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June 6, 2016

Mr. George Bower
Oil Conservation Division - District 1
1625 N. French Drive
Hobbs, New Mexico 88240

Subject: Western Refining Company, LP – State LPG Storage No. 1 MIT

Dear Mr. Bower,

Western Refining Company, LP has performed a nitrogen-brine MIT on one of their storage cavern wells, State LPG Storage No. 1 (API No. 30-025-35954), located in the Jal Station Field in Lea County, New Mexico.

Nitrogen was injected on April 26th, 2016. An hour casing test was performed successfully with the following parameters:

- Nitrogen-brine interface start depth: 1,509'
- Start Annulus Pressure: 1,058.25 psig
- Nitrogen-brine interface end depth: 1,509'
- End Annulus Pressure: 1,056.40 psig

The 60-minute casing test passed with the pressures following a stabilization trend throughout the casing test period. Nitrogen injection continued into the borehole and ceased with the nitrogen-brine interface at 1,531'. The well was shut in and allowed to stabilize overnight. The MIT was initialized on April 27th, 2016 at 09:10 with the following parameters:

- Annular pressure: 1,069.11 psig
- Tubing pressure: 331.36 psig
- Nitrogen-brine interface: 1,532.5'

The pressure was monitored throughout a 24 hour period and finalized on April 28th, 2016 at 09:17 with the following parameters:

- Annular pressure: 1,063.82 psig
- Tubing pressure: 323.43 psig
- Nitrogen-brine interface: 1,532.5'
- Test Gradient at Casing Shoe: 0.75 psi/ft
- Calculated Leak Rate: 55.94 bbls/yr
- Minimum Detectable Leak Rate: 244.18 bbls/year

It was determined that State LPG Storage No. 1, at the time of this test, demonstrated the mechanical integrity required for the storage of hydrocarbons.

Included in this package are:

- MIT Report for State LPG Storage No. 1
- Test Density Log
- Test Temperature Log

Please contact me by phone (832-216-0785) or via email (eric@lonquist.com) if you have any questions.

Sincerely,



Eric Busch
Senior Vice President

CC: Richard Lonquist – Lonquist Field Service, LLC

LONQUIST

FIELD

SERVICE

**Mechanical Integrity Test Report
State LPG Storage No.1
Operator: Western Refining Company, LP
API: 30-025-35954
Jal Station Field
Lea County, New Mexico, USA**

Prepared for:

Western Refining Company, LP

By:

**Lonquist Field Service, LLC
Texas Registered Firm No. F-9147
Houston, Texas**

May 2016

*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

Executive Summary

Lonquist Field Services, LLC was contracted by Western Refining Company, LP (“Western Refining”) to conduct a Mechanical Integrity Test on State LPG Storage No. 1 (“Well No. 1”), operated by Western Refining Company, LP at the Jal Station Field in Lea County, New Mexico. The Nitrogen-Brine Interface Test Method was used for this test. Nitrogen was injected on April 26th, 2016 to achieve the desired interface depth below the casing shoe. The well was allowed to stabilize for approximately 13 hours and on April 27th, 2016 at 09:10 the MIT was initialized with an annulus (nitrogen) pressure of 1,069.11 psig and a tubing (brine) pressure of 331.36 psig with the nitrogen-brine interface at 1,532.5’. The test was finalized on April 28th, 2016 at 09:17 with an annulus (nitrogen) pressure of 1,063.82 psig and a tubing (brine) pressure of 323.43 psig with the nitrogen-brine interface at 1,532.5’. The calculations yielded a calculated leak rate (“CLR”) of 48.38 barrels per year and a Minimum Detectable Leak Rate (“MDLR”) of 244.18 barrels per year. The well was tested to a test gradient of 0.75 psi/ft at the 7” cemented casing shoe (1,521’). Considering these results and the guidelines set forth by the State of New Mexico Oil Conservation Division, Well No. 1 at the Jal Station Field, at the time of this test, demonstrated the mechanical integrity required for the storage of hydrocarbons.

Reviewed By:
Lonquist Field Service, LLC
Ben H. Bergman, Sr. Staff Engineer



Date Signed: May 31st, 2016
Houston, Texas

*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

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*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

Introduction

Lonquist Field Service, LLC was contracted by Western Refining Company, LP to conduct a Mechanical Integrity Test on State LPG Storage No. 1 ("Well No. 1") at the Jal Station Field in Lea County, New Mexico.

Well No. 1 was tested using the Nitrogen-Brine Interface Test Method (See Appendix A). Typically this procedure begins with an initial injection of nitrogen into the well to check for wellhead and casing leaks. The initial injection is followed by continued injection of nitrogen into the storage well until the interface is located below the casing shoe and a sufficient test pressure has been reached. The interface depth and the nitrogen (annulus) pressure are monitored during the test period. The test is evaluated by calculating the nitrogen mass (volume) at the commencement and completion of the test period. This difference yields an apparent mass (volume) change. As the test occurs over a finite time period, the apparent mass (volume) rate of change can be calculated and linearly forecasted to an annual rate. The annual mass (volume) rate of change is usually expressed in barrels of nitrogen per year (at average well pressure and temperature conditions). The mass (volume) rate of change is subject to the accuracy of the test or Minimum Detectable Leak Rate (MDLR), also expressed in barrels per year.

The following report will outline the mechanical integrity test for Well No. 1. The report includes the cavern and wellbore configuration, temperature logs, and density logs completed during the test.

*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

Summary

On April 25th, 2016 at 07:30, wireline and nitrogen units were rigged up and a gauge run, base temperature log and base density log were completed. At 17:30, nitrogen was injected into Well No. 1 with a target temperature of 75° F. Nitrogen injection continued until operations were shut down for the night at 23:30.

On April 26th, 2016 at 08:55, nitrogen injection was resumed until the nitrogen-brine interface was measured at a depth of 1,509' at an adequate test pressure. The casing test began on April 26th, 2016 at 14:55 with the nitrogen-brine interface at 1,509' and with an annular (nitrogen) pressure of 1058.25 psig and a tubing (brine) pressure of 322.50 psig. The casing test ended with the nitrogen-brine interface at 1,509' and with an annular (nitrogen) pressure of 1056.40 psig and a tubing (brine) pressure of 320.40 psig. The 60-minute casing test passed with a stabilizing pressure trend throughout the testing period. Following the casing test, nitrogen injection continued until the nitrogen-brine interface was measured at a depth of 1,531' at an adequate test pressure.

After an approximate 13 hour stabilization period, on April 27th, 2016 at 09:10 the MIT on Well No. 1 was initialized with an annulus (nitrogen) pressure of 1,069.11 psig, a tubing (brine) pressure of 331.36 psig, and with the nitrogen-brine interface at a depth of 1,532.5'. The well was shut in for a 24 hour test period. On April 28th, 2016 at 09:17 the MIT on Well No. 1 was finalized with an annulus (nitrogen) pressure of 1,063.82 psig, a tubing (brine) pressure of 323.43 psig and with the nitrogen-brine interface at a depth of 1,532.5'. This concluded the MIT on Well No. 1.

*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

Conclusions

The mechanical integrity of Well No. 1 was established with the Nitrogen-Brine Interface Test Method. This test monitored the Nitrogen-Brine Interface for a 24 hour test period. Well No. 1 was initialized with an annulus (nitrogen) pressure of 1,069.11 psig and a tubing (brine) pressure of 331.36 psig and the nitrogen-brine interface at 1,532.5'.

Well No. 1 was finalized with an annulus (nitrogen) pressure of 1,063.82 psig and a tubing (brine) pressure of 323.43 psig and the nitrogen-brine interface at 1,532.5'. Well No. 1 had a test length of 24 hours and a test gradient of 0.75 psi/ft at the 7" cemented casing shoe.

The total gas volume in the annulus and the wellbore was calculated to be 11,856.10 SCF at the start of the test and 11,800.15 SCF at the end of the test for a calculated "decrease" in gas volume of 55.94 SCF. The calculated gas volume was based on the measured wellhead pressure, measured wellbore temperature, known casing annulus volume, and calculated borehole volumes (Appendix D).

The calculated leak rate ("CLR") was 48.38 barrels per year. Considering the calculations, the calculated leak rate is less than the Minimum Detectable Leak Rate ("MDLR") of 244.18 barrels per year.

At the completion of this test, Well No. 1 exhibited the characteristics of a well that has mechanical integrity as required for hydrocarbon storage, in accordance with industry standards and the guidelines established by the State of New Mexico Oil Conservation Division.

*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

Daily Activities

April 25th, 2016

Show up to location and spot equipment. Hold daily safety meeting and review JSAs. Rig up wireline, crane, and lubricator. Run in hole with gauge run and tag bend in tubing at 1,750'. Run in hole with wireline and record base temperature and density logs. Rig up fittings on 5-1/2" X 3-1/2" annulus for nitrogen injection. Start nitrogen injection. Rig down lubricator and crane. Secure well for the night.

