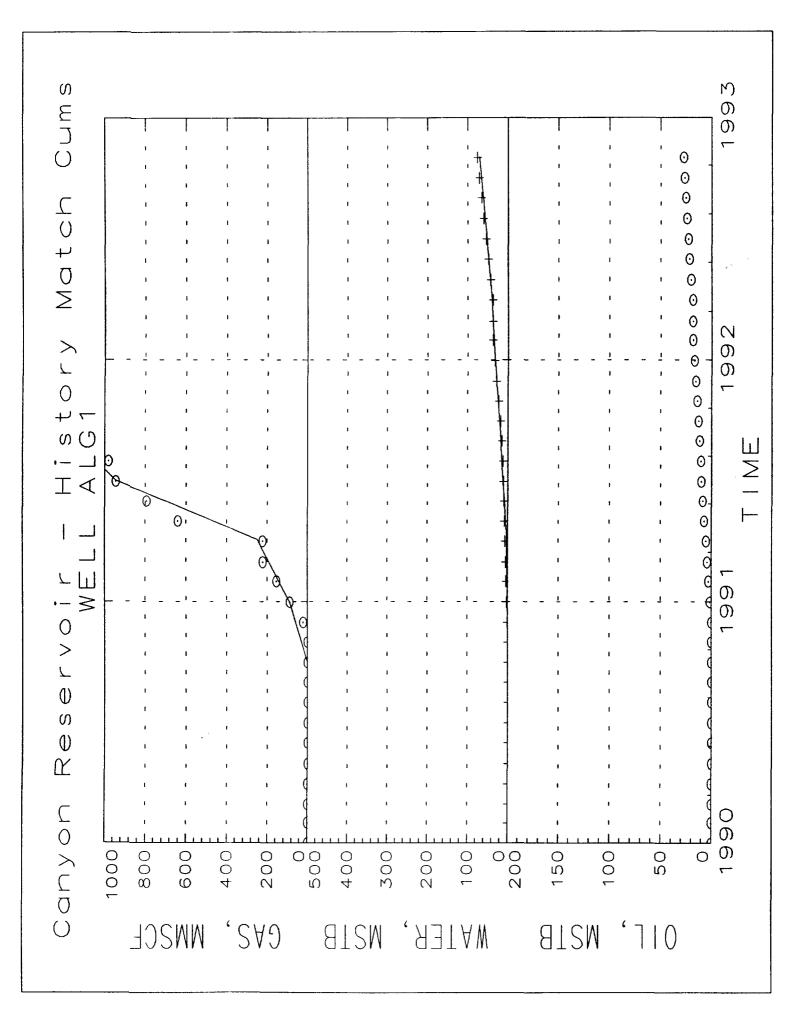
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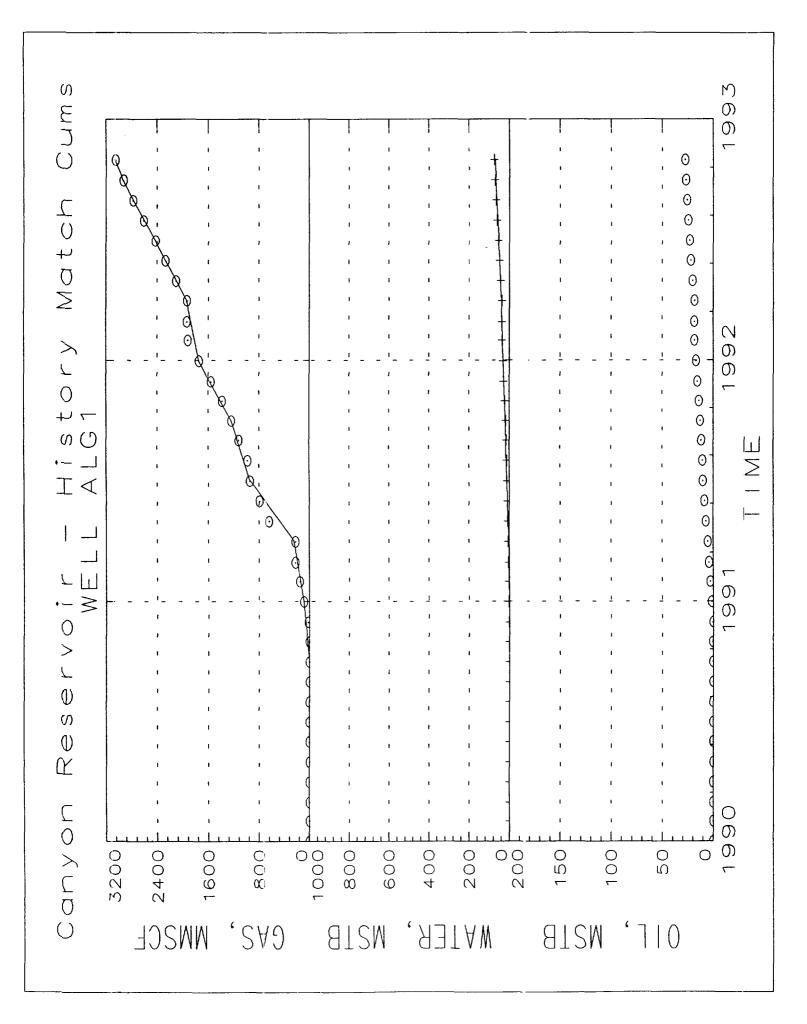
# APPENDIX IV

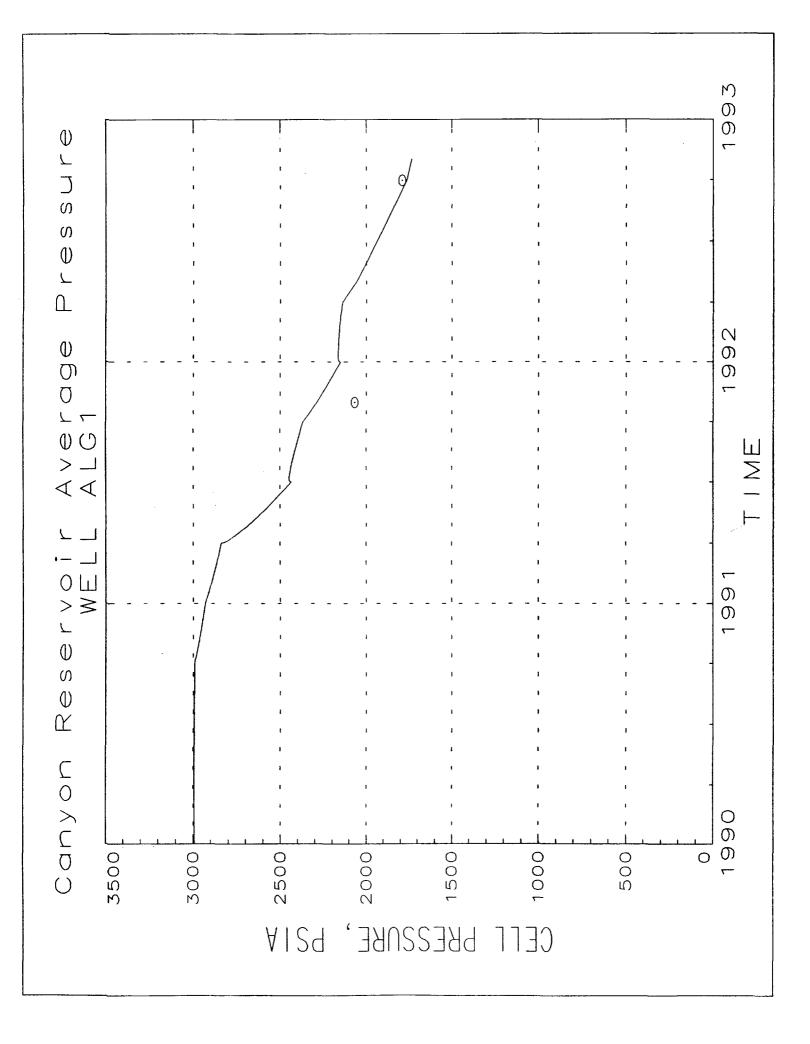
## **HISTORY MATCH**

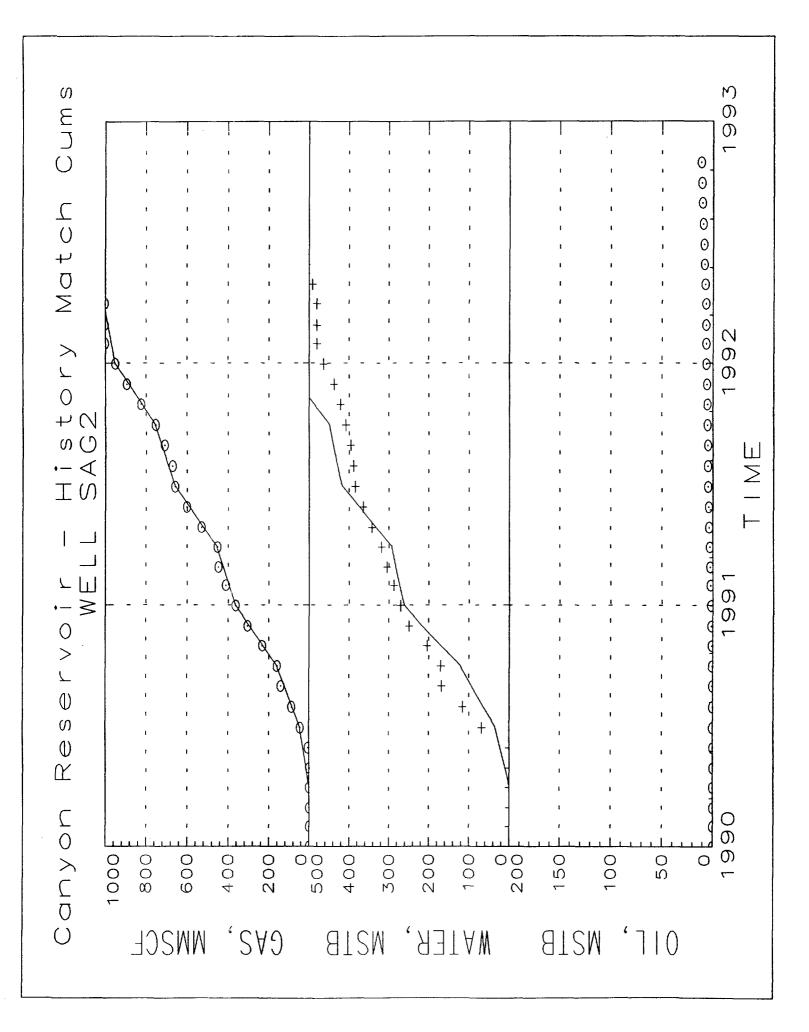
Model Performance Plot Well Performance Plots

