## OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. 10869 and 10881 Exhibit No. \_\_\_\_

Submitted by:\_ Yates Petroleum Corporation

Hearing Date: December 2, 1993

### BEFORE THE

### OIL CONSERVATION DIVISION

NEW MEXICO DEPARTMENT OF ENERGY, MINERALS AND NATURAL RESOURCES

IN THE MATTER OF THE APPLICATION
OF YATES PETROLEUM CORPORATION
FOR AMENDMENT OF THE SPECIAL
RULES AND REGULATIONS OF THE SOUTH
DAGGER DRAW-UPPER PENNSYLVANIAN
ASSOCIATED POOL (DIVISION ORDER NO. R-5353),
EDDY COUNTY, NEW MEXICO.

CASE NO. 10869

### **AFFIDAVIT**

STATE OF NEW MEXICO	)
	) ss
COUNTY OF SANTA FE	)

William F. Carr, attorney in fact and authorized representative of Yates Petroleum Corporation, the Applicant herein, being first duly sworn, upon oath, states that in accordance with the notice provisions of Rule 1207 of the New Mexico Oil Conservation Division the Applicant has attempted to find the correct addresses of all interested persons entitled to receive notice of this application and that notice has been given at the addresses shown on Exhibit "A" attached hereto as provided in Rule 1207.

William F. Carr

SUBSCRIBED AND SWORN to before me this

day of December, 1993.

Notary Public

My Commission Expires:

### **EXHIBIT A**

Clifford Cone Post Office Box 1629 Lovington, NM 88260

Kenneth G. Cone Post Office Box 11310 Midland, TX 79702

D.C. Trust Marilyn Cone, Trustee Post Office Box 64244 Lubbock, TX 79464

Cathie Cone Auvenshine
Post Office Box 658
Dripping Springs, TX 78620-0658

McKay Oil Corporation Post Office Box 2014 Roswell, NM 88201

Nearburg Producing Company 2200 North "A" Street, #8100 Midland, TX 79705-5421

Conoco Inc. 10 Desta Drive West Midland, TX 79705

Marathon Oil Company Post Office Box 552 Midland, TX 79702

Read & Stevens, Inc. Post Office Box 1518 Roswell, NM 88202-1518

### BEFORE THE OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. <u>10869 a</u>	nd 10881 Exhibit No. 1
Submitted by: Ya	tes Petroleum Corporation
Hearing Date:	December 2, 1993

AFFIDAVIT, Page 2 Citation Oil & Gas Corporation 8223 Willow Place South, Suite 250 Houston, TX 77070-5623

Barbara Fasken 303 W. Wall Avenue, Suite 1900 Midland, TX 79701-5116

### & SHERIDAN, P.A.

LAWYERS

MICHAEL B. CAMPBELL
WILLIAM F. CARR
BRADFORD C. BERGE
MARK F. SHERIDAN
WILLIAM P. SLATTERY

PATRICIA A. MATTHEWS
MICHAEL H. FELDEWERT
DAVID B. LAWRENZ
TANYA M. TRUJILLO
JACK M. CAMPBELL

OF COUNSEL

JEFFERSON PLACE
SUITE 1 - 110 NORTH GUADALUPE
POST OFFICE BOX 2208

SANTA FE, NEW MEXICO 87504-2208
TELEPHONE: (505) 988-4421
TELECOPIER: (505) 983-6043

October 28, 1993

### <u>CERTIFIED MAIL -</u> RETURN RECEIPT REQUESTED

Clifford Cone Post Office Box 1629 Lovington, NM 88260

Re:

Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

Dear Mr. Cone:

This letter is to advise you that Yates Petroleum Corporation has filed the enclosed application with the New Mexico Oil Conservation Division seeking amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool by deletion of Rule 5(b) thereby authorizing the simultaneous dedication of both gas wells and oil wells to the same spacing unit.

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Parties appearing in cases have been requested by the Division (Memorandum 2-90) to file a Pre-hearing Statement substantially in the form prescribed by the Division. Pre-hearing statements should be filed by 4:00 o'clock p.m., on the Friday before a scheduled hearing.

Very truly yours,

WILLIAM F. CARR

ATTORNEY FOR YATES PETROLEUM CORPORATION



Clifford Cone Post Office Box 1629 Lovington, NM 88260

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S Form Sout, June 1991	Postmark or Date	28, 1993

PS Form 3811, Mar. 1988 Article Addressed to: Post Office Box 1629 Lovington, NM 88260 Clifford Cone U.S.G.P.O. 1988-212-865 services are desired, and complete items Type of Service:

Registered

Centified

Express Mail Express Mail ys obtain signature of addresses 2. 

Restricted Delivery (Extra charge) DOMESTIC RETURN RECEIPT 070

### CAMPBELL, CARR, BERGE & SHERIDAN, P.A.

MICHAEL B. CAMPBELL
WILLIAM F. CARR
BRADFORD C. BERGE
MARK F. SHERIDAN
WILLIAM P SLATTERY

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OF COUNSEL

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SANTA FE, NEW MEXICO 87504-2208
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October 28, 1993

### <u>CERTIFIED MAIL -</u> RETURN RECEIPT REQUESTED

Kenneth G. Cone Post Office Box 11310 Midland, TX 79702

Re:

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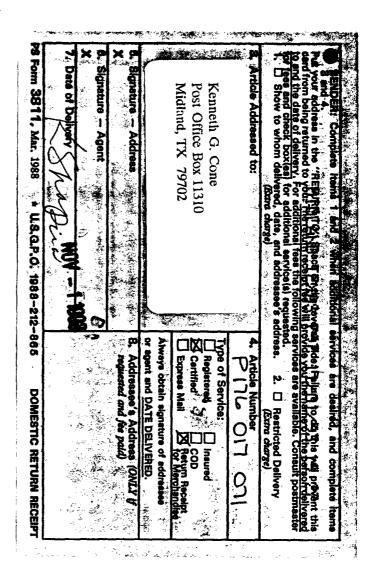
WILLIAM F. CARR

ATTORNEY FOR YATES PETROLEUM CORPORATION



Kenneth G. Cone Post Office Box 11310 Midland, TX 79702

ſ	Postage	\$
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### & SHERIDAN, P.A.

JACK M. CAMPBELL OF COUNSEL JEFFERSON PLACE
SUITE I - 110 NORTH GUADALUPE
POST OFFICE BOX 2208

SANTA FE, NEW MEXICO 87504-2208
TELEPHONE: (505) 988-4421

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October 28, 1993

### CERTIFIED MAIL -RETURN RECEIPT REQUESTED

D.C. Trust Marilyn Cone, Trustee Post Office Box 64244 Lubbock, TX 79464

Re:

Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County New Mariae

Eddy County, New Mexico

### Dear Ms Cone:

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WILLIAM F. CARR

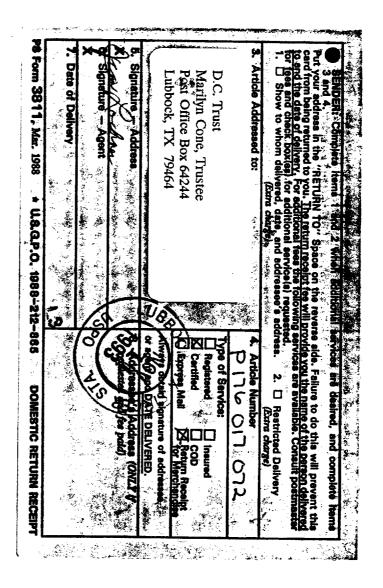
ATTORNEY FOR YATES PETROLEUM CORPORATION

WFC:mlh



D.C. Trust Marilyn Cone, Trustee Post Office Box 64244 Lubbock, TX 79464

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ıne 1991	Return Receipt Showing to Whom & Date Delivered	
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PS Form <b>3800</b> , June 1991	Postmark or Date	



### CAMPBELL, CARR, BERGE & SHERIDAN, P.A.

LAWYERS

MICHAEL B. CAMPBELL
WILLIAM F. CARR
BRADFORD C. BERGE
MARK F. SHERIDAN
WILLIAM P. SLATTERY

PATRICIA A. MATTHEWS
MICHAEL H. FELDEWERT
DAVID B. LAWRENZ
TANYA M. TRUJILLO

JACK M. CAMPBELL
OF COUNSEL

JEFFERSON PLACE
SUITE 1 - 110 NORTH GUADALUPE
POST OFFICE BOX 2208
SANTA FE, NEW MEXICO 87504-2208
TELEPHONE: (505) 988-4421
TELECOPIER: (505) 983-6043

October 28, 1993

### CERTIFIED MAIL RETURN RECEIPT REQUESTED

Cathie Cone Auvenshine Post Office Box 658 Dripping Springs, TX 78620-0658

Re.

Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

### Dear Ms Cone:

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WILLIAM F. CARR

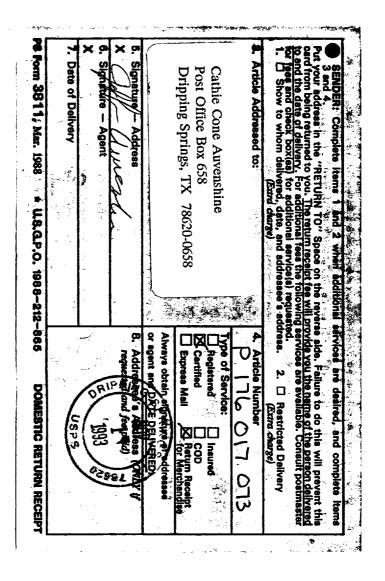
ATTORNEY FOR YATES PETROLEUM CORPORATION

176 017 073



Cathie Cone Auvenshine Post Office Box 658 Dripping Springs, TX 78620-0658

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### CAMPBELL, CARR, BERGE 8 SHERIDAN, P.A.

LAWYERS

MICHAEL B CAMPBELL
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JACK M. CAMPBELL
OF COUNSEL

JEFFERSON PLACE
SUITE 1 - 110 NORTH GUADALUPE
POST OFFICE BOX 2208

SANTA FE, NEW MEXICO 87504-2208

TELEPHONE: (505) 988-4421

TELECOPIER: (505) 983-6043

October 28, 1993

### <u>CERTIFIED MAIL -</u> <u>RETURN RECEIPT REQUESTED</u>

McKay Oil Corporation Post Office Box 2014 Roswell, NM 88201

Re.

Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

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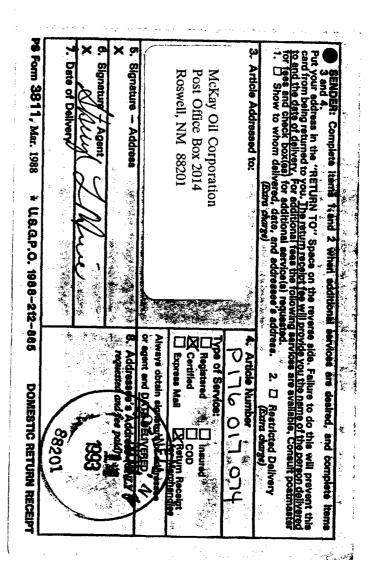
WILLIAM F. CARR

ATTORNEY FOR YATES PETROLEUM CORPORATION



McKay Oil Corporation Post Office Box 2014 Roswell, NM 88201

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### 8 SHERIDAN, P.A.

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POST OFFICE BOX 2208

SANTA FE, NEW MEXICO 87504-2208

TELECOPIER: (505) 988-4421
TELECOPIER: (505) 983-6043

October 28, 1993

### CERTIFIED MAIL RETURN RECEIPT REQUESTED

Nearburg Producing Company 2200 North "A" Street, #8100 Midland, TX 79705-5421

Re:

Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool,

Eddy County, New Mexico

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WILLIAM F. CARR

ATTORNEY FOR YATES PETROLEUM CORPORATION



Nearburg Producing Company 2200 North "A" Street, #8100 Midland, TX 79705-5421

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ine 1	Return Receipt Showing to Whom, Date, and Addressee's Address	
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PS Form <b>3800</b> , June 1991	Postmark or Date	

SENDER: Complete items 1 and 2 when additional services are desired, and complete items 2 and 4 services in the "RETURN TO" Space on the reverse side. Failure to do this will prevent this card from being returned to you. The return receipt fee will broyde you the name of the person delivered to and the date of delivery. For additional services is the following services are available. Consult postmaster to research delivered, date, and addresses address.

3. Article Addressed to:

Type of Services.

Near burg Producing Company
2200 North "A" Street, #8100

Midland, TX 79705-5421

Midland, TX 79705-5421

Always obtain agnature of addresses of addresses address

### CAMPBELL, CARR, BERGE & SHERIDAN, P.A.

LAWYERS

MICHAEL B. CAMPBELL
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SUITE I - 110 NORTH GUADALUPE
POST OFFICE BOX 2208

SANTA FE, NEW MEXICO 87504-2208

TELEPHONE: (505) 988-4421

TELECOPIER: (505) 983-6043

October 28, 1993

### <u>CERTIFIED MAIL -</u> <u>RETURN RECEIPT REQUESTED</u>

Conoco Inc. 10 Desta Drive West Midland, TX 79705

Re.

Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

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ATTORNEY FOR YATES PETROLEUM CORPORATION



Conoco Inc. 10 Desta Drive West Midland, TX 79705

	Postage	\$
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rs Form 3000, June	Postmark or Date	

SENDER: Complete hama 1 and 2 when Additional services are desired, and complete hama 3 and 4.

Put your address in the "RETURN TO" Space on the reverse side. Failure to do this will prevent this card from being returned to you. The return receipt fee will previous are available. Consult postmaster to additional rese the following services are available. Consult postmaster for readitional service in following services are address.

2. | Restricted Delivery (Extra charge)

3. Article Addressed to:

4. Article Number (Extra charge)

5. Signature - Addresse (Addressed addressed addr

rm **3800**. June 199

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MICHAEL B. CAMPBELL
WILLIAM F. CARR
BRADFORD C. BERGE
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JEFFERSON PLACE
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TELECOPIER: (505) 983-6043

October 28, 1993

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Marathon Oil Company Post Office Box 552 Midland, TX 79702

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PS Form <b>3800</b> , June 1991	Postmark or Date	

76 Form 3811, Mar. 1988 3. Article Addressed to: Midland, TX 79702 Post Office Box 552 Marathon Oil Company NOV - 1 1993 + U.S.G.P.O. 1988-212-865 TO" Space on the reverse side. Failure to do this will prevent this be return receipt fee will provide you the name of the person delivered sittonal fees the following services are available. Consult postmaster Type of Service:

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for Merchandir 8. Addressee or agent and DA Always obtain 2. Asstricted Delivery (Exira charge) DOMESTIC RETURN RECEIPT 110

### CAMPBELL, CARR, BERGE & SHERIDAN, P.A.

MICHAEL B. CAMPBELL
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SUITE 1 - 110 NORTH GUADALUPE

POST OFFICE BOX 2208

SANTA FE, NEW MEXICO 87504-2208

TELECOPIER: (505) 988-4421
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October 28, 1993

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Read & Stevens, Inc. Post Office Box 1518 Roswell, NM 88202-1518

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Eddy County, New Mexico

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PS Form <b>3800</b> , June 1991	Postmark or Date	L8, 1993

Roswell, NM 88202-1518 Read & Stevens, Inc. Post Office Box 1518 \* U.S.G.P.O. 1988-212-865 DOMESTIC RETURN RECEIPT 090

### & SHERIDAN, P.A.

LAWYERS
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WILLIAM F CARR
BRADFORD C. BERGE
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POST OFFICE BOX 2208

SANTA FE, NEW MEXICO 87504-2208
TELEPHONE: (505) 988-4421
TELECOPIER: (505) 983-6043

October 28, 1993

### CERTIFIED MAIL RETURN RECEIPT REQUESTED

Citation Oil & Gas Corporation 8223 Willow Place South, Suite 250 Houston, TX 77070-5623

Re۰

Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

### Gentlemen:

This letter is to advise you that Yates Petroleum Corporation has filed the enclosed application with the New Mexico Oil Conservation Division seeking amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool by deletion of Rule 5(b) thereby authorizing the simultaneous dedication of both gas wells and oil wells to the same spacing unit.

This application has been set for hearing before an Examiner of the Oil Conservation Division on December 2, 1993. As the operator of a well within this pool, or the operator of a well in the Upper Pennsylvanian formation within a mile of the pool, or an unleased mineral owner in the South Dagger Draw-Upper Pennsylvanian Pool, you may appear and present testimony. Failure to appear at that time or otherwise become a party of record will prevent you from challenging this application at a later date.

Parties appearing in cases have been requested by the Division (Memorandum 2-90) to file a Pre-hearing Statement substantially in the form prescribed by the Division. Pre-hearing statements should be filed by 4:00 o'clock p.m., on the Friday before a scheduled hearing.

enty truly yours,

WILLIAM F. CARR

ATTORNEY FOR YATES PETROLEUM CORPORATION



Citation Oil & Gas Corporation 8223 Willow Place South, Suite 250 Houston, TX 77070-5623

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### CAMPBELL, CARR, BERGE & SHERIDAN, P.A.

LAWYERS

MICHAEL B. CAMPBELL
WILLIAM F. CARR
BRADFORD C. BERGE
MARK F. SHERIDAN
WILLIAM P. SLATTERY

PATRICIA A. MATTHEWS
MICHAEL H. FELDEWERT
DAVID B. LAWRENZ
TANYA M. TRUJILLO

JACK M. CAMPBELL
OF COUNSEL

JEFFERSON PLACE

SUITE I - 110 NORTH GUADALUPE POST OFFICE BOX 2208 SANTA FE, NEW MEXICO 87504-2208

TELECOPIER: (505) 988-4421
TELECOPIER: (505) 983-6043

October 28, 1993

### <u>CERTIFIED MAIL -</u> <u>RETURN RECEIPT REQUESTED</u>

Barbara Fasken 303 W. Wall Avenue, Suite 1900 Midland, TX 79701-5116

Re:

Application of Yates Petroleum Corporation for Amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool, Eddy County, New Mexico

Dear Ms Fasken:

This letter is to advise you that Yates Petroleum Corporation has filed the enclosed application with the New Mexico Oil Conservation Division seeking amendment of the Special Rules and Regulations for the South Dagger Draw-Upper Pennsylvanian Pool by deletion of Rule 5(b) thereby authorizing the simultaneous dedication of both gas wells and oil wells to the same spacing unit.

This application has been set for hearing before an Examiner of the Oil Conservation Division on December 2, 1993. As the operator of a well within this pool, or the operator of a well in the Upper Pennsylvanian formation within a mile of the pool, or an unleased mineral owner in the South Dagger Draw-Upper Pennsylvanian Pool, you may appear and present testimony. Failure to appear at that time or otherwise become a party of record will prevent you from challenging this application at a later date.

Parties appearing in cases have been requested by the Division (Memorandum 2-90) to file a Pre-hearing Statement substantially in the form prescribed by the Division. Pre-hearing statements should be filed by 4:00 o'clock p.m., on the Friday before a scheduled hearing.

Very truly yours

WILLIAM F. CARR

ATTORNEY FOR YATES PETROLEUM CORPORATION



Barbara Fasken 303 W. Wall Avenue, Suite 1900 Midland, TX 79701-5116

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NETURN For a livered l	Always obtain signature of addressee or agent and DATE DELIVERED.	
RETURN YOU.	L -	303 W. Wall Avenue, Suite 1900 Midland, TX 79701-5116
RETURN For a livered a		Barbara Fasken
RETURN For an inversed.	4. Article Number Pイフに 017 092	L Article Addressed to:
SENDER: Complete Items 1 and 2 when additional services are desired, and complete Items 3 and 4. 3 and 4. 3 and 4. 3 and 4. 4 and complete Items 1 and complete Items 1 and complete Items 1 and from being returned to you. The return receipt fee will provide you the name of the person delivered and the date of delivery. For additional fees the following services are available. Consuit postmaster of fees and check boxides for additional services required services.	dress. 2. 🗆 Restricted Delivery (Extra charge)	. ☐ Show to whom delivered, date, and addressee's ad (Eara charge)
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	services are desired, and complete items	SENDER: Complete Items 1 and 2' when additional 3 and 4.

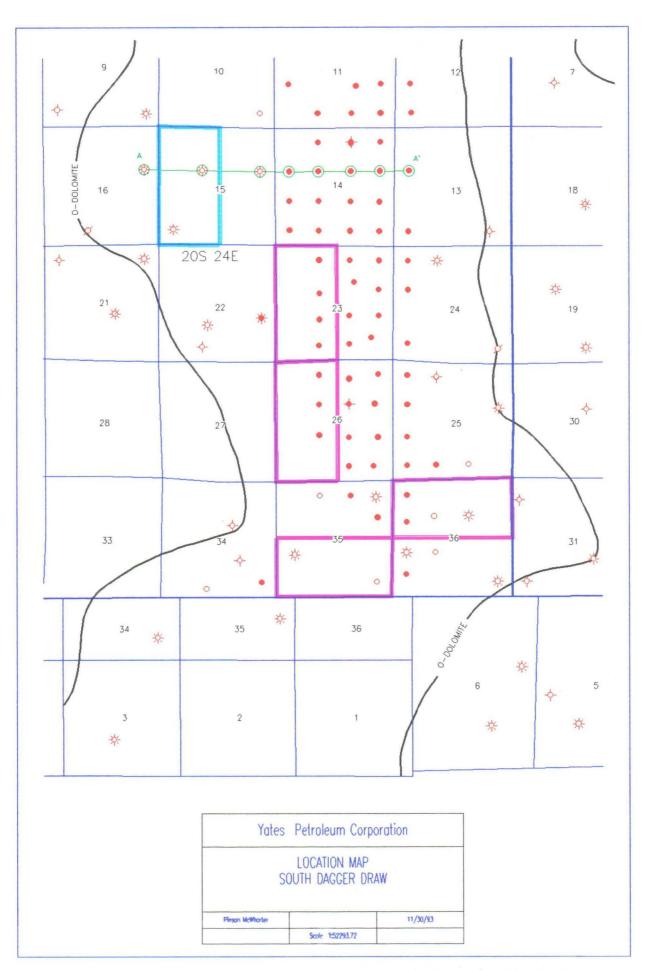
### BEFORE THE OIL CONSERVATION DIVISION

Santa Fe, New Mexico

Case Nos. 10869 and 10881 Exhibit No. 1

Submitted by: Yates Petroleum Corporation

Hearing Date: December 2, 1993



### BEFORE THE OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. <u>10869 and 10881</u> Exhibit No. <u>2</u>

Submitted by: Yates Petroleum Corporation

Hearing Date: December 2, 1993

# OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. 10869 and 10881 Exhibit No. 3

Submitted by: Yates Petroleum Corporation

Hearing Date: ecember 2, 1993

## GOR-2.XLS/pbs

## South Dagger Draw

### Oil Well GOR

				PRODUCTION	CTION			GAS	GAS-OIL RATIO	_
		July, 1993	993	August, 1993	1993	September, 1993	er, 1993	Jul-93	Aug-93	Sep-93
Well Name	Location	<u>ci</u>	Gas	<u>oi</u>	Gas	Oil	Gas	Scf/Bbl	Scf/Bbl	Scf/BbI
1 Saguaro AGS Federal Com #10	C 26-20S-24E	1848	37347	894	31732	1570	27559	20,209	35,494	17,554
2 Charolette McKay Federal Com #2	D 25-20S-24E	2084	37778	2668	37818	2701	36145	18,128	14,175	13,382
3 Ceniza AGZ Com #2	M 12-20S-24E	125	1733	107	1308	117	1144	13,864	12,224	9,778
4 Indian Hills State Com #3	D 36-20S-24E	1884	21725	755	15562	1865	29732	11,531	20,612	15,942
5 Conoco AGK Federal #9	P 26-20S-24E	4433	47141	4475	49358	3956	46002	10,634	11,030	11,628
6 Hillview AHE Federal Com #6	B 23-20S-24E	607	6054	555	6482	486	5958	9,974	11,679	12,259
7 Saguaro AGS Federal Com #5	F 23-20S-24E	1603	15971	1589	15631	1599	15081	9,963	9,837	9,432
8 Hillview AHE Federal Com #5	A 23-20S-24E	1422	13582	1117	14477	992	11048	9,551	12,961	11,137
9 John AGU #7	E 14-20S-24E	1359	12465	1186	17996	1069	14643	9,172	15,174	13,698
10 Saguaro AGS Federal Com #1	L 11-20S-24E	1220	10663	1150	10504	1063	8818	8,740	9,134	8,295
11 Sara AHA Com #4	0 11-20S-24E	922	7638	912	7451	816	6525	8,284	8,170	7,996
12 Dahlia ALA Com #1	L 25-20S-24E	2167	16590	1982	15529	1790	13554	7,656	7,835	7,572
13 Indian Hills State Com #4	E 36-20S-24E	2827	20682	3021	22706	3175	25132	7,316	7,516	7,916
14 Conoco AGK Federal Com #10	J 11-20S-24E	920	6479	854	7054	804	6104	7,042	8,260	7,592
15 Hillview AHE Federal #8	P 14-20S-24E	747	5060	725	4764	500	4162	6,774	6,571	8,324
16 Sara AHA Com #5	N 11-20S-24E	2253	14404	2103	14845	1931	13612	6,393	7,059	7,049
17 John AGU #4	H 14-20S-24E	1711	10086	1524	8758	1312	7938	5,895	5,747	6,050
18 John AGU #3	G 14-20S-24E	668	3646	637	3367	593	3024	5,458	5,286	5,099
19 Conoco AGK Federal #11	J 26-20S-24E	2697	14633	2457	15163	2292	14560	5,426	6,171	6,353
20 Ceniza AGZ Com #3	E 13-20S-24E	49	251	76	958	57	886	5,122	12,605	15,544
21 Prickly Pear AIE Federal Com #1	P 23-20S-24E	3955	19130	3599	19673	3043	18307	4,837	5,466	6,016
22 Hillivew AHE Federal Com #16	M 14-20S-24E	539	2519	490	2227	473	1892	4,673	4,545	4,000
23 Conoco AGK Federal #2	G 26-20S-24E	3228	13733	3196	10720	2875	8581	4,254	3,354	2,985
24 Saguaro AGS Federal Com #8	0 14-20S-24E	2310	9389	2428	9063	2112	9470	4,065	3,733	4,484
	J 23-20S-24E	1694	6571	1630	5621	1242	9023	3,879	3,448	7,265
26 Hillview AHE Federal Com #10	H 23-20S-24E	1401	5329	953	4944	735	4306	3,804	5,188	5,859
	A 26-20S-24E	4261	15767	3746	15277	3319	14286	3,700	4,078	4,304
28 Hillview AHE Federal Com #2	G 23-20S-24E	1630	5869	1407	5559	1190	5454	3,601	3,951	4,583
29 Saguaro AGS Federal Com #9	C 23-20S-24E	2148	7728	2025	8266	1824	7302	3,598	4,082	4,003
30 Charolette McKay Federal Com #4	E 25-20S-24E	3098	10609	1540	6226	687	9310	3,424	4,043	13,552
31 John AGU #1	C 14-20S-24E	3730	12460	3534	11767	2944	10499	3,340	3,330	3,566
_	N 23-20S-24E	4364	14516	4255	15205	3881	14823	3,326	3,573	3,819
33 Hillview AHE Federal Com #13	I 14-20S-24E	1549	5151	1476	5015	1210	4395	3,325	3,398	3,632

### Oil Well GOR

Oil Well Totals		54 Mayer 24 #1	53 Sara AHA Com #6	52 Staghorn AJG Federal Com #2	51 Hillview AHE Federal Com #17	so Palo Verde AJV Federal #1	49 Conoco AGK Federal #3	48 Conoco AGK Federal #15	47 Conoco AGK Federal #8	46 Conoco AGK Federal Com #6	45 John AGU #6	44 Hillview AHE Federal Com #12	43 Saguaro AGS Federal Com #4	42 Conoco AGK Federal #5	41 Saguaro AGS Federal Com #12	40 Ceniza AGZ Com #4	39 John AGU #5	38 Staghorn AJG Federal Com #1	37 Sara AHA Com #1	36 John AGU #2	35 Senita AIP Federal Com #1	34 Senita AIP Federal Com #2	Well Name		
<i>G</i>		H 13-20S-24E	•	N 25-20S-24E	0 23-20S-24E	M 24-20S-24E	I 26-20S-24E	0 26-20S-24E	H 26-20S-24E	K 26-20S-24E	B 14-20S-24E	I 23-20S-24E	J 14-20S-24E	B 26-20S-24E	L 14-20S-24E	L 12-20S-24E	F 14-20S-24E	M 25-20S-24E	I 11-20S-24E	A 14-20S-24E	K 14-20S-24E	N 14-20S-24E	Location		
132428	0 1	<i>~</i> c	2235	1230	5177	781	6567	7614	2925	1499	3395	6871	1633	11886	1780	1964	2916	2778	457	1847	1489	1928	<u>o</u> i	July, 1993	
581347	0 0	0 /2	2117	1685	8163	1335	11336	13994	5506	3330	7687	16158	3850	28434	4534	5342	8197	8308	1443	5989	4884	6329	Gas	993	
118341	0 0	o c	1959	1211	3458	705	6428	7043	2816	1644	3305	5147	1431	10375	1706	1805	2439	2586	326	1775	1327	1789	O <u>ii</u>	August, 1993	PRODUCTION
560786	38	<b>.</b>	1670	1613	5891	1132	10091	17670	5048	3346	7585	12523	3749	26857	4512	5215	7645	7750	746	5614	4816	6249	Gas	1993	CTION
104510	0 н	1 0	1720	1032	3572	628	5343	6074	2387	1530	2987	4521	1242	8223	1275	1466	1924	2206	138	1445	1088	1485	<u>o</u> i	September, 1993	
534471	0 0	320	1637	1364	5822	815	9524	16984	4418	2913	7288	11817	3575	22734	2800	4533	7272	6277	889	4275	4503	5436	Gas	er, 1993	
4,390	0 (	- C	947	1,370	1,577	1,709	1,726	1,838	1,882	2,221	2,264	2,352	2,358	2,392	2,547	2,720	2,811	2,991	3,158	3,243	3,280	3,283	Scf/Bbl	Jul-93	GAS
4,739	0 0	0	852	1,332	1,704	1,606	1,570	2,509	1,793	2,035	2,295	2,433	2,620	2,589	2,645	2,889	3,134	2,997	2,288	3,163	3,629	3,493	Scf/Bbl	Aug-93	GAS-OIL RATIO
5,114	0 0	0	952	1,322	1,630	1,298	1,783	2,796	1,851	1,904	2,440	2,614	2,878	2,765	2,196	3,092	3,780	2,845	6,442	2,958	4,139	3,661	Scf/Bbl	Sep-93	J

7 of 56 wells  $\geq$  10,000:1 (12.5%)

22 of 56 wells > 4500:1 (39%)

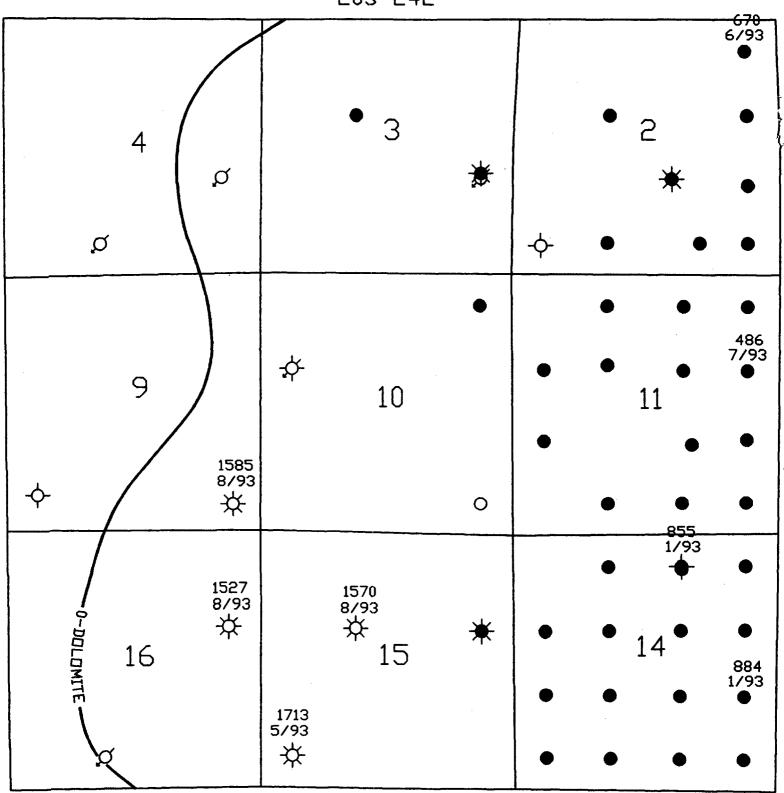
## BEFORE THE OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. 10869 and 10881 Exhibit No. 3

Submitted by: Yates Petroleum Corporation

Hearing Date: December 2, 1993

20S-24E





12/93 (VM) DRAFT\A93033D

BOTTOM HOLE PRESSURE -4000 DATUM EDDY COUNTY, NEW MEXICO

ENG PINSON MCVHORTER SCALE: 1'=2000'

BEFORE THE OIL CONSERVATION DIVISION

Santa Fe, New Mexico

Case Nos. <u>10869 and 10881</u> Exhibit No. <u>4</u>

Submitted by: Yates Petroleum Corporation

Hearing Date: <u>December 2, 1993</u>

### BEFORE THE OIL CONSERVATION DIVISION

Santa Fe, New Mexico

Case Nos. <u>10869 and 10881</u> Exhibit No. <u>5</u>

Submitted by: Yates Petroleum Corporation

Hearing Date: December 2, 1993



### SCIENTIFIC SOFTWARE-INTERCOMP

Advanced Technology for the Petroleum Industry

### RESERVOIR SIMULATION STUDY 3-D SECTOR AREA

### CANYON RESERVOIR DAGGER DRAW FIELD, NEW MEXICO

**FINAL REPORT** 

### **NOVEMBER 1993**

PERFORMED FOR:
YATES PETROLEUM CORPORATION

PERFORMED BY:
SCIENTIFIC SOFTWARE-INTERCOMP, INC.

