

File

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Type Test ☒ Initial ☐ Annual ☐ Special				Test Date 1-17-89							
Company McCLELLAN OIL CORP. ✓				Connection 1-11-89 RECEIVED							
Pool S. PECOS Slope ABO				Formation ABO							
Completion Date 1-11-89		Total Depth 4440		Plug Back TD 4400							
Csq. Size 4 1/2		Wt. d		Set At TD							
Thq. Size 2-3/8		Wt. 4.7		Set At 4200							
Type Well - Single - Bradenhead - G.G. or G.O. Multiple SINGLE				Packer Set At NONE							
Producing Thru TUBING		Reservoir Temp. °F #		Mean Annual Temp. °F 60							
L		H		Baro. Press. - P _g 13.2							
G _g .657		% CO ₂		% N ₂							
Prover		Meter Run 2"		Taps FLANGE							
FARM OR LEASE NAME JILL FED.											
UNIT #1											
COUNTY CHAVES											
STATE NEW MEXICO											
FLOW DATA											
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow
1.	2	x	1	290	4	55	779		808		1 hr.
2.	2	x	1	309	24	55	730		774		"
3.	2	x	1	317	34	60	710		755		"
4.	2	x	1	360	90	60	557		660		"
5.											
RATE OF FLOW CALCULATIONS											
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor F _t	Gravity Factor F _g	Super Compress. Factor, F _{pv}	Rate of Flow Q, Mcfd				
1	4.946	34.825	303.2	1.0048	1.2337	1.0302	220				
2	4.946	87.936	322.2	1.0048	1.2337	1.0323	557				
3	4.946	105.957	330.2	1.0000	1.2337	1.0320	667				
4	4.946	183.270	373.2	1.0000	1.2337	1.0368	1159				
5											
NO.	P _t	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.						
1					A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.						
2					Specific Gravity Separator Gas _____ XXXXXXXXXX						
3					Specific Gravity Flowing Fluid _____ XXXXX						
4					Critical Pressure _____ P.S.I.A. _____ P.S.I.A.						
5					Critical Temperature _____ R _____ R						
P _c 960.2 P _c ² 921.6											
NO.	P _i ²	P _w	P _w ²	P _c ² - P _w ²	(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 2.8577$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 2.66$						
1		935.2	874.6	47	AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 3000$						
2		897.2	805.0	117							
3		871.2	758.9	163							
4		765.2	585.5	336							
5											
Absolute Open Flow 3000 Mcfd @ 15.025					Angle of Slope 49			Slope, n = 8693			
Remarks: BOTTOM PRESSURES RECORDED WITH AMERADA TYPE GAUGE											
Approved By Division				Conducted By: KELTIC SERVICES				Calculated By: MIKE KELLY			
Checked By:											

McClellan Oil Corp

JILL PED #1

1/17/59

$(P^2 - P^2)_{0000}$ 457400

P^2 960

LOGARITHMIC 3 X 3 CYCLES
KEUFFEL & ESSER CO. MADE IN U.S.A.

θ 49.5° m .8541

Q
MSCFPD