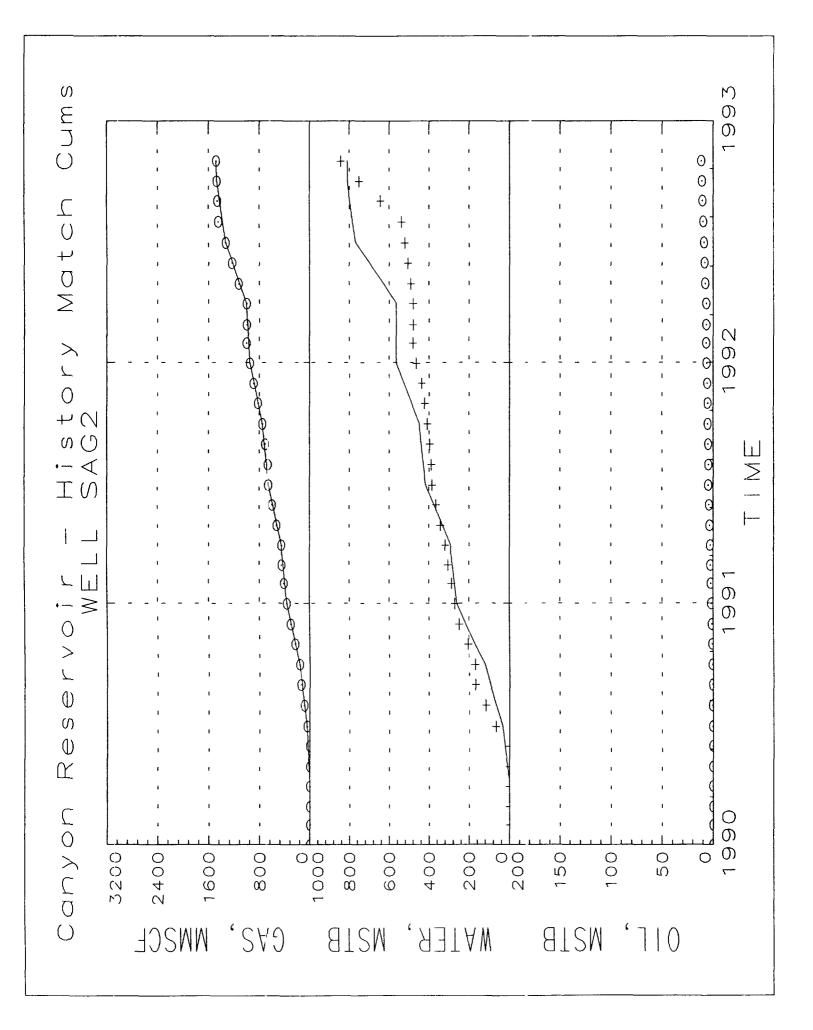


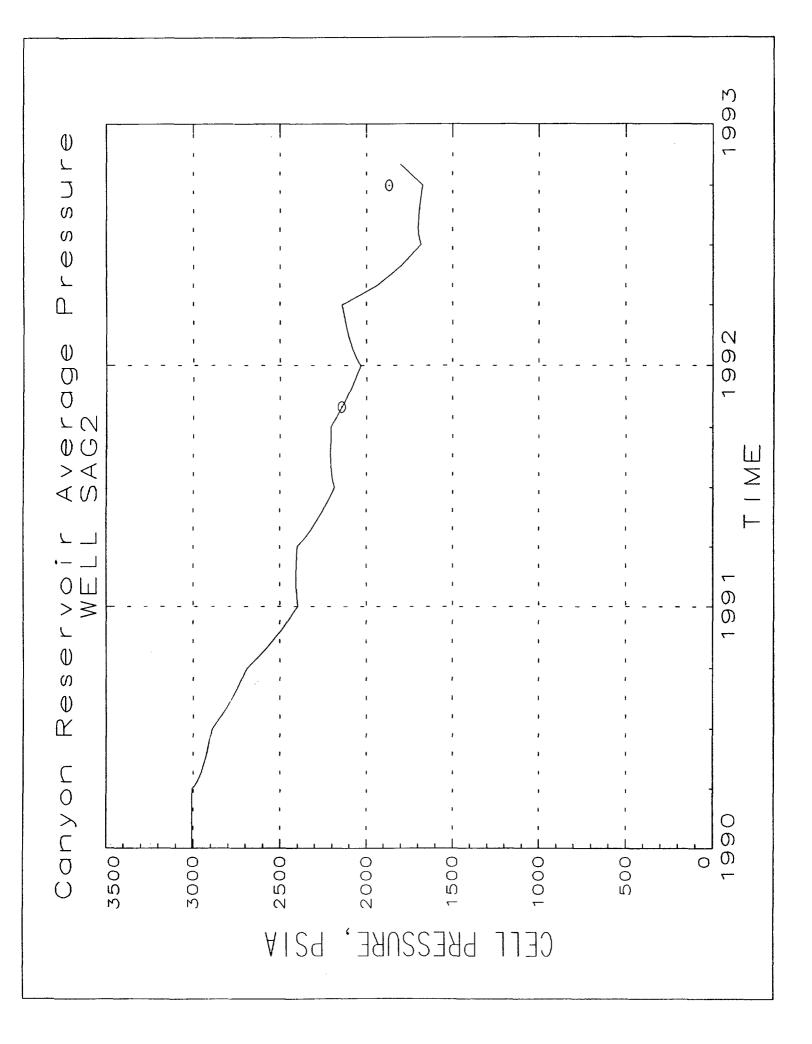


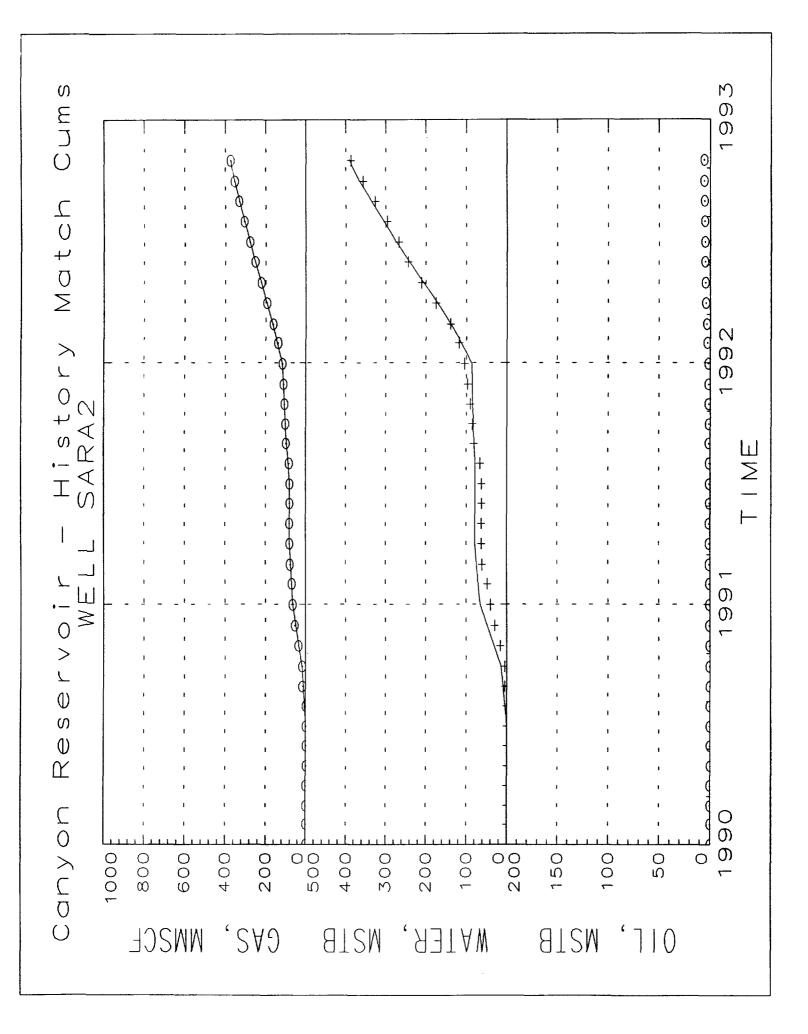


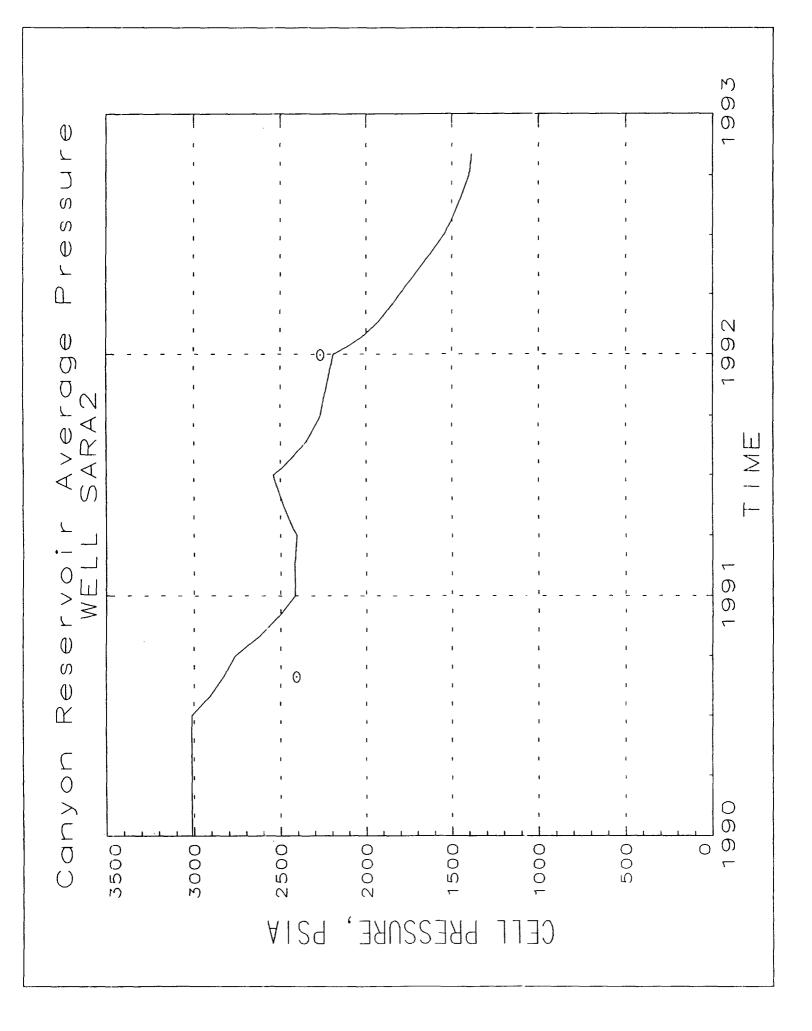


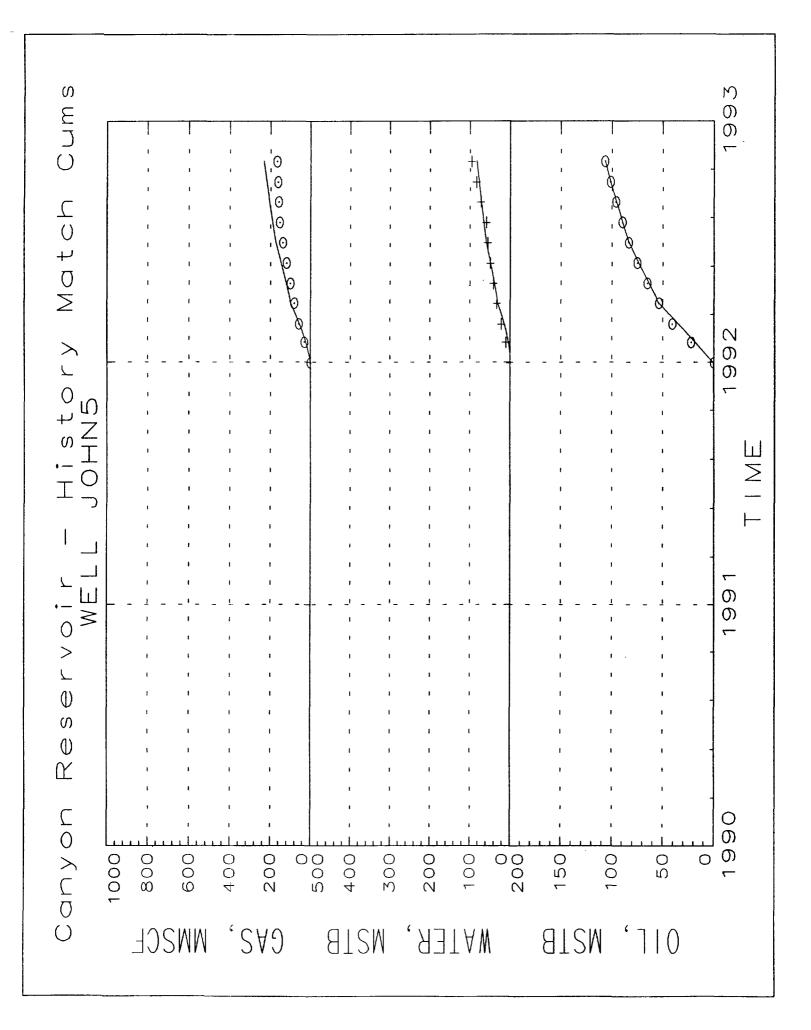