April 26th, 2016

Show up to location, hold daily safety meeting, and review JSAs. Rig up lubricator and crane. Alternate injecting nitrogen and pumping brine in order to spot nitrogen-brine interface above the 7" casing shoe at 1,509' for the 60 minute casing test. The test started with an annulus pressure of 1,058.25 psig and a tubing pressure of 322.50 psig. The test ended with an annulus pressure of 1056.40 psig and a tubing pressure of 320.40 psig. The interface at the beginning and end of the test was measured at 1,509'. The pressure trend during the 60 minute casing test showed a stabilization curve with pressure flattening out over the test. The test passed and nitrogen injection was continued into the cavern borehole. Alternate injecting nitrogen and pumping brine in order to spot the nitrogen-brine interface at 1,531' at an adequate test pressure. Rig down lubricator, crane, and nitrogen unit. Secure well and allow to stabilize overnight.

April 27th, 2016

Show up to location, hold daily safety meeting, and review JSAs. Rig up lubricator and crane. Run in hole with temperature log and initialize test with density log. The nitrogen-brine interface was located at 1,532.5'. Test initialization annulus pressure was 1,069.11 psig and initialization tubing pressure was 331.36 psig. Rig down crane and lubricator. Secure well for the night.

April 28th, 2016

Show up to location, hold daily safety meeting, and review JSAs. Rig up lubricator and crane. Run in hole with temperature log and finalize test with density log. The nitrogen-brine interface was located at 1,532.5'. Test finalization annulus pressure was 1,063.82 psig and finalization tubing pressure was 323.43 psig. Rig down crane and lubricator. Secure and return well to Western Refining.

*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

Test Participants

Western Refining Company, LP

Ken Parker.....Project Manager

Lonquist Field Service, LLC

Eric Busch.....Operations Manager

Will George.....Petroleum / Test Engineer

Ben Bergman.....Sr. Staff Engineer

Cased Hole Solutions

Cased Hole Solutions Personnel.....Wireline Operator

Pro Petro Services

Nitrogen Personnel.....Nitrogen Injection

Stone Oilfield Services

Stone Oilfield Personnel.....Pump Truck

*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

Calculations

Minimum Detectable Leak Rate – MDLR

The test sensitivity is defined as the ability of the test calculations and measurements to determine the status of the mechanical integrity of the well and wellbore. The conventional test sensitivity calculation using this test methodology is the Minimum Detectable Leak Rate (MDLR).

$$MDLR = \frac{[B_V * L_R * (T_c)]}{T_L}$$

Where:

B_V	=	1.34 bbls/ft (APPENDIX D)
L_R	=	0.50 feet
T_c	=	365 days/year
T_L	=	1 day
MDLR	=	244.18 bbls/year

Therefore: $(1.34 \times 0.50 \times 365)/1 = 244.18$ bbls/year*

*Hand calculations may yield different final MDLR due to rounding.

Volume Calculations – Annular Space & Borehole

Using the methodology outlined in the MIT procedure the following volumes were calculated:

Initial Wellbore Volume ($V_{I(Borehole)}$)

- Annulus Pressure – 1,069.11 psig
- Tubing Pressure – 331.36 psig
- Wellbore Temperature – Logged (APPENDIX F)
- Volume
 - 5-1/2" x 3-1/2" Annulus – 0.011 bbls/ft
 - 7" x 3-1/2" Annulus – 0.027 bbls/ft
 - Borehole – APPENDIX D

$$(V_I) = \sum_o^{I/F} (N_2)_i$$

$V_{I(Borehole)} = 11,856.10$ SCF

Final Wellbore Volume ($V_{F(Borehole)}$)

- Annulus Pressure – 1,063.82 psig
- Tubing Pressure – 323.43 psig
- Wellbore Temperature – Logged (APPENDIX F)
- Volume
 - 5-1/2" x 3-1/2" Annulus – 0.011 bbls/ft
 - 7" x 3-1/2" Annulus – 0.027 bbls/ft
 - Borehole – APPENDIX D

$$(V_F) = \sum_o^{I/F} (N_2)_i$$

$V_{F(Borehole)} = 11,800.15$ SCF

**MIT Report – Western Refining Company, LP
State LPG Storage No. 1**

Borehole Volume Change:

$$(\Delta V)_{STP(Borehole)} = (\Delta V)_{I(Borehole)} - (\Delta V)_{F(Borehole)}$$

$$(\Delta V)_{STP(Borehole)} = 55.94 SCF$$

The calculated volume/mass change is based on standard temperature and pressure and to evaluate the test results against the MDLR the calculated volume/mass change is converted to downhole conditions with the following equation:

$$(\Delta V_{WB}) = \left(\frac{[(Z_A) * (T_A) * R * (\Delta V)_{STP}]}{[(P_A) * N_{GC}]} \right)$$

Where:

(Z_A)	=	1.00002
(T_A)	=	534.68 °R
R	=	Specific Gas Constant
$(\Delta V)_{STP}$	=	55.94 SCF
(P_A)	=	1110.35 psi
N_{GC}	=	Nitrogen Gas Conversion (13.80 SCF = 1 lb)
(ΔV_{WB})	=	0.74 ft³/day

To calculate an annual volume change to compare to the MDLR the following calculations were completed:

$$(\Delta V_{ANNUAL}) = (\Delta V_{WB}) * 365(day/year)$$

Where:

(ΔV_{WB})	=	0.74 ft ³ /day
1 year	=	365 days
(ΔV_{ANNUAL})	=	271.64 ft³/yr

Where:

(ΔV_{ANNUAL})	=	271.64 ft ³ /yr
1 bbl	=	5.6146 ft ³
CLR (bbls/year)	=	$(\Delta V_{ANNUAL}) / 5.6146 \text{ ft}^3$
Calculated Leak Rate	=	48.38 bbls/year*

***Hand calculations may yield different final CLR due to rounding.**

MIT Report – Western Refining Company, LP
State LPG Storage No. 1

Well Data Sheet

TEST INFORMATION AND RESULTS

Well Name:	Well No. 1
Operator:	Western Refining
State:	New Mexico
County:	Lea
Field:	Jal Station
API Number:	30-025-35954

WELL INFORMATION

Cemented Casing			Casing Liner		
Casing Size	7	inches	Casing Size	5 1/2	inches
Casing ID	6.366	inches	Casing ID	4.825	inches
Casing Weight	23	lbs/ft	Casing Weight	NA	lbs/ft
Grade	H-40		Grade	NA	
Depth	1521	feet	Depth	1480	feet

Hanging String No. 1			Hanging String No. 2		
Casing Size	3 1/2	inches	Casing Size		inches
Casing ID	2.992	inches	Casing ID		inches
Casing Weight	9	lbs/ft	Casing Weight		lbs/ft
Grade	J-55		Grade		
Depth	2308	feet	Depth		feet

Cavern

Cavern Size	201,000.0	bbls
Compressibility	0.61	bbls/psi
Cavern TD	1900	feet

FINAL TEST INFORMATION

Effective Casing Shoe	1521	feet	Casing Shoe Pressure (avg)	1138.38	psi
Test Gradient	0.75	psi/ft	Interface Pressure (avg)	1138.82	psi
Brine Specific Gravity	1.2		Surface Tubing Pressure (avg)	327.39	psi
Nitrogen Temperature (avg)	75	deg F	Surface Annulus Pressure (avg)	1066.47	psi
Interface Depth	1532.5	feet	Pressure Increase	-5.30	psi
Gas Compressibility (avg)	1.00002		Conversion	14.70	psi

Volume			Nitrogen		
Annular Volume No. 1	0.011	bbls/ft	Surface to Casing Shoe (avg)	7134.74	SCF
Annular Volume No. 2	0.027	bbls/ft	Casing Shoe to Interface (avg)	4693.39	SCF
Surface to Casing Shoe	17.0	bbls	Total (avg)	11828.13	SCF
Liner Shoe to Casing Shoe	1.1	bbls			
Casing Shoe to Interface	11.4	bbls			
Total	28.4	bbls			