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Well Performance Plots

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#### **SUMMARY**

SSI was authorized by Yates to perform a reservoir simulation study on the Canyon reservoir, Dagger Draw field in New Mexico. The objective of the study was to determine the effect of gas cap depletion on down dip oil production.

SSI constructed a representative 3-D simulation model containing one row of wells (east-west) extending from the gas cap through the oil and water column. The simulation model was calibrated by performing history match simulation runs. After the simulation model was properly calibrated for the history period (January 1990 through October 1992), three 26-year prediction runs were made to investigate the effect of gas cap depletion on oil production down dip.

The following table summarizes the 26 year oil recoveries obtained from each prediction case:

	CASE 1	CASE 2	CASE 3
End of Case	December, 2018	December, 2018	December, 2018
Oil, MSTB	682	684	682
Gas, BSCF	19.5	9.7	21.5

Case 1 - Continued Depletion

Case 2 - Continued Depletion without Gas Cap Depletion

Case 3 - Continued depletion with Gas Cap Infills

Operational changes in the management of the gas cap have little effect on oil recoveries in the oil leg down dip. This is consistent with the geological evaluation that indicated a tortuous lateral connection (with some sedimentary barriers) between the gas cap and the oil leg.

The simulations in this study were performed using SSI's SimBest II simulator. The simulator was run in single porosity, three phase (black oil) mode. The simulation and post-processor modules

of WorkBench were used in construction of the initial reservoir model, in making modifications to the model during history matching, and in the display of the results (tables, plots, and maps) of all simulations.

The 3-D sector reservoir simulation model consisted of 552 grid cells (23 x 3 x 8). The model contained eight layers corresponding to the correlation units derived from geologic evaluation. The initial reservoir rock properties (net thickness, porosity, permeability, relative permeability, and capillary pressure) and fluid properties of the simulation model were derived from the results of geological, petrophysical, and engineering analyses.

The initial simulation model was calibrated through a history matching procedure. Well oil rates were specified in the model, and pressures, gas rates, and water rates were calculated by the simulation model. In order to account for high volumes of water production in the up dip portion of the reservoir, a modeling scheme was required to create high initial water saturations up dip without adversely affecting oil and gas production in the mid dip and down dip portions of the reservoir.

The resulting model utilized isolated model layers with high capillary pressures in Layers 5 and 6. This resulted in high water saturation values up dip for Layers 5 and 6. Layer 4 contained most of the hydrocarbon volumes. The initial input porosity and permeability values were modified accordingly to obtain history matches on pressure, gas production and water production. This calibrated model was then used for the prediction simulations.

The discussion section contains more detailed descriptions of the simulation model and the simulation runs.

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## **DISCUSSION**

#### RESERVOIR SIMULATION

The following sections of this report describe the construction of the initial reservoir simulation model and the calibration of the reservoir characterization within the model during history matching. The history period was defined as January, 1990 to the end of October, 1992.

The simulations in this study were performed using SimBest II (version 3.1 I5), SSI's three-dimensional, multi-phase, dual porosity reservoir simulator. The simulator was run in single-porosity, three-phase (black oil) mode. The simulation and post-processor modules of WorkBench were used in construction of the initial reservoir model, in making modifications to the model during history matching, and in the display of the results (tables, plots, and maps) of all simulations.

The methods and results of the simulation phases of this study are discussed in the following sections of this report and illustrated in the accompanying tables, figures, and appendices. In addition, listings of the final input and output data for all simulations have been provided to Yates in tape format.

#### **Model Construction**

The initial reservoir rock and fluid properties of the simulation model were derived from the results of the geological, petrophysical, and engineering analyses. The 3-D sector model covers an area 13,800 by 1,800 feet (2.6 by 0.3 miles). The grid is shown in Figures 1 and 2. The model contains one row of wells (east-west) extending from the gas cap (wells AIG 1, SAG 2, and SARA 2) through the oil column and into the water column (wells JOHN 5, JOHN 3, JOHN 4, and CEN 3). The grid contains 23 cells in the x-direction (east-west) and 3 cells in the y-direction (north-south). The model contains eight layers. This results in a total of 552 cells, but not all of these cells are active. The areal dimensions of each cell are 600 by 600 feet. Square cells were used to minimize the numerical dispersion effects of rectangular cells.

The structural depths of each of the layers at each grid location were determined from the structure and gross thickness maps constructed during the initial geological analyses.

The characteristics of the reservoir rock are defined in the simulator on a cell-by-cell basis. The reservoir characteristics include the following:

- net reservoir thickness
- effective porosity
- effective permeability (in the x, y and z directions)
- relative permeability
- capillary pressure

All the properties listed above are representative of the net reservoir. For example, the values of effective porosity are average values for the net reservoir rock and do not include porosities which are below the cutoffs.

Net thickness maps were input in digital form to the initial reservoir simulation model. Net thickness values are used in the model primarily in the calculation of volumetrics and conductivity. Any changes to the volumetrics ( $\phi$ h) or conductivity (kh) during history matching may imply change to the net thickness, porosity, or permeability. Changes to conductivity due to stratigraphic or structural barriers were implemented in the model as modifications to transmissibility between cells since these barriers do not require changes to the reservoir rock permeability.

Effective porosity maps were digitized and input into the initial reservoir simulation model. These values were entered on a cell-by- cell basis and are representative of the net reservoir, not the gross reservoir. These initial porosity values were used in the initial estimation of horizontal permeabilities. The primary effect of porosity in the simulation model is on the calculation of volumetrics. Porosities were modified heavily during the history matching phase.

The effective horizontal permeabilities used in the initial reservoir description of the simulation model were calculated on a cell-by-cell basis from the porosity-permeability relationships derived from cross plots of porosity and permeability. Plots of air permeability vs. core porosity were made

for each simulation model layer (Appendix I). Core data were not available for Layer 1. Based on these plots, the following equations were derived and used to transform average porosity for each simulation cell in each layer to horizontal permeability:

LAYER	HORIZONTAL PERMEABILITY EFFECTIVE POROSITY RELATIONSHIP
1	Log K = 22.9885 * (φ) - 1.0555
2	Log K = 22.9885 * (φ) - 1.0555
3	$Log K = 60.6061 * (\phi) - 2.1079$
4	Log K = 45.4545 * (φ) - 1.5017
5	$Log K = 23.2558 * (\phi) - 1.1367$
6	$Log K = 16.6436 * (\phi) - 0.9393$
7	$Log K = 20 * (\phi) - 0.8$
8	$Log K = 26.3158 * (\phi) - 0.8697$

Three permeability arrays were input to the reservoir simulation model. These correspond to permeabilities in the x, y, and z direction. There were no data to suggest that x and y permeabilities should differ. As far as the z direction permeability, vertical transmissibility between layers was reduced to zero to reflect the presence of permeability reductions and sealing barriers within the model layers.

The laboratory core analysis performed by Scal, Inc. (Appendix II) was the basis for the relative permeability used in the simulation model. The Scal relative permeability analysis was performed on extracted cores. Since the core samples were not preserved, the Scal analysis was used only as a starting point to determine saturation and relative permeability endpoints.

Through cross-sectional model simulation, pseudo relative permeability curves were developed in order to match oil and water rates in the reservoir. In particular, the water relative permeability at residual oil saturation was increased to .5947. This change was necessary for the model to calculate and match the high volumes of water produced throughout the reservoir especially in the up dip

areas within the gas cap. Also the oil relative permeability at critical gas saturation was increased to .7174 in order to match oil production rates in the mid dip areas of the reservoir.

Segregated flow was assumed, and straight-line relative permeabilities were used as depicted in Figure 3. Table 1 summarizes the relative permeability endpoints that were used for the water-oil and gas-oil relative permeability data in the simulation model.

High capillary pressure was used in Layers 5 and 6 to create a large water-oil transition zone in those layers in order to allow up dip water production in the simulation model. Figure 4 illustrates and Table 2 summarizes the capillary pressures which were used in the simulation model.

Only one set of fluid properties was required by the simulation model to characterize the fluids in this reservoir. These properties were derived from available fluid data and correlations. The saturated oil properties (gas-oil ratio, formation volume factor, compressibility, and viscosity) and the gas properties (formation volume factor and viscosity) were assigned to the model based on saturation pressure. Undersaturated oil properties were calculated by the model from the saturation pressure, the reservoir pressure, the compressibility, and the modified undersaturated viscosity slope. Table 3 and Figures 5 through 9 summarize the PVT data input.

Yates provided SSI with a Core Labs' reservoir fluid analysis report. This report is included in Appendix III. The analysis was performed in April 1990. At that time the reservoir pressure had dropped below 2000 psia, and the saturation pressure that was reported in the analysis was 2003 psig.

The original pressure of the reservoir is believed to be 3000 psig. The saturation pressure is also believed to be equal to the original reservoir pressure. Therefore, SSI used correlations provided within WorkBench to create PVT "data" giving a saturation pressure of 3015 psia and oil API gravity of 42.7, etc.

For wells located within the gas cap (wells Algerita 1, Saguaro 2, and Sara 2), gas production rates were specified in the simulation model. For all other wells in the model, oil production rates were

specified. The production data were derived from the monthly production reports provided by Yates. The production data were specified in the model on a quarterly basis.

Wells were completed in model layers according to perforation depths supplied by Yates. Since fracture treatments were performed on all wells, these initial well completions were not considered completely reliable. In order to account for hydraulic fracture production near the wellbore, well completions were altered as needed during the history match.

## **History Matching Procedure**

Most of the initial reservoir description was based, by necessity, on measurements made at the points in the reservoir which were penetrated by wells. Most of these measurements do not reveal information about the reservoir characteristics between and beyond wells. Due to the small percentage of the reservoir that is directly sampled, and the range of accuracy of some of the measurements themselves, even a carefully derived initial reservoir description may not represent the actual reservoir with complete accuracy.

The objective of the history matching phase of this study was to adjust the reservoir description to a more accurate representation of the field. Mathematical reservoir simulators have proven to be reliable in reproducing the physical processes taking place in petroleum reservoirs. The quality of the results derived from a simulator depends primarily on the quality of the final reservoir description. The quality of this final description depends partially on the quality and quantity of the basic data used to derive the initial description.

The quality of the simulation results also depends on the quality and quantity of the measurements of historical reservoir behavior and quality of the match of these measurements by the simulator. The quality of measurements of historical behavior is average for this reservoir. Oil, gas, and water volumes seem to be measured very well. However, pressure data are limited. Only a handful of wells within the study area have pressure data. Those wells that have pressure data have only one pressure point in time. In addition, there are no pressure data for isolated layers or zones. The length of the history period for most wells is two or three years, which is a fairly short period for a

history match. These facts, combined with the moderate quantity and quality of the data used to determine the initial reservoir description, indicate that the final reservoir description derived from a satisfactory history match can be used with moderate confidence to predict future reservoir behavior. The limitations imposed by the short history period for most wells and the quality of the initial reservoir description should be remembered when interpreting the results of the prediction cases.

It is through the iterative process of "matching" the measured reservoir behavior that the initial reservoir description is adjusted to its final form. Adjustments in this study were made only to reservoir characteristics which were not known with accuracy. Changes to these characteristics were maintained within a reasonable range for the particular parameter.

The history match parameters for this study were:

- reservoir pressure
- · gas production
- water production

The oil production rates were specified by well on a quarterly basis in the simulator. The three parameters listed above were calculated by the simulator for each well and compared to the values measured in the field. For wells within the gas cap, gas production was specified, and reservoir pressure and water production were calculated by the simulator for each well and compared to field measured data. The following section of this report discusses the procedures followed to match each of the parameters listed above.

### Reservoir Pressure Match

As mentioned previously, there was not an abundance of pressure data available for the sector area. However, the data that were available indicated that reservoir pressure had dropped quickly from an initial value of 3000 psig to around 1000 psig in three years of sustained field production.

Areal averages of pressure were made from existing pressure data so that well pressures could be matched to some "ball park" number depending upon the well's location within the sector area. In general pressures taken in the fall of 1992 were around 1800 psig for the up dip region of the gas cap, 1200 psig for the mid dip region and 800 to 1000 psig for the down dip region.

Since so few wells had pressure data and only a few had two pressure points, less emphasis was placed on pressure matching. The goal was to obtain pressures which were reasonable for each well, given its location within the reservoir.

Early simulation runs were made with all three phases (oil, gas, and water rates) specified. This was done to insure proper voidage in the early stages of history matching. With the proper voidage rate specified for each well, calculated pressures were compared to actual pressures and "ball park" estimates for each well. Most wells required porosity adjustments to all completed layers to correct the pressure level. Some wells required permeability adjustments to all completed layers to correct the shape of the pressure curve.

These porosity and permeability adjustments were first made on an areal basis and then on a well-by-well basis. Modifications were made equally to all completed layers since historical pressure data for isolated layers were not available.

#### **Saturation Match (Gas and Water Production)**

Better data were available for historical gas and water production. In the saturation match simulation runs, only oil rate was specified, and the simulation calculated pressures, gas rates, and water rates were compared to observed data. However for the gas cap wells, gas rate was specified, and the simulation calculated pressures and water rates were compared to observed data.

The biggest problem to overcome in history matching this reservoir was modeling water production up dip in the gas cap without affecting gas and oil production in the mid dip and down dip regions. The simulation model consisted of isolated layers with no vertical transmissibility between layers.

Layers 5 and 6 were assigned a very high capillary pressure to create a large water-oil transition zone resulting in high initial water saturations up dip in these layers.

With this model, most of the hydrocarbon production was obtained from Layer 4. By modifying permeabilities for Layers 4, 5 and 6, the correct mix of oil and water could be achieved in all wells up dip or down dip.

Similarly, additional gas production could be obtained by modifying permeabilities in Layers 2 and 3. In addition, well completions were altered if the existing completions could not allow for the proper production. This was within reason since all wells were fractured upon completion, and arguments could be made for communication with non completed layers close to the wellbore.

Table 4 summarizes the initial volumes in place by layer and for the entire simulation model. Note that Layer 4 has the highest oil and gas volumes in place, while Layers 5 and 6 contain very high volumes of initial water in place.

Figure 10 illustrates the quality of the history match with respect to model oil, gas, and water cumulative production data. The observed data is plotted as circles and the simulation calculated results are plotted as lines. If oil rates had been specified for all wells, the calculated oil production would match exactly with the observed oil production data. As can be seen in Fiugre 10, this is not the case because gas production was specified in the simulation for the three gas cap wells (Algerita 1, Saguaro 2, and Sara 2). However, the figure does illustrate that a satisfactory match was obtained for oil, gas, and water production.

Plots of individual well history matches are given for each well in the study area in Appendix IV. Aactual observed data is plotted as circles and the calculated simulation results are plotted as lines. A review of each individual well plot reveals that most wells were matched very well.

The plots contained in Appendix IV illustrate the quality of the history match more clearly. For the gas cap wells (Algerita 1, Saguaro 2, and Sara 2) gas production was specified, and the quality of the match is measured by inspecting the oil and water production curves and the pressure plots.

The plots for these three gas cap wells show very good matches for water production and pressure. These three wells have associated condensate production that was not matched, as seen on the oil production plot. However, this associated condensate production is a negligible amount (less than 10 MSTB of cumulative oil production per well).

For the remaining wells, oil rate was specified in the simulation, and the history match quality is measured by inspecting the gas and water production curves and the pressure plots. As the remaining plots in Appendix IV illustrate, satisfactory history matches were obtrained on all remaining wells (John 5, John 3, John 4, and Ceniza 3).

### **Predictions**

#### Well Productivity Calibration

Prior to simulation of the prediction cases, a productivity match was performed for each well. During history match runs, all wells have a specified oil rate or gas rate and are constrained by that rate. However, during the prediction runs, the wells must be pressure constrained since rates are being predicted.

All wells within the study area are produced with beam pumping units. Yates provided SSI with fluid level data for the wells, and these data were converted to bottomhole pressure (BHP) data.

For the productivity match, all wells were assigned their respective BHP's. In addition, each well was assigned an oil rate far above the rate it is capable of producing. This forces the well to be pressure constrained in the simulator. The productivity match run duration was short, about five days. Through an iterative process, well indices (WI's) were altered for each well until the calculated rate for each well (under bottomhole pressure constraint) matched the observed oil rate at the end of history.

### **Prediction Case Descriptions**

All prediction cases were simulated for a total of 26 years beginning in November 1992 and continuing through December 2018. No economic limit was input for any of the runs.

The completion intervals for new wells were determined from neighboring wells. Similarly the PI or WI values assigned to the new wells were average values for the given location of each new well.

Since current water cuts are above 90 percent for most wells in the study area, oil producing wells were assigned a maximum water cut limit of 99 percent. Oil wells were also assigned a maximum GOR limit of 100,000 SCF/STB. In the event that these limits are reached for a given well, the simulator shuts-in layers one by one to improve the water cut and/or GOR until there is only one layer completed. When only one layer remains completed and a limit is exceeded, the well is shut-in.

The following paragraphs briefly describe the characteristics of each prediction case. Unless otherwise specified, the general guidelines just discussed are applicable to each case.

### Prediction Case 1 (Continued Depletion - Base Case)

This case continued the existing depletion of the reservoir with the existing wells.

#### Prediction Case 2 (Continued Depletion without Gas Cap Depletion)

In order to determine the effect of gas cap production on field oil production, all gas cap wells were shut-in while the rest of the wells were allowed to deplete. The wells that were shut-in during this run were: Algerita 1, Saguaro 2, and Sara 2.

### Prediction Case 3 (Continued Depletion with Gas Cap Infills)

Two additional gas cap wells were drilled in order to deplete the gas cap at an increased rate. One well was placed between Sara 2 and Saguaro 2 in grid cell x = 8, y = 2. The other well was placed between Saguaro 2 and Algerita 1 in grid cell x = 4, y = 2 (see Figure 11).

#### **Prediction Case Results**

Prediction case results can be evaluated on several levels. The most common types of evaluations are based on:

- cumulative oil recovery
- rate of oil recovery
- recovery efficiency
- · economics

Although a great deal of importance is frequently given to the final oil recovery the items shown above should all be taken into consideration. The results of economic analyses should normally control the development of a reservoir, rather than simply trying to maximize ultimate oil recovery. The optimum development scheme is frequently different for each of the criteria listed above. In some situations, outside factors may take precedence over the need for economic efficiency. An example is the case where contractual obligations require production at a certain rate over a given period of time. Yates should include any such external factors in their final evaluation of the results of this study. A comparison of case results, according to the categories above, is discussed in the following sections of this report.

## Case Comparisons

Table 5 shows a comparison of the cumulative recoveries at the end of each of the prediction cases. Note that the recoveries in Table 5 and those discussed in the text that follows are 26-year recoveries. Note that there is little difference in oil recovery with and without gas cap depletion (Cases 1 and 2). Also note that accelerated depletion of the gas cap with two additional gas cap wells (Case 3) does not affect ultimate oil recoveries. The case comparison plot in Figure 12 illustrates that gas cap management does not affect oil production down dip. Although cumulative gas production varies for each of the three prediction cases, the ultimate oil recovery is the same.

Since the oil recoveries for all three prediction cases are very similar (Table 5), plots of model oil, gas, and water production have been provided only for prediction Case 1 (continued depletion) (Figures 13 through 15). Plots of individual well production for Case 1 are given in Appendix V. Also, plots of individual well production for Case 3 (Gas Cap Infills) are included in Appendix VI including production plots for the two infill gas cap wells (NEW 1 and NEW 2).

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Table 1
Relative Permeability Endpoints
Canyon Reservoir - Dagger Draw Field

	Water-C	Water-Oil Relative Permeability	meability		Gas-Oi	Gas-Oil Relative Permeability	eability
	Scal Sample 3	Scal Sample 4w	Simulation <u>Model</u>		Scal Sample 3	Scal Sample 4w	Simulation <u>Model</u>
Swc	.3103	.2456	.2456	Slr	.6437	.5969	
Sorw	.3992	.3019	.3019	Sgc	.2076	.1305	
krocw	1.0000	1.0000	1.0000	krgro	.1240	.0490	
krwro	.1886	.1330	.5947	krogc	.1230	.4160	

Table 2
Water-Oil and Gas-Oil Contacts &
Water-Oil Capillary Pressure Endpoints
Canyon Reservoir - Dagger Draw Field

Model Pcow at Swc ( <u>psia</u> )	20	20	20	20	200	200	20	70
Model WOC (subsea feet)	4053	4092	4123	4179	4228	4343	4366	4403
Model GOC (subsea feet)	3832	4030	3997	3959	4020	4285	4125	4158
Model <u>Layer</u>	,	2	ı m	4	· v	9	7	∞ ∞

Table 3 Reservoir Fluid Properties Canyon Reservoir - Dagger Draw Field

OIR GAS PR	OPERTIES	R	ESERVOIR C	IL PROPE	RTIES
FVF	Viscosity	Pressure	e Rso	FVF	Viscosity
rb/mscf	CD	<u>psia</u>	scf/stb	rb/stb	CD
205.83	0.012	14.6	9.79	1.026	1.285
29.86	0.012	99.7	36.12	1.034	1.197
13.62	0.012	214.6	65.03	1.044	1.133
6.83	0.012	414.6	112.25	1.061	1.027
4.47	0.012	614.7	159.12	1.080	0.933
3.27	0.013	814.7	206.81	1.100	0.873
2.55	0.013	1014.7	255.78	1.122	0.818
2.07	0.014	1214.7	306.26	1.145	0.765
1.73	0.015	1414.7	358.41	1.170	0.715
1.49	0.016	1614.7	412.35	1.197	0.668
1.30	0.017	1814.7	468.15	1.225	0.624
1.16	0.018	2017.7	526.79	1.255	0.583
1.10	0.018	2114.6	555.54	1.270	0.565
1.05	0.019	2214.6	585.69	1.286	0.547
1.00	0.019	2314.6	616.35	1.302	0.530
0.92	0.020	2514.6	679.29	1.335	0.498
0.86	0.022	2714.6	744.43	1.371	0.468
0.81	0.023	2914.6	811.82	1.407	0.441
0.79	0.023	*3014.6	846.38	1.426	0.428
0.70	0.026	3514.6	1028.25	1.526	0.369
0.65	0.029	4014.6	1226.04	1.635	0.320
0.61	0.031	4514.6	1441.02	1.753	0.277
0.58	0.034	5014.6	1674.56	1.881	0.238
0.55	0.036	5514.6	1928.22	2.017	0.203
0.53	0.038	6014.6	2203.74	2.164	0.171
	FVF rb/mscf 205.83 29.86 13.62 6.83 4.47 3.27 2.55 2.07 1.73 1.49 1.30 1.16 1.10 1.05 1.00 0.92 0.86 0.81 0.79 0.70 0.65 0.61 0.58 0.55	rb/mscf	FVF         Viscosity         Pressure           rb/mscf         CD         Dsia           205.83         0.012         14.6           29.86         0.012         99.7           13.62         0.012         214.6           6.83         0.012         414.6           4.47         0.012         614.7           3.27         0.013         814.7           2.55         0.013         1014.7           2.07         0.014         1214.7           1.73         0.015         1414.7           1.49         0.016         1614.7           1.30         0.017         1814.7           1.16         0.018         2017.7           1.10         0.018         2114.6           1.05         0.019         2214.6           1.00         0.019         2314.6           0.92         0.020         2514.6           0.86         0.022         2714.6           0.81         0.023         2914.6           0.79         0.023         2914.6           0.65         0.029         4014.6           0.65         0.029         4014.6	FVF         Viscosity         Pressure         Rso           rb/mscf         CD         psia         scf/stb           205.83         0.012         14.6         9.79           29.86         0.012         99.7         36.12           13.62         0.012         214.6         65.03           6.83         0.012         414.6         112.25           4.47         0.012         614.7         159.12           3.27         0.013         814.7         206.81           2.55         0.013         1014.7         255.78           2.07         0.014         1214.7         306.26           1.73         0.015         1414.7         358.41           1.49         0.016         1614.7         412.35           1.30         0.017         1814.7         468.15           1.16         0.018         2017.7         526.79           1.10         0.018         2114.6         555.54           1.05         0.019         2214.6         585.69           1.00         0.019         2314.6         616.35           0.92         0.020         2514.6         679.29           0.86	FVF         Viscosity         Pressure         Rso         FVF           rb/mscf         CD         psia         scf/stb         rb/stb           205.83         0.012         14.6         9.79         1.026           29.86         0.012         99.7         36.12         1.034           13.62         0.012         214.6         65.03         1.044           6.83         0.012         414.6         112.25         1.061           4.47         0.012         614.7         159.12         1.080           3.27         0.013         814.7         206.81         1.100           2.55         0.013         1014.7         255.78         1.122           2.07         0.014         1214.7         306.26         1.145           1.73         0.015         1414.7         358.41         1.170           1.49         0.016         1614.7         412.35         1.197           1.30         0.017         1814.7         468.15         1.225           1.16         0.018         2017.7         526.79         1.255           1.10         0.018         2114.6         555.54         1.270           1.05 </td

<sup>\*</sup> Values extrapolated beyond Bubble Point for simulation purposes

Table 4
Simulation Model - Initial in Place Volumes and Pressures
Canyon Reservoir - Dagger Draw Field

	Layer 1	Layer 2	Layer 3	Layer 4	Layer 5	Layer 6	Layer 7	Layer 8	Total
Oil (MMSTB)	0.325	0.019	0.257	4.788	0.372	0.000	0.224	0.137	6.122
Water (MMSTB)	869'0	0.539	0.775	8.442	20.347	8.261	0.510	0.703	40.276
Gas (BSCF)	0.878	1.139	1.580	21.621	3.593	1.325	0.190	0.116	30.442
Free Gas (BSCF)	0.603	1.123	1.362	17.565	3.278	1.325	0.000	0.000	25.256
Average Pressure	3033	3002	3011	3017	3017	3001	3064	3074	3016

TABLE 5

PREDICTION SIMULATIONS - RESERVOIR PERFORMANCE SUMMARY CANYON RESERVOIR, DAGGER DRAW FIELD , NEW MEXICO

	CASE 1	CASE 2	CASE 3
End of Case	December, 2018	December, 2018	December, 2018
Oil, MSTB	682	684	682
Gas, BSCF	19.5	9.7	21.5
Water, MSTB	7435	4890	8398

Case 1 - Continued Depletion

Case 2 - Continued Depletion without Gas Cap Depletion

Case 3 - Continued Depletion with Gas Cap Infills

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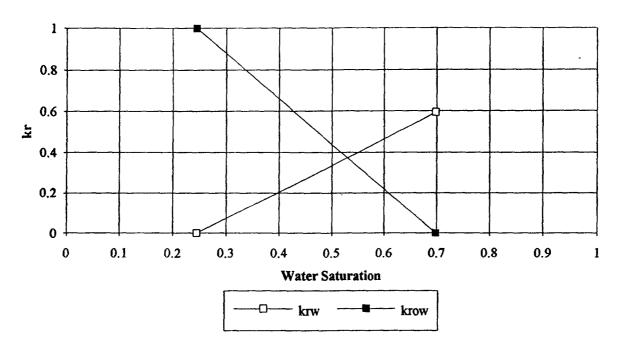
Figure 1
Sector Model Grid - Plan View
Canyon Reservoir - Dagger Draw Field

	12		<del>ر</del> ب			24					
HILLI		CEN4			CENS	R	HILL7	MAYR2	MAYR1 O		PALV1
SARA3		SARA1	SARAG	JOHN2	P O	6 - CO	HILLB	HTLLS		HILLIZ	PRIC1 O
SAG13	Sec O	CON18	SHRR4		JOHNS O	. O .	SAG8	HILLE	HILL2 O 5.0	HILL4	
CONI	CON7		SARPS	OUHNI	JOHNS	i i	SEN2	SAG	S98. O	HILLI	HILL3
	CON12	SAGI				SHG12					
000T1					SARAZ					CARLI	
0			SNG2 0 15 								
			) UDI			-					
	<u></u>				16						

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Figure 2
Sector Model Grid - Cross Section (J = 2)
Canyon Reservoir - Dagger Draw Field

Figure 3
Water - Oil Relative Permeability - Simulation



Gas - Liquid Relative Permeability - Simulation

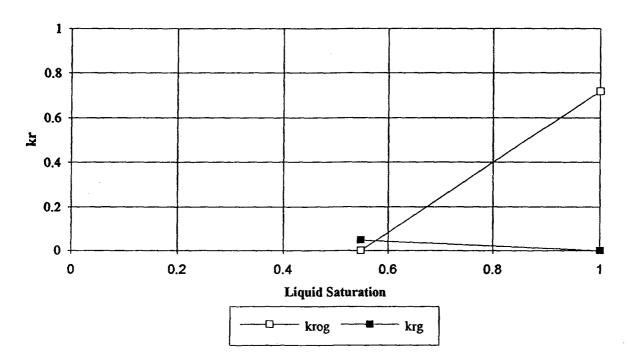
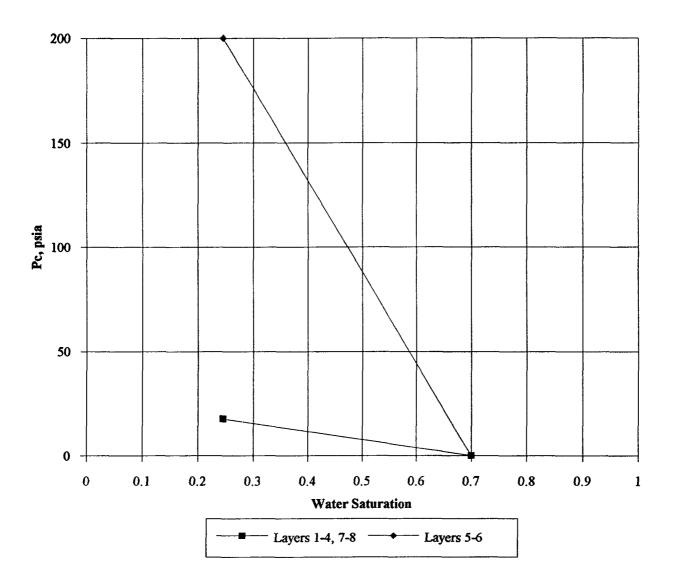