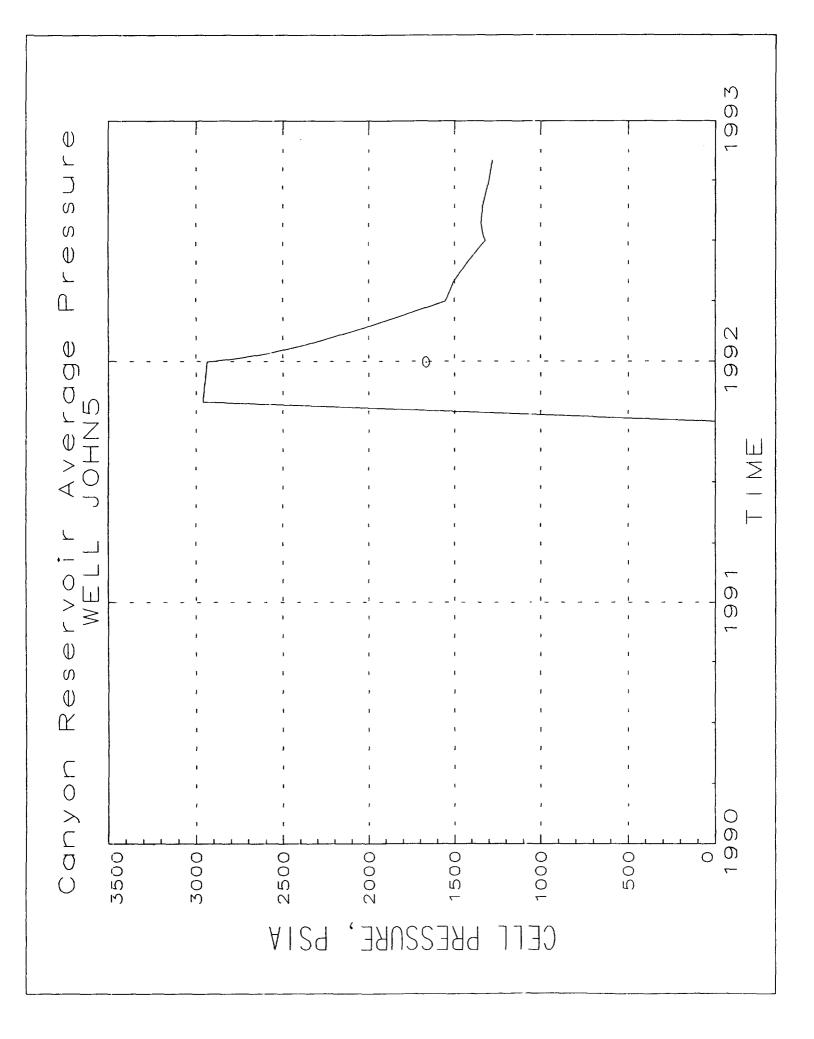


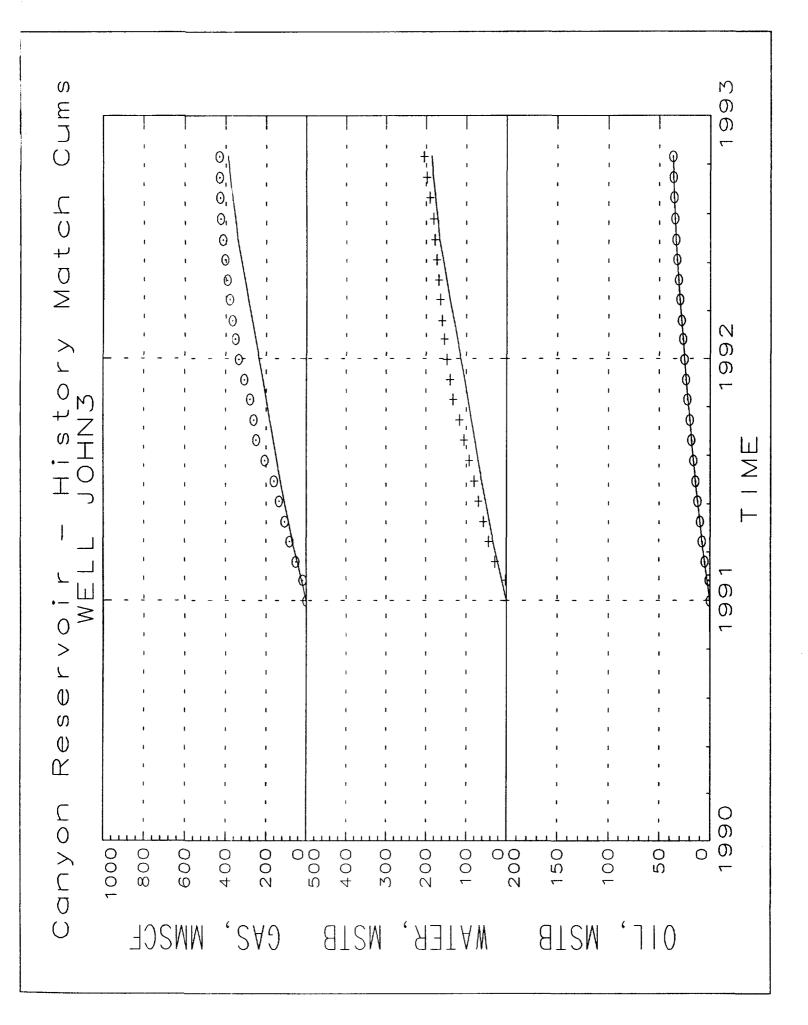


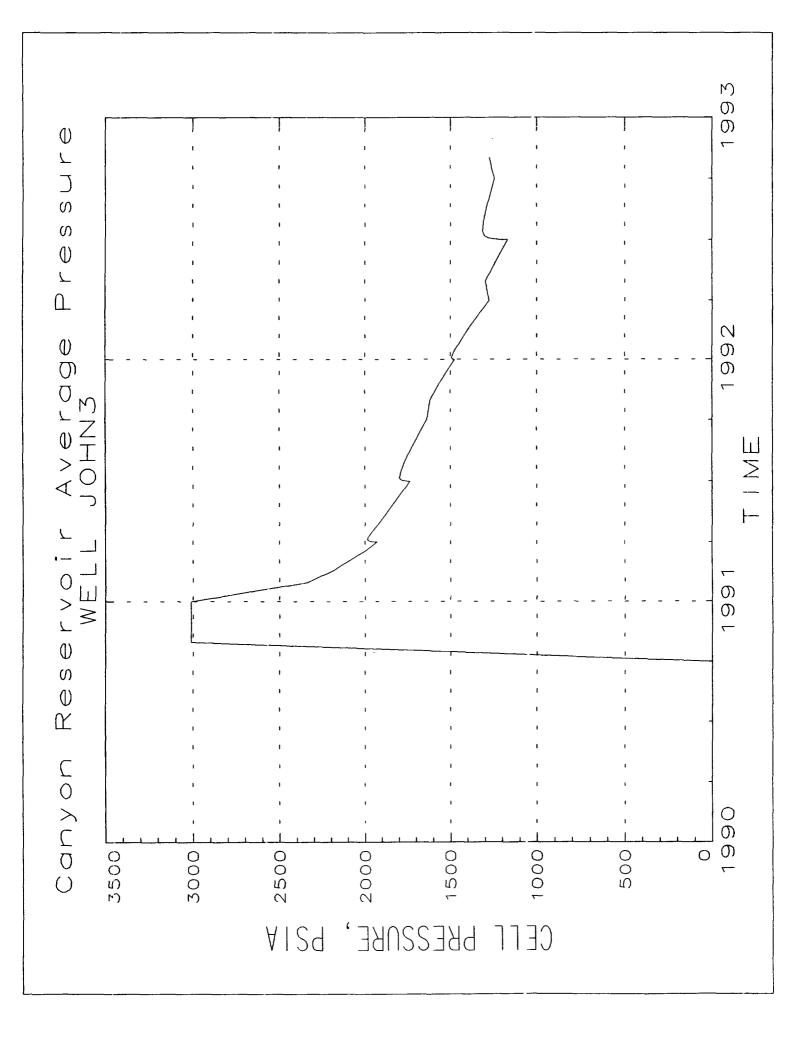


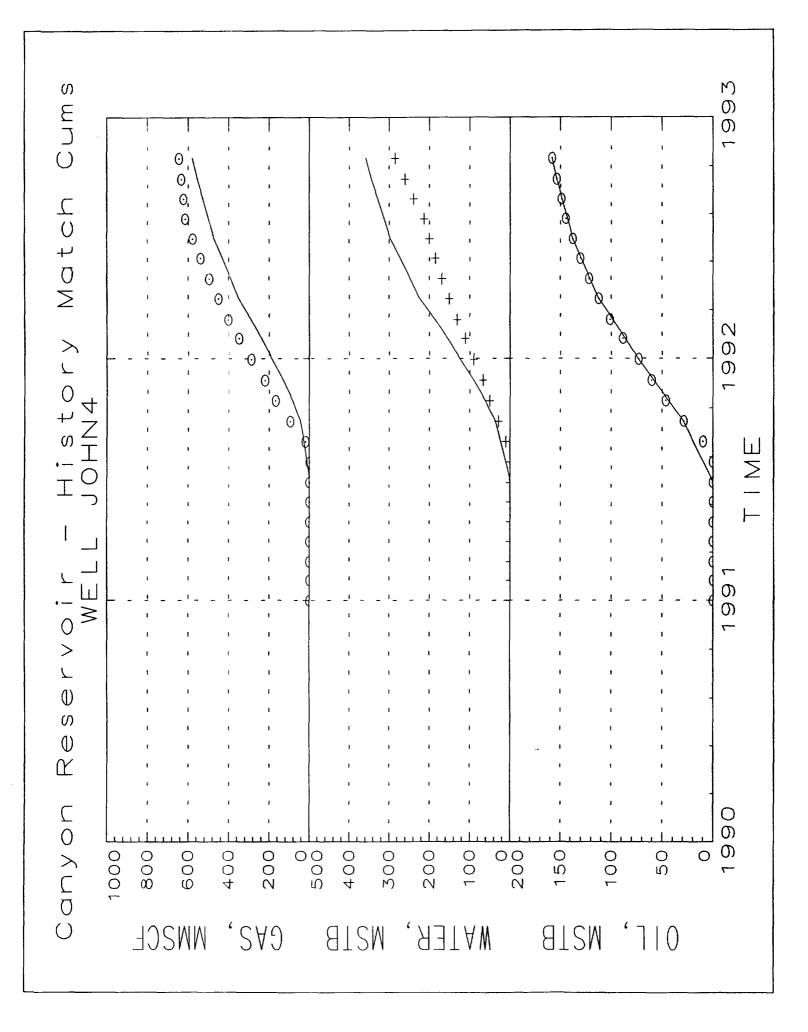


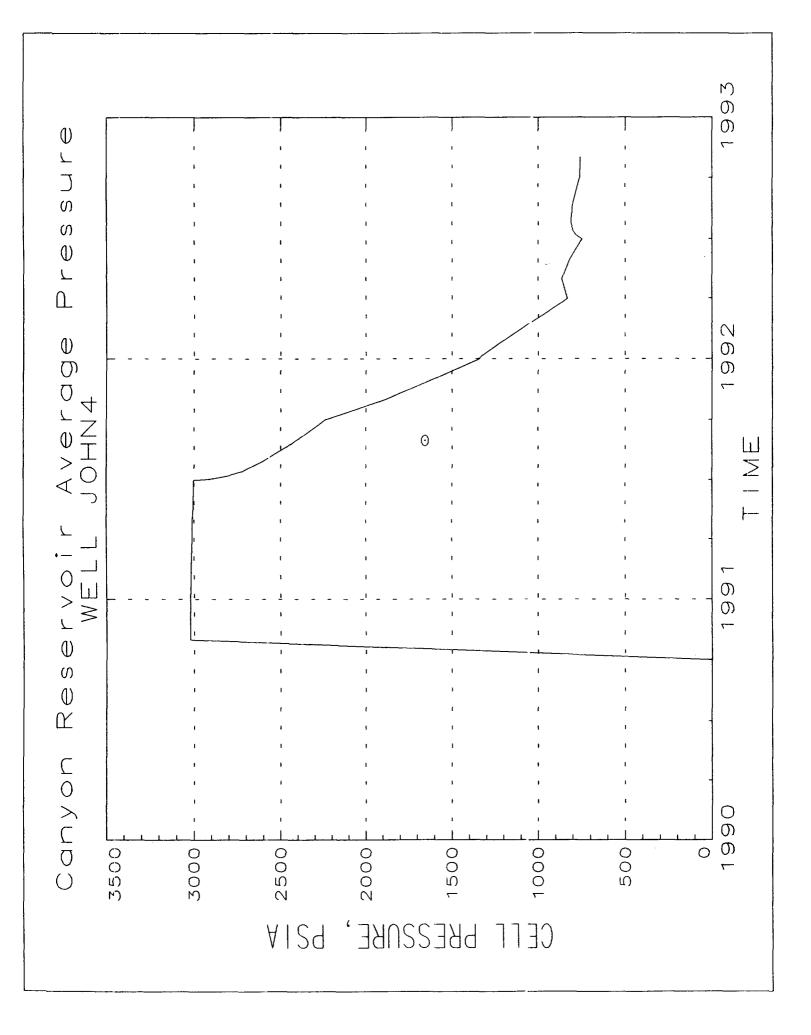


