

OIL CONSERVATION DIVISION

STATE OF NEW MEXICO
ENERGY AND MINERALS DEPARTMENT

P. O. BOX 2088
SANTA FE, NEW MEXICO 87501

Fern C-122
Revised 10-1-78 *d5r file*

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Type Test <input checked="" type="checkbox"/> Initial <input type="checkbox"/> Annual <input type="checkbox"/> Special						Test Date 07-02-90					
Company TXO Texas Oil & Gas				Connection 6-27-90							
Pool <i>D. Shugart Morrow</i>				Formation Morrow				Unit			
Completion Date 6-31-90		Total Depth 11,900		Plug Back TD 11,856		Elevation 3623 CR		Farm or Lease Name Shugart St. Com. A			
Csg. Size		Wt.		Set At		Perforations: From 11,618 To 11,736		Well No. 1			
Tbg. Size 2 3/8		Wt. 4.7		Set At 11,549		Perforations: From To		Unit Sec. Twp. Rge. C 16 18 31			
Type Well - Single - Brocnehead - G.C. or G.O. Multiple Single						Packer Set At		County Eddy			
Producing Thru Tbg		Reservoir Temp. °F 191 @ 11,676		Mean Annual Temp. °F 60		Baro. Press. - P _a 13.2		State New Mexico			
L *11,676		H *11,676		C _g .678		% CO ₂ .57		% N ₂ 1.04			
						% H ₂ S ---		Prover 3.068			
								Meter Run 3.068			
								Taps Flg			
FLOW DATA					TUBING DATA			CASING DATA		Duration of Flow	
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. In. H ₂ O	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow
5.							2327		PKR		72 hrs.
1.	3	X	.750	131	112.50	106	2092		PKR		1 hr.
2.	3	X	.750	131	162.00	100	1825		PKR		1 hr.
3.	3	X	2.000	139	5.12	99	1410		PKR		1 hr.
4.	3	X	2.00	139	6.48	103	1202		PKR		1 hr.
5.											
RATE OF FLOW CALCULATIONS											
NO.	Coefficient (24 Hour)	$\sqrt{P_{1,2}}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor F _g	Super Compress. Factor, F _{sc}	Rate of Flow O, Mcid				
1.	2.672	127.37	144.2	.9585	1.214	1.011	400				
2.	2.672	152.84	144.2	.9636	1.214	1.012	483				
3.	21.32	27.92	152.2	.9645	1.214	1.012	705				
4.	21.32	31.41	152.2	.9610	1.214	1.012	791				
5.											
NO.	P ₁	Temp. °R	T _g	Z	Gas Liquid Hydrocarbon Ratio <u>198.4</u> Mcf/bbl.						
1.	.21	566	1.50	.978	A.P.I. Gravity of Liquid Hydrocarbons <u>53.9 @ 60</u> Deg.						
2.	.21	560	1.48	.977	Specific Gravity Separator Gas <u>.678</u> X X X X X X X X X						
3.	.22	559	1.48	.976	Specific Gravity Flowing Fluid <u>X X X X X</u>						
4.	.22	563	1.49	.976	Critical Pressure <u>**666</u> P.S.I.A. P.S.I.A.						
5.					Critical Temperature <u>**376</u> R R						
P _c <u>2569.5</u> P _c ² <u>6602.3</u>					(1) $\frac{P_c^2}{P_1^2 - P_w^2} = 2.846$ (2) $\left[\frac{P_c^2}{P_1^2 - P_w^2} \right]^n = 2.846$						
NO.	P ₁ ²	P _w	P _c ²	P _c ² - P _w ²	AOF = Q $\left[\frac{P_c^2}{P_1^2 - P_w^2} \right]^n = 2.251$						
1		2334.2	5444.5	1157.8							
2		2295.0	5267.0	1335.3							
3		2210.8	4887.6	1714.7							
4		2069.5	4282.8	2319.5							
5											
Absolute Open Flow <u>2,251</u> Mcid @ 15.025					Angle of Slope @ <u>45</u>			Slope, n <u>1.000</u>			
Remarks: * = BHP's extrapolated to this depth											
** = corrected to 1.04% N ₂											
Well made $\frac{1}{2}$ BBL 53.9 API condensate & 6.5 BBL H ₂ O											
Approved By Division				Conducted By				Calculated By BM		Checked By BM	