Brine

Cavern Pre-Pressure	107	psi
Brine Injection	600	bbls

TEST RESULTS

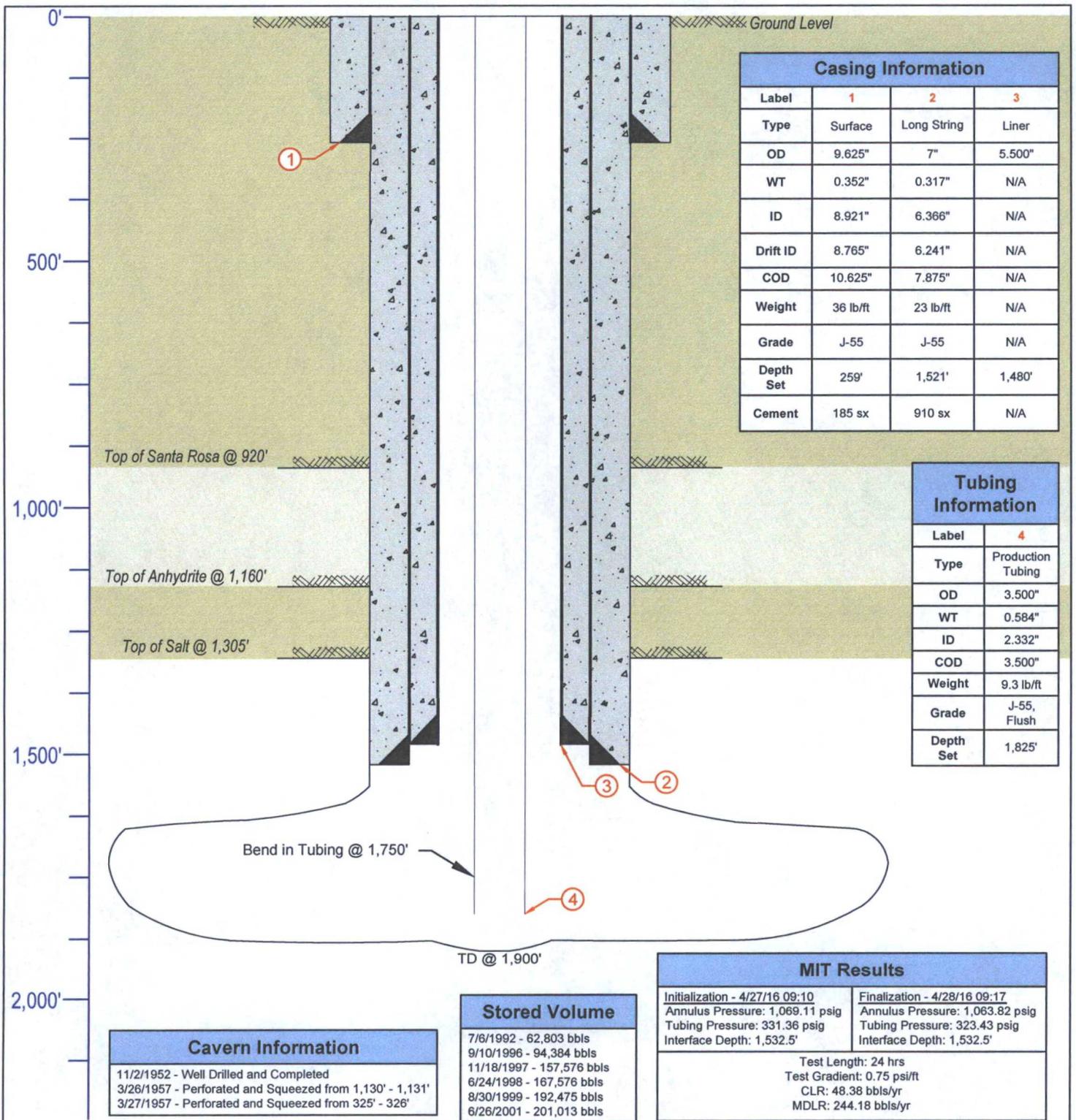
Test Initialization Information			Test Finalization Information		
Date / Time	4/27/16	9:10	Date / Time	4/28/16	9:17
Tubing Pressure	331.36	psig	Tubing Pressure	323.43	psig
Annulus Pressure	1069.11	psig	Annulus Pressure	1063.82	psig
Wellbore Temperature (avg)	75	deg F	Wellbore Temperature (avg)	75	deg F
Nitrogen/Brine Interface	1532.5	feet	Nitrogen/Brine Interface	1532.5	feet

Test Results

MDLR	244.18	bbls/yr	Test Length	24	hours
Calculated Volume Change	55.94	bbls/yr	Test Length	1.0	days
Test Gradient	0.75	psi/ft	Logging Resolution	0.50	feet
Tubing Pressure Change	7.9	psi	Wireline TD	1750	feet
Annulus Pressure Change	5.3	psi			

*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

MIT/Well Schematic



LONQUIST & CO. LLC PETROLEUM ENGINEERS ENERGY ADVISORS AUSTIN HOUSTON WICHITA CALGARY	Western Refining Company, LP		State LPG Well No. 1 - MIT Results	
	Country: USA	State/Province: New Mexico	County/Parish: Lea	
Survey/STR: M-32-23S-37E	API No.: 30-025-35954	Site: Jal	Status: Storage	
Texas License: F-8952	Serial No.:	Field:	Ground Elevation: 3,312'	
3345 Bee Cave Road, Suite 201 Austin, Texas 78746 Tel: 512.732.9812 Fax: 512.732.9816	Drawn: WHG	Project No.:	Date: 5/10/2016	
Rev No.:	Reviewed: BHB	Approved: ETB		
Notes:				

*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

Appendix A – MIT Test Procedure

LONQUIST

FIELD**SERVICE**

WELL TEST

Project No.:

**Western Refining Company, LP
Well No. 1
Mechanical Integrity Test**

Date: March 2016

Page: 1 of 11

Well: No. 1**State:** New Mexico**County:** LEA**Field:** Jal Station**API:** 30-025-35954**Oper:** Western Refining Company, LP**Location:** Jal**Status:** State LPG Well

INTRODUCTION

Well No. 1 is operated by Western Refining Company, LP located in the Jal Station Field in Lea County, New Mexico. The purpose of the Mechanical Integrity Test (MIT) procedure is to test the integrity of the underground storage system that includes the cavern, cemented casing, and wellhead to determine if the system demonstrates the mechanical integrity required to support hydrocarbon storage operations.

In accordance with the Oil Conservation Divisions of New Mexico Well No 1 is undergoing an MIT to remain compliant.

The test procedure will consist of the following basic steps:

1. Pre-pressure the cavern to the required pre pressure.
 - o Annulus Pressure: **310.52 psig**
 - o 0.75 psi/ft final test gradient at the effective casing shoe (1,521').
2. Complete pre-test density and temperature logs.
3. Inject nitrogen into Well No. 1 and monitor nitrogen/brine interface location to place above cemented casing to complete a preliminary test on the cemented casing.
4. Inject nitrogen into Well No. 1 and monitor nitrogen/brine interface location to place interface below the effective cemented casing shoe.
5. Monitor wellhead pressures, wellbore temperature, and the nitrogen/brine interface location during the specified test period.
6. Complete and submit MIT report to Western Refining Company, LP and the Oil Conservation Division of New Mexico within 45 days.
7. Place Well No. 1 in operation and return to Western Refining personnel.

The test procedure includes the following information:

- Nitrogen/Brine Interface Test Planning Sheet
- Wellbore Schematic
- Contact Information
- 2008 Sonar Data (Incomplete Sonar)

PREPARED BY	DATE	APPROVED BY	DATE	CLIENT APPROVAL	DATE	Lonquist Field Service, LLC
TMH	3/1/2016	ETB	3/1/2016			Texas Registration No. F-9147

LONQUIST

FIELD**SERVICE**

WELL TEST

Western Refining Company, LP
Well No. 1
Mechanical Integrity Test

Project No.:

Date: March 2016

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Well: No. 1

State: New Mexico

County: LEA

Field: Jal Station

API: 30-025-35954

Oper: Western Refining Company, LP

Location: Jal

Status: State LPG Well

Well Preparation

1. Wellhead should be isolated from all surface piping during the test. This may include blind flanges, skillet flanges, and 1" or 2" test flanges.
 - a. Wellhead should keep the ability to bleed excess brine pressure back into surface system during the test.
2. Install pressure recording equipment on wellhead. Pressure equipment should be able to record wellhead pressures and wellhead temperatures during the test period. Additional equipment to measure the nitrogen stream injected into the well will be necessary.
 - a. All equipment calibration certifications to be provided with final reports.
3. Wellhead configuration should permit the use of a wireline lubricator and logging tools.
4. Pre-pressure the cavern to predetermined pressure with saturated brine
 - a. See MIT Data Sheet
5. Wellhead pressure should be stable prior to starting the test.
 - a. Stable wellhead pressure – Decline less than 10 psi/day

Well Injection Phase

6. Move in and rig up wireline unit, logging tools, pressure equipment, and nitrogen services.
7. Run CCL and a sinker bar as a gauge run to ensure density tools will pass through the tubing.
8. Complete base density log and wellbore temperature log
 - a. Base Temperature Log – (0' – TD)
 - b. Base Density Log – (TD' – 200' above effective casing shoe depth)
 - c. Density logs should include: tubing collars, effective casing shoe, and approved logging scales.
 - d. All depths are approximate
9. Start Nitrogen Injection at a slow rate (<500 SCFM). Nitrogen temperature should be regulated to the average wellbore temperature.
10. Monitor the nitrogen/brine interface and wellbore pressures to locate the interface above the casing shoe and conduct a preliminary casing test.
 - a. Casing Test – Minimum of 60 minutes
 - b. Monitor and record wellhead pressures and interface at the start and completion of the test
11. Continue nitrogen injection and monitor the nitrogen/brine interface and wellbore pressures to locate the nitrogen/brine interface below the effective casing shoe. The targeted gradient is 0.75 psi/ft at the effective casing shoe and cannot exceed a test pressure gradient of 0.81 psi/ft at the effective casing shoe at any time.
12. After nitrogen/brine interface is located sufficiently below the cemented casing shoe stop nitrogen injection and shut well in for a short stabilization period.