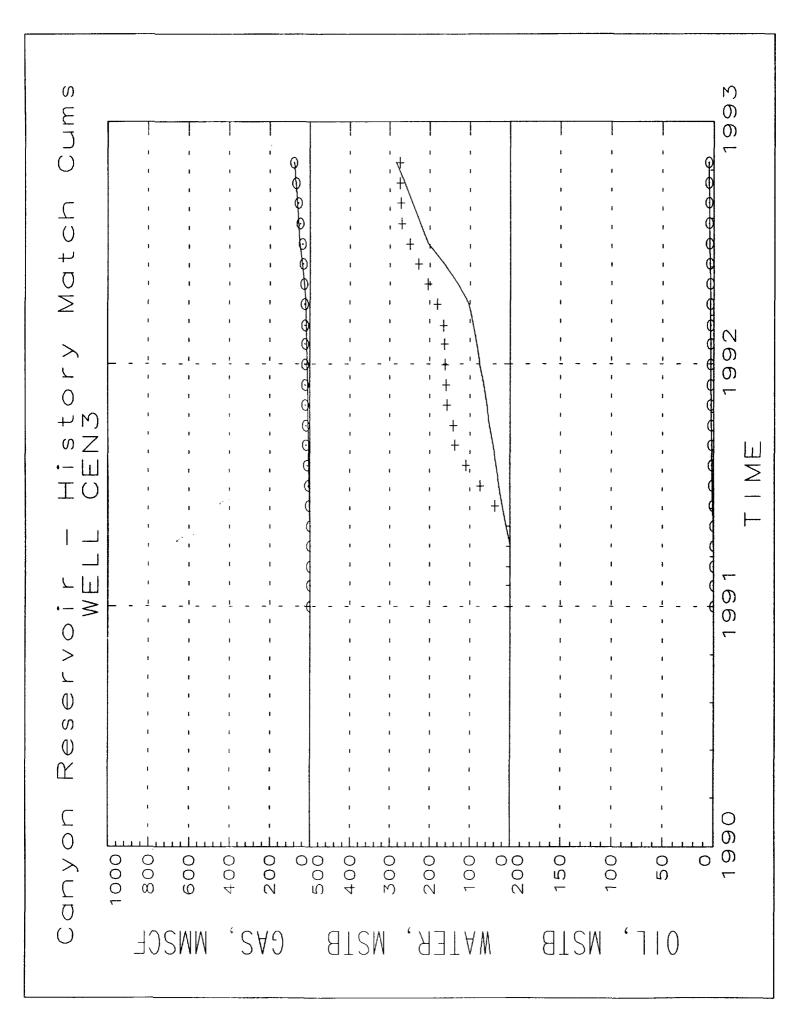


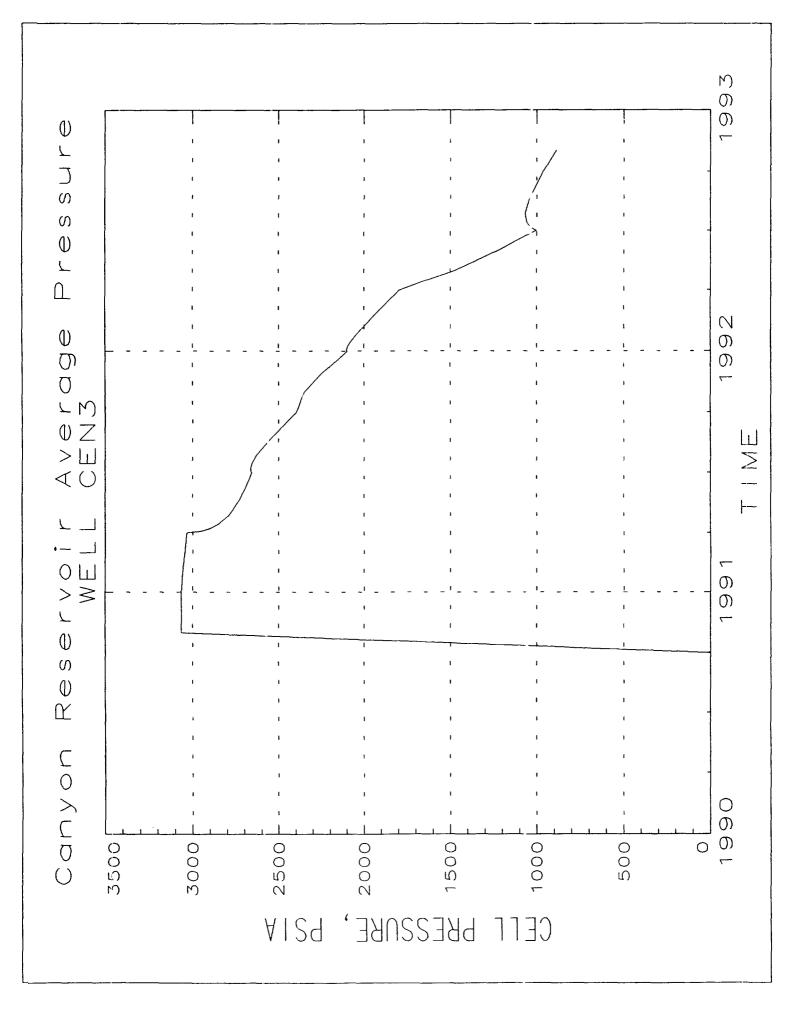












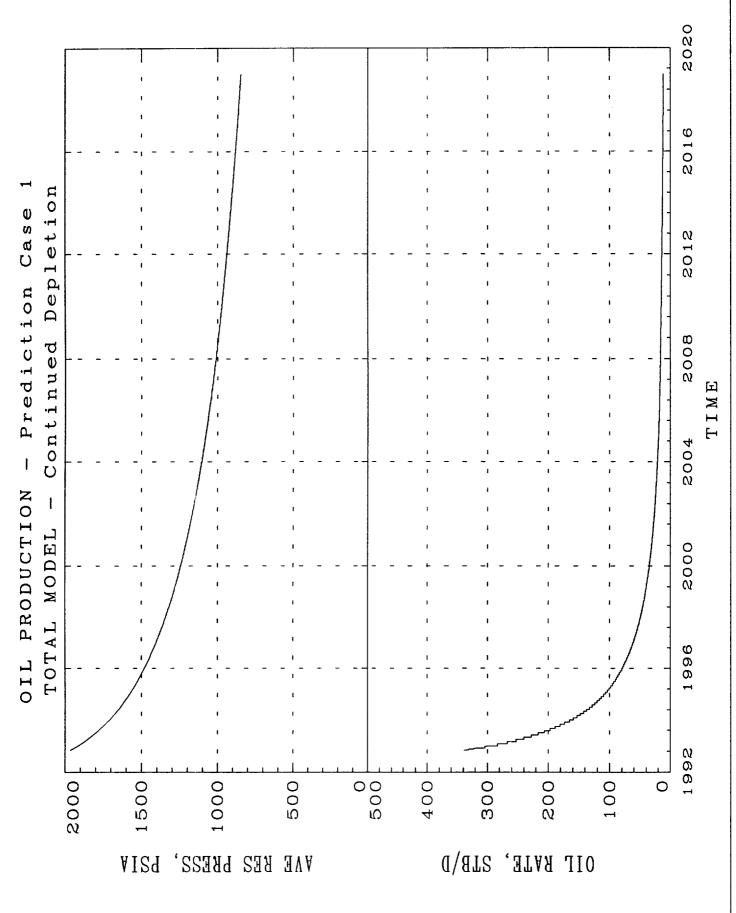
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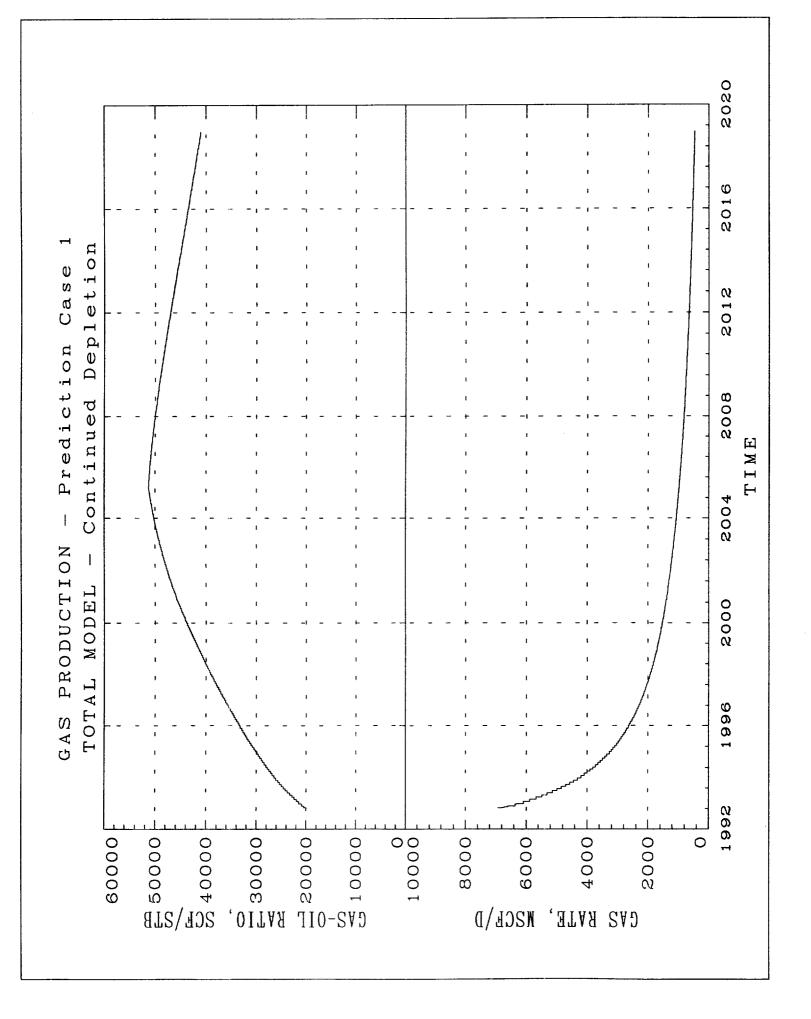
# APPENDIX V