Figure 4
Water - Oil Capillary Pressure - Simulation



. 0009 Figure 5
Oil Formation Volume Factor vs Pressure - Simulation
Canyon Reservoir - Dagger Draw Field 5000 4000 Pressure, psia 3000 2000 1000

Oil Formation Volume Factor, RB/STB

7000

Pressure, psia Solution Gas Oil Ratio, SCF/STB

Figure 6
Solution Gas Oil Ratio vs Pressure - Simulation
Canyon Reservoir - Dagger Draw Field

7000 . 0009 2000 4000 Pressure, psia 3000 2000 1000 Oil Viscosity, cp 1.4 0.5 0 0.4

Figure 7
Oil Viscosity vs Pressure - Simulation
Canyon Reservoir - Dagger Draw Field

Pressure, psia Gas Formation Volume Factor, RB/MSCF

Figure 8
Gas Formation Volume Factor vs Pressure - Simulation
Canyon Reservoir - Dagger Draw Field

0009 2000 4000 Pressure, psia 3000 2000 1000 0.05 Gas Viscosity, cp 0 0.04 0.01

7000

Figure 9
Gas Viscosity vs Pressure - Simulation
Canyon Reservoir - Dagger Draw Field

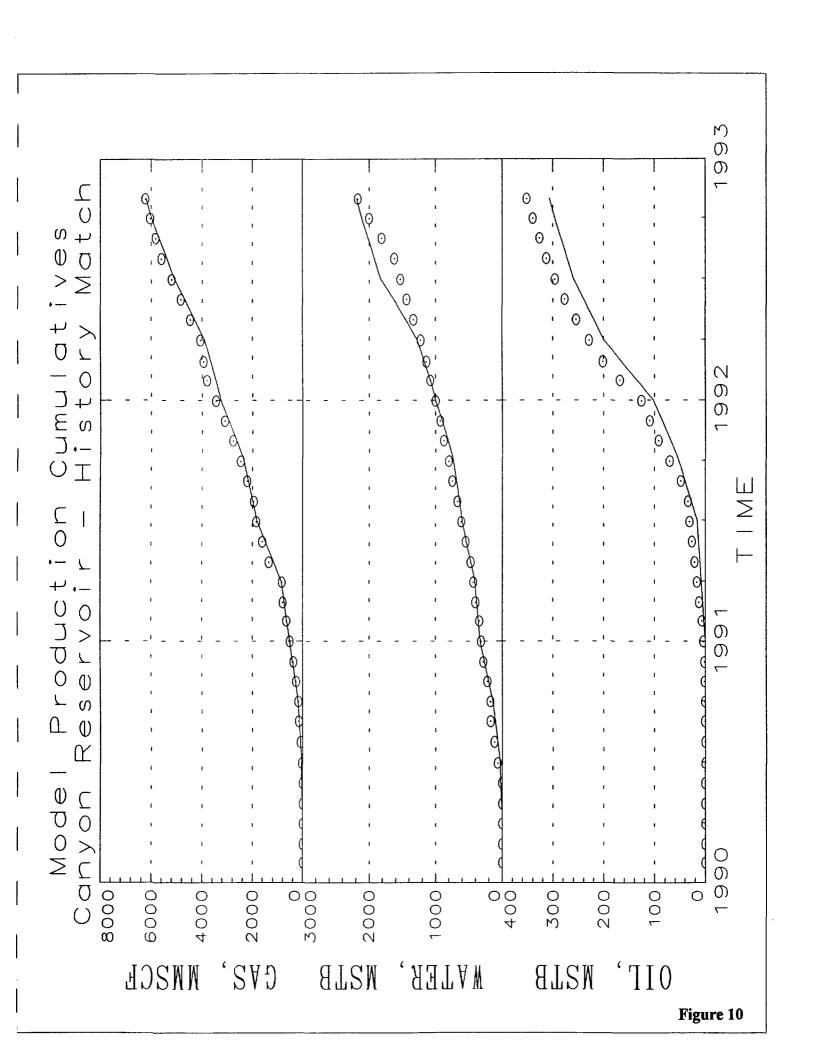
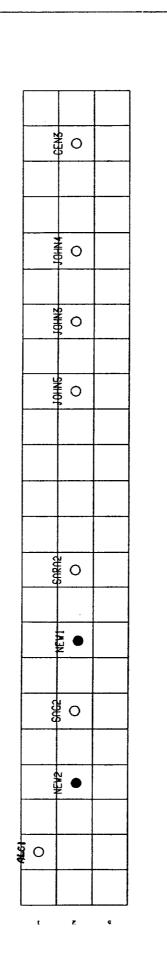
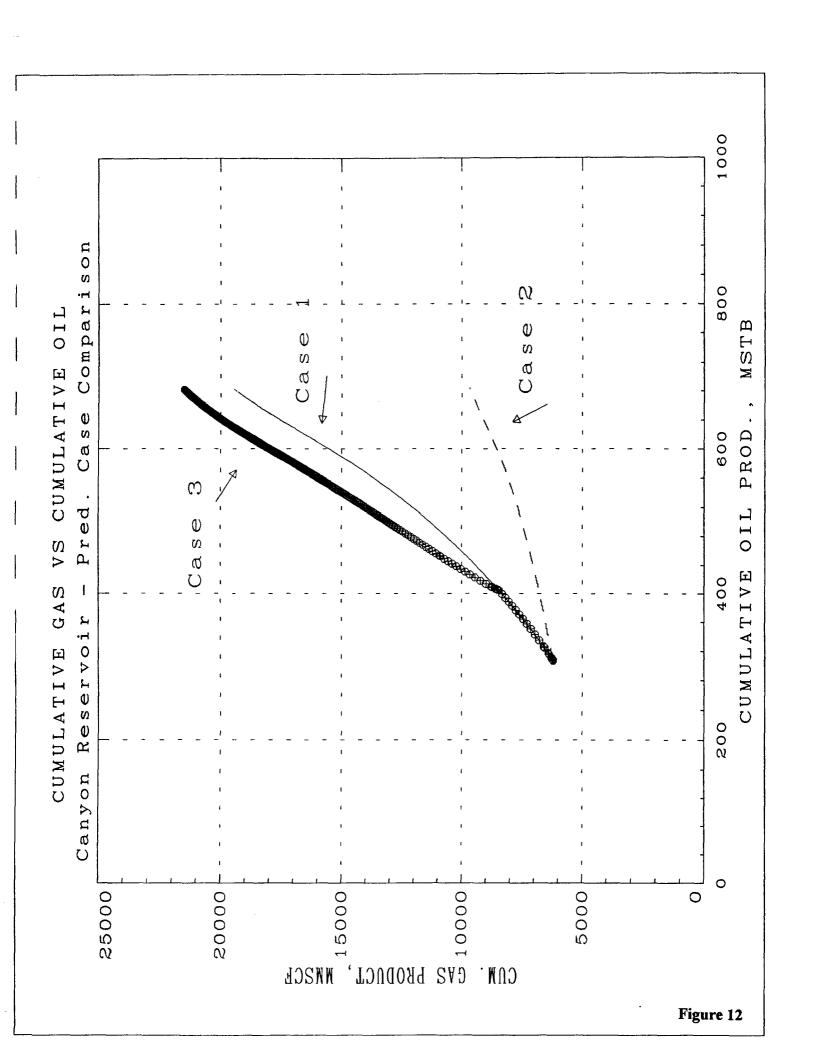
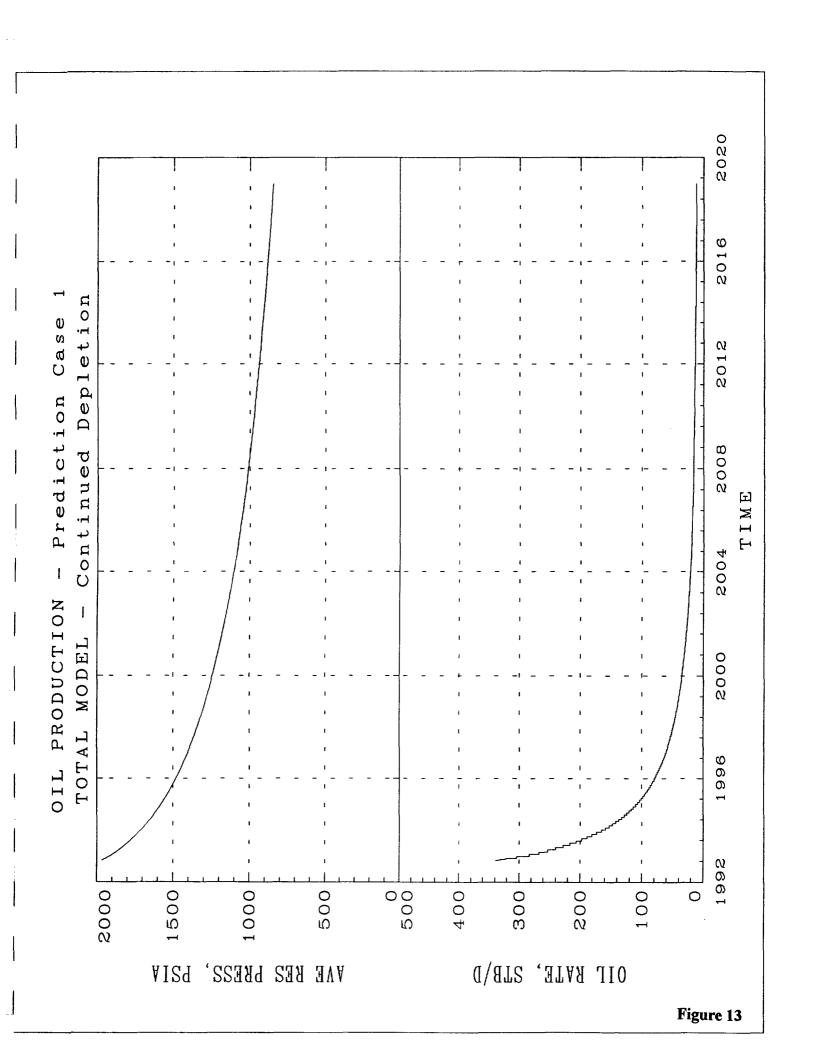
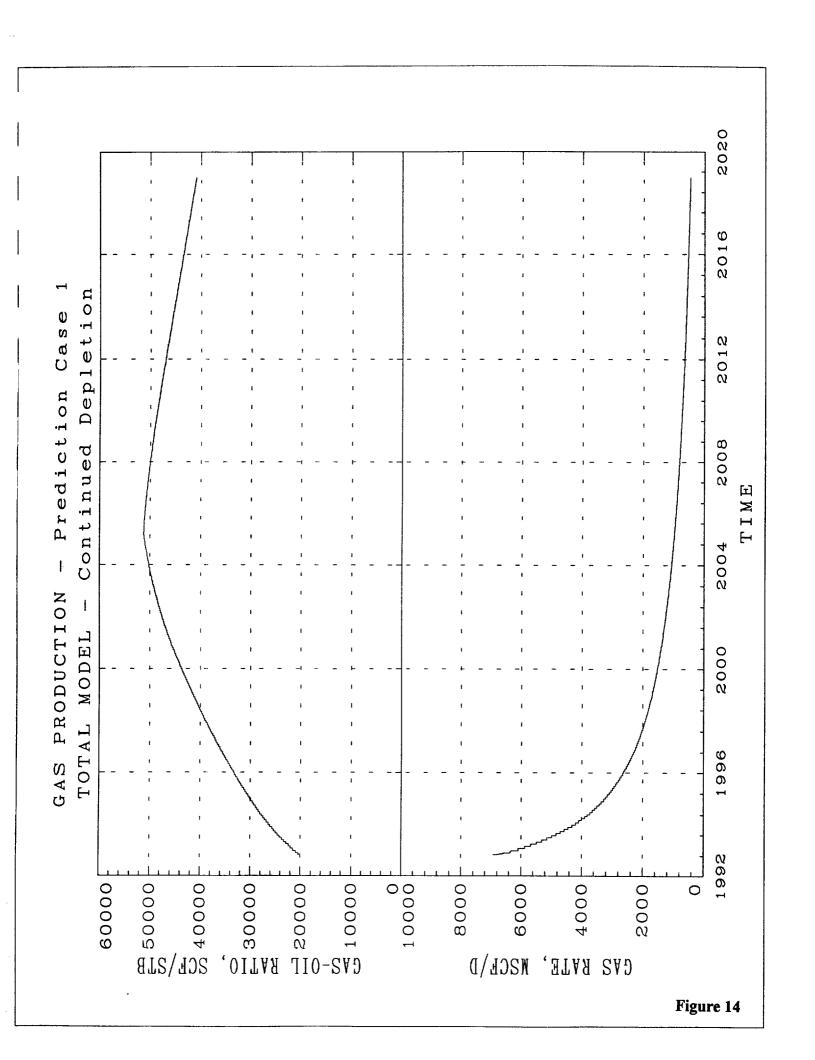


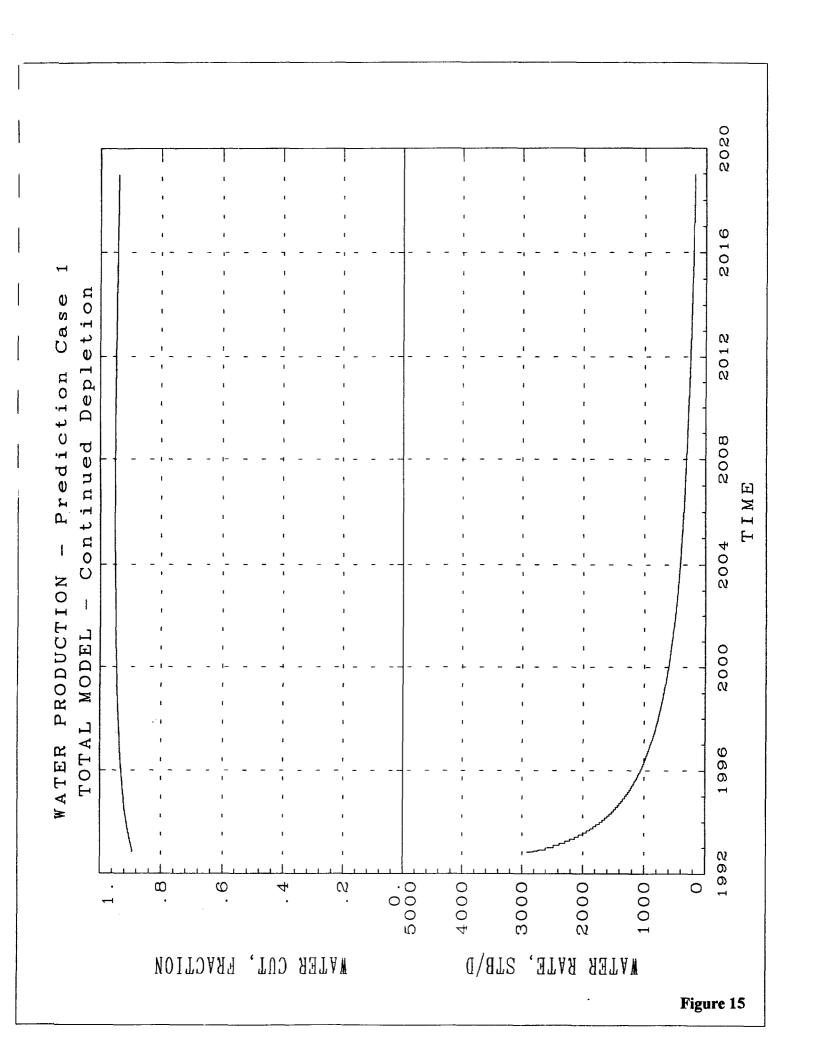
Figure 11
Sector Model Grid - Plan View
Prediction Case 3
Canyon Reservoir - Dagger Draw Field





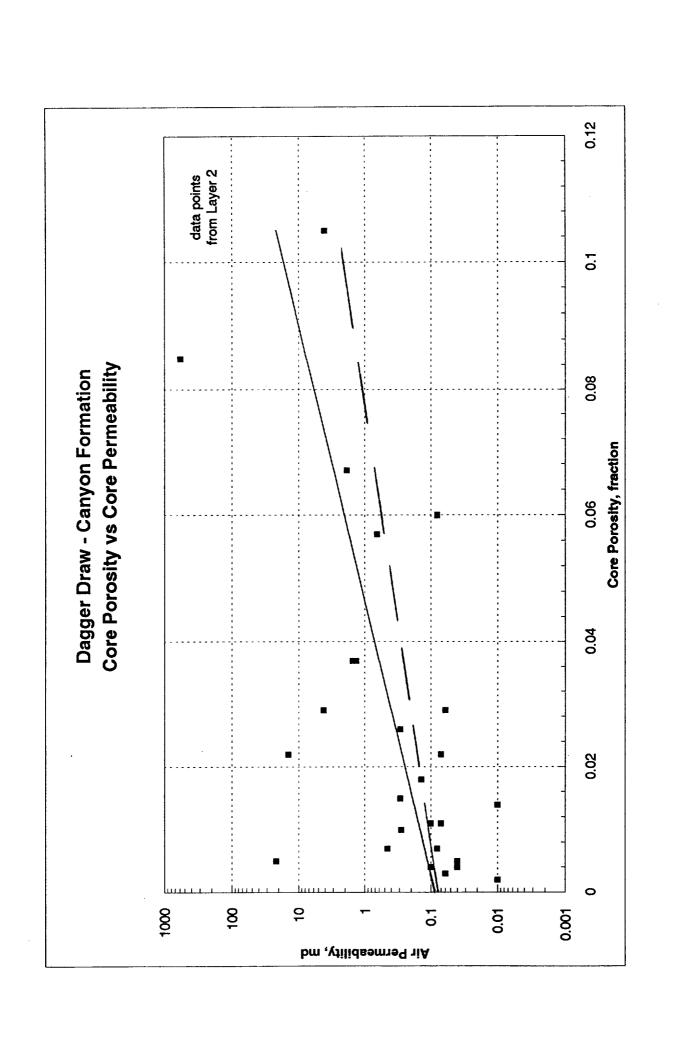


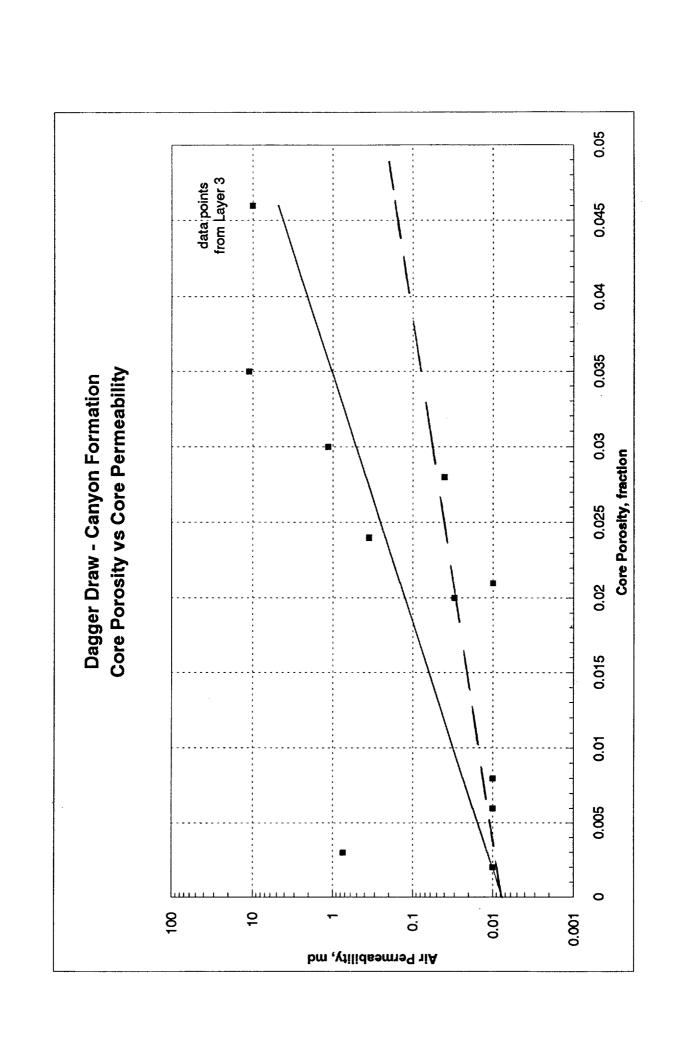


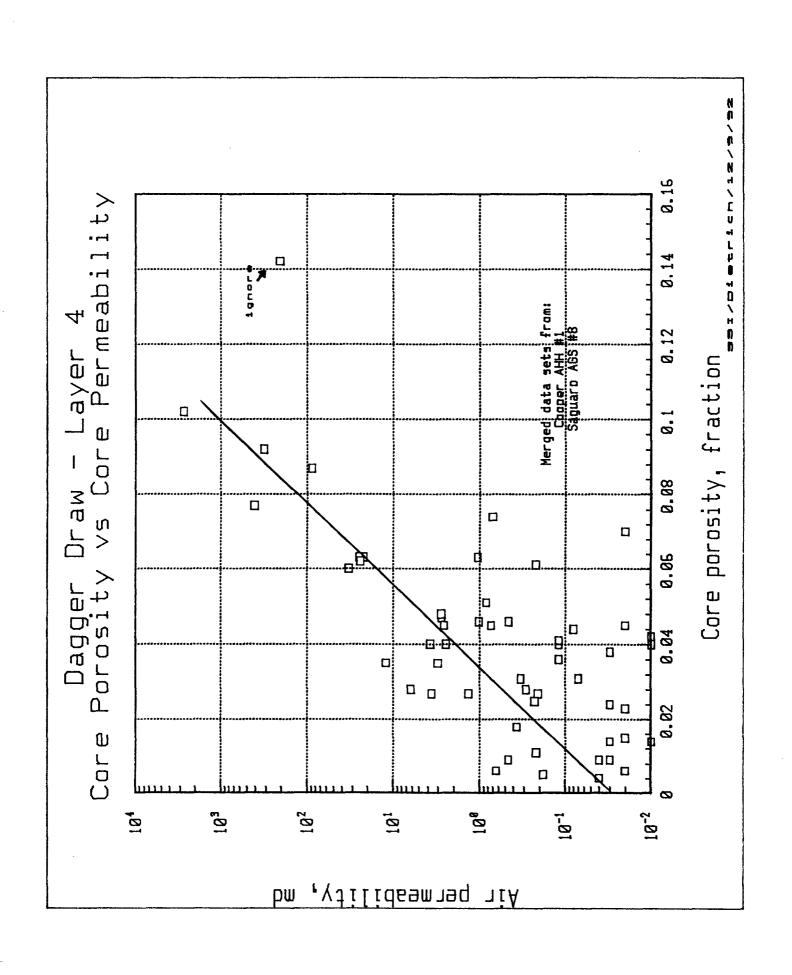


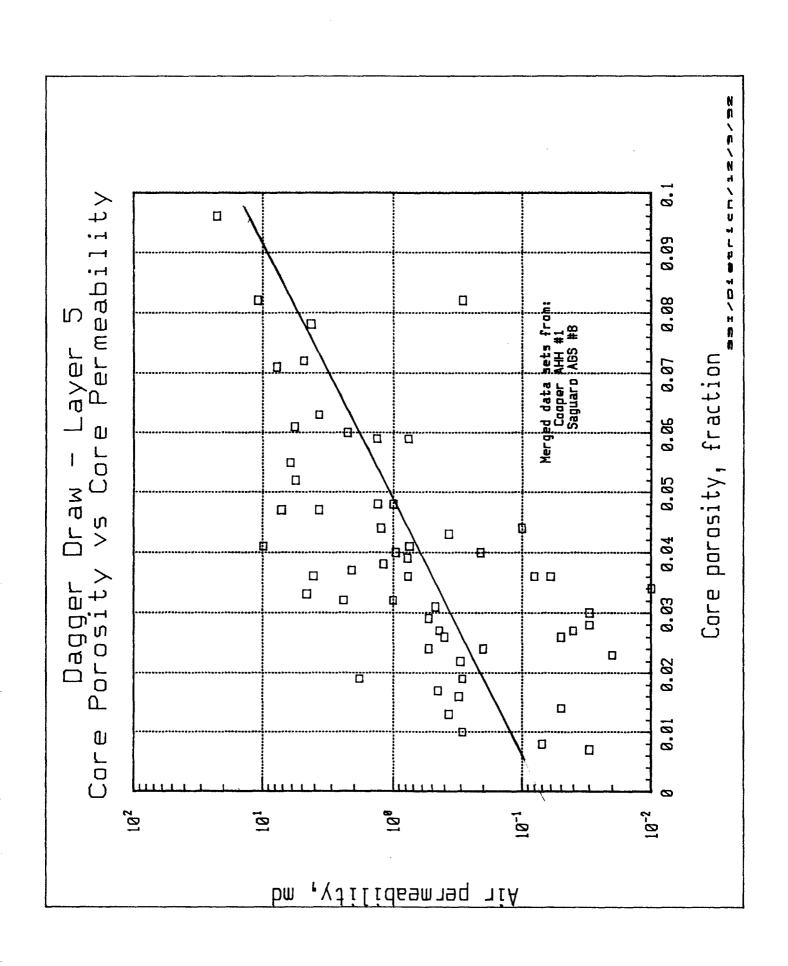
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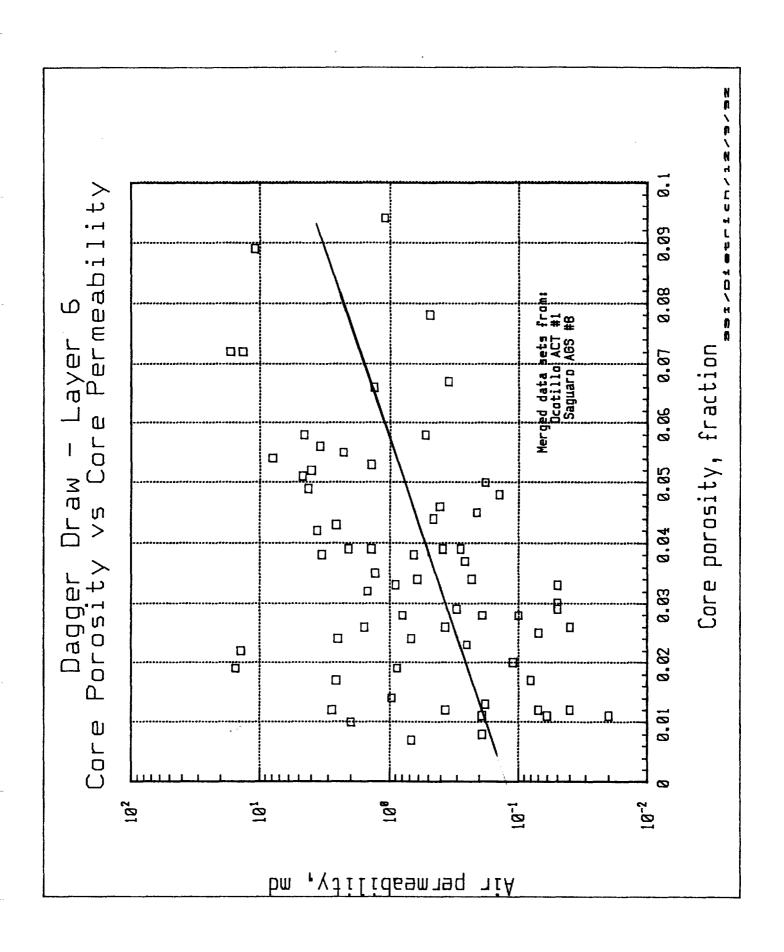
# APPENDIX I CORE ANALYSIS PLOTS

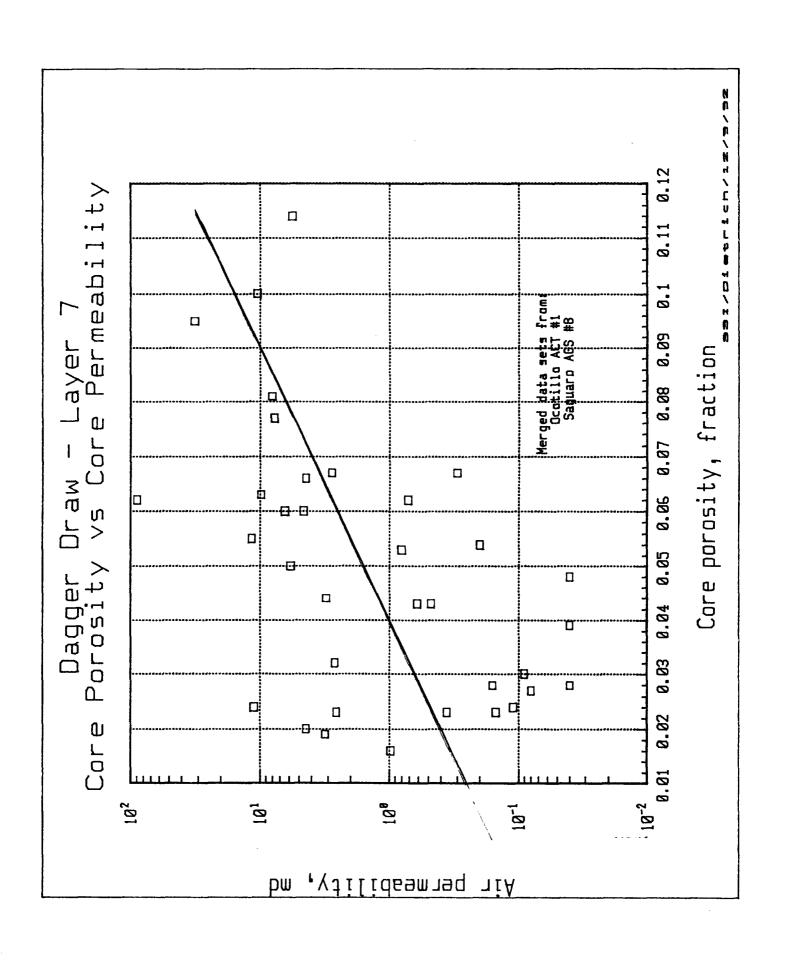


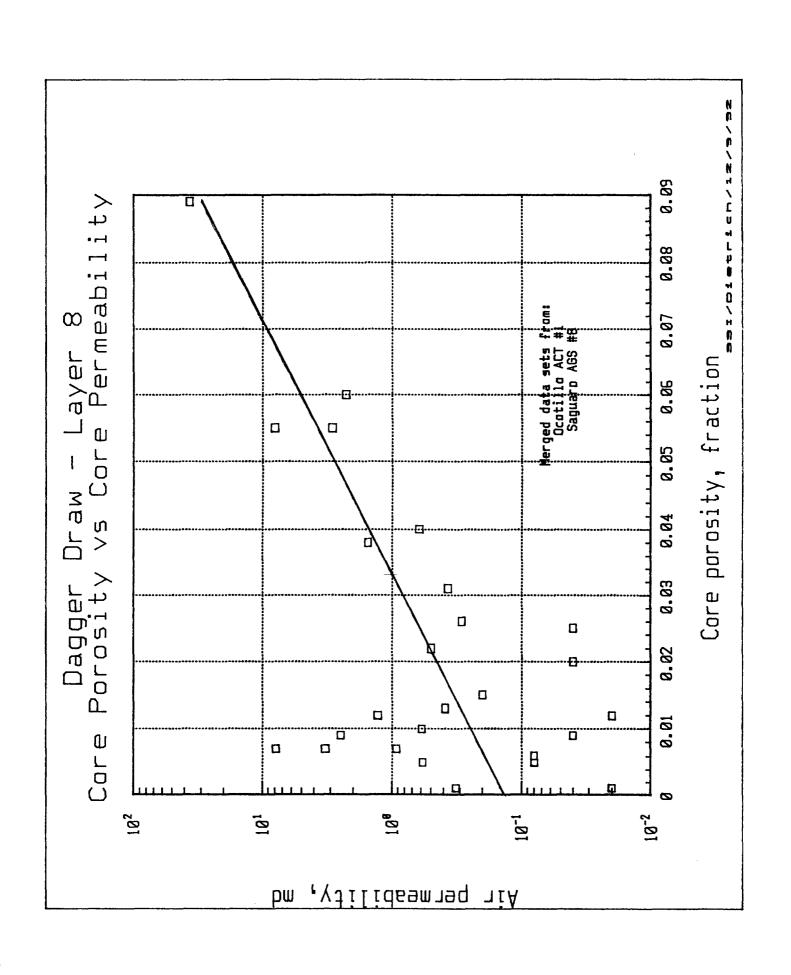


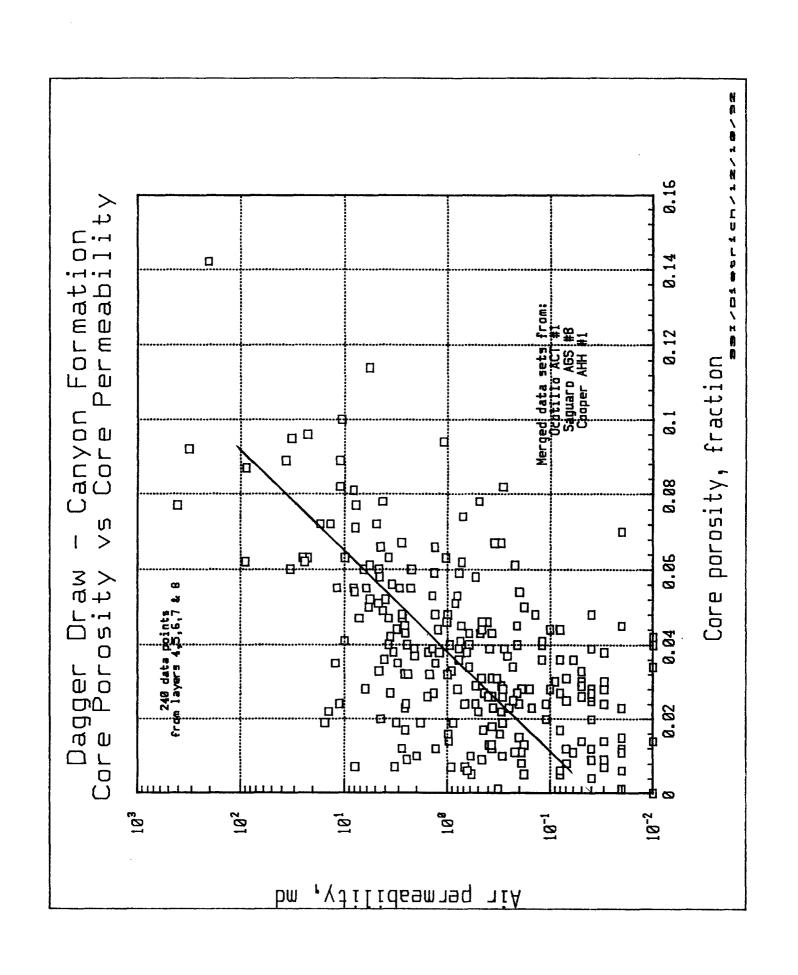












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#### APPENDIX II

# SCAL, INC. RELATIVE PERMEABILITY LAB ANALYSIS

### **Gas-Oil Relative Permeability**

### Dagger Draw Federal No. 12 Eddy County, New Mexico

The analysis, interpretations or opinions expressed in our reports represent the best judgement of Special Core Analysis Laboratories Inc.. Special Core Analysis Laboratories Inc. assumes no responsibility and makes no warranties of any kind as to the productivity, proper operation or profitability of any oil, gas or any other mineral in connection which such a report is used or relied upon.