PREPARED BY	DATE	APPROVED BY	DATE	CLIENT APPROVAL	DATE	Lonquist Field Service, LLC
TMH	3/1/2016	ETB	3/1/2016			Texas Registration No. F-9147

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FIELD SERVICE

WELL TEST

Western Refining Company, LP
Well No. 1
Mechanical Integrity Test

Project No.:

Date: March 2016

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Well: No. 1

State: New Mexico

County: LEA

Field: Jal Station

API: 30-025-35954

Oper: Western Refining Company, LP

Location: Jal

Status: State LPG Well

13. Shut in for 30 minutes – Monitor pressures, interface location, and check wellhead for possible leak paths.
14. Complete post injection density logs
 - a. Post Injection Density Log – (TD' – 200' above effective casing shoe).
 - b. Record wellhead pressures.
 - c. Density logs should include: tubing collars, nitrogen/brine interface, production casing shoe, and approved logging scales.
 - d. All depths are approximate
15. Remove logging tools and shut well for the stabilization period.
16. Complete pre-test calculations based on wellhead pressure measurements, nitrogen volume measurements, wellbore temperatures, and interface locations.
 - a. Refer to Test Calculations Section
17. MIRU sonar tools and perform a sonar survey on the cavern
 - a. Shoot the roof of the cavern with upshots
 - b. Shoot the floor of the cavern with downshots
 - c. Record data every 10'

Test Initialization

18. Move in and rig up wireline unit, logging tools, and pressure equipment.
19. Complete initial density log and wellbore temperature log
 - a. Base Temperature Log – (0' – TD')
 - b. Initial Density Log – (TD' – 200' above effective casing shoe)
 - c. Density logs should include: tubing collars, nitrogen/brine interface, production casing shoe, and approved logging scales.
 - d. All depths are approximate
20. Shut well in for test period – Minimum of 24 hours

Test Finalization

21. After planned test duration, move in and rig up wireline unit, logging tools, and pressure equipment.
 - a. Complete final density log and wellbore temperature log
 - b. Final Temperature Log – (0' – TD')
 - c. Final Density Log – (TD' – 200' above effective casing shoe)
 - d. Density logs should include: tubing collars, nitrogen/brine interface, production casing shoe, and approved logging scales.
 - e. All depths are approximate
22. Determine if the test is complete based on results or if the test should be extended. Repeat Steps 15 - 17 if required.

PREPARED BY	DATE	APPROVED BY	DATE	CLIENT APPROVAL	DATE	Lonquist Field Service, LLC
TMH	3/1/2016	ETB	3/1/2016			Texas Registration No. F-9147

		WELL TEST		Project No.:	
		Western Refining Company, LP Well No. 1 Mechanical Integrity Test		Date: March 2016	
Well: No. 1		State: New Mexico		County: LEA	
API: 30-025-35954		Oper: Western Refining Company, LP		Location: Jal	
				Field: Jal Station	
				Page: 4 of 11	
				Status: State LPG Well	

Nitrogen/Brine Interface Test Calculations

The test methodology proposed in this procedure is developed using the industry standard nitrogen/brine interface test method.

The wellhead pressures and temperature, wellbore temperatures, nitrogen volumes, and interface location will be recorded throughout the test period and will allow for the calculation of the borehole volumes, test sensitivity, minimum test durations, and final test calculations.

All test calculations are based on the following measured parameters: wellhead pressure, nitrogen volumes, annular casing unit volume, wellbore temperatures, and interface locations. In addition to the measured parameters, the following calculated parameters are important in completing the test: unit borehole volume, MDLR, and test length.

To evaluate the test the calculated nitrogen volume/mass at the start of the test is compared to the calculated nitrogen volume/mass at the end of the test. This rate of volume change and its comparison to the test sensitivity is one of the components in determining the final results of the MIT.

TEST SENSITIVITY AND TEST LENGTH

Test sensitivity calculations are the functions of three factors:

- Casing volume – Calculated
- Log Resolution – Recommended: 5":100' logging scale
- Minimum test duration – 24 hours

The test sensitivity is defined at the ability of the test calculations and measurements to determine the status of the mechanical integrity of the well and wellbore. The conventional test sensitivity calculation using this test methodology is the Minimum Detectable Leak Rate (MDLR).

$$MDLR = \frac{[B_v * L_R * (T_c)]}{T_L}$$

Where:

- MDLR = Minimum Detectable Leak Rate (bbl/year)
- B_v = Borehole Volume (bbls/ft)
- L_R = Log Resolution (feet)
- T_c = Time Constant (365 days/year)
- T_L = Test Length (days)

Using the MDLR method a reasonable and acceptable test accuracy and sensitivity can be calculated for the Mechanical Integrity Test. The MDLR calculation is based on downhole measurements of the test conditions.

PREPARED BY	DATE	APPROVED BY	DATE	CLIENT APPROVAL	DATE	Lonquist Field Service, LLC
TMH	3/1/2016	ETB	3/1/2016			Texas Registration No. F-9147

LONQUIST

FIELD SERVICE

WELL TEST

Western Refining Company, LP
Well No. 1
Mechanical Integrity Test

Project No.:

Date: March 2016

Page: 5 of 11

Well: No. 1

State: New Mexico

County: LEA

Field: Jal Station

API: 30-025-35954

Oper: Western Refining Company, LP

Location: Jal

Status: State LPG Well

The MDLR must be less than 1000 bbl/year for the designated test period. The length of the test must a minimum of 24 hours and sufficient in length to keep the MDLR below 1000 bbl/year and allow for a proper evaluation of the well test.

TEST EVALUATIONS

The volume/mass of nitrogen located in the wellbore can be affected by following: temperature stabilization, cavern leaching/creep, and volume changes. Using P-V-T gas calculations, any changes in the volume/mass of the nitrogen in the wellbore can be evaluated based on wellbore temperature changes, pressure changes, and/or wellbore leakage.

Pressure Calculations

The average wellbore pressure is calculated based on the wellhead surface pressure, wellbore temperature, and depth of the specific interval. The following equation is used to calculate the average wellbore pressure

$$(P_A)_i = (P_A)_{i-1} \left[1 + \left(\frac{D}{(R)(Z_A)_i(T)_i} \right) \right]$$

Where:

- $(P_A)_i$ = Pressure @ Depth Interval (Calculated) (psia)
- $(P_A)_{i-1}$ = Pressure @ Previous Depth Interval (Calculated) (psi)
- D = Depth Interval (ft)
- $(Z_A)_i$ = Gas Compressibility Factor @ Depth Interval
- R = Specific Gas Constant
- $(T)_i$ = Wellbore Temperature ($^{\circ}$ R)

Nitrogen Calculations

The following calculation is used to calculate the volume/mass of nitrogen for specific intervals over the entire wellbore at the start and end of the test period:

$$(N_2)_i = \left(\frac{[(P_A)_i * (B_v)_i]}{[(Z_A)_i * (T_A)_i * R]} \right) * N_{GC}$$

Where:

- $(N_2)_i$ = Nitrogen Volume (SCF)
- $(P_A)_i$ = Average Wellbore Pressure (psi)
- $(B_v)_i$ = Wellbore Volume (ft³)

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LONQUIST

FIELD SERVICE

WELL TEST

Western Refining Company, LP
Well No. 1
Mechanical Integrity Test

Project No.:

Date: March 2016

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Well: No. 1

State: New Mexico

County: LEA

Field: Jal Station

API: 30-025-35954

Oper: Western Refining Company, LP

Location: Jal

Status: State LPG Well

$(Z_A)_i$ = Gas Compressibility Factor
 $(T_A)_i$ = Wellbore Temperature (°R)
 R = Specific Gas Constant
 N_{GC} = Nitrogen Gas Conversion (13.8 SCF = 1 lb)

Upon completion of each specific volume/mass calculation the sum of the each interval is calculated to determine the volume/mass of nitrogen in the wellbore at the beginning of the test. After the test is complete the calculation and summation is repeated to determine the final test results.

