

RECEIVED

NEW MEXICO OIL CONSERVATION DIVISION

P. O. DRAWER "DD"

ARTESIA, NEW MEXICO 88210

MAY - 6 1982

O. C. D.
ARTESIA OFFICE

NOTICE OF GAS CONNECTION

DATE May 4, 1982

This is to notify the Oil Conservation Division that connection for the
purchase of gas from the Viking Petroleum, Inc. ✓
Operator

Grynberg "16" State
Lease

Well #4 - Unit Letter ^G Unknown
Well Unit

16-5S-24E, Chaves County
S.T.R.

Recas ~~State~~ Wildcat (Abo) Gas
Pool

Transwestern
Name of purchaser

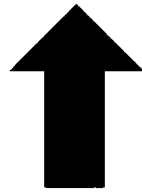
was made on May 3, 1982

Transwestern Pipeline Company
Company

 H. N. Aicklen
Representative

Supervisor Gas Purchase Contract Administration
Title

cc: Operator
Oil Conservation Division - Santa Fe



LTR



Job separation sheet

NEW MEXICO OIL CONSERVATION COMMISSION
MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122
Revised 9-1-65

RECEIVED

C/SF
C-122

Type Test <u>USGS</u> ☒ Initial ☐ FOUR POINT ☐ Annual ☐ Special		Test Date <u>1-29-82</u>	1980 FNL <u>1000</u>	
Company <u>Viking Petroleum, Inc.</u>		Connection <u>AIR NEW WELL</u>		1980 FEL <u>1000</u>
Pool <u>Pecos Slope Abo Gas</u>		Formation <u>ABO</u>		Unit <u>G</u> <u>OFFICE</u>
Completion Date <u>1-30-82</u>	Total Depth <u>3910</u>	Plug Back TD <u>3700</u>	Elevation <u>4020 KB</u>	Farm or Legse Name <u>Grynberg 16 State</u>
Coq. Size <u>4.5</u>	Wt. <u>10.5</u>	d <u>4.052</u>	Set At <u>3700</u>	Perforations: From <u>3545</u> To <u>3650</u>
Trq. Size <u>2.375</u>	Wt. <u>4.7</u>	d <u>1.995</u>	Set At <u>3510 GR</u>	Perforations: From <u>OPEN</u> To <u>ENDED</u>
Type Well - Single - Brdenhead - G.G. or G.O. Multiple <u>SINGLE</u>				Packer Set At <u>NONE</u>
Producing Thru <u>TUBING</u>		Reservoir Temp. °F <u>110 @ 3516</u>	Mean Annual Temp. °F <u>60°</u>	Baro. Press. - P _a <u>13.2</u>
L <u>3598</u>	H <u>3598</u>	G _g <u>.7613</u>	% CO ₂ <u>11.44</u>	% N ₂ <u>8.66</u>
		% H ₂ S <u>2.00</u>	Prover <u>2.00</u>	Meter Run <u></u>
				Taps <u></u>
COUNTY <u>CHAVES</u>				
STATE <u>NEW MEXICO</u>				

FLOW DATA							TUBING DATA			Duration of Flow	
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	B.H.P. PSIA	Temp. °F	Duration of Flow
SI							959		1078		72 HRS +
1.	2.00	X	500	50	0	32	900	37	1017		1
2.	2.00	X	500	129	0	28	770	43	883		1
3.	2.00	X	500	149	0	40	570	45	660		1
4.	2.00	X	500	116	0	45	385	50	425		1
5.											

RATE OF FLOW CALCULATIONS							
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor F _g	Super Compress. Factor, F _{pv}	Rate of Flow Q, Mcfd
1	4.3880	.00	63.2	1.0281	1.1463	1.0066	329
2	4.3880	.00	142.2	1.0218	1.1463	1.0148	742
3	4.3880	.00	162.2	1.0198	1.1463	1.0164	846
4	4.3880	.00	129.2	1.0147	1.1463	1.0127	668
5							

NO.	P _f	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio	A.P.I. Gravity of Liquid Hydrocarbons	Specific Gravity Separator Gas	Specific Gravity Flowing Fluid	Critical Pressure	Critical Temperature
1	.09	492	1.35	.978			.4610	X X X X X X X X	701	366
2	.20	498	1.36	.971			X X X X X			
3	.23	500	1.37	.968						
4	.18	505	1.38	.975						
5										

NO.	P _c	P _w	P _w ²	P _c ² - P _w ²
1	1019.2	1190.7	1030.2	1061.3
2			896.2	803.2
3			673.2	453.2
4			438.2	192.0
5				

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.6134$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1.3090$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1,107.4$

Absolute Open Flow	<u>1,107.4</u>	Mcf @ 15.025	Angle of Slope θ	<u>60.6</u>	Slope, n	<u>.5628</u>
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Remarks: BOTTOM HOLE PRESSURES MEASURED WITH AMERADA PRESSURE ELEMENTS

Approved By Commission:	Conducted By: <u>RICHARD TOWNLEY</u>	Calculated By: <u>BENNETT-CATHEY</u>	Checked By:
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