#### **Unsteady-State Gas-Oil Relative Permeability**

Company:

Conoco Inc.

Field:

Dagger Draw

Well Name:

Dagger Draw Federal # 12

Eddy County, New Mexico

Sample:

3

Porosity:

9.82 % 507 mD

Depth:

7658' 11"

Permeability:

----

Temperature:
Oil Viscosity:
Gas Viscosity:

22.00 22.40 0.018 deg. C cP cP Keo @ Siw: Keg @ Sro: 72.9 mD 9.04 mD 31.03 %

Siw Sro

···33.34 %

#### **TEST RESULTS:**

No.	Sg	* Krg	* Kro	Krg/Kro
-	%	-	-	-
1	20.76	0.034	0.123	0.280
2	23.51	0.061	0.064	0.959
3	25.17	0.097	0.046	2.106
4	26.41	0.104	0.033	3.170
5	26.84	0.108	0.031	3.521
6	27.54	0.110	0.027	4.124
7	28.23	0.115	0.024	4.781
8	29.43	0.117	0.020	5.698
9	30.62	0.120	0.016	7.675
10	35.63	0.124	0.000	

<sup>\*</sup> Relative to Keo @ Swi

#### Notations:

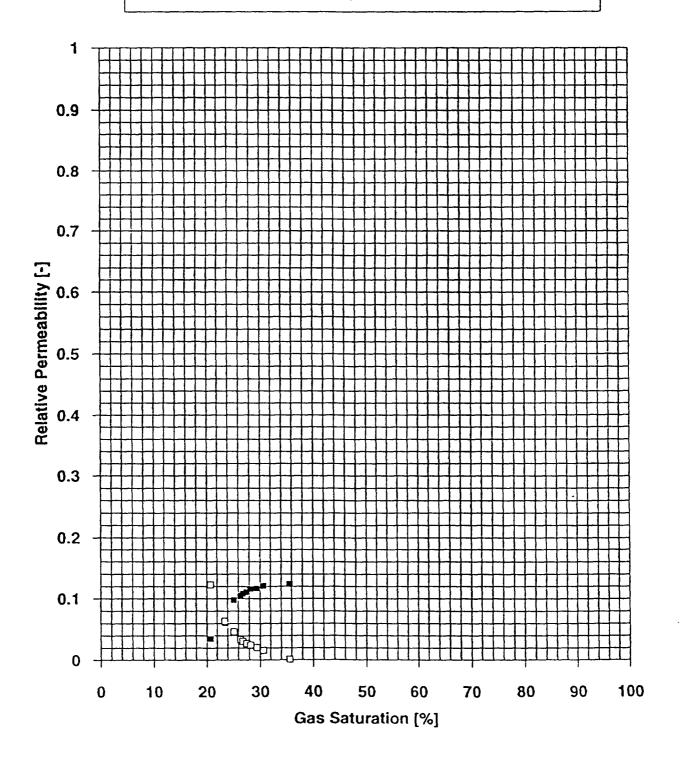
Keo Effective Oil Premeability
Keg Effective Gas Permeability

Sro Residual Oil Saturation

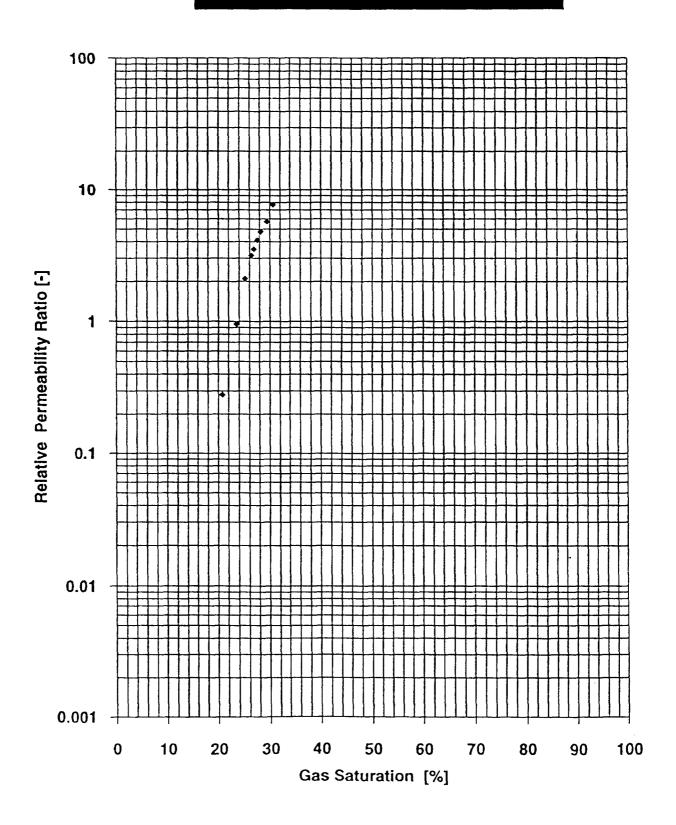
Siw Irreducible Water Saturation

# Unsteady-State Gas-Oil Relative Permeability Sample 3

Gas Relative Permeability Oil Relative Permeability



# Gas-Oil Relative Permeability Ratio Sample 3



#### Unsteady-State Gas-Oil Relative Permeability

Company:

Conoco Inc.

Field:

**Dagger Draw** 

Well Name:

Dagger Draw Federal # 12

Eddy County, New Mexico

Sample: Depth:

4W 7806' 6" Porosity: Permeability: 10.27 % 29.8 mD

Temperature:

22.00 22.40

Keo @ Siw: deg. C Keg @ Sro: 11.7 mD 0.57 mD

Oil Viscosity: Gas Viscosity:

сР 0.018 сР

Siw

24.56 %

Sro

35.13 %

#### **TEST RESULTS:**

No.	Sg	* Krg	* Kro	Krg/Kro
-	%	•	-	•
1	13.05	0.018	0.416	0.043
2	14.90	0.027	0.254	0.106
3	17.34	0.029	0.126	0.229
4	22.50	0.029	0.037	0.796
5	29.23	0.038	0.022	1.708
6	30.11	0.040	0.020	1.961
7	31.88	0.042	0.016	2.650
8	32.49	0.044	0.015	2.964
9	33.12	0.046	0.014	3.327
10	33.88	0.047	0.012	3.838
11	40.31	0.049	0.000	

<sup>\*</sup> Relative to Keo @ Swi

#### Notations:

Effective Oil Premeability Keo

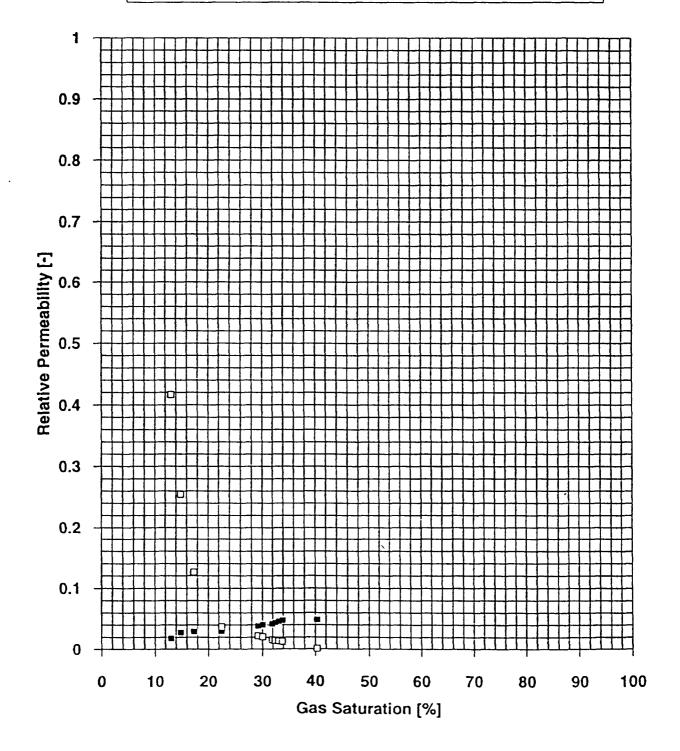
Keq Effective Gas Permeability

Residual Oil Saturation

Irreducible Water Saturation Siw

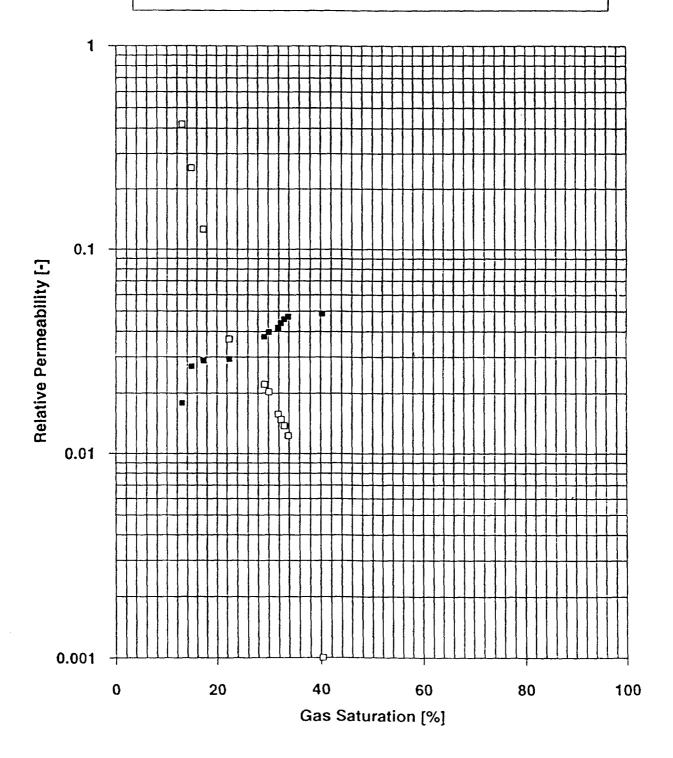
### Unsteady-State Gas-Oil Relative Permeability Sample 4W

Gas Relative Permeability
 Oil Relative Permeability

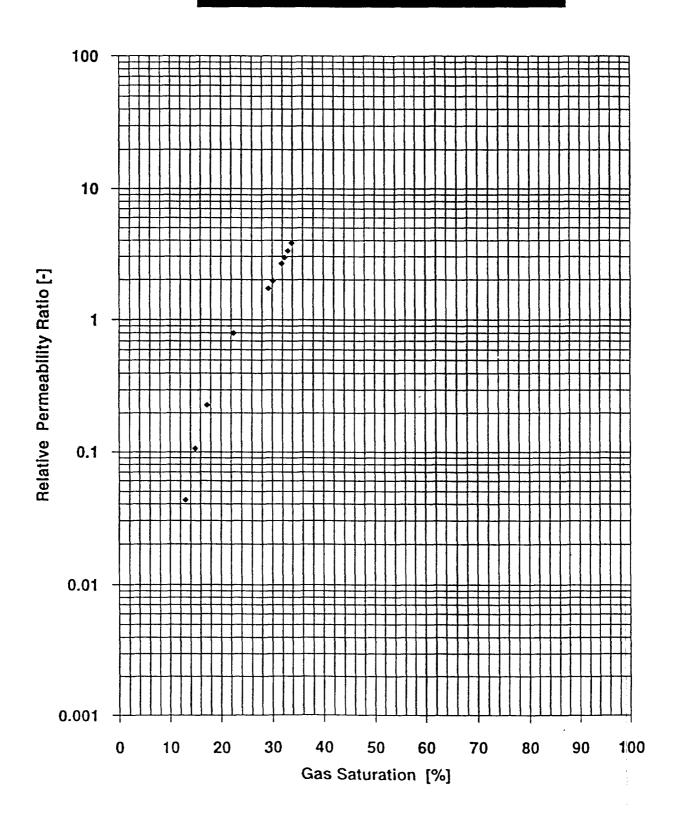


# Unsteady-State Gas-Oil Relative Permeability Sample 4W

Gas Relative Permeability
 Oil Relative Permeability



# Gas-Oil Relative Permeability Ratio Sample 4W



### **Water-Oil Relative Permeability**

### Dagger Draw Federal No. 12 Eddy County, New Mexico

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#### **Unsteady-State Water-Oil Relative Permeability**

Company:

Conoco Inc.

Field:

Dagger Draw

Location:

Dagger Draw Federal # 12

Well Name:

Eddy County, New Mexico

Sample: Depth:

3

Porosity:

9.82 %

7658' 11"

Permeability:

507 mD

Temperature:

22 deg. C

Keo @ Siw:

72.9 mD

Oil Viscosity:

22.4 cP

Kew @ Sro:

13.8 mD

Brine Viscosity:

1.03 cP

#### **TEST RESULTS:**

No.	Sw	* Krw	* Kro	Krw/Kro
-	%	-	-	-
1	31.03	0.0000	1.0000	0.000
2	34.22	0.0697	0.6272	0.111
3	41.89	0.0996	0.2391	0.417
4	43.80	0.1049	0.1625	0.646
5	45.33	0.1112	0.1182	0.940
6	48.33	0.1387	0.0708	1.958
7	52.78	0.1426	0.0215	6.625
8	54.12	0.1637	0.0176	9.292
9	55.89	0.1742	0.0084	20.792
10	60.08	0.1886	0.0000	

<sup>\*</sup> Relative to Keo @ Siw

#### Notations:

Keo Effective Oil Permeability
Kew Effective Water Permeability

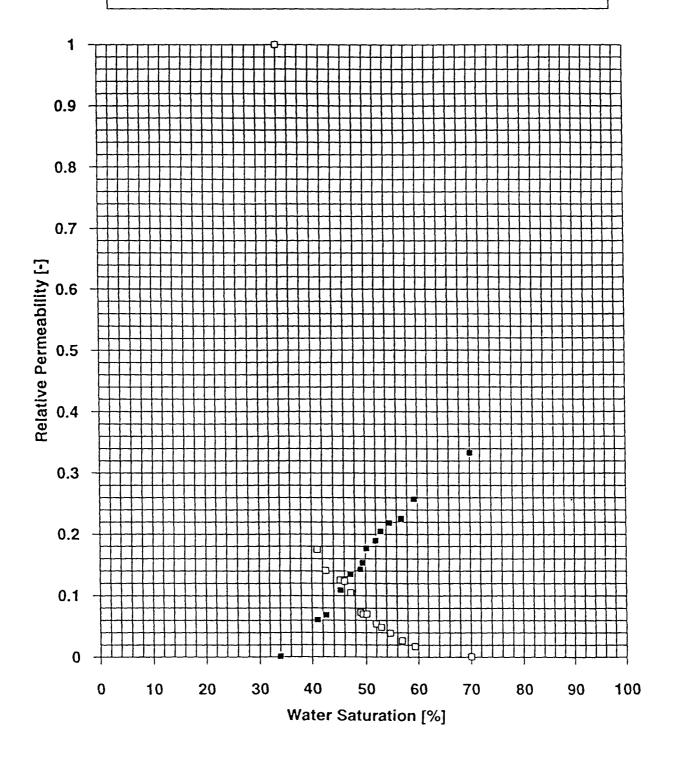
Sro Residual Oil Saturation

Siw

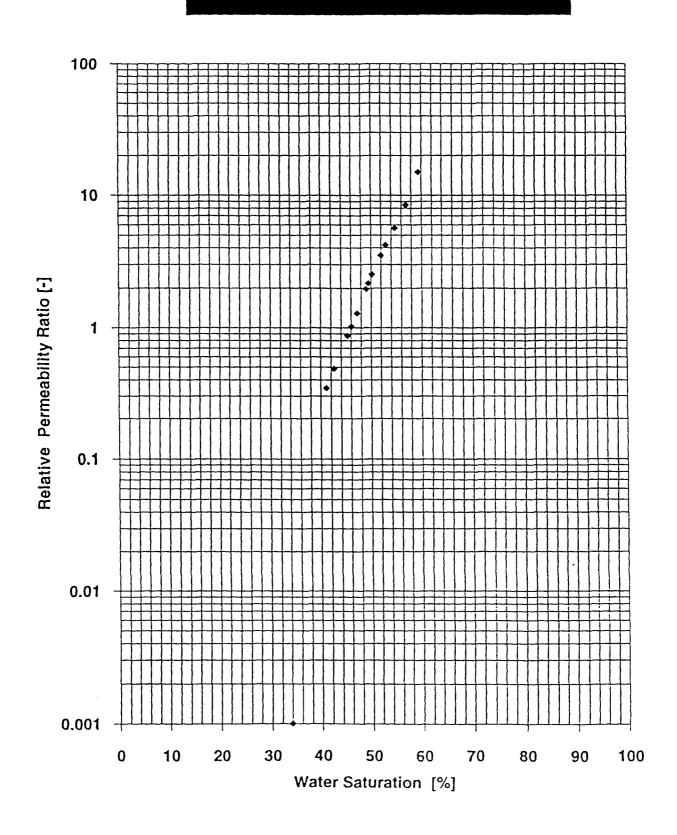
Irreducible Water Saturation

# Unsteady-State Water-Oil Relative Permeability Sample 3

■ Water Relative Permeability □ Oil Relative Permeability



# Water-Oil Relative Permeability Ratio Sample 3



#### **Unsteady-State Water-Oil Relative Permeability**

Company:

Conoco Inc.

Field:

Dagger Draw

Location:

Dagger Draw Federal # 12

Well Name:

Eddy County, New Mexico

Sample:

4W

Porosity:

10.27 %

Depth:

7806' 6"

Permeability:

29.8 mD

Temperature :

22 deg. C

Keo @ Siw:

11.7 mD

Oil Viscosity:

22.4 cP

Kew @ Sro:

1.556 mD

Brine Viscosity:

1.03 cP

#### **TEST RESULTS:**

No.	Sw	* Krw	* Kro	Krw/Kro
-	%	_	-	-
1	24.56	0.0000	1.0000	0.000
2	31.12	0.0331	0.9084	0.036
3	43.21	0.0953	0.4085	0.233
4	44.75	0.0987	0.3268	0.302
5	46.88	0.1021	0.2451	0.417
6	49.60	0.1055	0.1634	0.646
7	52.91	0.1089	0.0817	1.333
8	57.39	0.1157	0.0411	2.815
9	59.24	0.1177	0.0237	4.958
10	62.37	0.1227	0.0132	9.292
11	69.81	0.1330	0.0000	

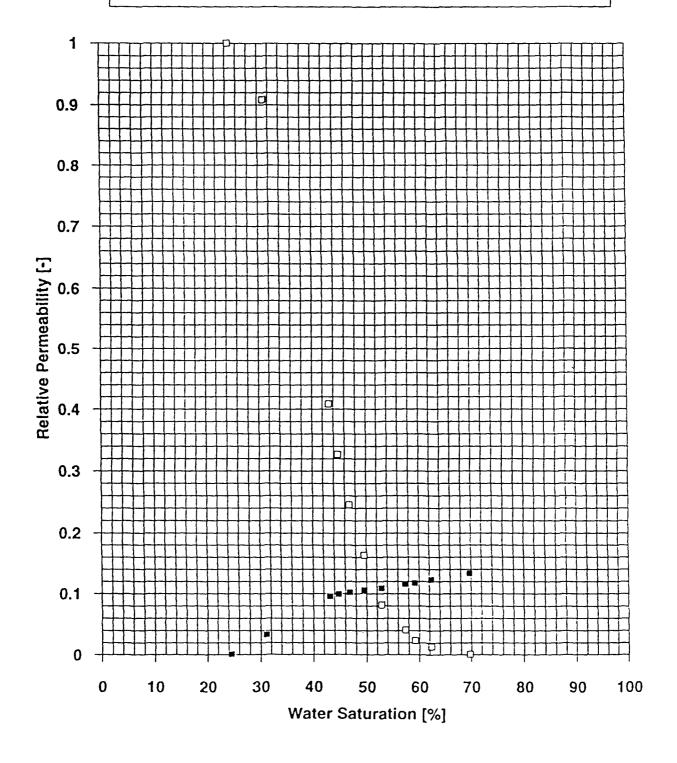
<sup>\*</sup> Relative to Keo @ Siw

#### Notations:

Keo Effective Oil Permeability
Kew Effective Water Permeability
Sro Residual Oil Saturation
Siw Irreducible Water Saturation

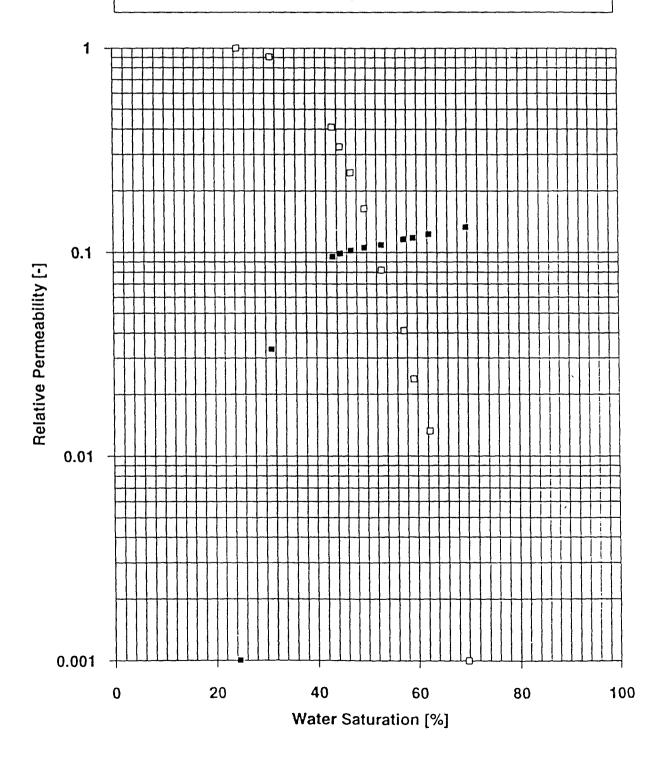
# Unsteady-State Water-Oil Relative Permeability Sample 4W

Water Relative Permeability Oil Relative Permeability

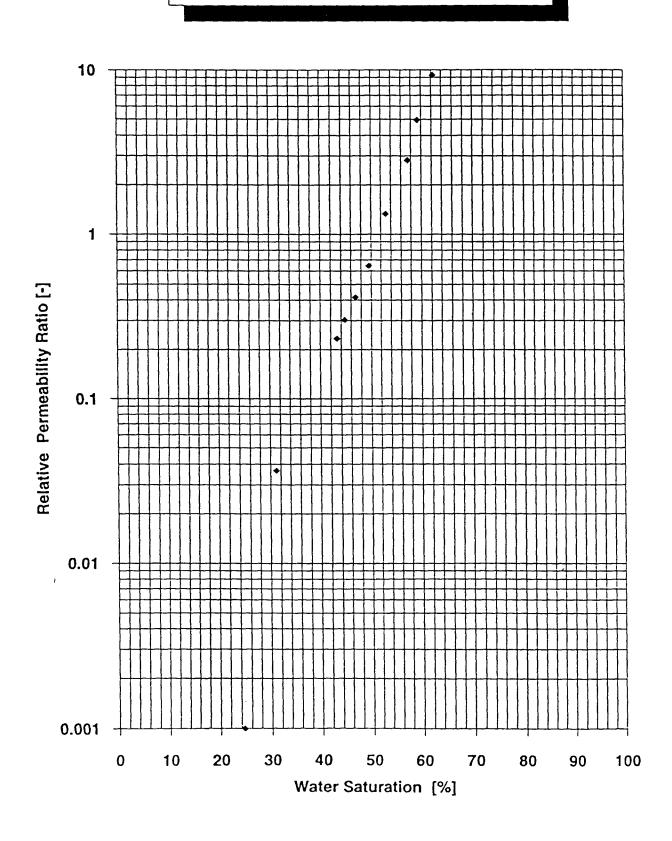


### Unsteady-State Water-Oil Relative Permeability Sample 4W

■ Water Relative Permeability □ Oil Relative Permeability



# Water-Oil Relative Permeability Ratio Sample 4W



### APPENDIX III CORE LABS RESERVOIR DATA FLUID ANALYSIS

### RESERVOIR FLUID ANALYSIS

FOR

YATES PETROLEUM CORPORATION
State CO #2
Dagger Draw North Field
Eddy County, New Mexico



April 3, 1990

YATES PETROLEUM CORPORATION 105 South 4th Street Artesia, New Mexico 88210

Attention: Mr. Pinson McWhorter

Subject: Reservoir Fluid Study

State CO #2

Dagger Draw North Field Eddy County, New Mexico

File: RFLM 90017

### Gentlemen:

Duplicate separator liquid and gas samples were collected from the subject well and were submitted to our Midland laboratory on December 1, 1989 for use in a reservoir fluid study. Presented in the following report are the results of this study as requested by Yates Petroleum Corporation.

The subject well is currently producing a gas/oil ratio greater than what is expected for this reservoir. This indicates that there is free-gas production associated with the solution gas. Therefore, it was decided to recombine the separator products to create a reservoir fluid that has a bubble point of 2000 psig at 130°F. This fluid was used for the remainder of the study.

The hydrocarbon composition of the reservoir fluid was determined by spike-flash/chromatographic technique. The results in terms of both mol percent and weight percent are presented on page four.

A small quantity of the reservoir fluid was charged to a high pressure windowed cell and thermally expanded to the reservoir temperature of 130°F. During a constant composition expansion at this temperature, the fluid was found to have a bubble point pressure of 2003 psig. The results of the pressure-volume measurements at reservoir temperature may be found on page seven. When subjected to differential pressure depletion at the reservoir temperature. The fluid evolved a total of 485 cubic feet of gas at 15.025 psia and 60°F. per barrel of residual oil at 60°F. The resulting relative oil volume factor was 1.247 barrels of saturated fluid per barrel of residual oil. The oil density and the properties of the evolved gases were measured at each point during the differential pressure depletion and these data are included in the summary of the differential depletion data on page eight.

The viscosity of the reservoir fluid was measured over a wide range of pressures at 130°F. in a rolling ball viscosimeter. The viscosity of the fluid was found to vary from a minimum of 0.77 centipoise at the saturation pressure to a maximum of 1.92 centipoise at atmospheric pressure. The results of the viscosity measurements are tabulated on page fifteen.

One multi-stage separator test was performed to measure gas-oil ratio, stock tank oil gravity, and formation volume factor. The results of the separator test can be found on page eleven.

For your convenience, differential data has been adjusted to separator conditions. The results can be found on page twelve.

Thank you for the opportunity to be of service to Yates Petroleum Corporation. If you have any question or if we may be of further assistance in any way, please feel free to call upon us.

Very truly yours,

CORE LABORATORIES, a division of WESTERN ATLAS INTERNATIONAL, INC.