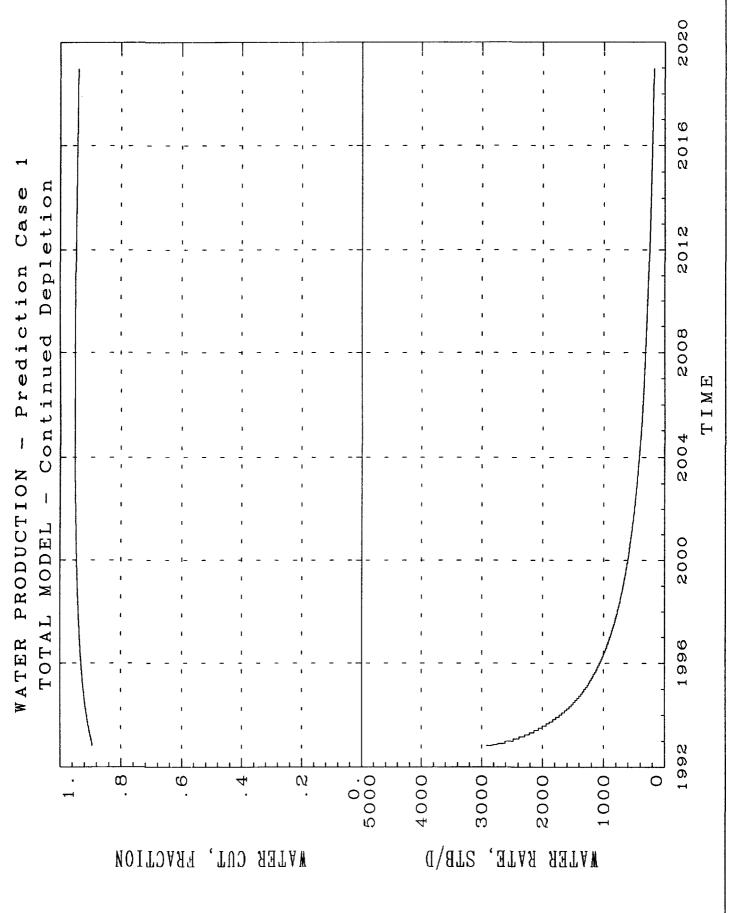
### **PREDICTION CASE 1**

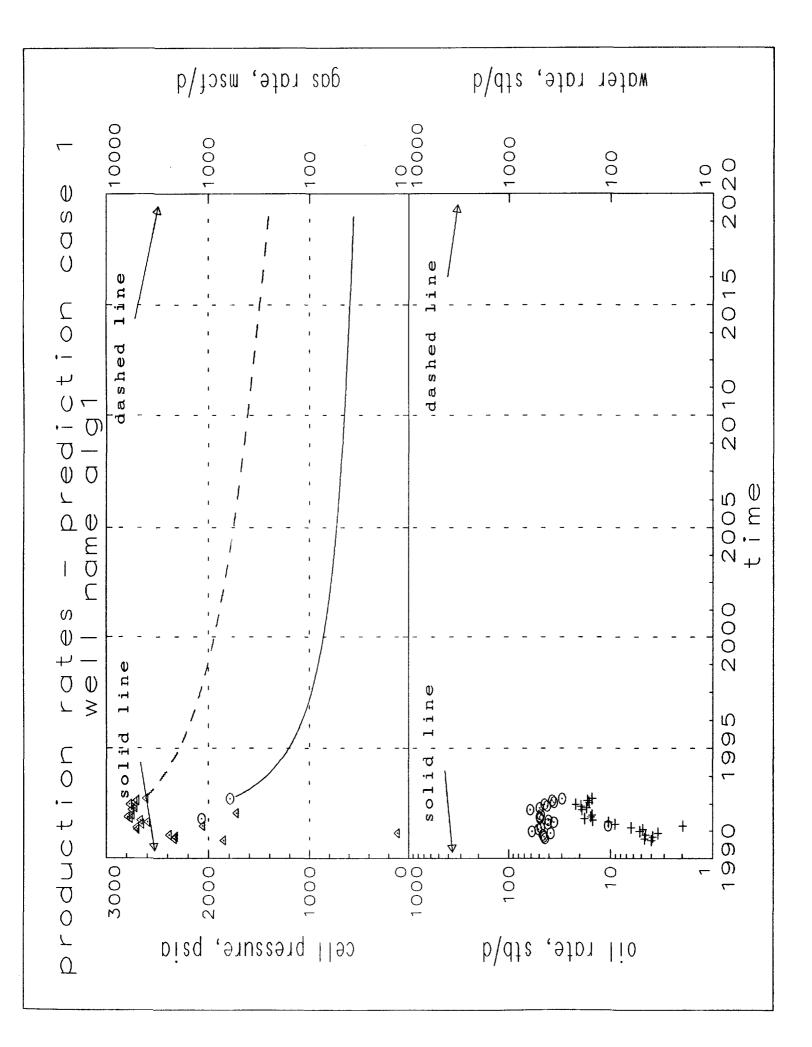
Model Performance Plots Well Performance Plots

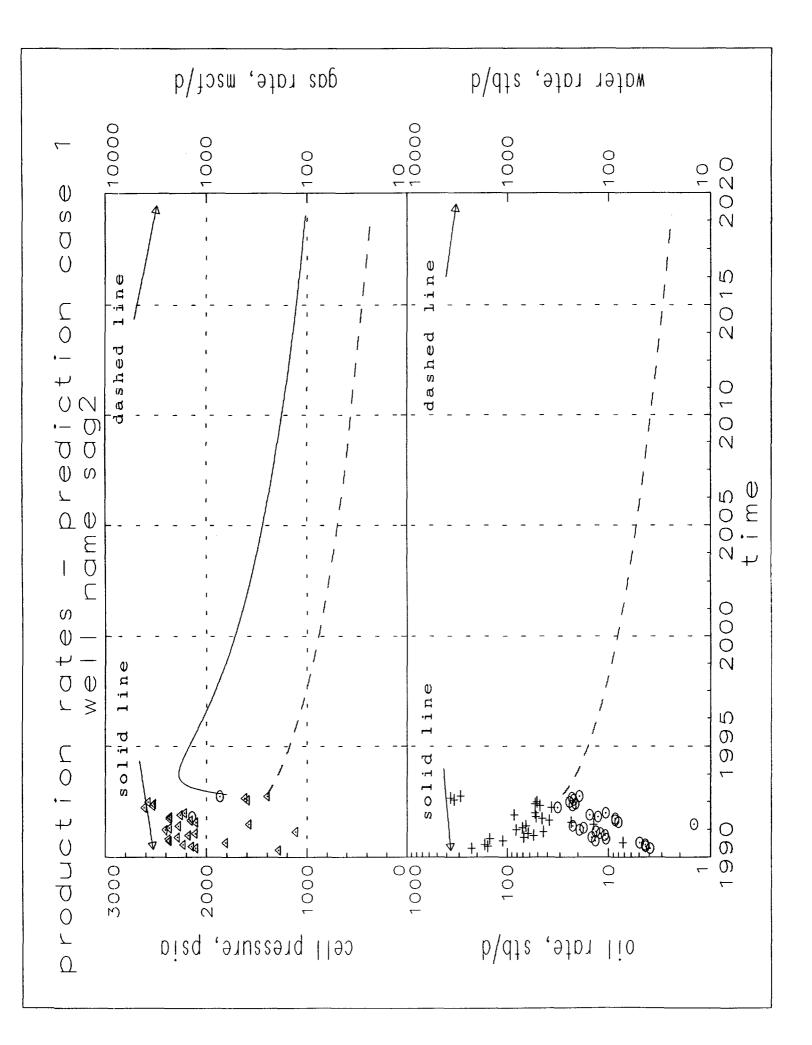
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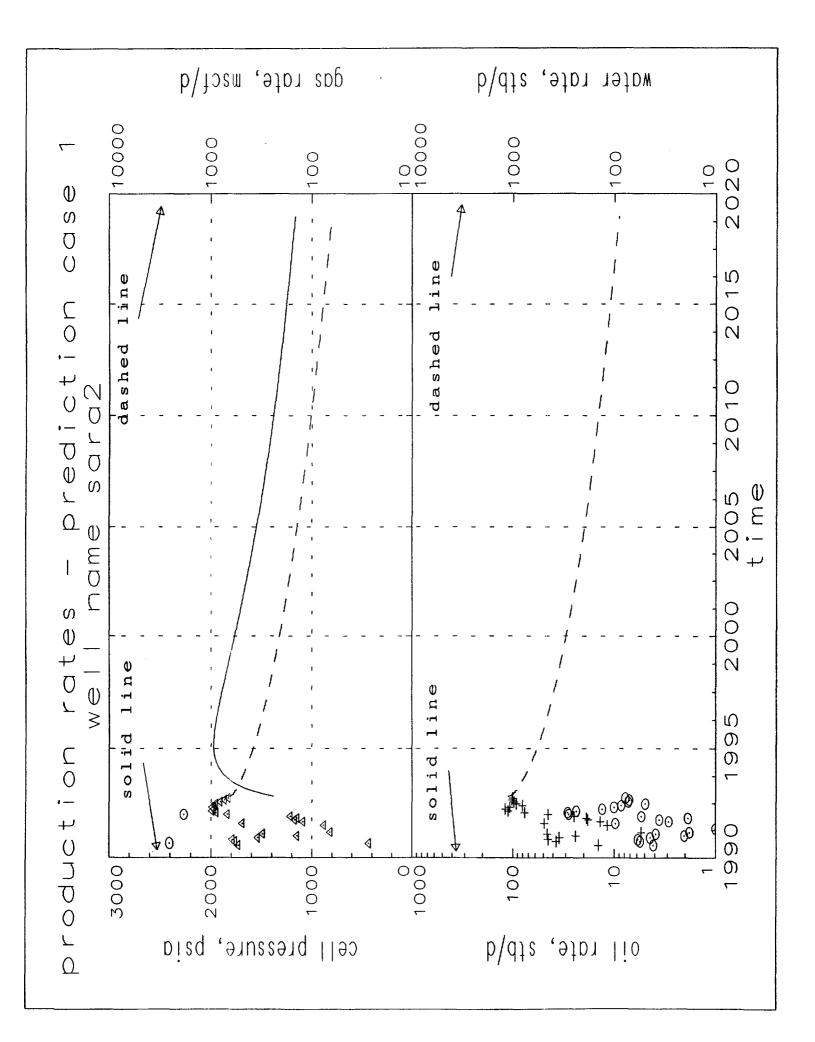


