

NEW MEXICO OIL CONSERVATION COMMISSION  
MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

1-C-122 file  
1-File  
Form C-122  
Revised 9-1-65

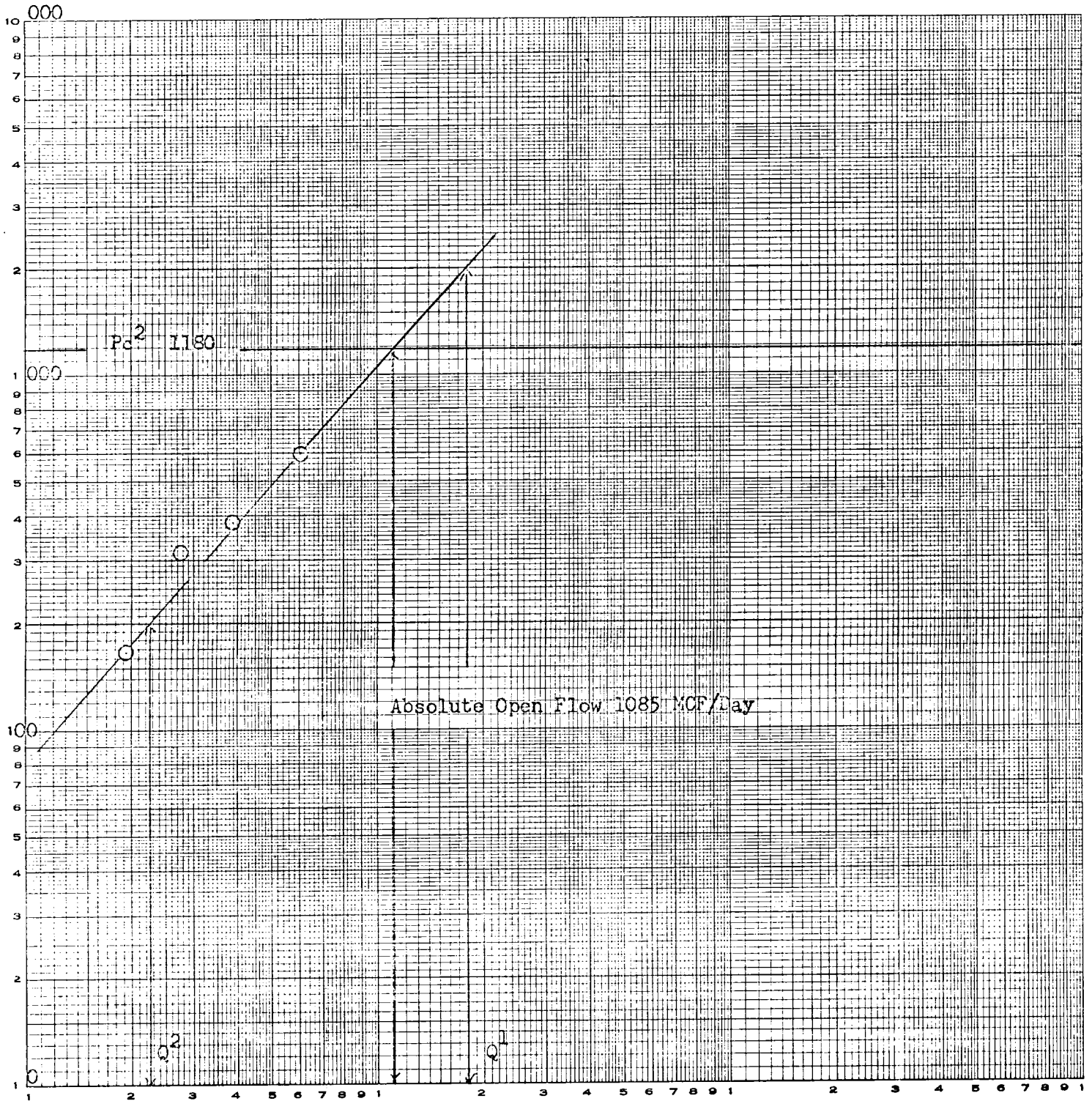
RECEIVED

Type Test <input type="checkbox"/> Initial <input type="checkbox"/> Annual <input checked="" type="checkbox"/> Special				Test Date 2-8-78		FEB 13 1978					
Company R.L. Foree ✓			Connection Phillips			O. C. C.					
Pool Sams Ranch <i>Grayburg</i>			Formation Premier Grayburg			Unit ARTESIA, OFFICE					
Completion Date 11-10-73		Total Depth 1873		Plug Back TD 1873		Elevation 3605					
Farm or Lease Name McClellan <i>Com</i>		Well No. # 2		Perforations: From 1848 To 1873		Unit Sec. Twp. Rge. G 14 14S 28E					
Cog. Size 4.5		Wt. 11.6		d 4.0		Set At 1848					
Tag. Size 2 3/8		Wt. 4.9		d 1.995		Set At 1840					
Type Well - Single - Bradenhead - G.G. or G.O. Multiple Single Gas Well				Packer Set At None		County Chaves					
Producing Thru Tubing		Reservoir Temp. °F 83° Perf		Mean Annual Temp. °F 60°		Baro. Press. - P <sub>a</sub> 13.2					
L 1840		H 1840		G <sub>g</sub> .733		% CO <sub>2</sub>					
				% N <sub>2</sub> 24.00		% H <sub>2</sub> S					
				Prover		Meter Run Four-Inch					
						Taps Flange					
FLOW DATA				TUBING DATA				CASING DATA		Duration of Flow	
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h <sub>w</sub>	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow
SI							1076		1076		
1.	4	X	1	247	4.5	60	998		1003		1 hr
2.	4	X	1	247	9.2	60	914		917		1 hr
3.	4	X	1	247	18.0	60	875		880		1 hr
4.	4	X	1	257	42.3	60	742		750		1 hr
5.											
RATE OF FLOW CALCULATIONS											
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P <sub>m</sub>	Flow Temp. Factor Ft.	Gravity Factor F <sub>g</sub>	Super Compress. Factor, F <sub>pv</sub>	Rate of Flow Q, Mcfd				
1	4.753	34.22	260.2	1.0	1.168	1.018	193.				
2	4.753	48.93	260.2	1.0	1.168	1.018	277.				
3	4.753	68.44	260.2	1.0	1.168	1.018	387.				
4	4.753	106.90	270.2	1.0	1.168	1.021	606.				
5											
NO.	P <sub>r</sub>	Temp. °R	T <sub>r</sub>	Z	Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.						
1	.42	520	1.55	.9615	A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.						
2	.42	520	1.55	.9615	Specific Gravity Separator Gas .733 XXXXX						
3	.42	520	1.55	.9615	Specific Gravity Flowing Fluid XXXXX						
4	.43	520	1.55	.9610	Critical Pressure 668 - 41 = 627 P.S.I.A. P.S.I.A.						
5					Critical Temperature 401 - 66 335 R R						
P <sub>c</sub> 1086.2 P <sub>c</sub> <sup>2</sup> 1180.											