Richard Hulme Supervisor

Reservoir Fluid Lab

### File RFLM 90017

YATES PETROLEUM CORPORATION State CO #2

Date Sampled: December 1, 1989 Eddy County, New Mexico

Dagger Draw North Field

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Date Sampled: December 1, 1989

Flowing Tubing Pressure

### FORMATION CHARACTERISTICS

Formation Name	Canyon
Date First Well Completed	N/A
Original Reservoir Pressure	3010 psig @ 7572 ft.
Original Produced Gas/Liquid Ratio	N/A SCF/Bbl
Production Rate	N/A Bbls/Day
Separator Pressure and Temperature	N/A psig N/A°F.
Liquid Gravity at 60°F.	N/A °API
Datum	N/A ft. Subsea

### WELL CHARACTERISTICS

Elevation	3618 ft. KB, 3605 ft. GL
Total Depth	9427 ft. TD 8800 ft. PBTD
Producing Interval	7751-7843 ft.
Tubing Size and Depth	2 7/8 In. to 7699 ft.
Open Flow Potential	409 BOPD,817 MCFD,979 BWPD
Last Reservoir Pressure	2000 psig @ N/A ft.
Date	N/A
Reservoir Temperature	130°F. @ 7565 ft.
Status of Well	N/A
Pressure Gauge	N/A

### SAMPLING CONDITIONS

331 psig

	1		
Flowing Bottom Hole Pressure	931 psig		
Primary Separator Pressure	67 psig		
Primary Separator Temperature	100°F.		
Secondary Separator Pressure	29 psig	•	
Secondary Separator Temperature	108°F.		
Field Stock Tank Liquid Gravity	44.5°API	@ 60°F.	
Primary Separator Gas Production	Rate 709.711 I	MSCF/Day	
Pressure Base	15.025 psia		
Temperature Base	60°F.		
Compressibility Factor (Fpv)	1.000		
Gas Gravity (Laboratory)	0.737		
(- 5)	1.000		
Stock Tank Liquid Production Rate	e <b>0</b> 60°F.	735.55	Bbls/Day
Primary Separator Gas/Stock Tank	Liquid Ratio	965	SCF/Bbl

Sampled by REMARKS:

Tefteller Inc.



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### SUMMARY OF RESERVOIR FLUID PVT DATA

### Volumetric Data

Bubble point pressure (Pb) at 130°F. = 2003 psig

Thermal expansion of reservoir fluid at 5000 psig = V at 130°F. = 1.03111
V at 67°F.

Compressibility of reservoir fluid at 130°F. from 3000 psig to 2500 psig =  $9.45 \times 10^{-6} \text{ V/V/psi}$  from 2500 psig to 2003 psig =  $10.06 \times 10^{-6} \text{ V/V/psi}$ 

### Differential Vaporization Data

Solution gas/oil ratio at 2003 psig and 130°F. = 485 standard cubic feet of gas at 15.025 psia and 60°F. per barrel of residual oil at 60°F.

Relative oil volume at 2003 psig and 130°F. = 1.247 barrels of oil per barrel of residual oil at 60°F.

Density of reservoir fluid at 2003 psig and 130°F. = 0.7177 qm/cc

### Viscosity Data

Viscosity of reservoir fluid at 2003 psig and 130°F. = 0.77 centipoise

### Separator Test Data

Separator Conditions Bo(1) Rs(2) API at 60°F.

67 psig and 100°F.

to
29 psig and 110°F.

to
0 psig and 68°F. 1.233 430 42.7

- (1) Formation volume factor, barrels of oil at 2003 psig and 130°F. per barrel of stock tank oil at 60°F.
- (2) Total solution gas/oil ratio at 2003 psig and 130°F., total standard cubic feet of gas at 15.025 psia and 60°F. per barrel of stock tank oil at 60°F.



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### SUMMARY OF QUALITY CONTROL DATA OF SEPARATOR LIQUID SAMPLES

Cylinder Number	Sampling Conditions Pressure, PSIG	Temperature,	Laboratory <u>Bubble point</u> Pressure, <u>PSIG</u>	Temperature,
1*	28	108	20	68
2	28	108	18	68

<sup>\*</sup> Selected for use in study.



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### HYDROCARBON ANALYSIS OF RESERVOIR FLUID SAMPLE

Component	Mol <u>Percent</u>	Weight <u>Percent</u>	Density	API	Mol <u>Weight</u>
Hydrogen Sulfide	0.00	0.00			
Carbon Dioxide	0.34	0.14			
Nitrogen	0.18	0.05			
Methane	37.33	5.56			
Ethane	4.96	1.38			
Propane	3.43	1.40			
iso-Butane	1.03	0.56			
n-Butane	2.36	1.27			
iso-Pentane	1.27	0.85			
n-Pentane	1.43	0.96			
Hexanes	1.33	1.04			
Heptanes plus	46.34	86.79	0.8240	40.1	202.
	100.00	100.00			

Sample Molecular Weight = 107.8



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### HYDROCARBON ANALYSIS OF SEPARATOR GAS SAMPLE

	Mol	
Component	<u>Percent</u>	<u>GPM</u>
Hydrogen	0.00	
Hydrogen Sulfide	1.24	
Carbon Dioxide	0.74	
Nitrogen	0.39	
Methane	80.17	
Ethane	8.43	2.242
Propane	4.38	1.200
iso-Butane	0.94	0.306
n-Butane	1.77	0.555
iso-Pentane	0.56	0.204
n-Pentane	0.53	0.191
Hexanes	0.42	0.162
Heptanes	0.29	0.121
Octanes	0.12	0.054
Nonanes	0.01	0.005
Decanes	0.00	0.000
Undecanes	0.01	0.006
Dodecanes	0.00	0.000
	100.00	5.046

Calculated Gas Gravity = 0.737

Calculated Gross Heating Value = 1248 BTU per cubic foot of dry gas at 15.025 and 60°F.

Collected at 67 psig and 99°F.



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### VOLUMETRIC DATA OF RESERVOIR FLUID SAMPLE

Saturation pressure (bubble point pressure) = 2003 PSIG 130°F.

Specific volume at saturation pressure = 0.02223 ft <sup>3</sup>/lb @ 130°F.

Thermal expansion @ 5000 PSIG = 1.03111 V @ 130°F./V @ 67°F.

Compressibility @ 130°F.:

From 5000 PSIG to 4000 PSIG =  $7.65 \times 10^{-6} \text{ V/V/PSI}$ From 4000 PSIG to 3000 PSIG =  $9.29 \times 10^{-6} \text{ V/V/PSI}$ From 3000 PSIG to 2500 PSIG =  $9.45 \times 10^{-6} \text{ V/V/PSI}$ From 2500 PSIG to 2003 PSIG =  $10.06 \times 10^{-6} \text{ V/V/PSI}$ 



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PRESSURE-VOLUME RELATIONS OF RESERVOIR FLUID AT 130°F.

(Constant Composition Expansion)

Pressur	e l	Relative	Y		Density
PSIG		Volume(1)	Functi	on(2)	_Gm/cc
				<del></del>	
5000		0.9736			0.7372
4500		0.9771			0.7345
4000		0.9811			0.7315
3500		0.9856			0.7282
3000		0.9903			0.7247
2500		0.9950			0.7213
2400		0.9961			0.7205
2300		0.9972		•	0.7197
2200		0.9981			0.7191
2100		0.9992			0.7183
2003	Pb	1.0000			0.7177
1971		1.0029			
1948		1.0050			
1925		1.0070			
1900		1.0091			
1858		1.0205			
1760		1.0448	3.	057	
1600		1.0855	2.	918	
1422		1.1462	2.	766	
1249		1.2286	2.	609	
1088		1.3355	2.	473	
955		1.4590	2.	354	
869		1.5631	2.	278	
765		1.7274	2.	182	
683		1.8929	2.	118	
533		2.3541	1.	981	
410		3.0023	1.	872	
300		4.0356	1.	781	

(1) Relative Volume: V/Vsat is barrels at indicated pressure barrel at saturation pressure.



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## DIFFERENTIAL VAPORIZATION AT 130°F

Incremental Gas Gravity	0.651 0.651 0.652 0.655 0.659 0.667 0.768 0.768		
Gas Formation Volume Factor(4)	0.00790 0.00899 0.01040 0.01231 0.01500 0.02570 0.03894 0.07707		,
Deviation Factor, Z	0.841 0.852 0.853 0.877 0.909 0.927 0.948 0.972		
oil Density, Gm/Cc	0.7177 0.7218 0.7269 0.7323 0.7382 0.7442 0.7507 0.7507 0.7577 0.7743 0.7743		ļ
Relative Total Volume(3)	1.247 1.288 1.344 1.530 1.530 1.974 2.463 3.545 6.699		
Relative Oil Volume, Bod(2)	1.247 1.233 1.217 1.182 1.163 1.097 1.071 1.035	n = 1.000	
Solution Gas/Oil Ratio,Rsd(1)	485 446 406 326 326 132 132 37	at 60°F =	•
Pressure, psig	2003 1800 1600 1200 1000 800 600 200 85		

Gravity of Residual Oil = 42.5°API @ 60°F.

£0.00

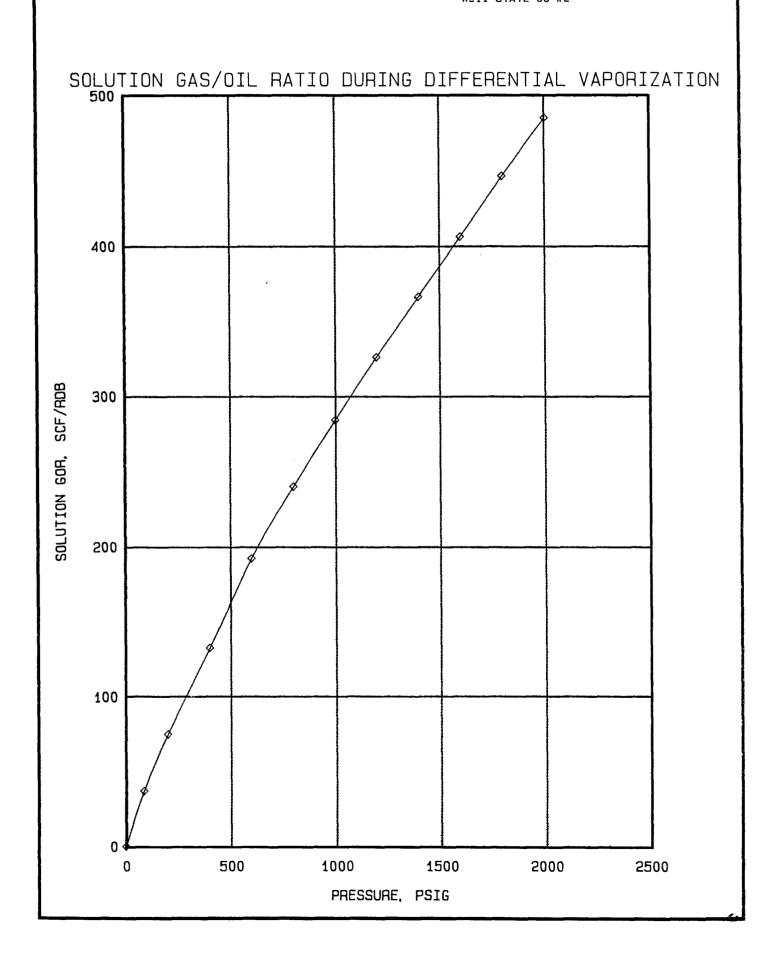
Cubic feet of gas at 15.025 psia and 60°F. per barrel of residual oil at 60°F.

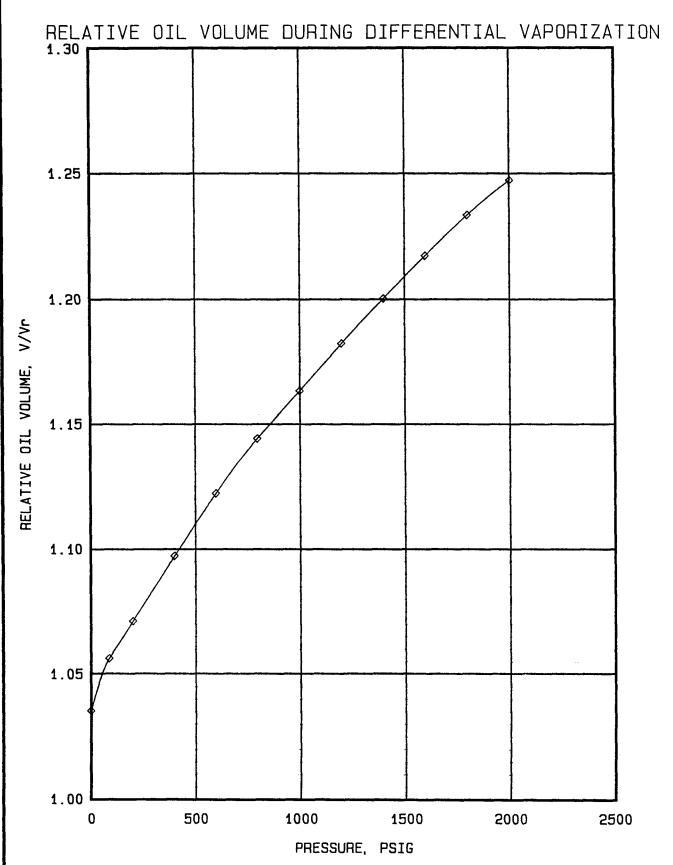
Barrels of oil at indicated pressure and temperature per barrel of residual oil at 60°F.

Barrels of oil plus liberated gas at indicated pressure and temperature per barrel of residual oil at 60°F.

Oubic feet of gas at indicated pressure and temperature per cubic foot at 15.025 psia and 60°F.

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Page 11 of 17 File RFIM 90017 State  $\infty$  #2

# SEPARATOR TEST OF RESERVOIR FILLID SAMPLE

Specific Gravity of Flashed Gas	0.724	0.868*	1.148	
Separator Volume Factor (4)	1.048	1.054	1.004	
Formation Volume Factor, Bofb(3)			1.233	
Stock Tank Gravity, API @ 60°F			42.7	
Gas/Oil Ratio (2)	404	ĸ	23	Rsfb = 430
Gas/Oil Ratio (1)	386	ю	23	Rsf
Separator Temperature,	100	110	89	
Separator Pressure, PSI Gauge	to 92	23	0	

\* Theoretical value

Gas/Oil Ratio in cubic feet of gas 0 60°F. and 15.025 PSI absolute per barrel of oil 0 indicated pressure and temperature. <del>(</del>1

Gas/Oil Ratio in cubic feet of gas @ 60°F. and 15.025 PSI absolute per barrel of stock tank oil @ 60°F. Formation Volume Factor is barrels of saturated oil @ 2003 PSI gauge and 130°F. per barrel of stock tank oil ®®

Separator Volume Factor is barrels of oil @ indicated pressure and temperature per barrel of stock tank oil @ 60°F. (4)

The analyses, opinons or interpretations contained in this report are based upon observations and material supplied by the client for whose exclusive and confidential use this report has been made. The interpretations or opinons expressed the best judgement of Core Laboratories. Gore Laboratories assumes no responsibility and makes no warranty or representations, express or implied, as to the productivity, proper operations, or profitableness however of any oil, gas, coal or other material, property, well or sand in connection with which such report is used or relied upon for any reason whatsoever.



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### DIFFERENTIAL VAPORIZATION DATA ADJUSTED TO SEPARATOR CONDITIONS\*

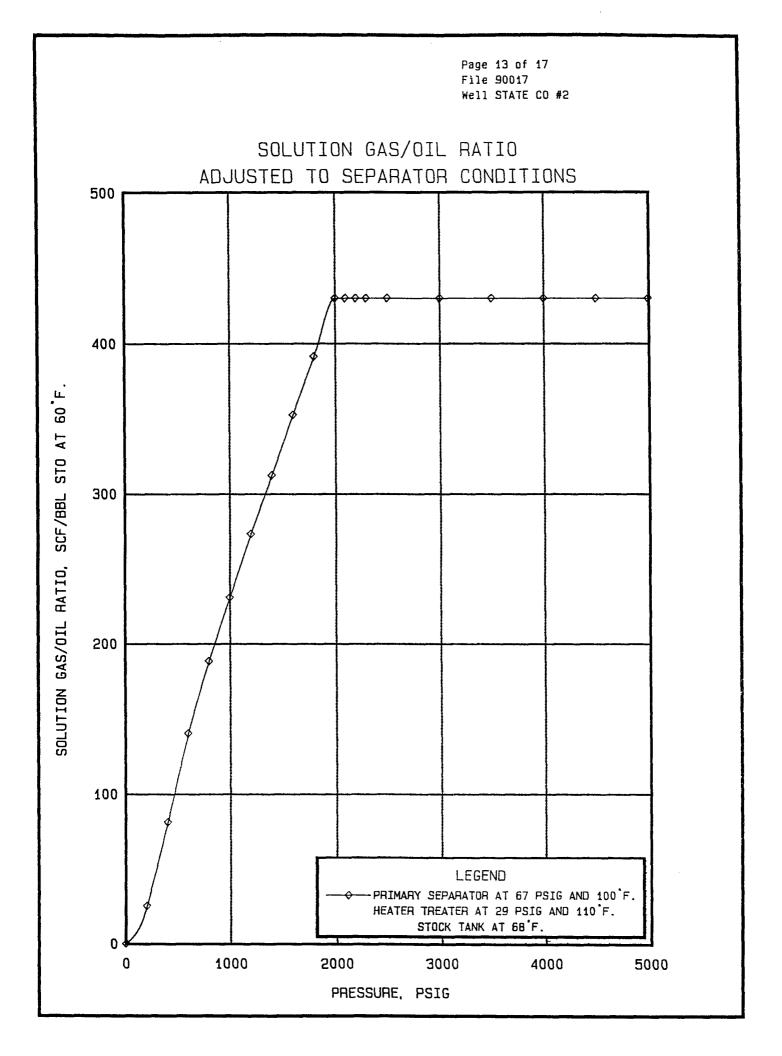
Pressure, psig	Solution Gas/Oil Ratio, Rs(1)	Formation Volume Factor, Bo(2)	Gas Formation Volume Factor, Bg(3)	Oil Density, gm/cc	Oil/Gas Viscosity Ratio
5000	430	1.200		0.7372	
4500	430	1.205		0.7345	
4000	430	1.210		0.7315	
3500	430	1.215		0.7282	
3000	430	1.221		0.7247	
2500	430	1.227		0.7213	
2300	430	1.223		0.7197	
2200	430	1.231		0.7191	
2100	430	1.232		0.7183	
2003 Pb	430	1.233		0.7177	
1800	391	1.219	0.00790	0.7218	49.7
1600	352	1.203	0.00899	0.7269	54.5
1400	312	1.187	0.01040	0.7323	60.5
1200	273	1.169	0.01231	0.7382	66.7
1000	231	1.150	0.01500	0.7442	73.5
800	188	1.131	0.01901	0.7507	81.7
600	140	1.109	0.02570	0.7577	91.3
400	81	1.085	0.03894	0.7656	103.3
200	25	1.059	0.07707	0.7743	126.7
85	0	1.044	0.16826	0.7798	150.0
0	0	1.023			223.3

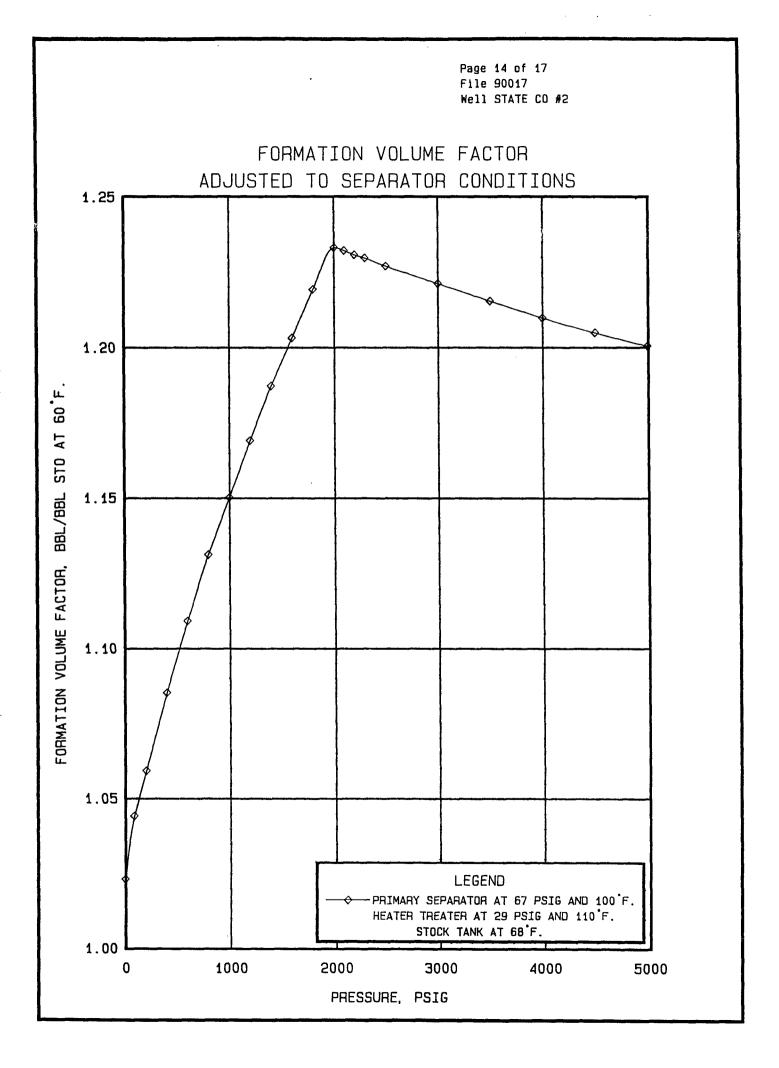
 $@ 60^{\circ}F. = 1.000$ 

Gravity of Stock Tank Oil = 42.7°API @ 60°F.

\*Separator Conditions: Separator at 67 psig and 100°F., Heater Treater at 29 psig and 110°F., stock tank at 68°F.

- (1) Cubic feet of gas at 15.025 psia and 60°F. per barrel of stock tank oil at 60°F.
- (2) Barrels of oil at indicated pressure and 130°F. per barrel of stock tank oil at 60°F.
- (3) Cubic feet of gas at indicated pressure and 130°F. per cubic foot at 15.025 psia and 60°F.





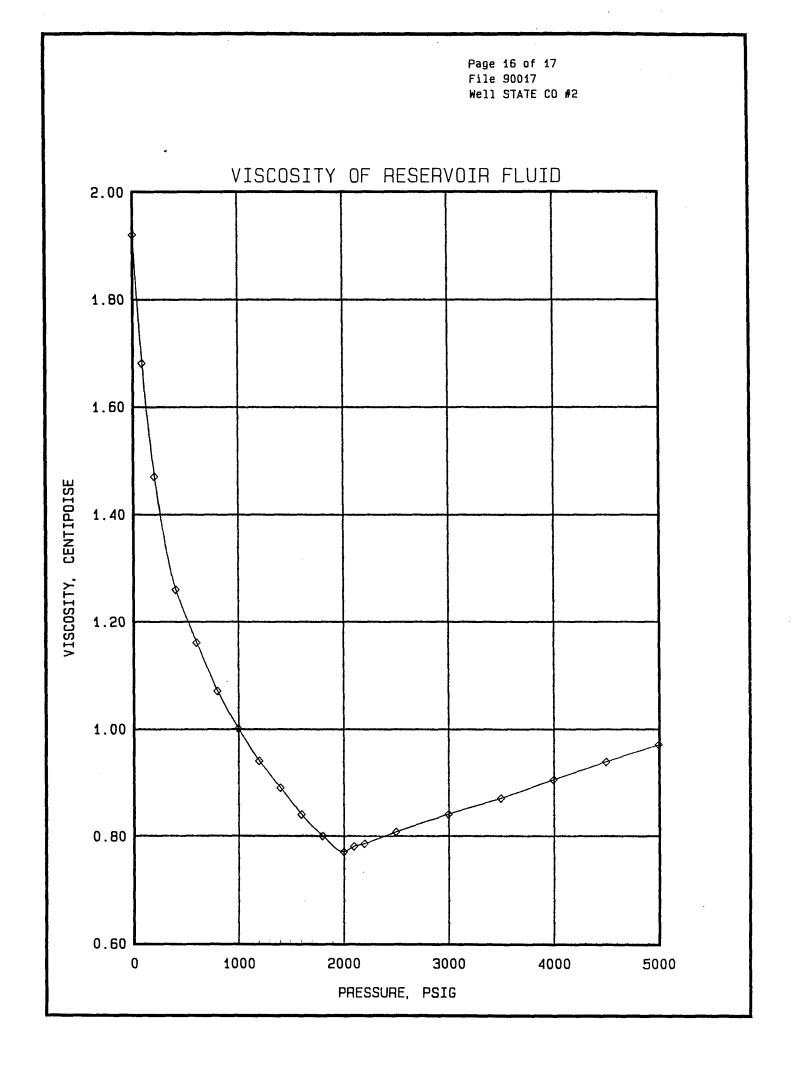


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### VISCOSITY DATA AT 130°F

Pressur psig	e,	Oil Viscosity Centipoise	Calculated Gas Viscosity, Centipoise	Oil/Gas Viscosity <u>Ratio</u>
5000		0.97		
4500		0.94		
4000		0.90		
3500		0.87		
3000		0.84		
2500		0.80		
2200		0.78		
2100		0.78		
2003	Pb	0.77		
1800		0.80	0.0161	49.7
1600		0.84	0.0154	54.5
1400		0.89	0.0147	60.5
1200		0.94	0.0141	66.7
1000		1.00	0.0136	73.5
800		1.07	0.0131	81.7
600		1.16	0.0127	91.3
400		1.26	0.0122	103.3
200		1.47	0.0116	126.7
85		1.68	0.0112	150.0
0		1.92	0.0086	223.3





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### NOMENCLATURE AND EQUATIONS TO ADJUST DIFFERENTIAL VAPORIZATION DATA TO SURFACE CONDITIONS

Pb = Bubble point pressure

Bo = Oil formation volume factor

Bofb = Formation volume factor from field conditions (or optimum)
 separator flash test.

Bob = Relative oil volume from differential vaporization test.

Bodb = Value of Bod at the bubble point pressure.

R.V. = Relative volume from pressure-volume relations test.

For Bo above the bubble point pressure:

Bo =  $R.V. \times Bofb$ 

For Bo below the bubble point pressure:

Bo = (Bod)(Bofb/Bodb)

- Rs = Gas in solution, standard cubic feet per barrel of stock tank oil.
- Rsfb = Sum of separator gas and the stock tank gas from field conditions (or optimum) separator flash test, standard cubic feet per barrel of stock tank oil.
- Rsd = The gas in solution from the differential vaporization test.
- Rsdb = The value of Rsd at the bubble point pressure.

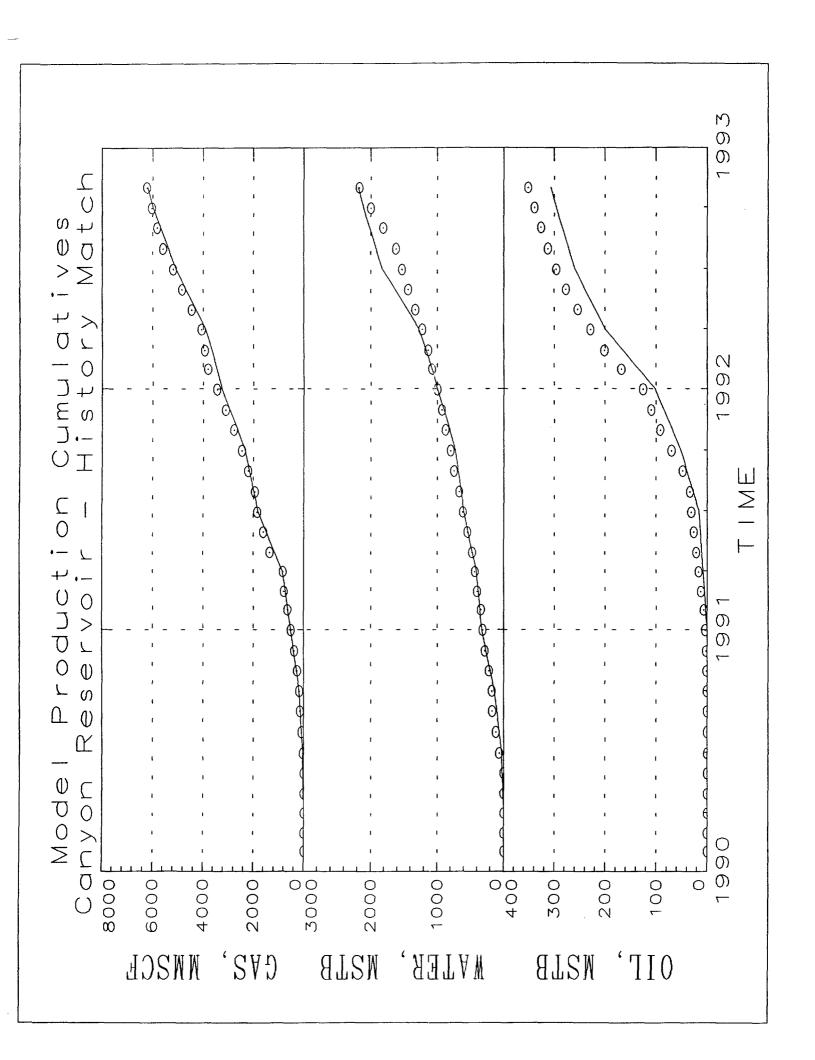
Rs - Rsfb - [(Rsdb - Rsd)(Bofb/Bodbl)]

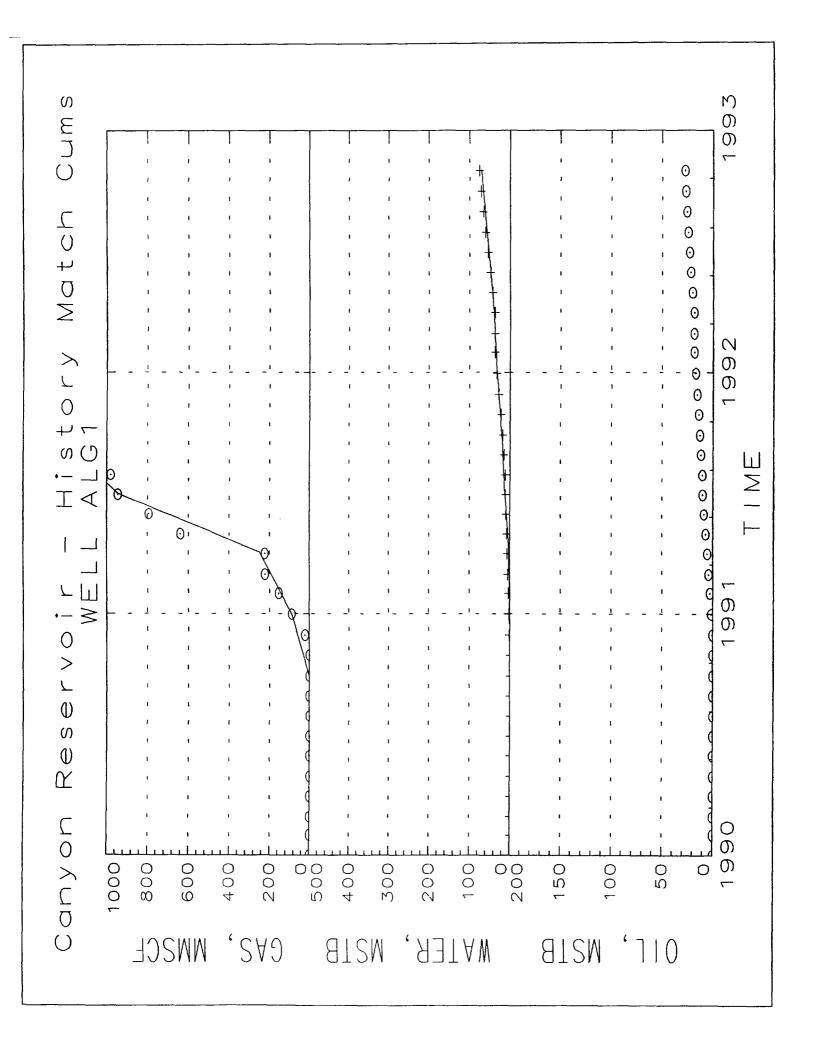
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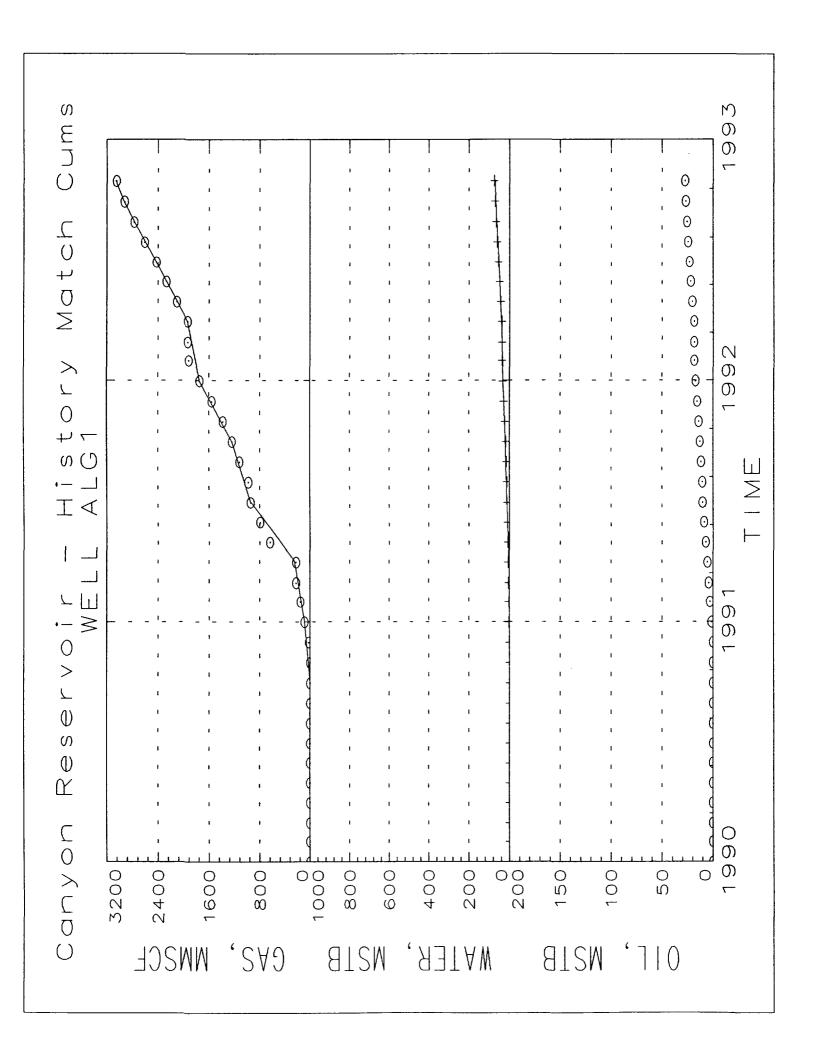
### APPENDIX IV

