

Facility : C-1 Pipeline

Date : 5/28/2019

Enter data in shaded fields to calculate gas volumes released due to leak and blowdown of system.

Circular Hole

|                           |           |
|---------------------------|-----------|
| Hours of leak             | 0.0416667 |
| Diameter of hole (inches) | 0.0625    |
| Upstream Pressure         | 300       |
| Volume of Gas Leaked      | 0.05      |

Crack

|                          |      |
|--------------------------|------|
| Hours of leak            |      |
| Length of Crack (inches) |      |
| Width of Crack (inches)  |      |
| Upstream Pressure        |      |
| Volume of Gas Leaked     | 0.00 |

Calculations:

Volume of Gas Leaked (MSCF) = Diameter\*Diameter\*(Upstream Gauge Pressure + Atmospheric Pressure)\*Hours of Leak

\*\*Reference: Pipeline Rules of Thumb Handbook, 3rd Edition, McAllister. Page 260. Assuming Standard Temperature and Pressure (14.7 psi and 60 F)

|                           |           |         |
|---------------------------|-----------|---------|
| Footage of Pipe blowdown  | 22123.2   |         |
| Initial line pressure     | 300       |         |
| Diameter of Pipe (inches) | 6         |         |
| Volume of Gas Blown Down  | 107.74763 | 0.00000 |

Calculations:

Volume of Gas Blown Down (MSCF) = Volume at pipeline conditions (ft3)\*(Gauge Pressure (psig)+Atmospheric Pressure 13.7 psi)\*Standard Temperature (60F) / (1000 scf/mscf)\*Standard Pressure (14.7psi)\*Temperature(F)\*Z Factor

Volume at pipeline conditions (scf) = Diameter/12 (ft)\*Diameter/12 (ft)\*PI/4\*Length of pipe (ft)

\*\*Reference: Gas Pipeline Hydraulics, Menon (2005) Pages 132-134. Assuming the Ideal Gas Law and Tpipeline = Tatm.

|                |             |            |
|----------------|-------------|------------|
| Total Gas Loss | 107.80 MSCF | 0.11 MMSCF |
|----------------|-------------|------------|

Comments:

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