NO	P <sub>r</sub> <sup>2</sup>	P <sub>w</sub>	P <sub>w</sub> <sup>2</sup>	P <sub>c</sub> <sup>2</sup> - P <sub>w</sub> <sup>2</sup>	(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.98$		(2) $\left[ \frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1.79$				
1		1016.2	1012.	168							
2		930.2	865.	315							
3		893.2	798.	382							
4		763.2	583.	597	ACF = Q $\left[ \frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1085$						
5											
Absolute Open Flow 1085				Mcf/d @ 15.025				Angle of Slope θ 42.8		Slope, n .903	
Remarks:											
Approved by Commission:			Conducted By: John Davis			Calculated By: Larry Davis			Checked By:		

Company: R.D. TORRE  
 Lease: McClellan  
 Well No: # 2  
 Field: Sams Ranch  
 County: Chaves  
 Date: 2-8-78

EUGENE DIETZGEN CO.  
 MADE IN U. S. A.

NO. 340R-L33 DIETZGEN GRAPH PAPER  
 LOGARITHMIC  
 3 CYCLES X 3 CYCLES



Q = MCF  
 $Q^1 = 1800$ ;  $\text{Log of } Q^1 = 3.2552725$   
 $Q^2 = 225$ ;  $\text{Log of } Q^2 = 2.3521825$   
 $N = .90309$

*McCallum # 2*

PHILLIPS PETROLEUM COMPANY  
GAS CHROMATOGRAPH ANALYSIS - VAPOR  
PROGRAM 6335

RUN NO N-957  
DATE RUN 11-23-77  
DATE SEC 11-17-77  
TIME  
SEC BY BROCK  
RUN BY RM-JB

SAMPLE OF  
SECURED FROM--STA #76544  
LOCATION--LUSK AREA  
ATMOS T--58 GAS T--46  
TRAP T-- TRAP--  
GAS TO LUSK PLT  
R.L. FOREE PRODUCER  
CO.--  
LINE P--250# FTP--  
RX GVITY-- .738 CHOKE--  
STATE--NEW MEX  
PURP--N2-CO2 CK  
TRAP P--

DISTRIBUTION

MISCELLANEOUS DATA

Z FACTOR = 0.9980

	UNCORR	FINAL	BTU-CF-SB	BTU-CF-SB	BTU-CF-SB	BTU-CF-SB
O2	0.0	0.0	0.0	0.0	0.0	0.0
HE	0.0	0.0	0.0	0.0	0.0	0.0
CO2	23.1916	23.5629	0.2052	0.2052	0.2052	0.2052
H2S	65.4648	66.5130	0.2172	0.2172	0.2172	0.2172
N2	5.6060	5.6958	0.1957	0.1957	0.1957	0.1957
C1			0.0914	0.0914	0.0914	0.0914
C2			99.9999	99.9999	99.9999	99.9999
C3	2.4204	2.4592	0.735	0.735	0.735	0.735
IC4	0.3010	0.3058	0.0	0.0	0.0	0.0
NC4	0.7419	0.7538	0.0	0.0	0.0	0.0
IC5	0.2020	0.2052	0.0	0.0	0.0	0.0
NC5	0.2138	0.2172	1.29	1.29	1.29	1.29
C6	0.1926	0.1957	14.7345	14.7345	14.7345	14.7345
C7+	0.0899	0.0914	890.83	890.83	890.83	890.83
TOTAL	98.4240	99.9999	14.7350	14.7350	14.7350	14.7350

BTU-CF-SB 886.23  
CALC SG 0.735  
H2S + CO2 0.0  
H2S GRS 0.0  
N VALUE 1.29

BTU-CF-SB 890.83  
BTU-CF-SB 890.92

BTU-CF-SB 890.83

ADDITIONAL INFORMATION

BTU REPORTED ON (SB) SATURATED BASIS  
SUPER-COMP. FACTORS INCLUDED IN CALCULATIONS  
BARO NONE H2S STLA

H.R. HARRIS  
T.R. BLACHLY  
S.W. MAPEL  
C. EDGE - M.H.A.  
KEN MOORE (2)  
CENTRAL FILES  
LAB FILES

*R J Foree McCallum # 2-6-14-14-28*

*0.4 1848-73*