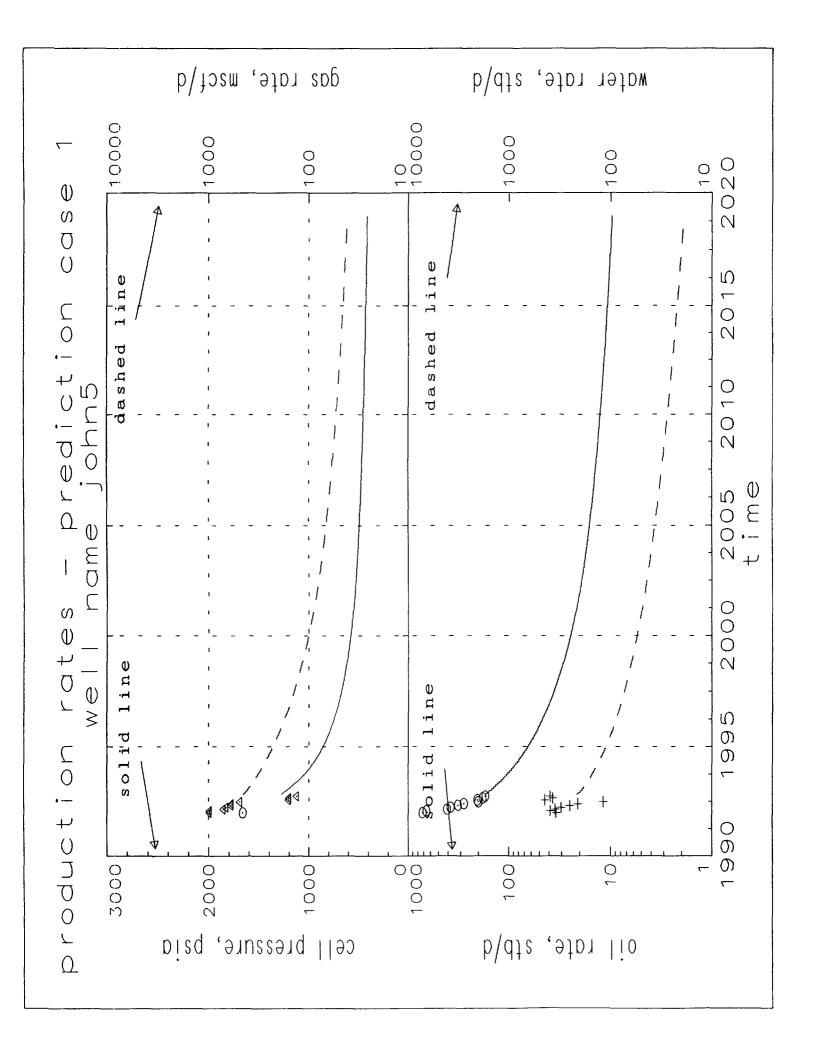


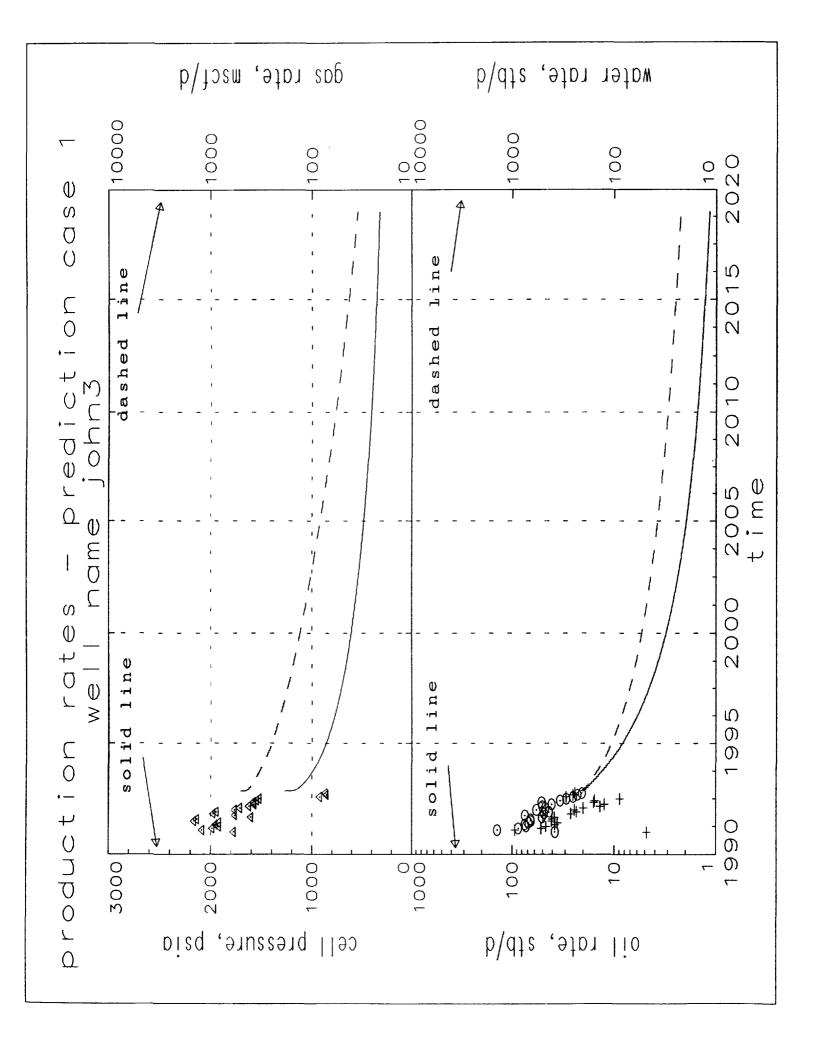


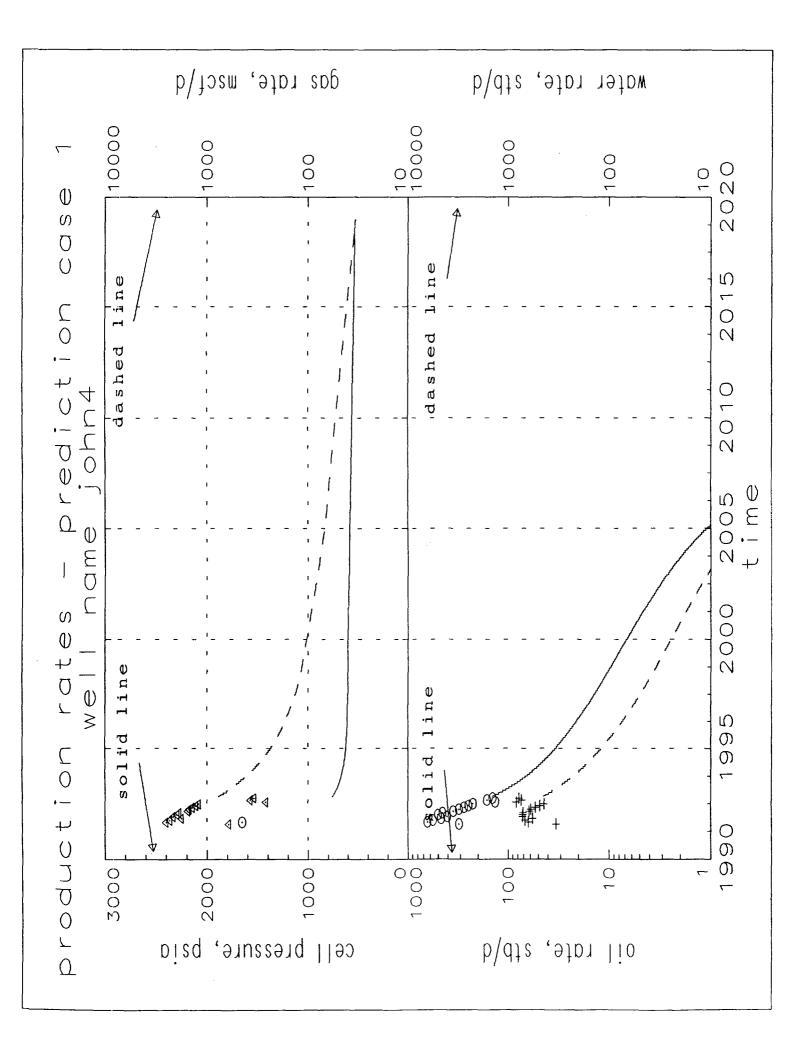


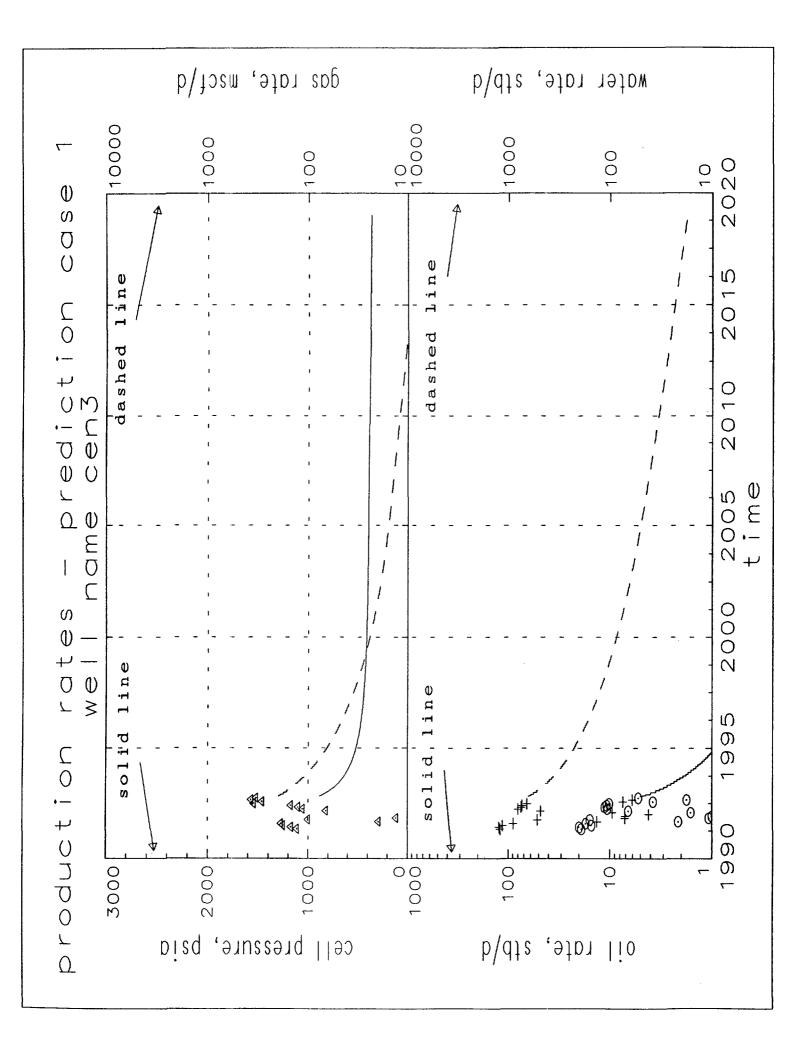








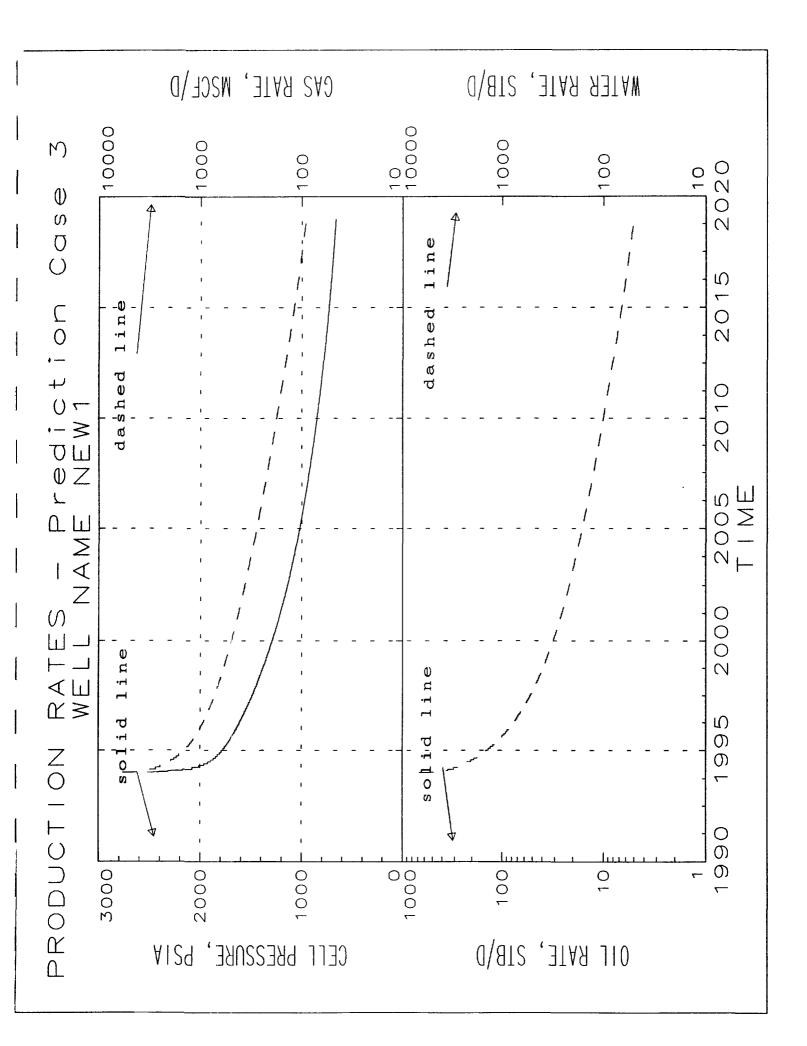


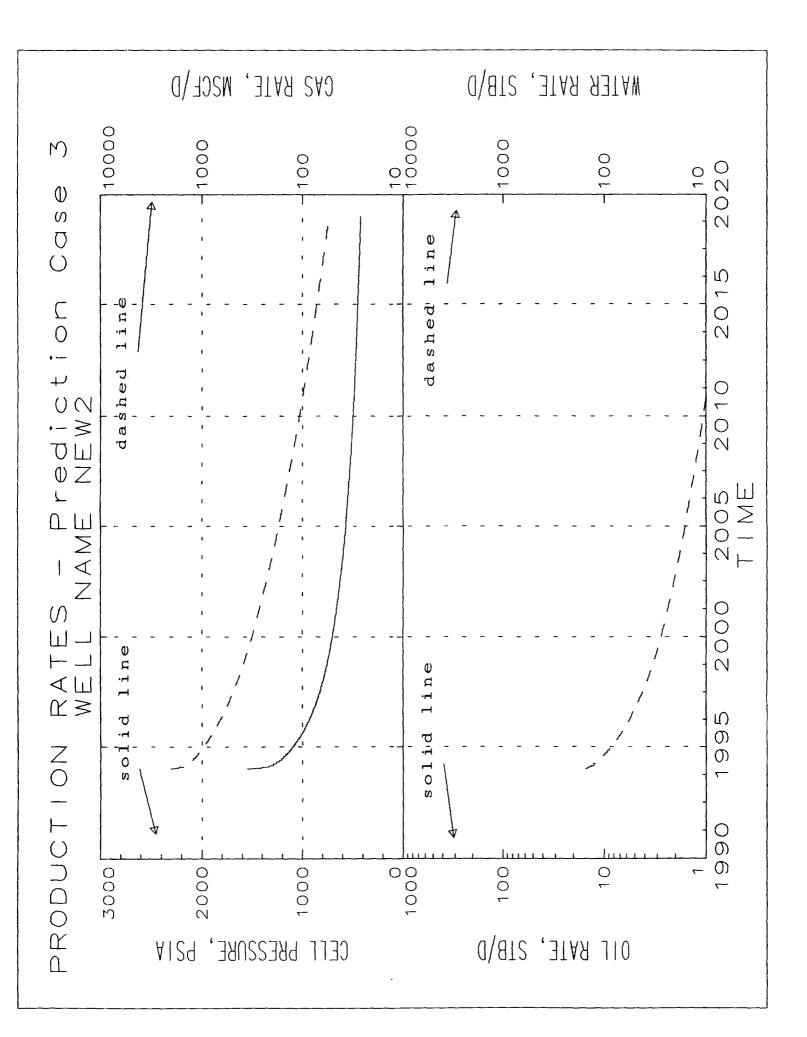


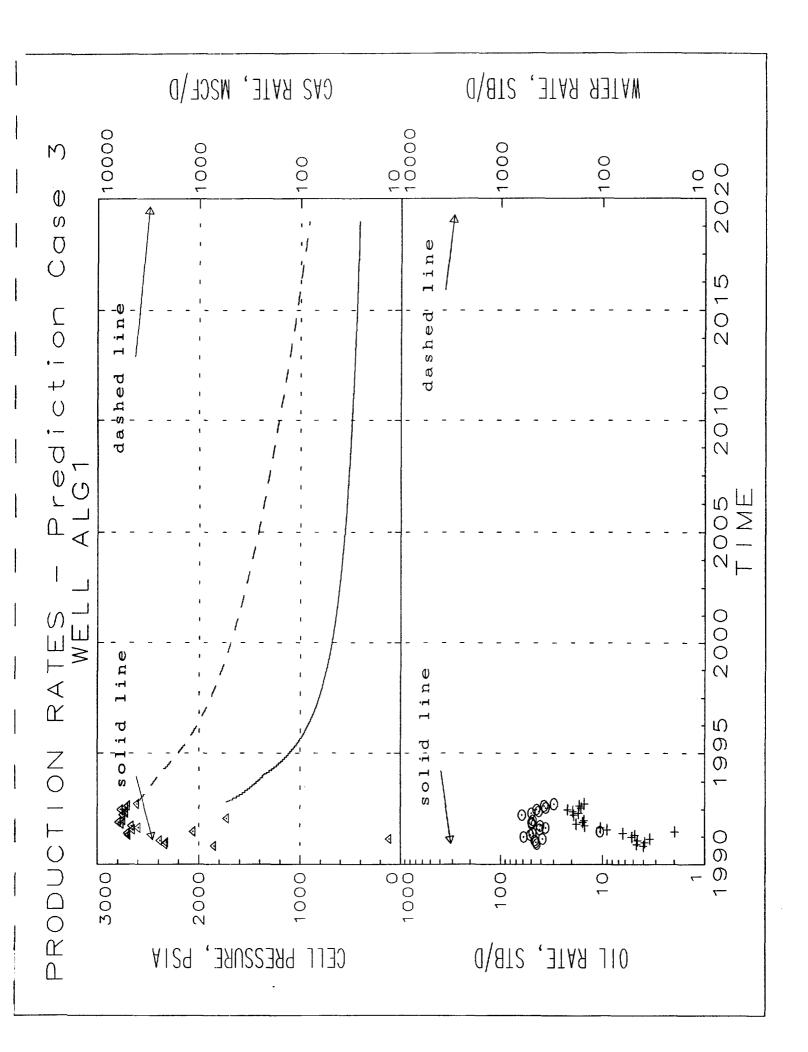
## **APPENDIX VI**

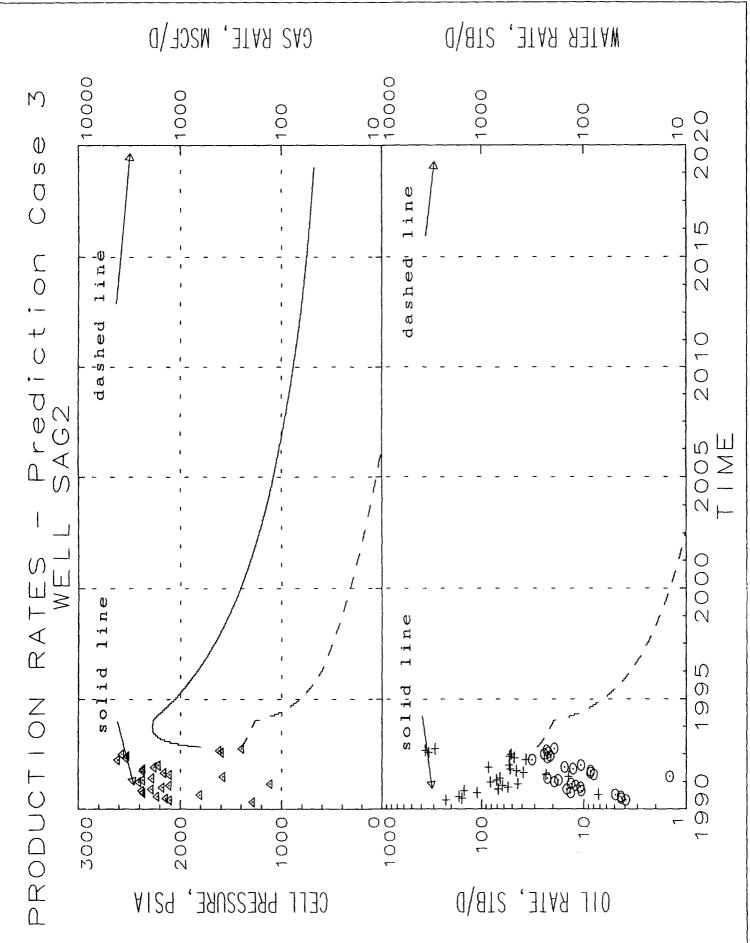
## **PREDICTION CASE 3**

**Well Performance Plots** 



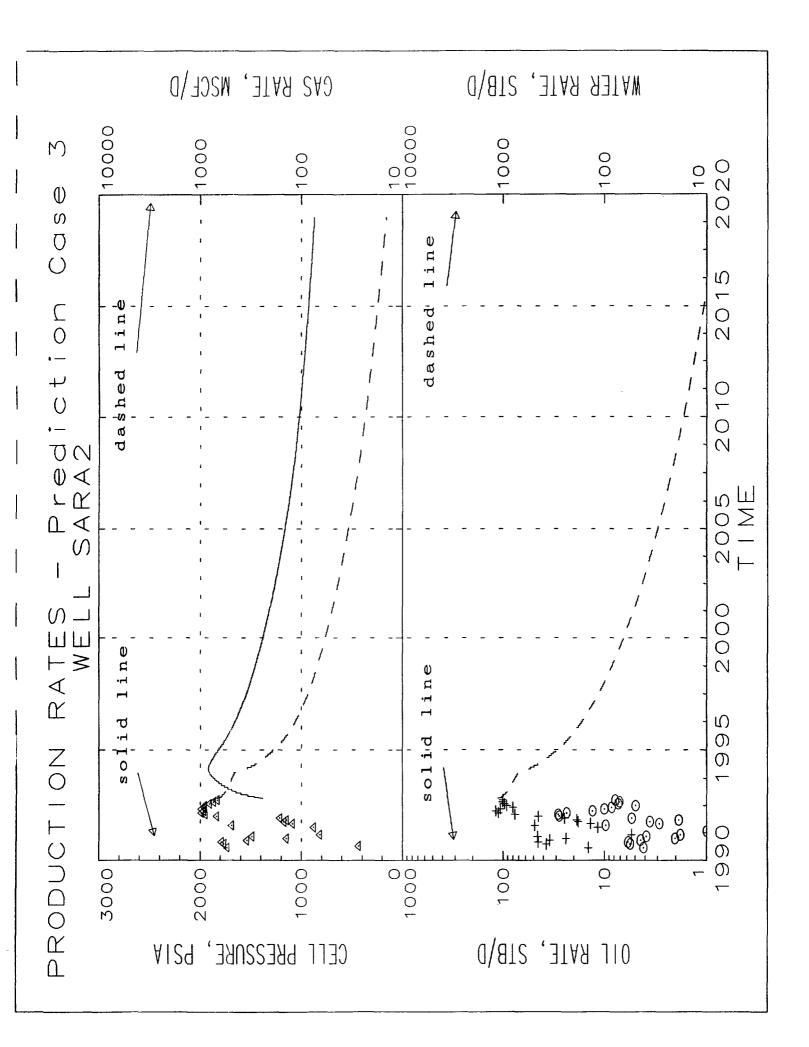