The following equations represent the summation of the intervals to the nitrogen/brine interface at the start and completion of the test:

$$(V_I) = \sum_o^{I/F} (N_2)_i$$

$$(V_F) = \sum_o^{I/F} (N_2)_i$$

The results of the beginning and completion of the test are compared and evaluated to determine the change in nitrogen volume during the test period. The following equation is used for the comparison:

$$(\Delta V)_{STP} = (V_I) - (V_F)$$

The calculated volume/mass change is based on standard temperature and pressure and to evaluate the test results against the MDLR the calculated volume/mass change is converted to downhole conditions with the following equation:

$$(\Delta V_{WB}) = \left(\frac{[(Z_A) * (T_A) * R * (\Delta V)_{STP}]}{[(P_A) * N_{GC}]} \right)$$

Where:

(ΔV_{WB}) = Nitrogen Volume Change (ft³) – Wellbore Conditions
 (Z_A) = Average Gas Compressibility Factor for Test Period
 (T_A) = Average Wellbore Temperature (°R) for Test Period
 R = Specific Gas Constant
 $(\Delta V)_{STP}$ = Nitrogen Volume Change (SCF) – Standard Conditions
 (P_A) = Average Wellbore Pressure for Test Period (psi)
 N_{GC} = Nitrogen Gas Conversion (13.8 SCF = 1 lb)

PREPARED BY	DATE	APPROVED BY	DATE	CLIENT APPROVAL	DATE	Lonquist Field Service, LLC
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LONQUIST

FIELD SERVICE

WELL TEST

Western Refining Company, LP
Well No. 1
Mechanical Integrity Test

Project No.:

Date: March 2016

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Well: No. 1

State: New Mexico

County: LEA

Field: Jal Station

API: 30-025-35954

Oper: Western Refining Company, LP

Location: Jal

Status: State LPG Well

The change in wellbore volume for the test period is converted into a calculated annual volume change. The following equation determines this volume change:

$$(\Delta V_{ANNUAL}) = \frac{[(\Delta V_{WB}) * 24(hr/day) * 365(day/yr)]}{T_L}$$

Where:

- (ΔV_{ANNUAL}) = Calculated Volume Change (bbls/year)
 (ΔV_{WB}) = Nitrogen Volume Change (ft³) – Wellbore Conditions
 (T_L) = Test Length (hrs)

A positive change in wellbore volume indicates a calculated loss of nitrogen from the wellbore during the test period. A negative change in wellbore volume indicates a calculated increase (apparent nitrogen influx) in nitrogen volume during the test period.

Pass/Fail Criteria

Test results are evaluated for a successful test using the following criteria:

- MDLR less than 1000 bbls/day
- Calculated Annual Volume Change less than the MDLR
- Pressure response, wellbore temperature, and interface movement should respond in a way that represents the cavern has mechanical integrity

Test Reporting

A written report will be prepared within 45 days of completion and submitted to the Oil Conservation Division of New Mexico. The report will include the test procedures, test chronology, test results and conclusions, wireline logs, pressure information, and all supporting documentation.

PREPARED BY	DATE	APPROVED BY	DATE	CLIENT APPROVAL	DATE	Lonquist Field Service, LLC
TMH	3/1/2016	ETB	3/1/2016			Texas Registration No. F-9147

LONQUIST

FIELD SERVICE

WELL TEST

Western Refining Company, LP
Well No. 1
Mechanical Integrity Test

Project No.:

Date: March 2016

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Well: No. 1

State: New Mexico

County: LEA

Field: Jal Station

API: 30-025-35954

Oper: Western Refining Company, LP

Location: Jal

Status: State LPG Well

TEST PLANNING SHEET

Well Name:	Well No. 1
Operator:	Western Refinery
State:	New Mexico
County:	Lea
Field:	Jal Station
API No:	30-025-35954

WELL INFORMATION

Cemented Casing			Casing Liner		
Casing Size	7	inches	Casing Size	5 1/2	inches
Casing ID	6.366	inches	Casing ID	4.825	inches
Casing Weight	23	lbs/ft	Casing Weight		lbs/ft
Grade	J-55		Grade		
Depth	1521	feet	Depth	1480	feet

Hanging String No. 1			Hanging String No. 2		
Casing Size	3 1/2	inches	Casing Size		inches
Casing ID	2.992	inches	Casing ID		inches
Casing Weight	9.3	lbs/ft	Casing Weight		lbs/ft
Grade	J-55		Grade		
Depth	1825	feet	Depth		feet

Cavern		
Cavern Size		201,000.0 bbls
Compressibility		0.61 bbls/psi
Cavern TD		1900 feet

TEST INFORMATION

Effective Casing Shoe	1521	feet	Casing Shoe Pressure	1140.75	psig
Test Gradient	0.75	psi/ft	Interface Pressure	1141.11	psig
Brine Specific Gravity	1.2		Surface Tubing Pressure	346.12	psig
Nitrogen Temperature	65	deg F	Surface Annulus Pressure	1083.01	psig
Interface Depth	1530	feet	Pressure Increase	35.60	psi
Gas Compressibility	0.9983		Conversion	14.70	psi

Volume			Nitrogen		
Annular Volume No. 1	0.011	bbls/ft	Surface to Casing Shoe	7288.652	SCF
Annular Volume No. 2	0.027	bbls/ft	Casing Shoe to Interface	2069.57	SCF
Surface to Liner Shoe	15.859	bbls	Total	9358.222	SCF
Liner Shoe to Casing Shoe	1.13	bbls	Brine		
Casing Shoe to Interface	4.70	bbls	Cavern Pre-Pressure	310.52	psig
Total	21.68	bbls	Brine Injection	189.13	bbls

PREPARED BY	DATE	APPROVED BY	DATE	CLIENT APPROVAL	DATE	Lonquist Field Service, LLC
TMH	3/1/2016	ETB	3/1/2016			Texas Registration No. F-9147

LONQUIST

FIELD

SERVICE

WELL TEST

Project No.:

