

NE MEXICO OIL CONSERVATION COMMISSION
MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL RECEIVED

Form C-122
Revised 9-1-65

OCT 16 1968

Type Test <input checked="" type="checkbox"/> Initial <input type="checkbox"/> Annual <input type="checkbox"/> Special				Test Date 9-24-68											
Company David Fasken			Connection None			D.F.S. ARTEDIA, OFFICE									
Pool Undesignated			Formation Morrow												
Completion Date 9-24-68		Total Depth 10130		Plug Back TD 10100		Elevation 4216 KB									
Csg. Size 4 1/2		Wt. 11.6		Set At 10130		Perforations: From 9839 To 9982									
Thq. Size 2 3/8		Wt. 4.7		Set At 9795		Perforations: From To									
Type Well - Single - Bradenhead - G.G. or G.O. Multiple Single				Packer Set At 9788		Unit Indian Hills									
Producing Thru Tubing		Reservoir Temp. °F 174 ^a 9710		Mean Annual Temp. °F 60		Baro. Press. - P _g 13.2									
L 9910		H 9910		G _g 0.600		Prover 2"									
				% CO ₂		% H ₂ S									
				% N ₂		Meter Run									
						Taps									
FLOW DATA				TUBING DATA		CASING DATA									
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow				
SI	363 hours			2964			2964								
1.	2"		3/32	2967		60	2967	60			1 hour				
2.	2"		1/8	2937		60	2937	60			1 hour				
3.	2"		3/16	2831		60	2831	60			1 hour				
4.	2"		7/32	2710		60	2710	60			1 hour				
5.															
RATE OF FLOW CALCULATIONS															
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor F _g	Super Compress. Factor F _{pv}	Rate of Flow Q, Mcfd								
1.	0.1410		2980.2	1.000	1.291	1.146	621.7								
2.	0.2648		2950.2	1.000	1.291	1.148	1157.8								
3.	0.6082		2844.2	1.000	1.291	1.152	2572.7								
4.	0.8393		2723.2	1.000	1.291	1.157	3413.9								
5.															
NO.	P _r	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.										
1.	4.44	520	1.45	0.761	A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.										
2.	4.40	520	1.45	0.759	Specific Gravity Separator Gas _____ X X X X X X X X X										
3.	4.24	520	1.45	0.753	Specific Gravity Flowing Fluid _____ X X X X X										
4.	4.06	520	1.45	0.747	Critical Pressure _____ P.S.I.A. 671 P.S.I.A.										
5.					Critical Temperature _____ R 358 R										
P _g 3780.2 P _s 14290					$(1) \frac{P_c^2}{P_c^2 - P_w^2} = \text{_____}$ $(2) \left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = \text{_____}$										
NO.	P _i	P _s	P _g	P _w	AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = \text{_____}$										
1.		P _s	P _g	P _g - P _s											
2.		3766.2	14184	106											
3.		3747.2	14042	248											
4.		3685.2	13581	709											
5.		3660.2	13397	893											
Absolute Open Flow 34,000 Mcfd @ 15.025					Angle of Slope 50° 13'			Slope, n 0.8327							
Remarks: BHP measured with Amerada RPC-3 gauge.															
Approved By Commission:				Conducted By: Teffeller, Inc.				Calculated By: Farrest Tefteller				Checked By:			