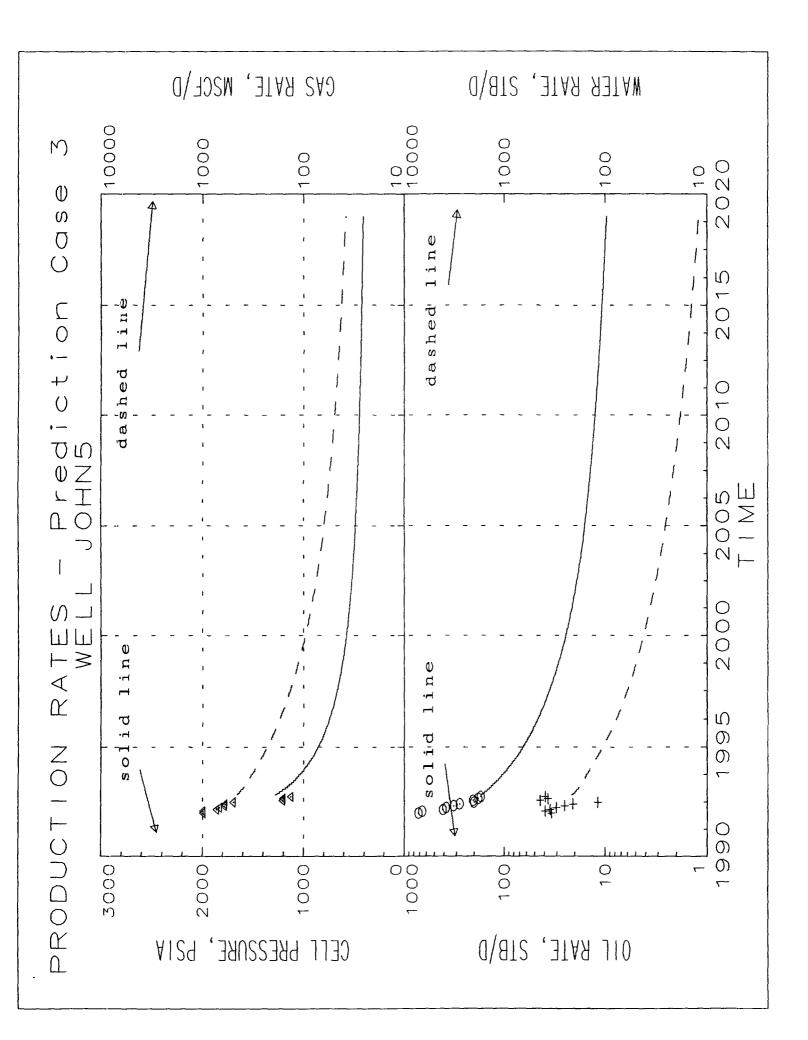


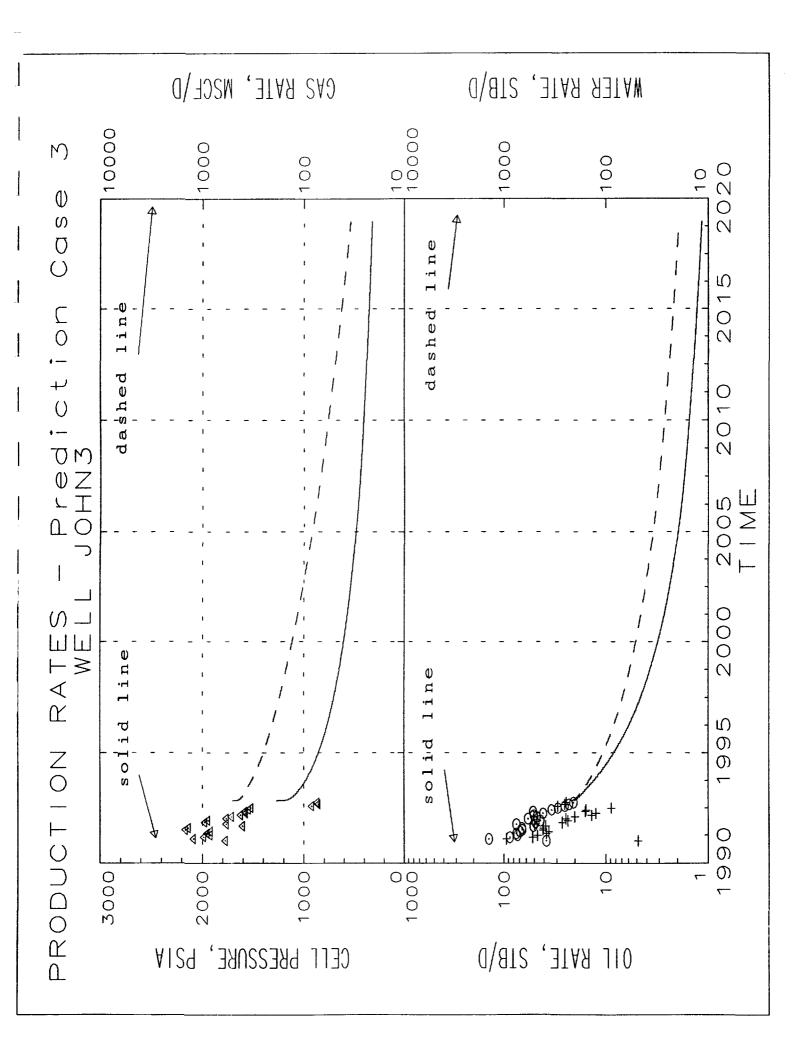


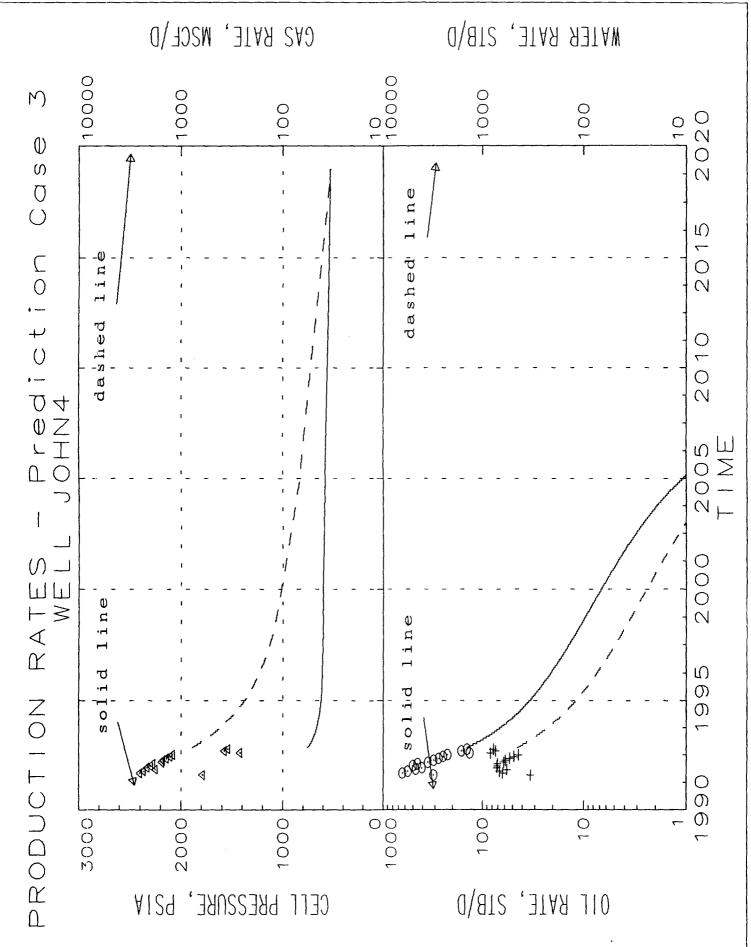
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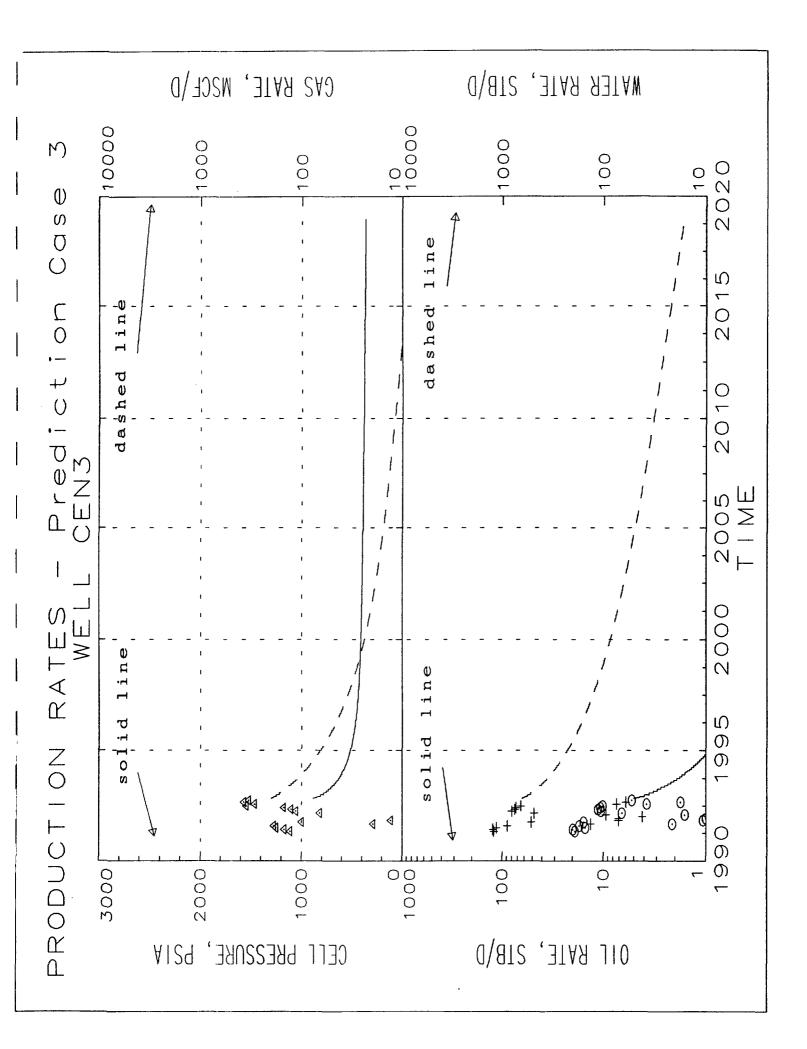






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### Economic Analyses Gas Cap Drainage Scenarios Dagger Draw South (Upper Penn)

#### **Continue with Current Operations:**

Oil Gas Present Worth Profit 682 MBO 19450 MMCF 10490 M\$

### Continue Oil Production and Shut In Gas Wells:

Oil Gas Present Worth Profit 684 MBO 9682 MMCF 6750 M\$

### Continue Oil Production and Accelerate Gas Well Production:

Oil Gas Present Worth Profit 682 MBO 21490 MMCF 11080 M\$

BEFORE THE OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. 10869 and 10881 Exhibit No. 6

Submitted by: Yates Petroleum Corporation

Hearing Date: December 2, 1993

\* Discount rate = 5%