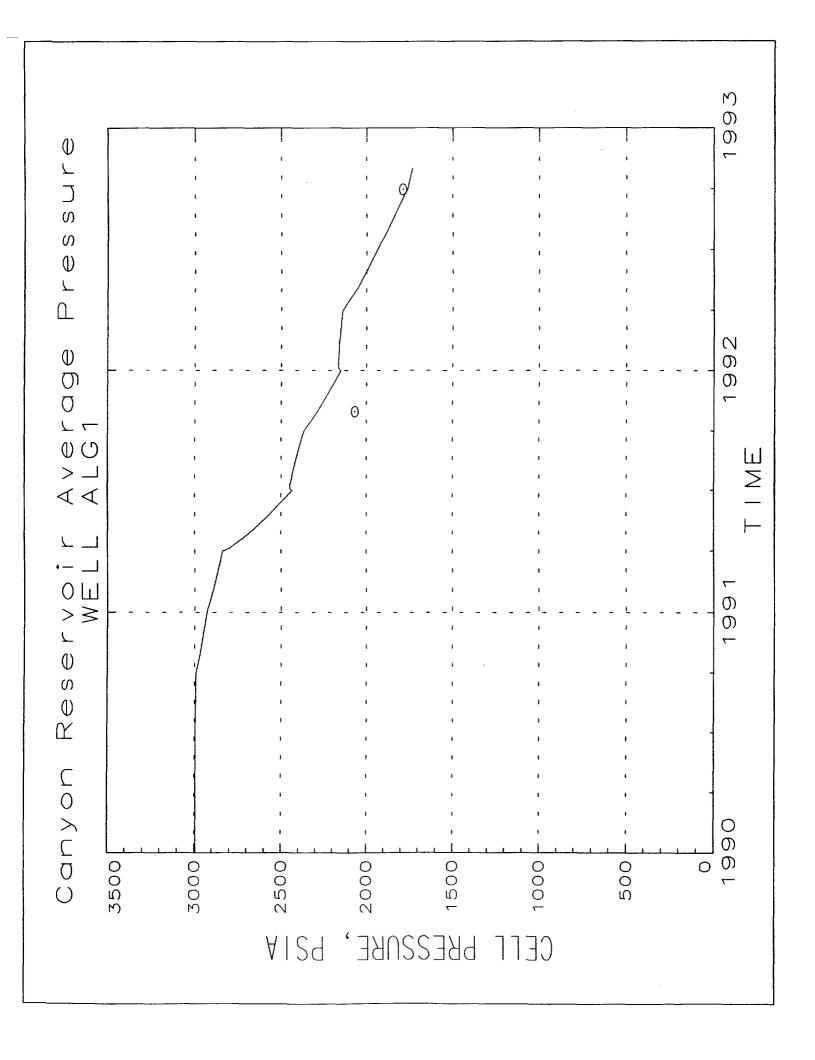
### **HISTORY MATCH**

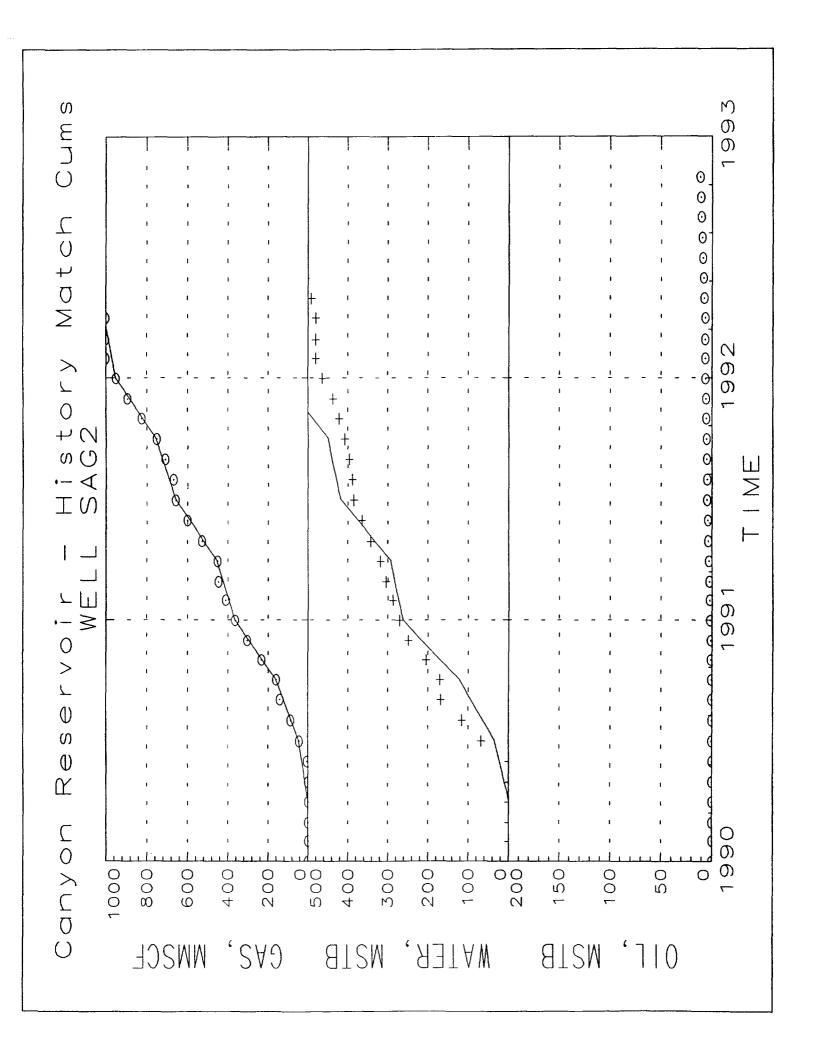
Model Performance Plot Well Performance Plots