Western Refining Company, LP
Well No. 1
Mechanical Integrity Test

Date: March 2016

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Well: No. 1

State: New Mexico

County: LEA

Field: Jal Station

API: 30-025-35954

Oper: Western Refining Company, LP

Location: Jal

Status: State LPG Well

WELL SCHEMATIC

PREPARED BY

DATE

APPROVED BY

DATE

CLIENT
APPROVAL

DATE

Lonquist Field Service, LLC

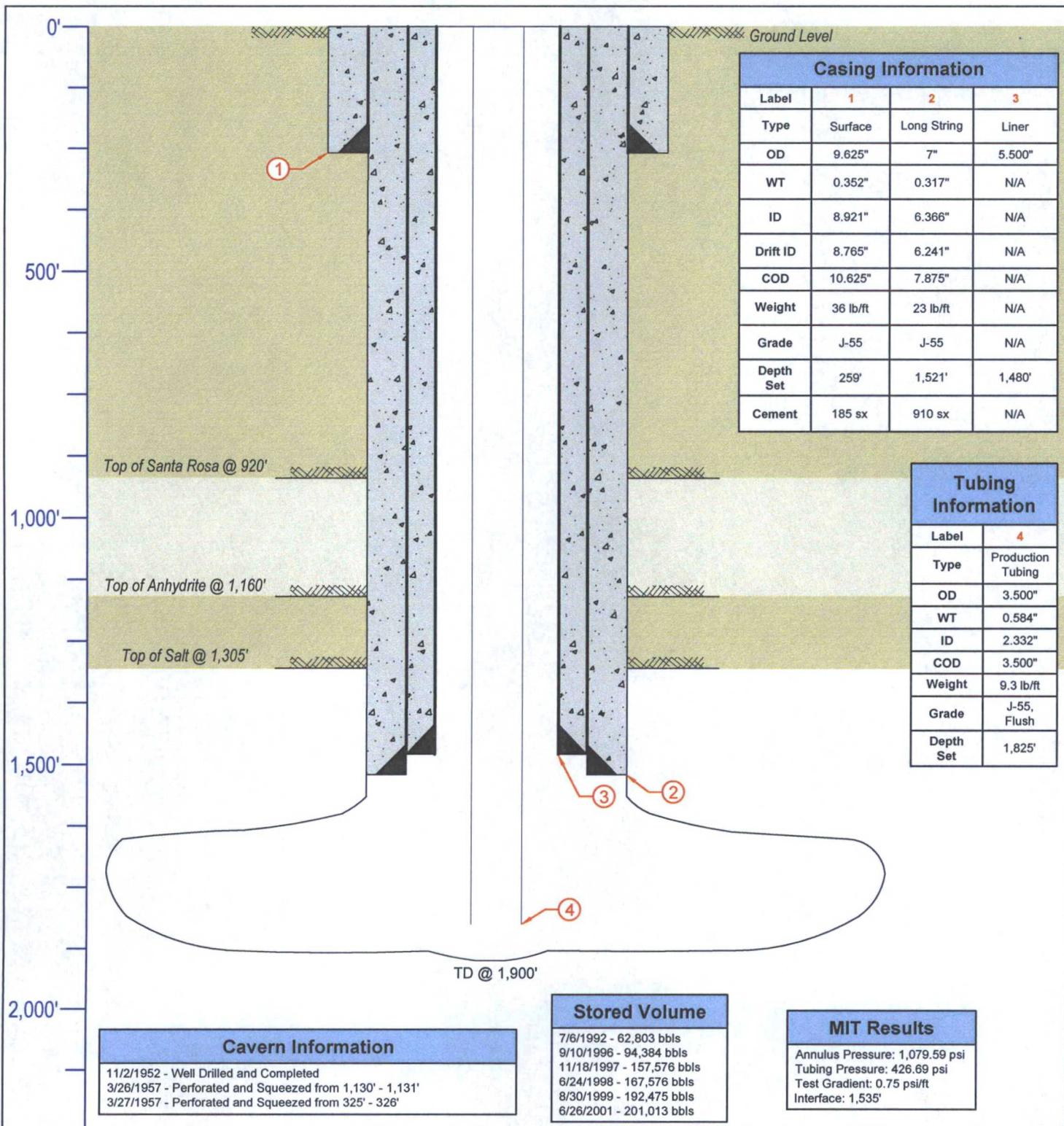
TMH

3/1/2016

ETB

3/1/2016

Texas Registration No. F-9147



LONQUIST & CO. LLC PETROLEUM ENGINEERS ENERGY ADVISORS AUSTIN HOUSTON WICHITA CALGARY	Western Refining Company, LP		State LPG Well No. 1	
	Country: USA	State/Province: New Mexico	County/Parish: Lea	
Survey/STR: M-32-23S-37E	API No.: 30-025-35954	Site: Jal	Status: Storage	
Texas License F-8952	Serial No.:	Field:	Ground Elevation: 3,312'	
3345 Bee Cave Road, Suite 201 Austin, Texas 78746 Tel: 512.732.9812 Fax: 512.732.9816	Project No.:	Date: 3/1/2016	Date: 3/1/2016	
Drawn: MMC	Reviewed:	Approved:		
Rev No:	Notes:			

LONQUIST

FIELD SERVICE

WELL TEST

Western Refining Company, LP
Well No. 1
Mechanical Integrity Test

Project No.:

Date: March 2016

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Well: No. 1

State: New Mexico

County: LEA

Field: Jal Station

API: 30-025-35954

Oper: Western Refining Company, LP

Location: Jal

Status: State LPG Well

CONTACT INFORMATION

Well Owner

Western Refining
PO Box 1345
Jal, New Mexico 88252

- Ken Parker – Site Manager
 - Telephone – (505) 395-2632
 - Mobile – (915) 471-1607
 - Email – ken.parker@westernrefining.com

Engineering Consultants

Lonquist Field Service, LLC
1001 McKinney, Suite 1650
Houston, Texas 77002

- Eric Busch – Senior Vice President
 - Telephone – (832) 216-0785
 - Fax – (713) 559-9959
 - Email – eric@lonquist.com
- Tyler Hendrickson – Petroleum Engineer
 - Telephone – (713) 559 9988
 - Fax – (713) 559-9959
 - Email – tyler@lonquist.com

PREPARED BY	DATE	APPROVED BY	DATE	CLIENT APPROVAL	DATE	Lonquist Field Service, LLC
TMH	3/1/2016	ETB	3/1/2016			Texas Registration No. F-9147

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FIELD

SERVICE

WELL TEST

Project No.:

Western Refining Company, LP
Well No. 1
Mechanical Integrity Test

Date: March 2016

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Well: No. 1

State: New Mexico

County: LEA

Field: Jal Station

API: 30-025-35954

Oper: Western Refining Company, LP

Location: Jal

Status: State LPG Well

2008 SONAR VOLUME TABLE

PREPARED BY	DATE	APPROVED BY	DATE	CLIENT APPROVAL	DATE	Lonquist Field Service, LLC
TMH	3/1/2016	ETB	3/1/2016			Texas Registration No. F-9147

1-0804.inv
SONARWIRE GLOBAL, LLC
Depth versus Volume

WESTERN REFINING
STORAGE WELL NO. 1

JAL, NM
Fri, Apr 18, 2008

Depth	Cubic ft. per ft.	Cubic ft. total	Barrels per ft.	Barrels total
1522	1.5	1.5	0.3	0.3
1523	1.6	3.1	0.3	0.6
1524	1.8	4.9	0.3	0.9
1525	2.1	7.0	0.4	1.2
1526	2.3	9.3	0.4	1.7
1527	3.6	13.0	0.6	2.3
1528	5.2	18.2	0.9	3.2
1529	4.5	22.7	0.8	4.0
1530	3.8	26.4	0.7	4.7
1531	3.1	29.6	0.6	5.3
1532	1116.8	1146.3	198.9	204.2
1533	1110.1	2256.5	197.7	401.9
1534	514.8	2771.3	91.7	493.6
1535	145.5	2916.8	25.9	519.5
1536	2.1	2918.8	0.4	519.9
1537	2.4	2921.2	0.4	520.3
1538	2.7	2924.0	0.5	520.8
1539	521.1	3445.1	92.8	613.6
1540	512.9	3958.0	91.3	704.9
1541	506.7	4464.7	90.3	795.2
1542	538.2	5002.9	95.9	891.0
1543	571.2	5574.0	101.7	992.8
1544	561.5	6135.5	100.0	1092.8
1545	552.0	6687.5	98.3	1191.1
1546	1.5	6689.0	0.3	1191.4
1547	546.6	7235.5	97.3	1288.7
1548	519.7	7755.2	92.6	1381.3
1549	493.6	8248.9	87.9	1469.2
1550	476.6	8725.5	84.9	1554.1
1551	460.3	9185.8	82.0	1636.1
1552	453.6	9639.5	80.8	1716.9
1553	447.3	10086.8	79.7	1796.5
1554	447.7	10534.5	79.7	1876.3
1555	448.6	10983.1	79.9	1956.2
1556	455.4	11438.5	81.1	2037.3
1557	462.7	11901.2	82.4	2119.7
1558	434.6	12335.8	77.4	2197.1
1559	408.0	12743.9	72.7	2269.8
1560	378.6	13122.4	67.4	2337.2
1561	352.4	13474.8	62.8	2400.0
1562	310.9	13785.6	55.4	2455.3
1563	273.7	14059.4	48.8	2504.1
1564	234.7	14294.1	41.8	2545.9
1565	199.2	14493.3	35.5	2581.4
1566	295.0	14788.3	52.5	2633.9
1567	418.9	15207.2	74.6	2708.5
1568	411.5	15618.6	73.3	2781.8
1569	404.7	16023.4	72.1	2853.9
1570	351.5	16374.9	62.6	2916.5
1571	302.5	16677.5	53.9	2970.4
1572	333.3	17010.7	59.4	3029.7
1573	366.0	17376.7	65.2	3094.9

*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

Appendix B – Injection Pressure Data

Nitrogen Injection

Well Name:	Well No. 1
Operator:	Western Refining
State:	New Mexico
County:	Lea
Field:	Jal Station
API Number:	30-025-35954

Flow Conditions

Date / Time	Annulus Gauge		Tubing Gauge		Flow Conditions
	Pressure psig	Temp deg F	Pressure psig	Temp deg F	Temp deg F
4/25/16 18:11	254.17	92.16	109.38	92.81	100.34
4/25/16 18:20	255.09	91.89	109.11	92.47	97.55
4/25/16 18:30	255.98	90.56	109.12	91.09	94.78
4/25/16 18:40	276.54	90.11	109.23	90.62	92.98
4/25/16 18:50	392.81	89.62	110.79	90.10	92.51
4/25/16 19:00	637.08	89.24	115.87	89.68	89.04
4/25/16 19:10	722.08	88.90	119.25	89.31	87.84
4/25/16 19:20	721.81	88.39	118.61	88.80	87.10
4/25/16 19:30	721.79	86.74	118.81	87.85	84.90
4/25/16 19:40	728.71	86.31	97.91	86.83	82.99
4/25/16 19:50	730.17	85.82	64.08	86.14	82.35
4/25/16 20:00	743.88	84.50	157.62	87.28	81.90
4/25/16 20:10	758.86	83.74	175.35	87.40	81.28
4/25/16 20:20	773.20	82.02	193.45	83.65	80.48
4/25/16 20:30	777.80	79.65	60.55	79.81	79.29
4/25/16 20:40	776.94	77.17	59.29	77.14	78.08
4/25/16 20:50	776.31	73.74	58.52	74.01	77.13
4/25/16 21:00	775.77	72.18	58.02	72.16	75.97
4/25/16 21:10	783.71	71.08	57.78	70.96	73.95
4/25/16 21:20	811.88	70.19	59.02	70.07	73.40
4/25/16 21:30	811.43	69.44	58.04	69.32	71.75
4/25/16 21:40	822.55	68.80	199.85	69.54	71.14
4/25/16 21:50	839.35	68.55	231.44	70.48	70.32
4/25/16 22:00	855.51	67.92	252.55	71.09	69.19
4/25/16 22:10	871.23	67.25	274.46	71.62	68.22
4/25/16 22:20	871.60	66.42	131.78	66.65	67.23
4/25/16 22:30	874.41	65.95	130.71	65.91	67.12
4/25/16 22:40	879.56	65.10	131.86	65.02	64.91
4/25/16 22:50	878.70	64.05	2.99	63.95	65.48
4/25/16 23:00	878.16	63.10	2.52	62.96	64.58
4/25/16 23:10	877.70	62.41	127.32	62.31	63.83
4/25/16 23:20	877.31	61.54	127.21	61.39	62.91
4/25/16 23:30	876.94	60.75	126.80	60.60	62.24
4/25/16 23:40	876.66	60.42	126.43	60.29	61.70
4/25/16 23:50	876.38	61.65	126.09	61.62	61.56
4/26/16 0:00	876.05	62.29	125.77	62.25	61.59
4/26/16 0:10	875.81	61.48	125.48	61.43	60.99
4/26/16 0:20	875.59	60.02	125.22	59.96	60.06
4/26/16 0:30	875.34	60.09	124.96	59.96	60.08
4/26/16 0:40	875.14	60.30	124.72	60.23	60.22
4/26/16 0:50	874.93	60.44	124.49	60.39	60.35
4/26/16 1:00	874.75	60.45	124.27	60.41	60.31
4/26/16 1:10	874.55	60.40	124.07	60.40	60.17