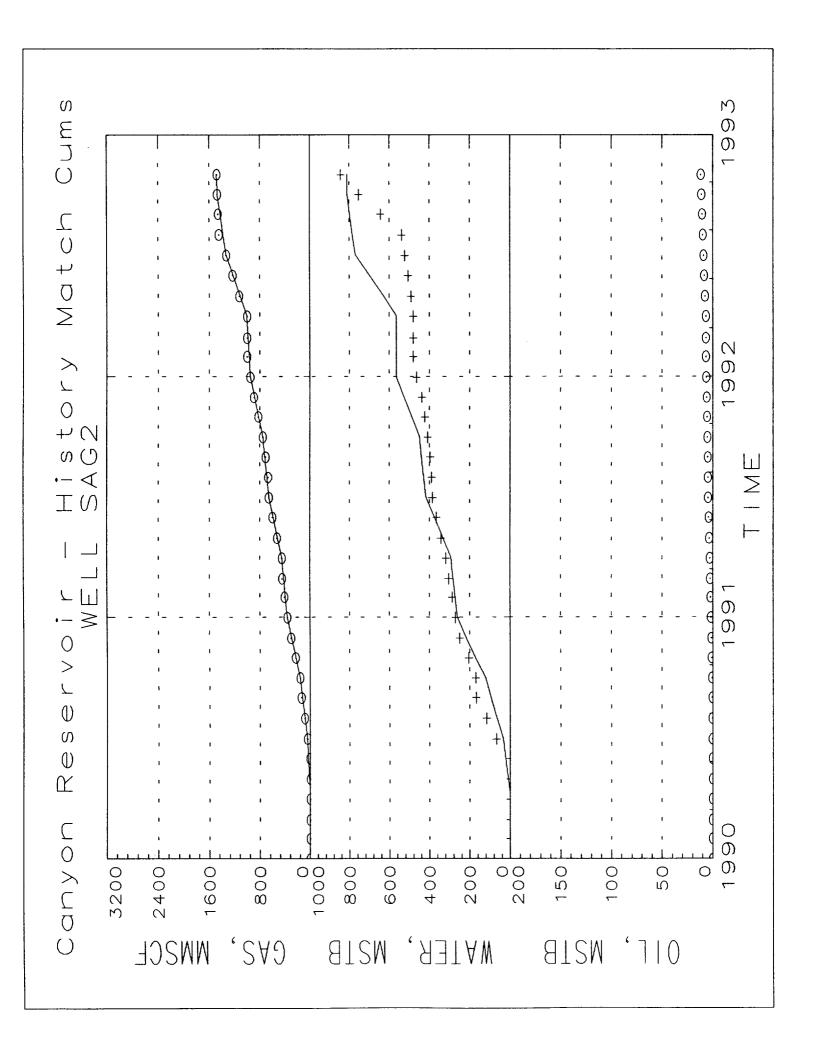


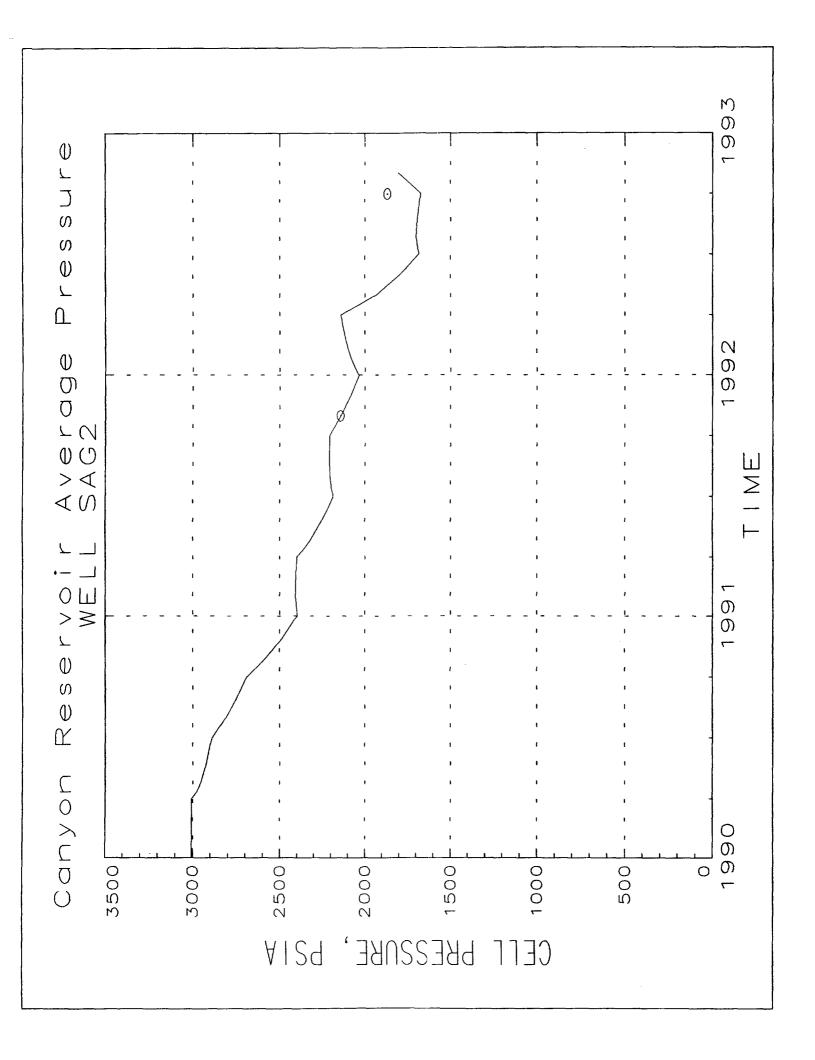


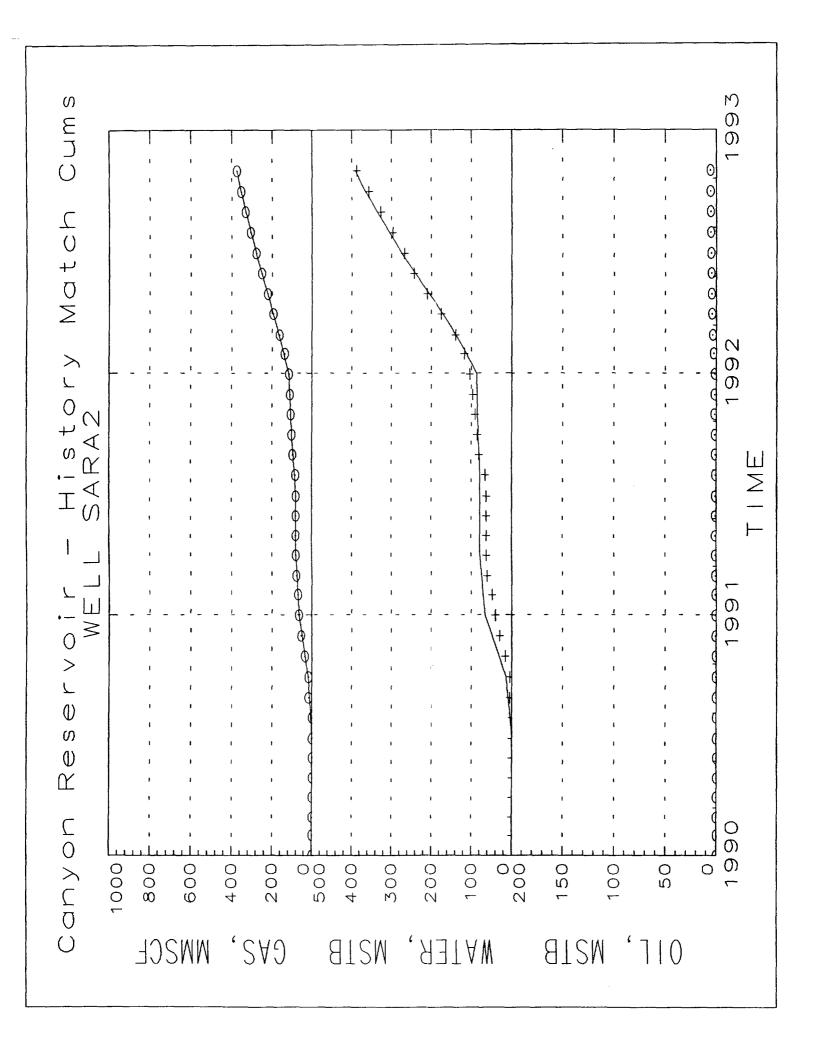


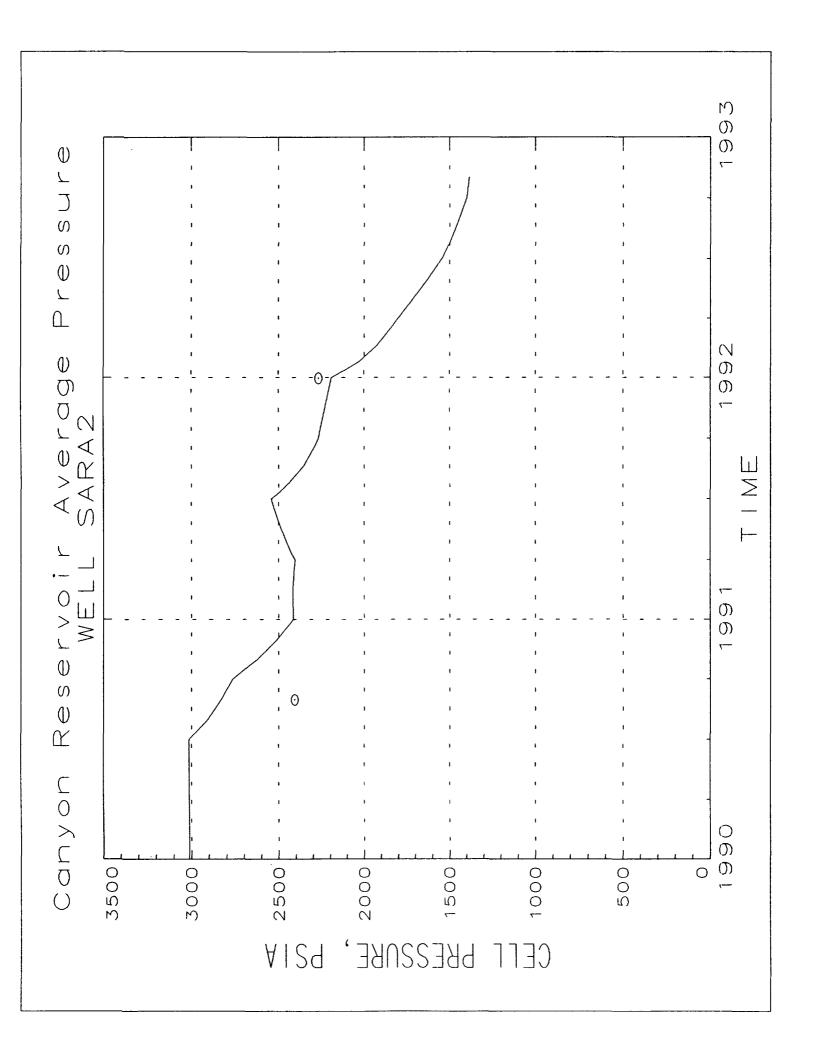


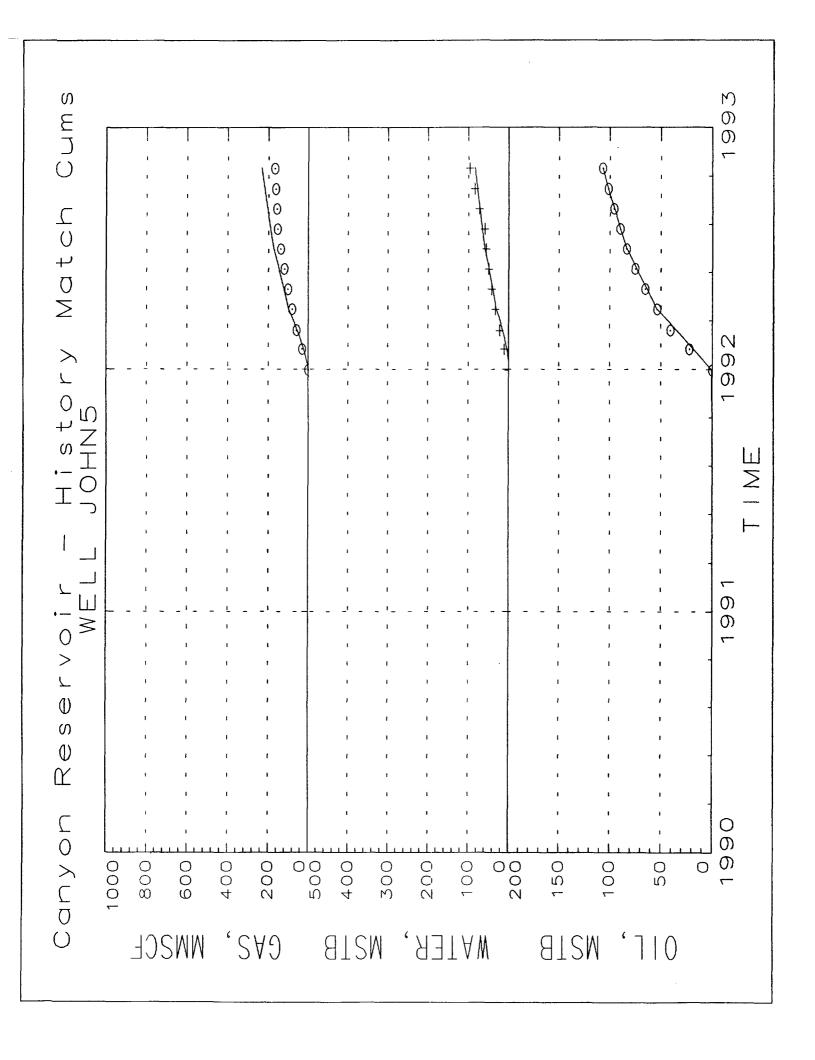


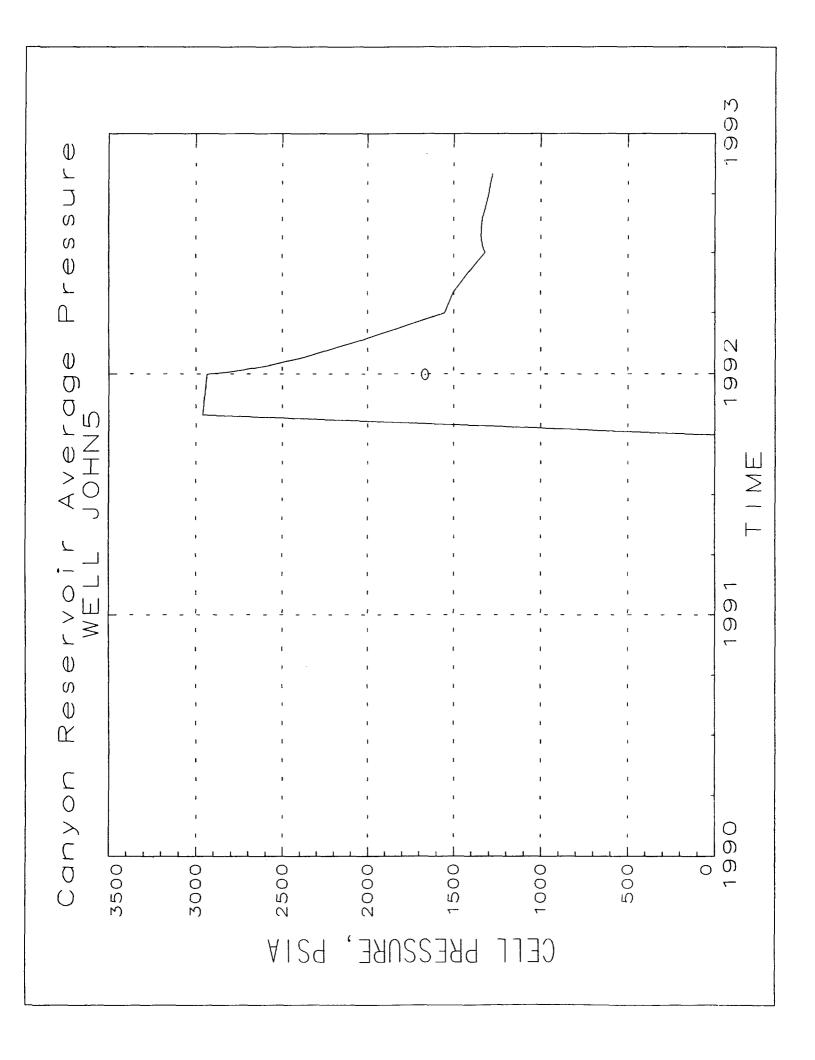


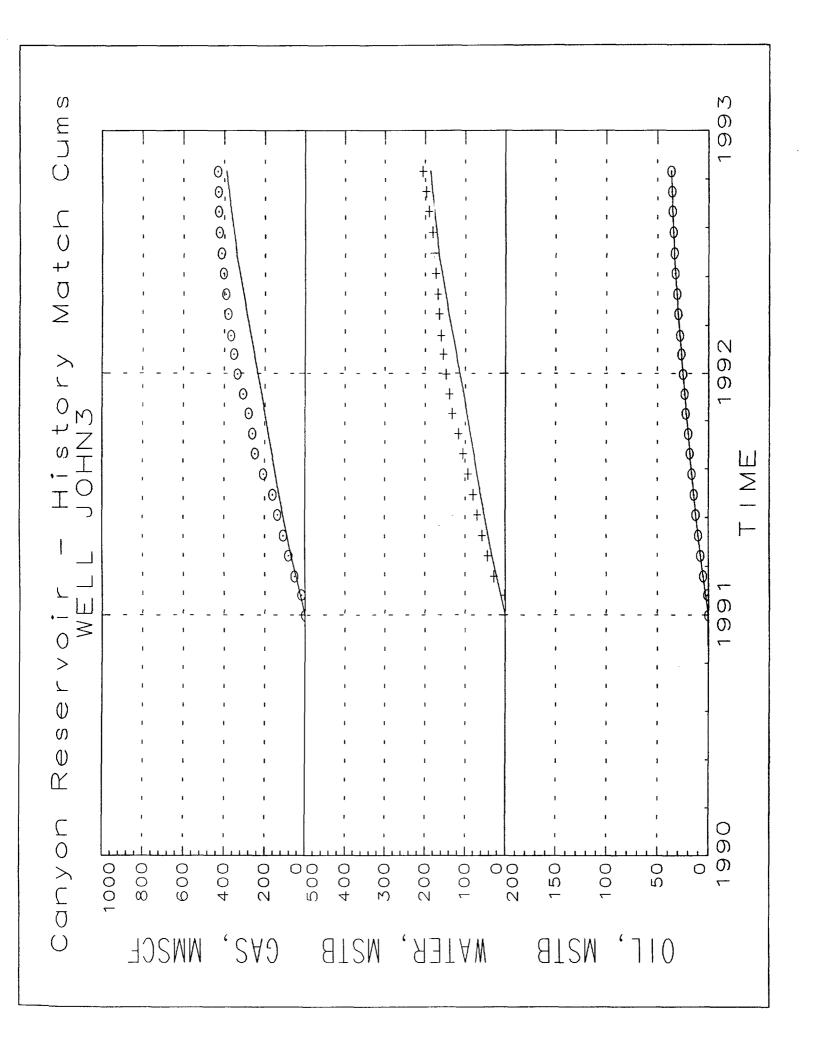


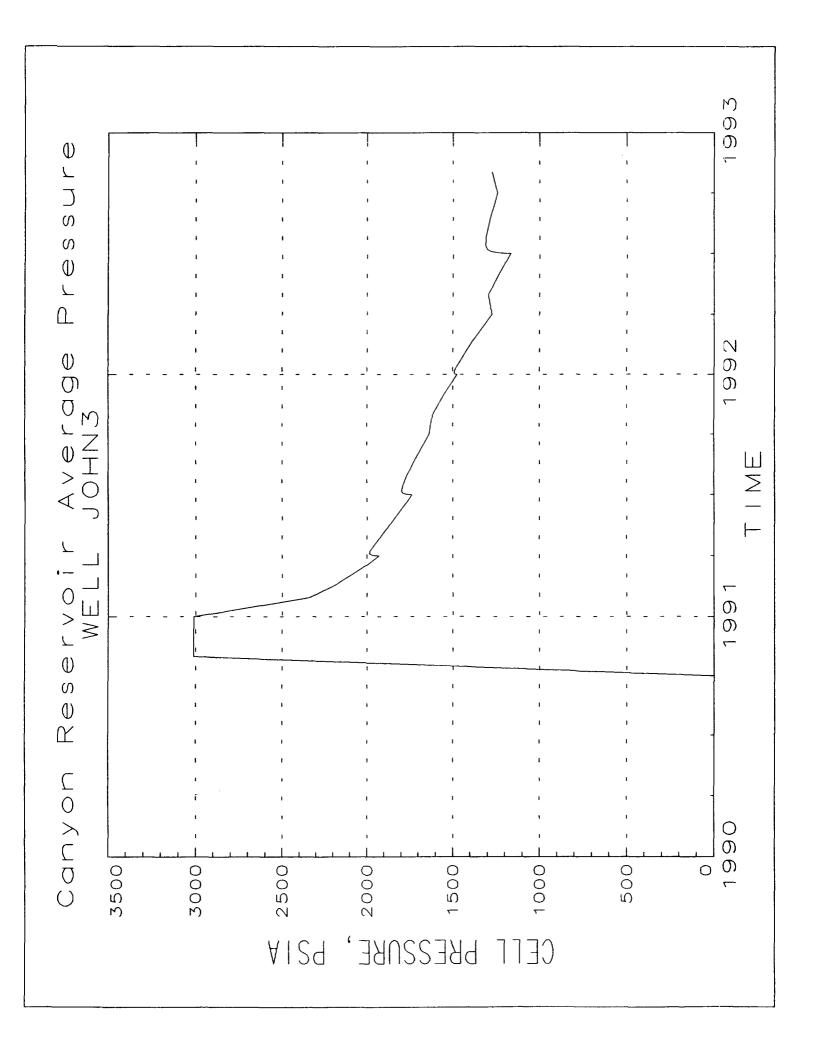


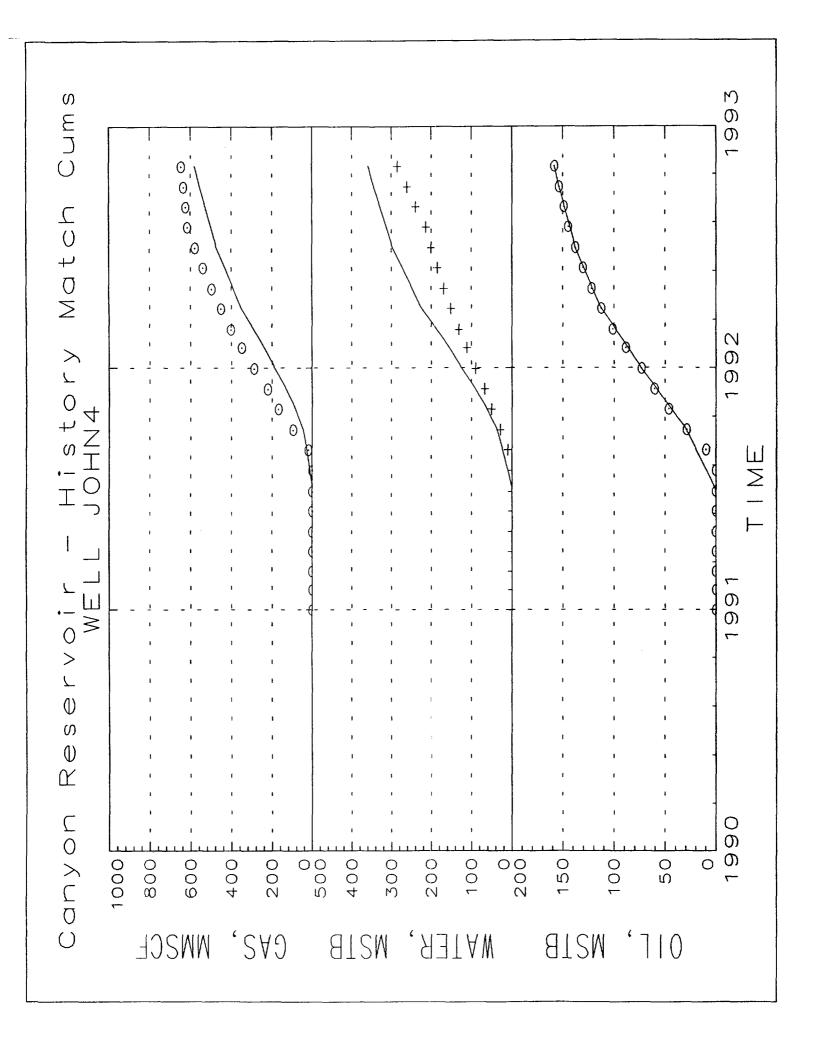


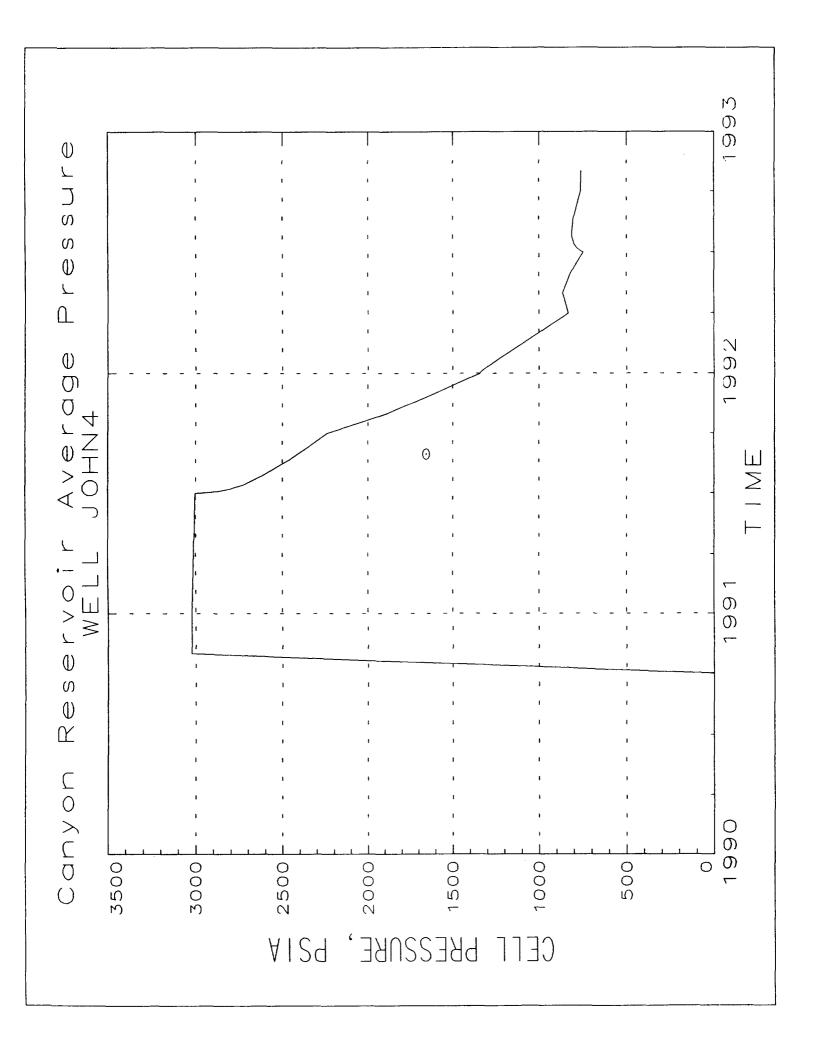


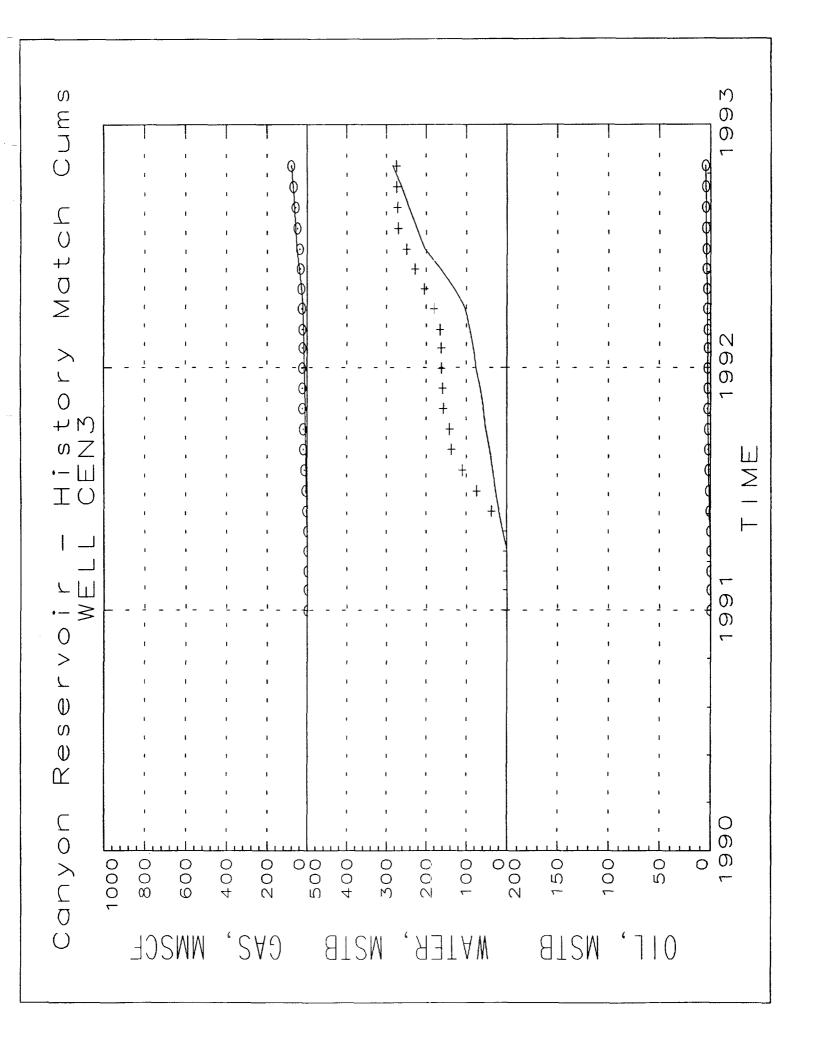


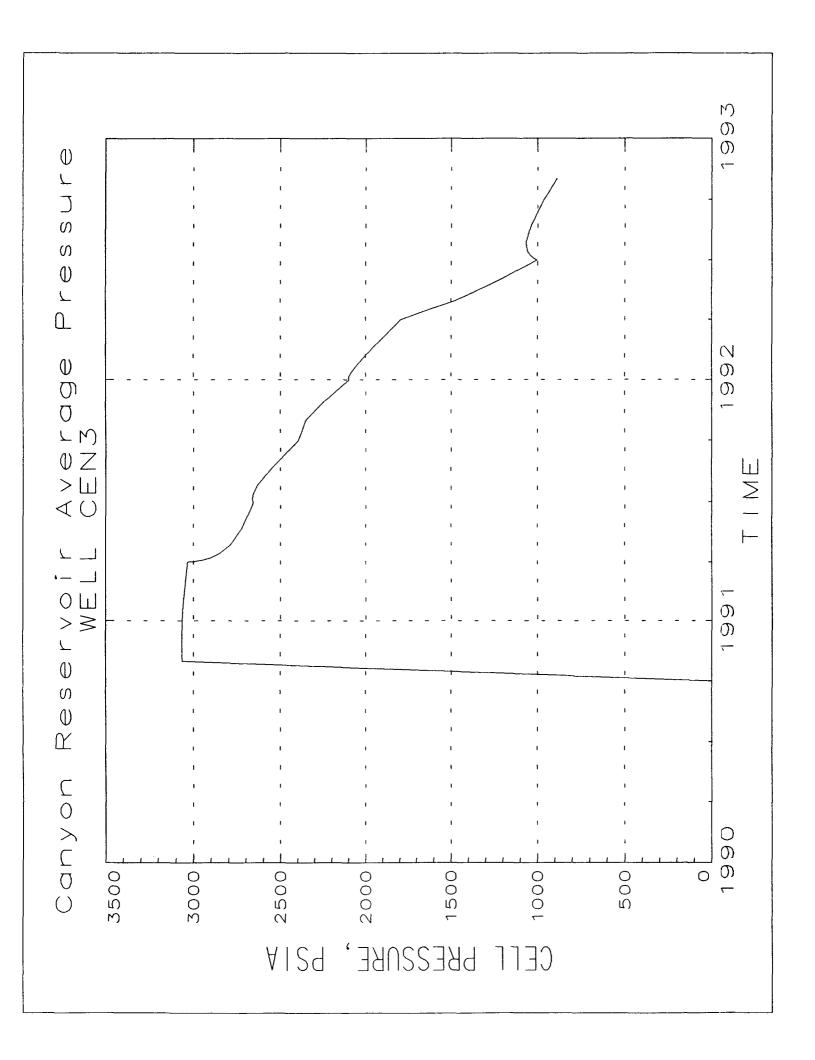










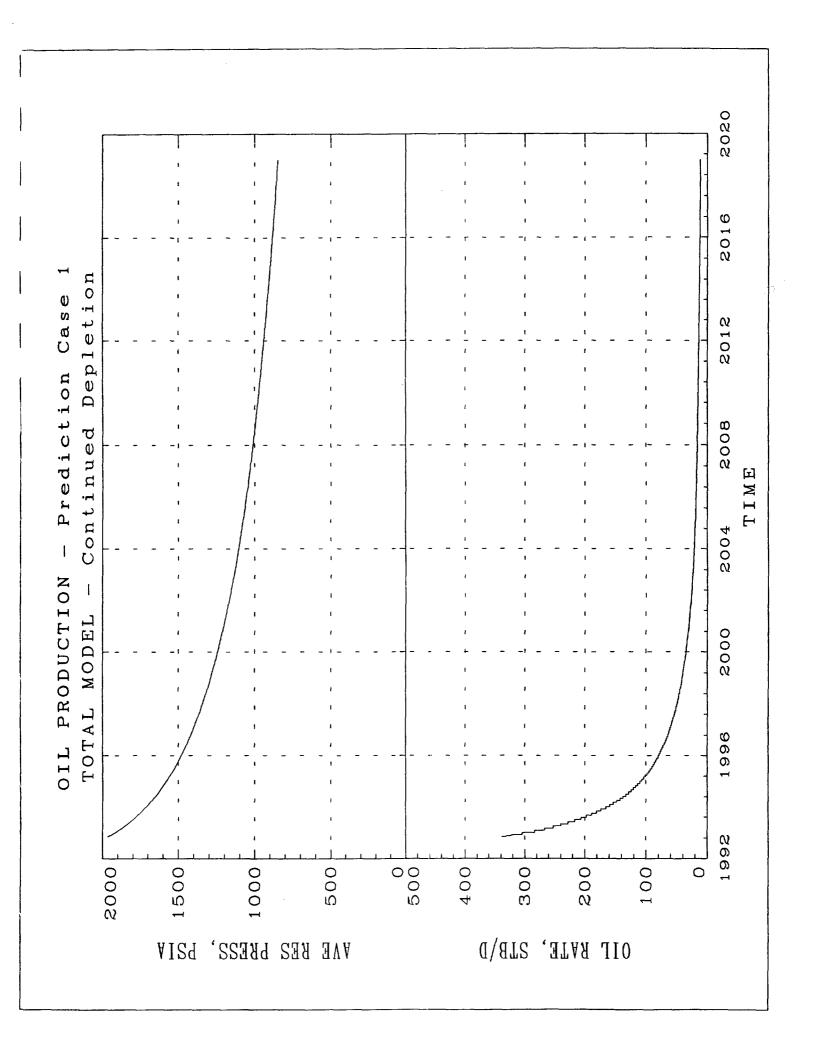


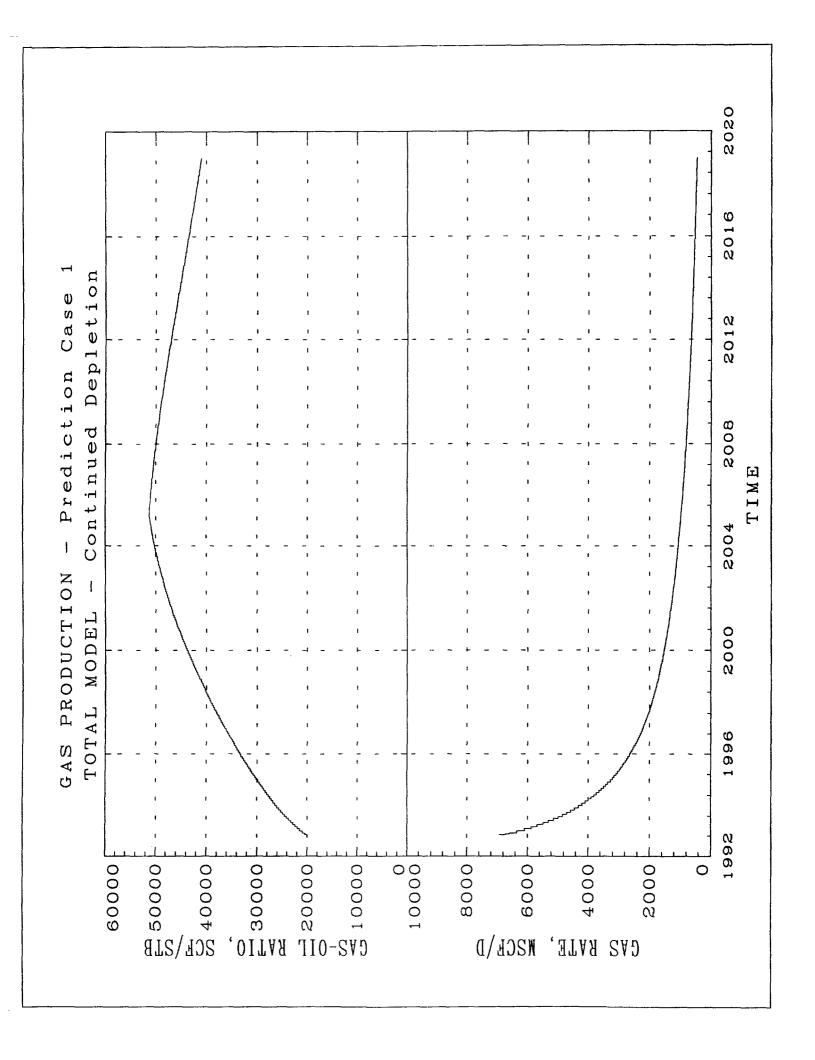
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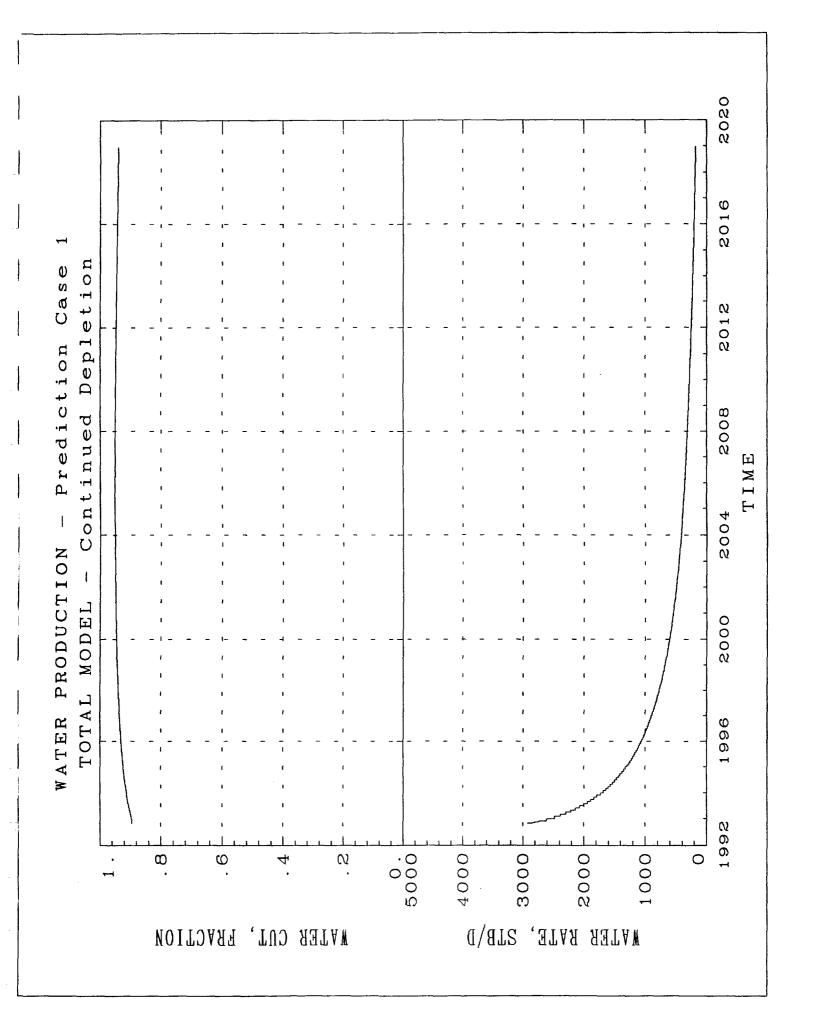
### APPENDIX V

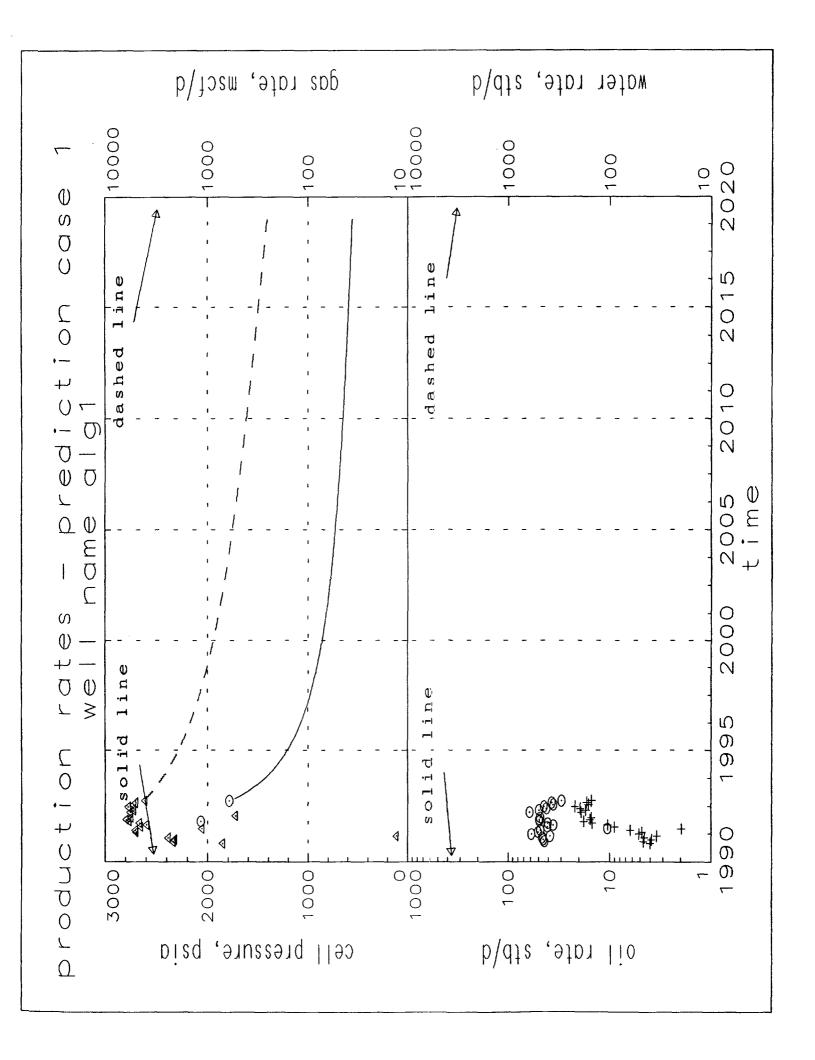
#### PREDICTION CASE 1

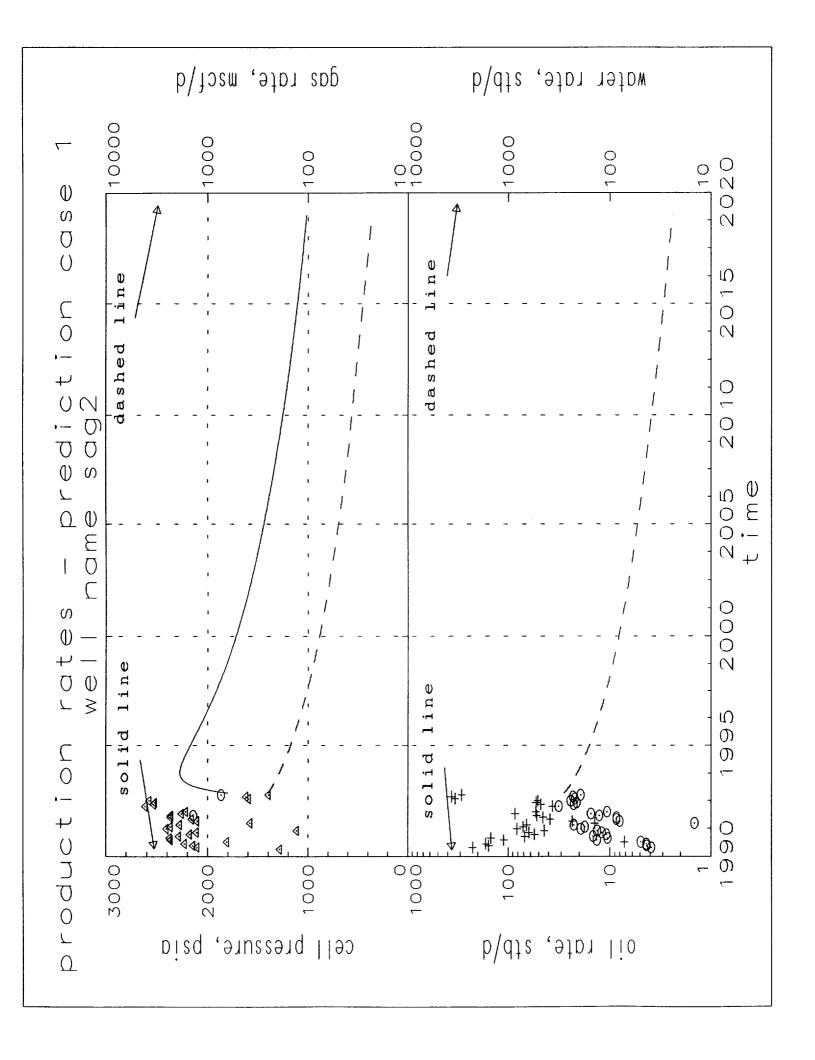
Model Performance Plots
Well Performance Plots