Nitrogen Injection

Well Name:	Well No. 1
Operator:	Western Refining
State:	New Mexico
County:	Lea
Field:	Jal Station
API Number:	30-025-35954

Flow Conditions

Date / Time	Annulus Gauge		Tubing Gauge		Flow Conditions
	Pressure psig	Temp deg F	Pressure psig	Temp deg F	Temp deg F
4/26/16 1:20	874.36	60.08	123.88	60.07	59.91
4/26/16 1:30	874.21	59.99	123.69	59.98	59.67
4/26/16 1:40	874.01	59.93	123.50	59.92	59.53
4/26/16 1:50	873.88	59.04	123.34	58.98	58.96
4/26/16 2:00	873.77	58.28	123.18	58.22	58.39
4/26/16 2:10	873.60	57.72	123.02	57.66	57.97
4/26/16 2:20	873.46	57.42	122.85	57.37	57.65
4/26/16 2:30	873.32	56.92	122.70	56.87	57.21
4/26/16 2:40	873.20	55.98	122.57	55.91	56.62
4/26/16 2:50	873.05	55.34	122.42	55.24	56.22
4/26/16 3:00	872.94	54.78	122.29	54.68	55.81
4/26/16 3:10	872.84	54.37	122.16	54.25	55.44
4/26/16 3:20	872.70	53.99	122.04	53.90	55.10
4/26/16 3:30	872.60	53.46	121.91	53.36	54.66
4/26/16 3:40	872.50	53.14	121.79	53.06	54.25
4/26/16 3:50	872.41	52.93	121.68	52.85	53.87
4/26/16 4:00	872.30	52.92	121.56	52.90	53.66
4/26/16 4:10	872.20	53.15	121.45	53.14	53.50
4/26/16 4:20	872.11	52.98	121.34	52.98	53.28
4/26/16 4:30	872.03	53.37	121.23	53.39	53.20
4/26/16 4:40	871.91	53.40	121.13	53.44	53.07
4/26/16 4:50	871.83	53.12	121.03	53.15	52.85
4/26/16 5:00	871.74	52.73	120.93	52.74	52.61
4/26/16 5:10	871.63	51.53	120.85	51.52	52.11
4/26/16 5:20	871.56	50.14	120.74	50.09	51.55
4/26/16 5:30	871.48	49.18	120.66	49.15	51.05
4/26/16 5:40	871.42	48.51	120.57	48.47	50.60
4/26/16 5:50	871.34	47.95	120.48	47.91	50.12
4/26/16 6:00	871.25	48.16	120.40	48.17	49.89
4/26/16 6:10	871.17	49.04	120.30	49.10	49.90
4/26/16 6:20	871.09	49.58	120.21	49.65	49.81
4/26/16 6:30	870.99	49.37	120.13	49.41	49.59
4/26/16 6:40	870.95	48.70	120.05	48.72	49.20
4/26/16 6:50	870.86	47.88	119.97	47.88	48.74
4/26/16 7:00	870.80	47.26	119.90	47.26	48.35
4/26/16 7:10	870.74	46.78	119.84	46.79	48.07
4/26/16 7:20	870.67	46.26	119.76	46.26	47.79
4/26/16 7:30	870.61	46.80	1.93	46.82	47.85
4/26/16 7:40	870.53	48.46	1.96	48.44	48.71
4/26/16 7:50	9.17	51.04	-1.59	51.31	-76.00
4/26/16 8:00	-1.60	51.80	-1.58	51.86	-76.00
4/26/16 8:10	-1.61	51.78	-1.58	51.75	-76.00
4/26/16 8:20	-1.60	52.68	-1.59	52.73	-76.00

Nitrogen Injection

Well Name:	Well No. 1
Operator:	Western Refining
State:	New Mexico
County:	Lea
Field:	Jal Station
API Number:	30-025-35954

Flow Conditions

Date / Time	Annulus Gauge		Tubing Gauge		Flow Conditions
	Pressure psig	Temp deg F	Pressure psig	Temp deg F	Temp deg F
4/26/16 8:30	-1.61	52.67	-1.57	52.74	-76.00
4/26/16 8:40	-1.60	52.68	-1.58	52.75	-76.00
4/26/16 8:50	869.89	55.06	118.52	54.91	-76.00
4/26/16 9:00	876.44	58.38	240.29	58.45	68.80
4/26/16 9:10	889.73	60.53	221.51	60.69	71.98
4/26/16 9:20	902.26	62.72	243.96	62.92	75.14
4/26/16 9:30	913.72	65.51	254.95	65.71	77.87
4/26/16 9:40	925.72	67.97	284.33	68.21	81.21
4/26/16 9:50	934.20	70.57	214.92	70.82	84.44
4/26/16 10:00	932.96	72.47	214.17	72.64	80.79
4/26/16 10:10	934.51	73.98	213.50	74.05	84.20
4/26/16 10:20	937.29	74.41	213.09	74.37	83.25
4/26/16 10:30	940.32	76.36	212.76	76.16	85.29
4/26/16 10:40	940.84	76.15	227.01	76.86	89.39
4/26/16 10:50	954.16	77.40	305.17	77.63	91.76
4/26/16 11:00	966.96	78.74	313.64	78.89	94.70
4/26/16 11:10	978.33	80.06	322.69	80.21	96.91
4/26/16 11:20	989.29	81.93	336.36	81.81	98.60
4/26/16 11:30	999.29	83.45	341.00	83.06	100.10
4/26/16 11:40	1001.01	83.87	265.91	83.34	100.13
4/26/16 11:50	1004.43	84.39	265.04	83.89	99.09
4/26/16 12:00	1004.45	84.29	264.17	83.78	101.69
4/26/16 12:10	1003.75	84.12	263.37	83.61	102.31
4/26/16 12:20	1003.16	84.55	262.93	84.18	103.43
4/26/16 12:30	1012.93	84.54	350.11	84.18	104.65
4/26/16 12:40	1024.32	82.85	371.24	82.81	105.72
4/26/16 12:50	1035.05	83.67	389.90	83.98	107.05
4/26/16 13:00	1045.83	84.49	402.78	84.51	105.80
4/26/16 13:10	1056.32	87.48	409.30	87.44	107.34
4/26/16 13:20	1059.36	89.76	329.11	89.78	108.85
4/26/16 13:30	1058.18	89.68	327.78	89.65	108.91
4/26/16 13:40	1058.87	89.29	326.83	89.37	108.20
4/26/16 13:50	1059.97	88.34	326.13	88.29	106.16
4/26/16 14:00	1060.83	84.31	325.51	84.25	102.86
4/26/16 14:10	1060.21	84.99	324.80	84.92	102.01
4/26/16 14:20	1059.74	85.57	324.17	85.96	101.73
4/26/16 14:30	1059.23	86.46	323.82	86.53	101.68
4/26/16 14:40	1058.82	88.38	323.18	88.51	103.12
4/26/16 14:50	1058.45	88.71	322.73	88.80	103.76
4/26/16 15:00	1058.03	89.02	322.35	89.22	104.55
4/26/16 15:10	1057.74	88.59	321.88	88.81	103.91
4/26/16 15:20	1057.42	87.16	321.57	87.35	102.63
4/26/16 15:30	1057.09	88.72	321.27	89.00	103.48

Nitrogen Injection

Well Name:	Well No. 1
Operator:	Western Refining
State:	New Mexico
County:	Lea
Field:	Jal Station
API Number:	30-025-35954