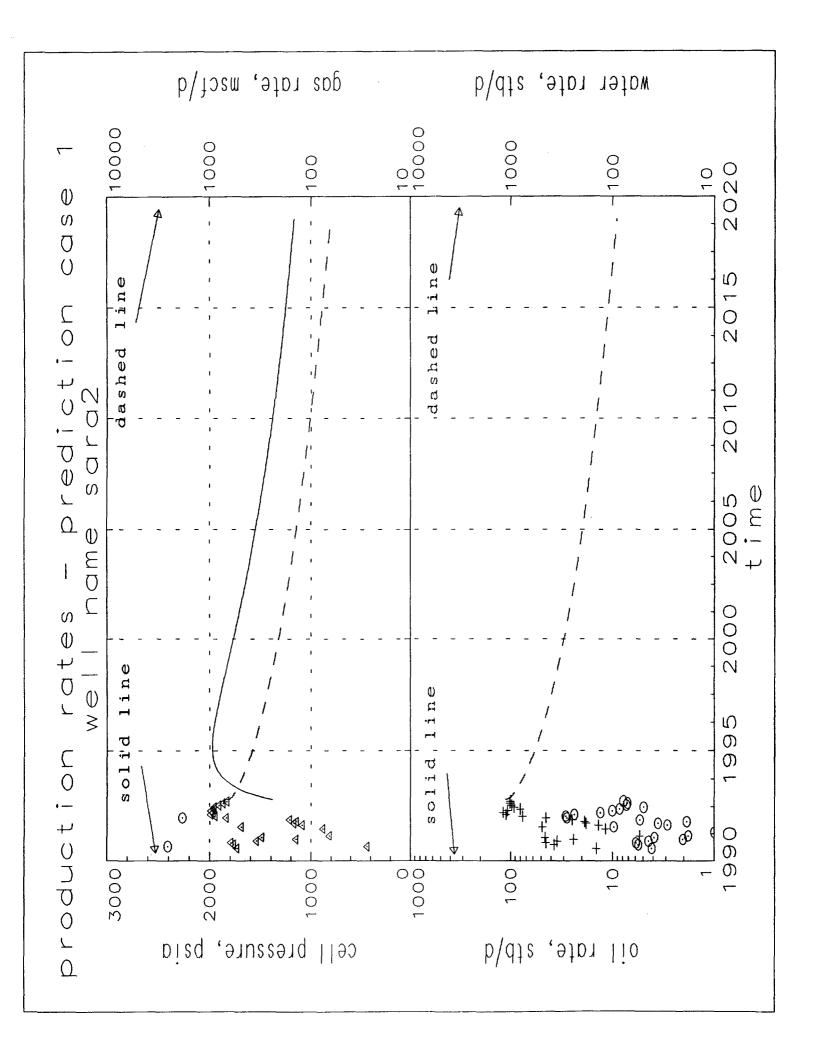


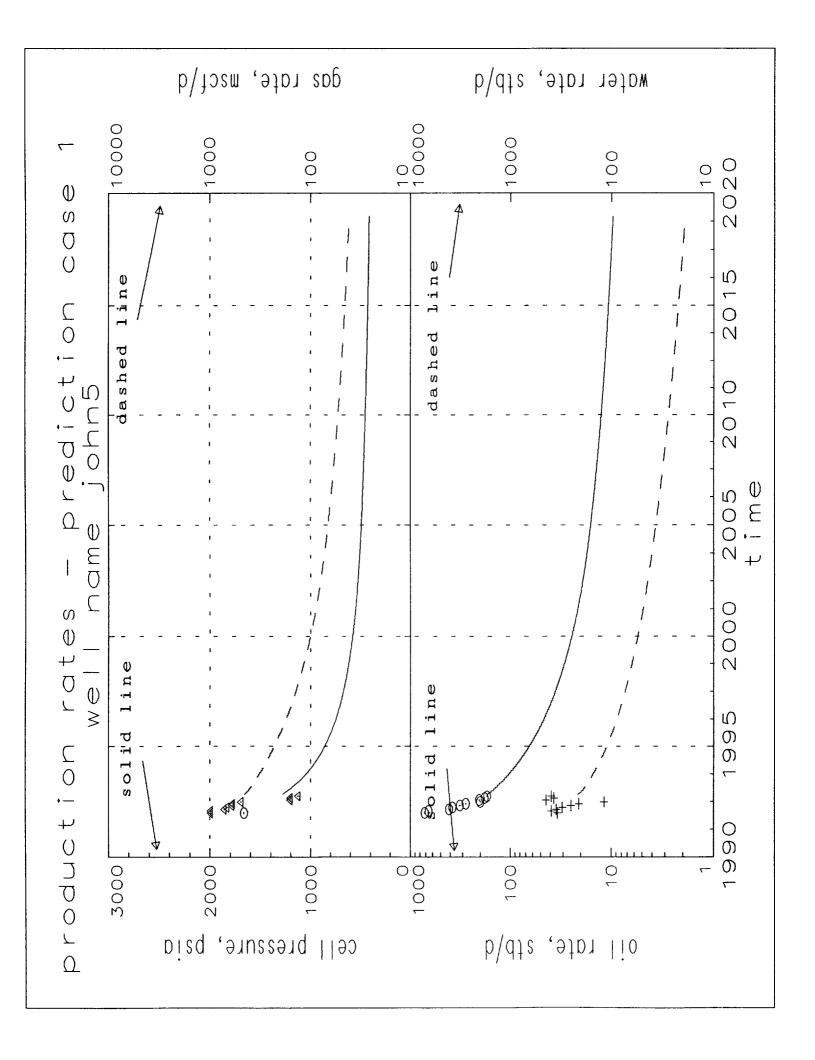


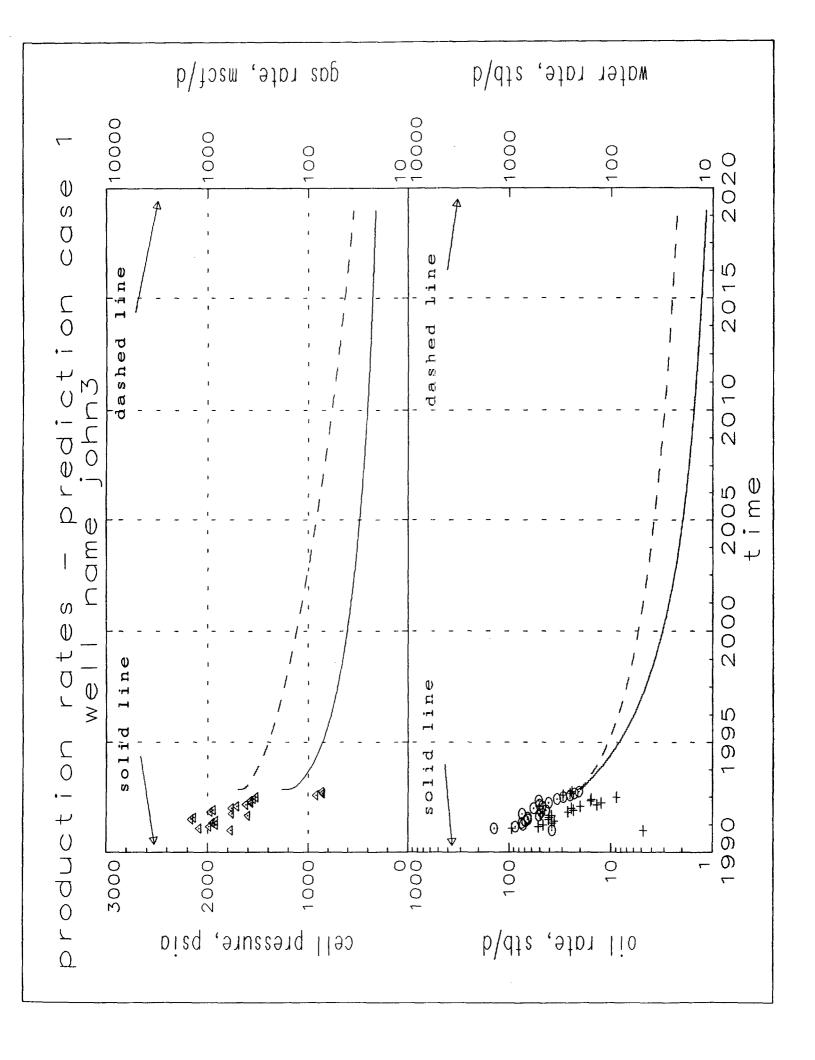


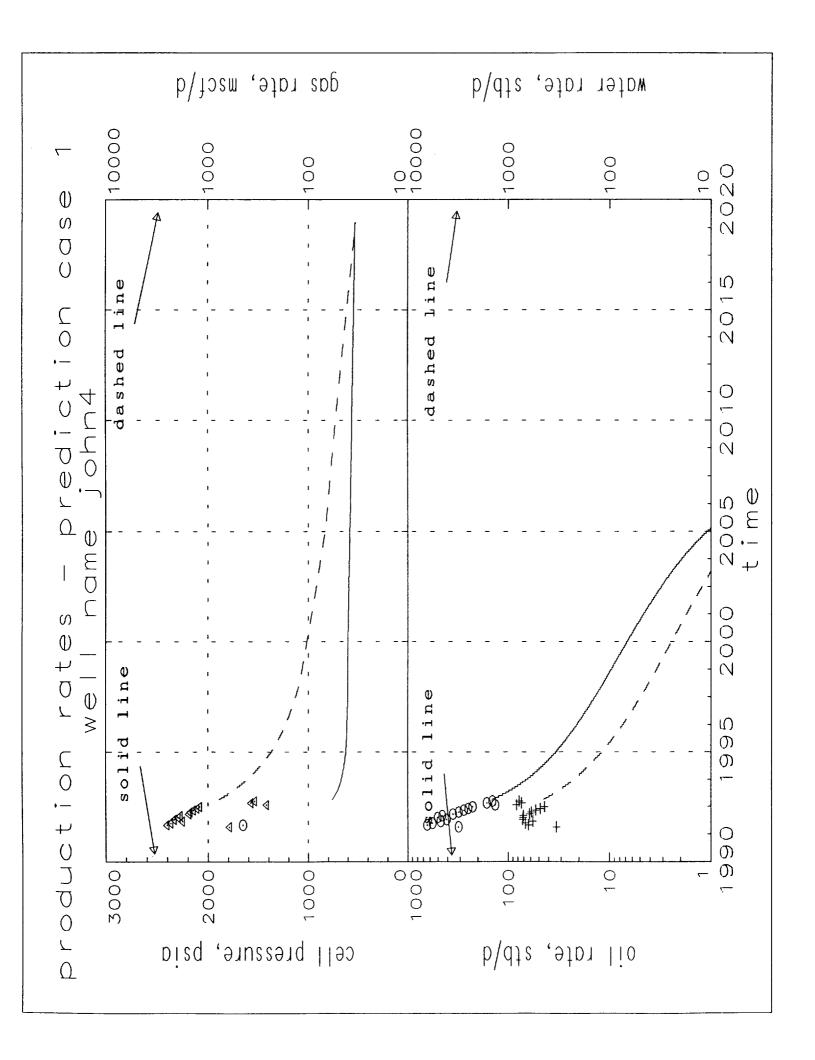


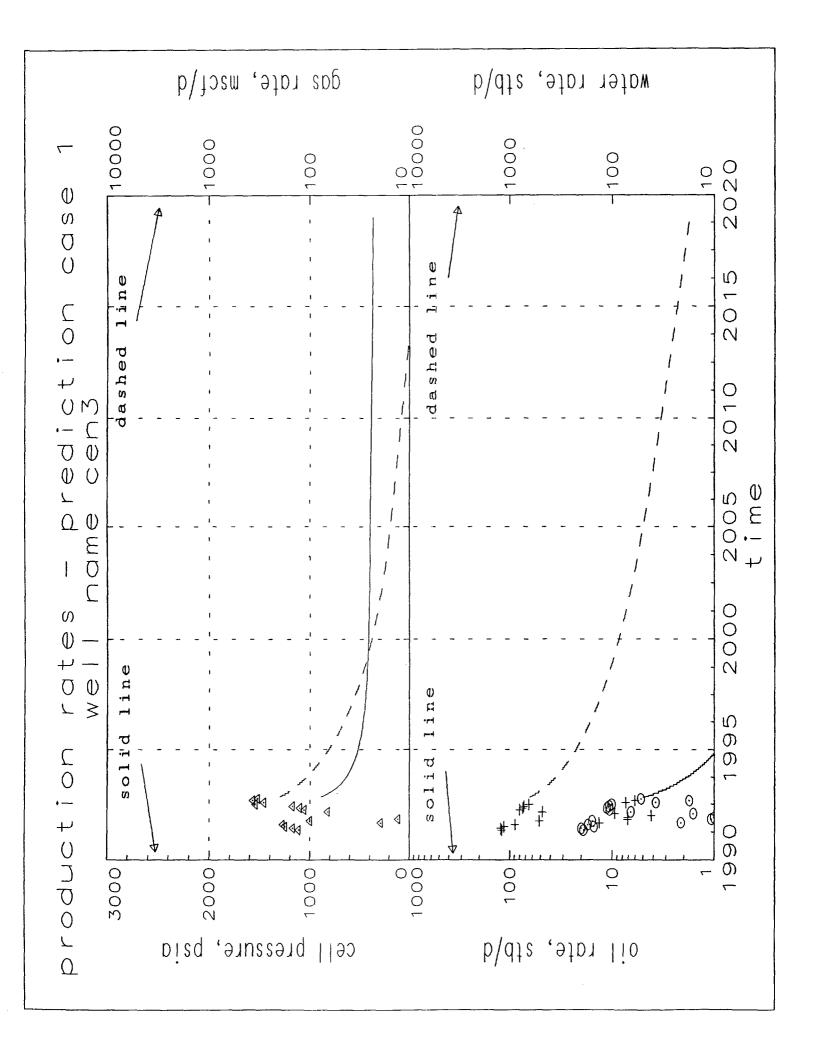








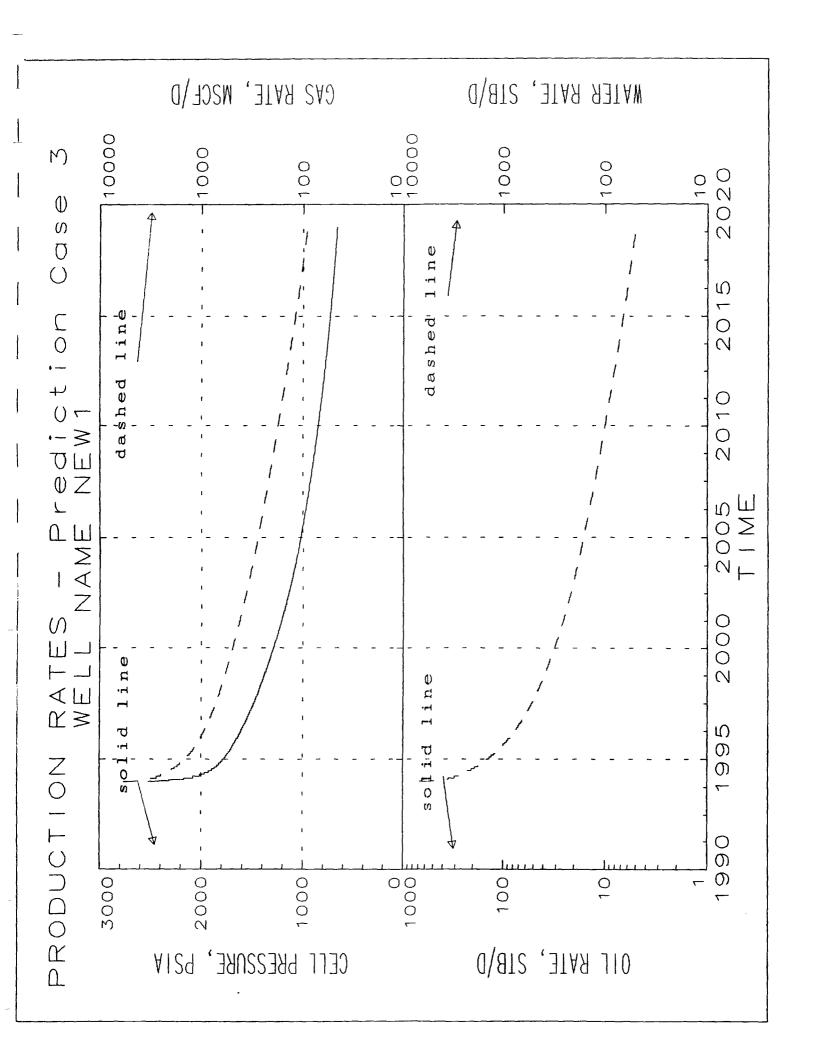


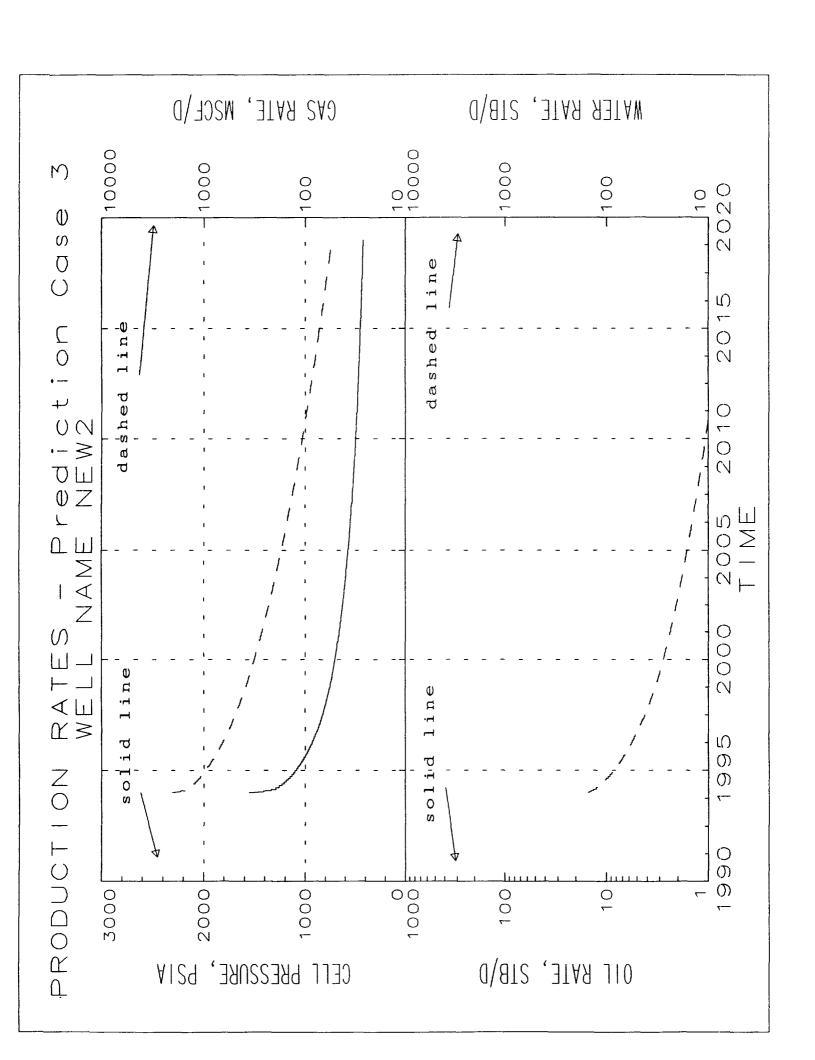


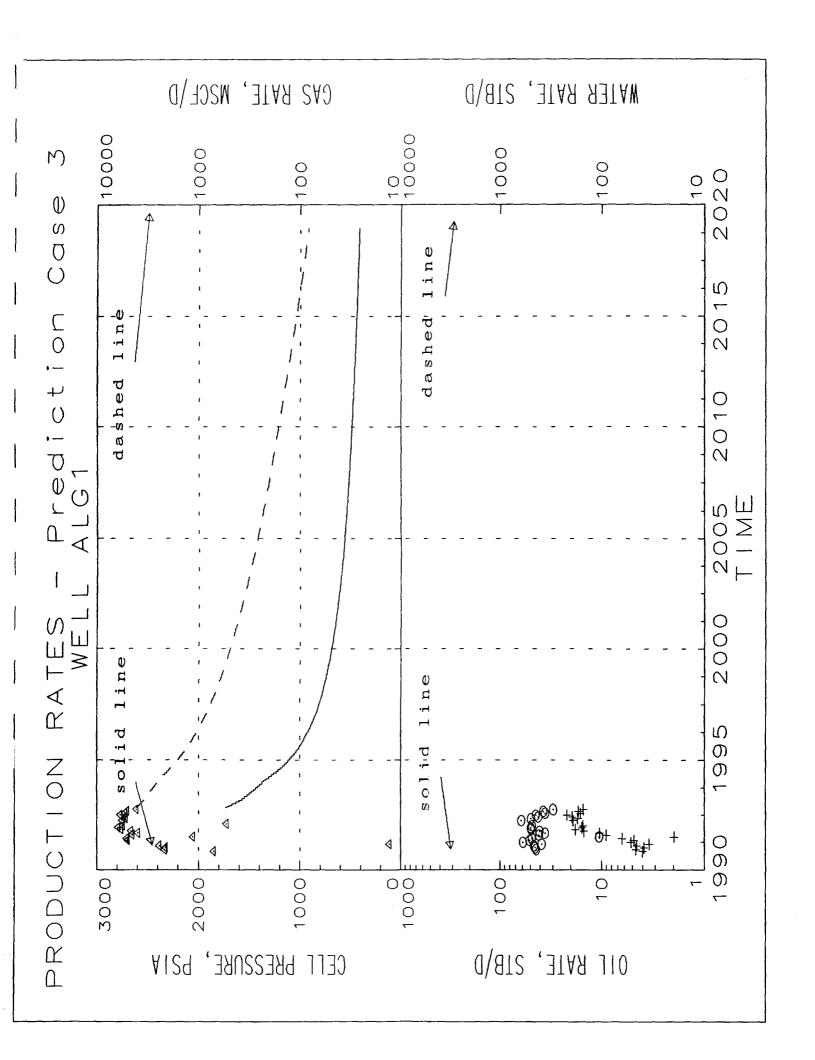
#### APPENDIX VI

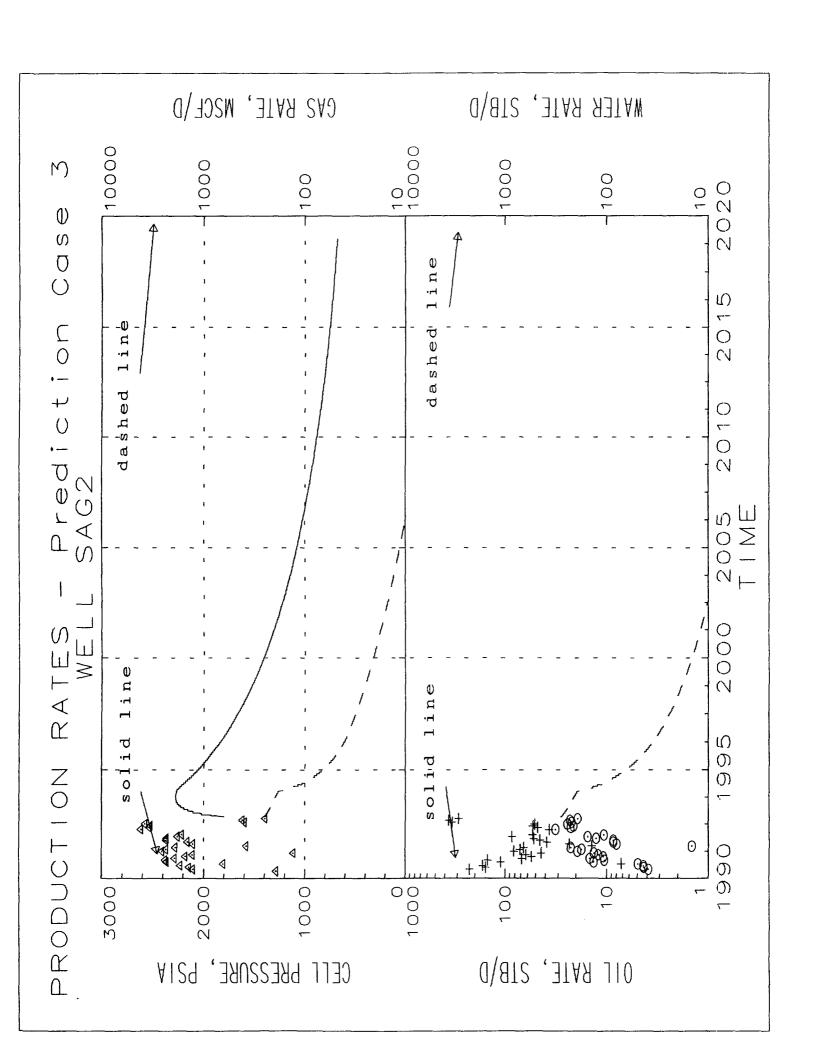
#### PREDICTION CASE 3

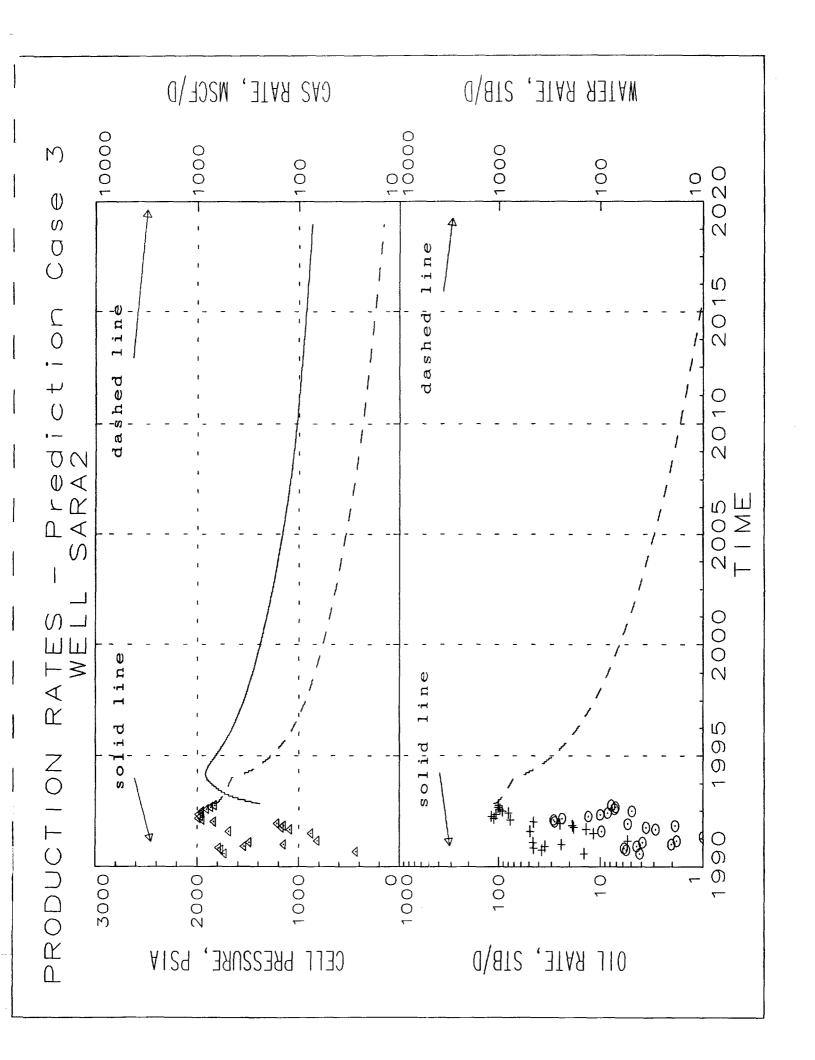
**Well Performance Plots** 

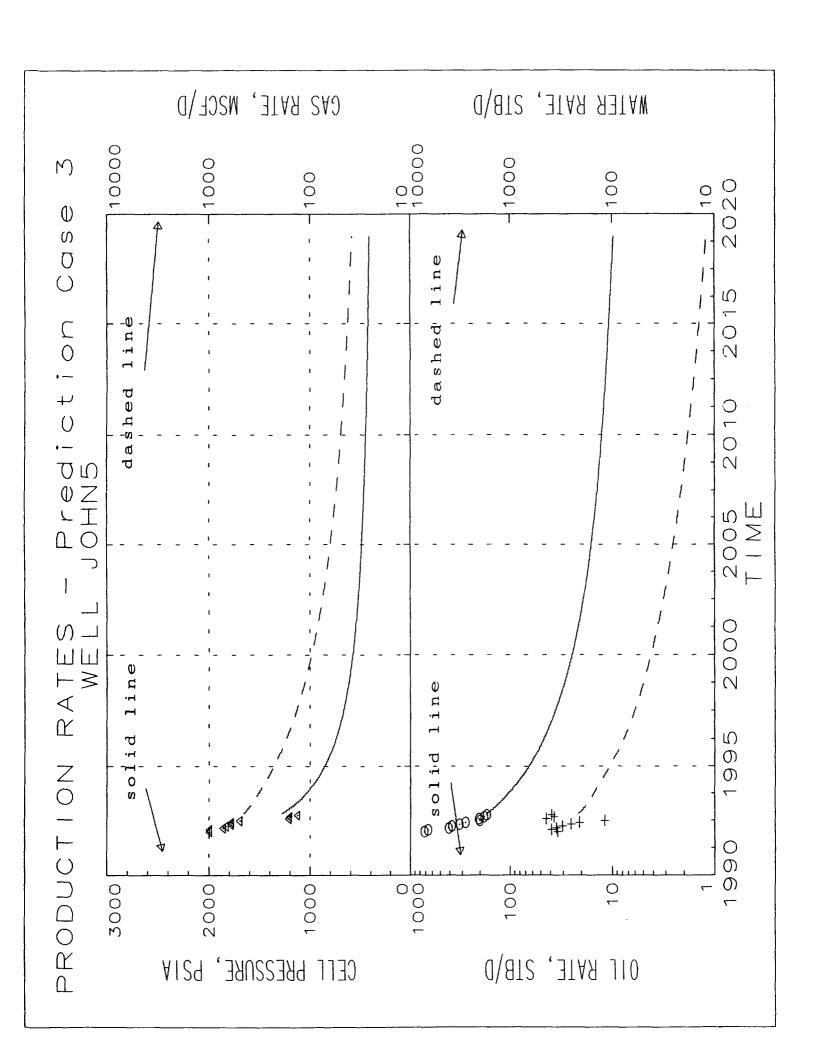


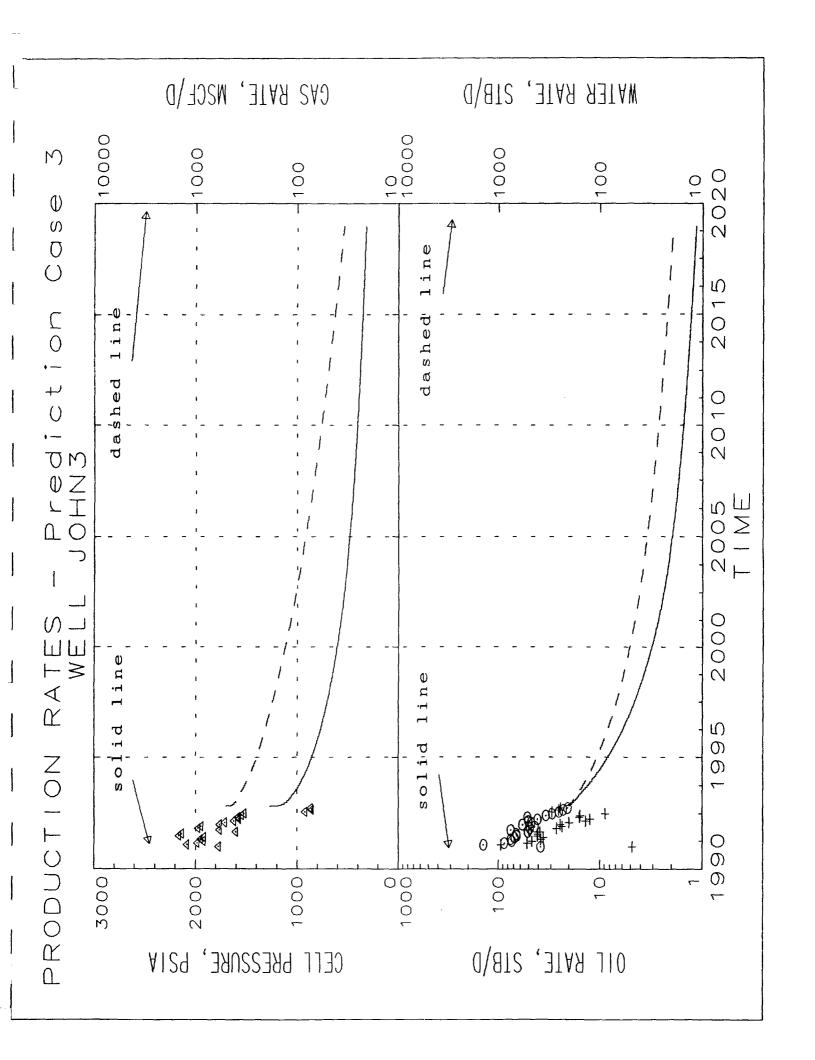


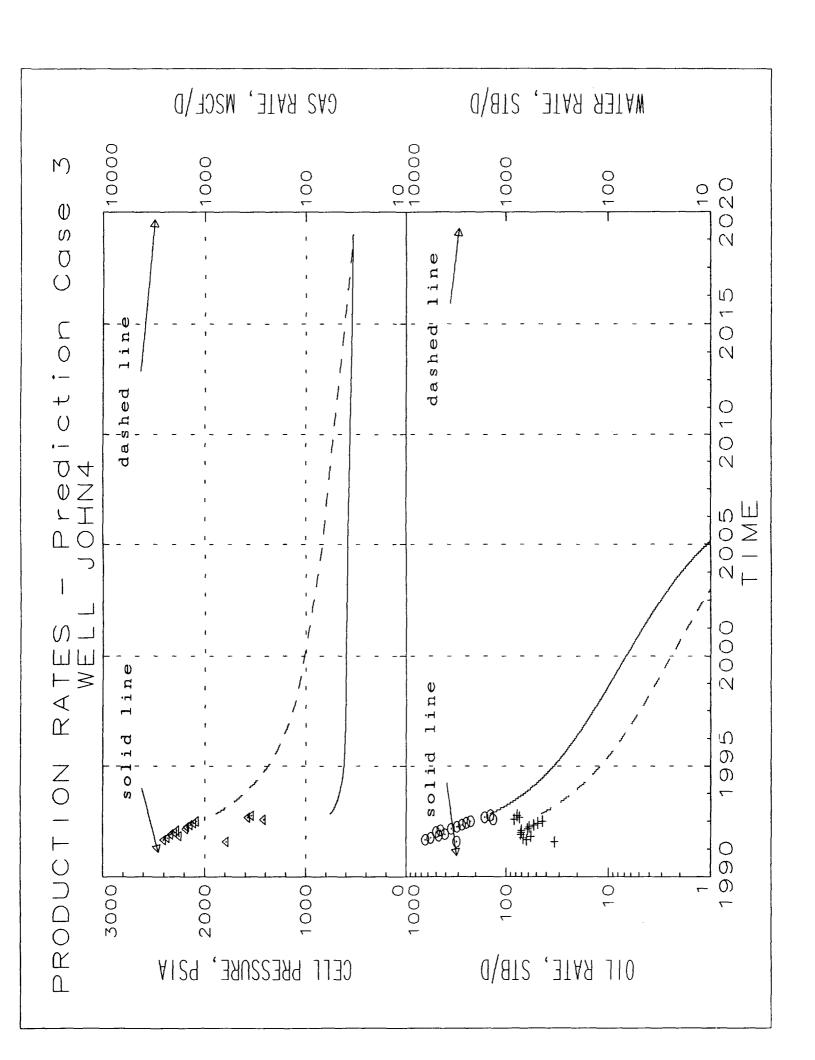


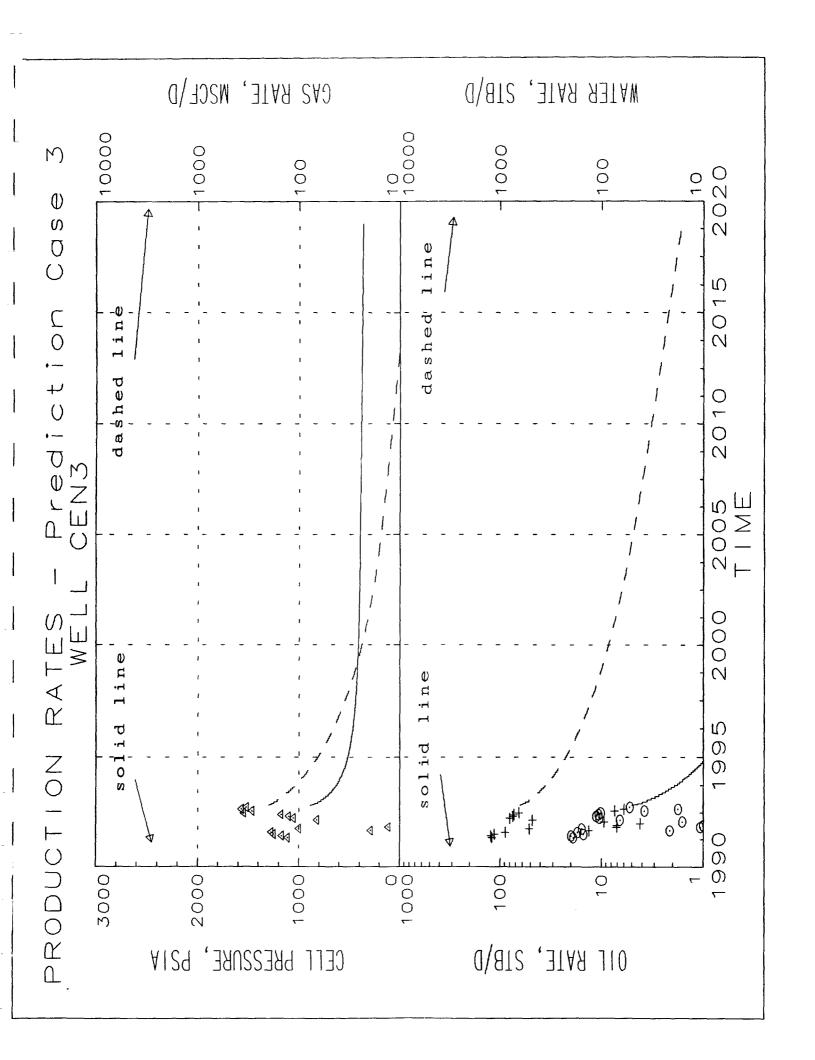












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# Economic Analyses Gas Cap Drainage Scenarios Dagger Draw South (Upper Penn)

**Continue with Current Operations:** 

Oil

**682 MBO** 

Gas

19450 MMCF

Present Worth Profit

10490 M\$

Continue Oil Production and Shut In Gas Wells:

Oil

**684** MBO

Gas

9682 MMCF

Present Worth Profit

6750 M\$

**)**-

Continue Oil Production and Accelerate Gas Well Production:

Oil

682 MBO

Gas

21490 MMCF

Present Worth Profit

11080 M\$

- dulled wells for in more additions of studies.

## BEFORE THE OIL CONSERVATION DIVISION Santa Fe, New Mexico

Case Nos. <u>10869 and 10881</u> Exhibit No. <u>6</u>

Submitted by: Yates Petroleum Corporation

Hearing Date: December 2, 1993

\* Discount rate = 5%