Flow Conditions

Date / Time	Annulus Gauge		Tubing Gauge		Flow Conditions
	Pressure psig	Temp deg F	Pressure psig	Temp deg F	Temp deg F
4/26/16 15:40	1056.80	88.80	320.82	89.12	103.41
4/26/16 15:50	1056.50	87.87	320.52	88.22	102.88
4/26/16 16:00	1056.23	87.33	320.25	87.69	102.07
4/26/16 16:10	1055.99	86.78	319.92	87.15	101.40
4/26/16 16:20	1055.77	85.83	319.67	86.22	100.36
4/26/16 16:30	1056.74	85.88	319.51	86.33	100.08
4/26/16 16:40	1057.13	84.89	319.50	85.36	98.04
4/26/16 16:50	1057.22	84.69	318.28	85.16	97.22
4/26/16 17:00	1059.11	84.44	319.21	84.92	92.54
4/26/16 17:10	1061.30	83.86	320.64	84.35	83.92
4/26/16 17:20	1062.63	83.48	392.85	84.03	87.09
4/26/16 17:30	1074.92	83.46	417.15	84.02	88.74
4/26/16 17:40	1080.85	83.62	346.24	84.19	89.79
4/26/16 17:50	1081.48	83.40	345.98	83.95	89.66
4/26/16 18:00	1081.30	82.78	345.38	83.31	89.16
4/26/16 18:10	1080.84	82.28	344.87	82.81	87.45
4/26/16 18:20	1080.44	82.10	344.41	82.61	85.15
4/26/16 18:30	1080.06	81.57	343.99	82.08	82.83
4/26/16 18:40	1079.79	81.22	343.61	81.71	81.29
4/26/16 18:50	1079.41	80.50	343.31	80.98	79.97
4/26/16 19:00	1080.42	79.33	343.29	79.75	80.70

*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

Appendix C – Test Pressure Data

TEST PRESSURE

Well Name:	Well No. 1
Operator:	Western Refining
State:	New Mexico
County:	Lea
Field:	Jal Station
API Number:	30-025-35954

PRESSURE INFORMATION

Date / Time	Annulus Pressure		Tubing Pressure	
	Pressure psig	Temp deg F	Pressure psig	Temp deg F
4/27/16 9:10	1069.114	62.07	331.357	61.92
4/27/16 9:25	1069.105	62.95	330.085	63.02
4/27/16 9:40	1069.061	64.57	0.638	64.61
4/27/16 9:55	1069.002	66.46	0.750	66.55
4/27/16 10:10	1068.987	68.35	330.744	68.43
4/27/16 10:25	1068.962	70.21	330.631	70.16
4/27/16 10:40	1068.931	71.76	330.535	71.58
4/27/16 10:55	1068.878	72.25	330.430	72.27
4/27/16 11:10	1068.891	73.91	330.347	74.07
4/27/16 11:25	1068.858	77.58	330.271	76.96
4/27/16 11:40	1068.934	81.11	330.172	80.23
4/27/16 11:55	1069.152	82.16	330.087	81.14
4/27/16 12:10	1069.477	83.12	329.989	82.27
4/27/16 12:25	1069.553	83.17	329.892	82.62
4/27/16 12:40	1069.488	83.95	329.772	83.57
4/27/16 12:55	1069.403	82.88	329.691	82.78
4/27/16 13:10	1069.303	84.90	329.614	84.60
4/27/16 13:25	1069.259	85.96	329.501	85.75
4/27/16 13:40	1069.264	85.91	329.428	85.89
4/27/16 13:55	1069.150	85.94	329.326	86.10
4/27/16 14:10	1069.054	87.61	329.206	87.79
4/27/16 14:25	1069.008	87.96	329.150	88.02
4/27/16 14:40	1068.934	88.72	329.045	89.00
4/27/16 14:55	1068.849	89.06	328.940	89.45
4/27/16 15:10	1068.794	90.56	328.834	91.08
4/27/16 15:25	1068.706	88.52	328.771	89.17
4/27/16 15:40	1068.642	89.39	328.686	89.92
4/27/16 15:55	1068.562	89.00	328.595	89.77
4/27/16 16:10	1068.545	88.31	328.520	89.11
4/27/16 16:25	1068.364	88.94	328.404	89.73
4/27/16 16:40	1068.344	88.88	328.345	89.72
4/27/16 16:55	1068.255	87.46	328.253	88.32
4/27/16 17:10	1068.186	87.70	328.167	88.53
4/27/16 17:25	1068.091	86.36	328.083	87.17
4/27/16 17:40	1067.991	86.11	327.994	86.92
4/27/16 17:55	1067.885	86.21	327.903	87.00
4/27/16 18:10	1067.790	86.01	327.820	86.71
4/27/16 18:25	1067.717	85.42	327.733	86.17

TEST PRESSURE

Well Name:	Well No. 1
Operator:	Western Refining
State:	New Mexico
County:	Lea
Field:	Jal Station
API Number:	30-025-35954

PRESSURE INFORMATION

Date / Time	Annulus Pressure		Tubing Pressure	
	Pressure psig	Temp deg F	Pressure psig	Temp deg F
4/27/16 18:40	1067.630	84.41	327.654	85.13
4/27/16 18:55	1067.545	83.28	327.583	83.93
4/27/16 19:10	1067.500	82.43	327.509	83.00
4/27/16 19:25	1067.395	81.24	327.434	81.77
4/27/16 19:40	1067.325	79.79	327.359	80.23
4/27/16 19:55	1067.268	78.02	327.299	78.27
4/27/16 20:10	1067.180	76.15	327.253	76.38
4/27/16 20:25	1067.102	73.71	327.197	73.75
4/27/16 20:40	1067.042	70.75	327.131	70.72
4/27/16 20:55	1066.980	68.25	327.081	68.17
4/27/16 21:10	1066.897	66.11	327.016	66.06
4/27/16 21:25	1066.856	64.29	326.930	64.21
4/27/16 21:40	1066.799	64.37	326.859	64.29
4/27/16 21:55	1066.720	63.67	326.781	63.63
4/27/16 22:10	1066.716	63.04	326.721	62.99
4/27/16 22:25	1066.670	61.84	326.685	61.80
4/27/16 22:40	1066.615	60.97	326.612	60.91
4/27/16 22:55	1066.527	59.31	326.549	59.24
4/27/16 23:10	1066.475	58.00	326.498	57.91
4/27/16 23:25	1066.419	57.00	326.437	56.91
4/27/16 23:40	1066.351	55.88	326.365	55.80
4/27/16 23:55	1066.290	54.40	326.301	54.35
4/28/16 0:10	1066.195	53.02	326.217	52.94
4/28/16 0:25	1066.139	51.86	326.172	51.78
4/28/16 0:40	1066.078	51.20	326.088	51.14
4/28/16 0:55	1066.009	50.31	326.018	50.25
4/28/16 1:10	1065.973	49.74	325.974	49.63
4/28/16 1:25	1065.868	49.35	325.895	49.31
4/28/16 1:40	1065.850	48.64	325.836	48.60
4/28/16 1:55	1065.803	48.25	325.772	48.23
4/28/16 2:10	1065.721	47.89	325.706	47.87
4/28/16 2:25	1065.665	47.16	325.649	47.12
4/28/16 2:40	1065.603	47.84	325.590	47.76
4/28/16 2:55	1065.546	47.99	325.522	47.93
4/28/16 3:10	1065.472	48.55	325.447	48.53
4/28/16 3:25	1065.420	47.84	325.399	47.84
4/28/16 3:40	1065.379	47.39	325.341	47.36
4/28/16 3:55	1065.331	47.91	325.287	47.88

TEST PRESSURE

Well Name:	Well No. 1
Operator:	Western Refining
State:	New Mexico
County:	Lea
Field:	Jal Station
API Number:	30-025-35954

PRESSURE INFORMATION

Date / Time	Annulus Pressure		Tubing Pressure	
	Pressure psig	Temp deg F	Pressure psig	Temp deg F
4/28/16 4:10	1065.252	48.38	325.205	48.39
4/28/16 4:25	1065.203	48.49	325.145	48.50
4/28/16 4:40	1065.130	48.59	325.089	48.60
4/28/16 4:55	1065.087	48.98	325.025	48.99
4/28/16 5:10	1065.075	49.09	324.987	49.12
4/28/16 5:25	1064.967	48.71	324.916	48.75
4/28/16 5:40	1064.913	48.48	324.856	48.52
4/28/16 5:55	1064.852	47.99	324.800	48.03
4/28/16 6:10	1064.803	47.61	324.751	47.64
4/28/16 6:25	1064.749	47.61	324.700	47.66
4/28/16 6:40	1064.684	47.82	324.634	47.87
4/28/16 6:55	1064.640	47.83	324.577	47.90
4/28/16 7:10	1064.571	47.86	6.007	47.92
4/28/16 7:25	1064.563	47.68	0.581	47.89
4/28/16 7:40	1064.222	48.10	323.739	48.22
4/28/16 7:55	1064.138	49.76	323.696	49.71
4/28/16 8:10	1064.104	52.08	323.647	52.09
4/28/16 8:25	1064.056	55.66	323.654	55.36
4/28/16 8:40	1063.927	61.20	323.748	60.62
4/28/16 8:55	1063.865	66.32	323.477	65.71
4/28/16 9:10	1063.840	67.96	323.365	67.91
4/28/16 9:17	1063.817	68.00	323.427	68.10

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State LPG Storage No. 1*

Appendix D – Calculated Borehole Volumes

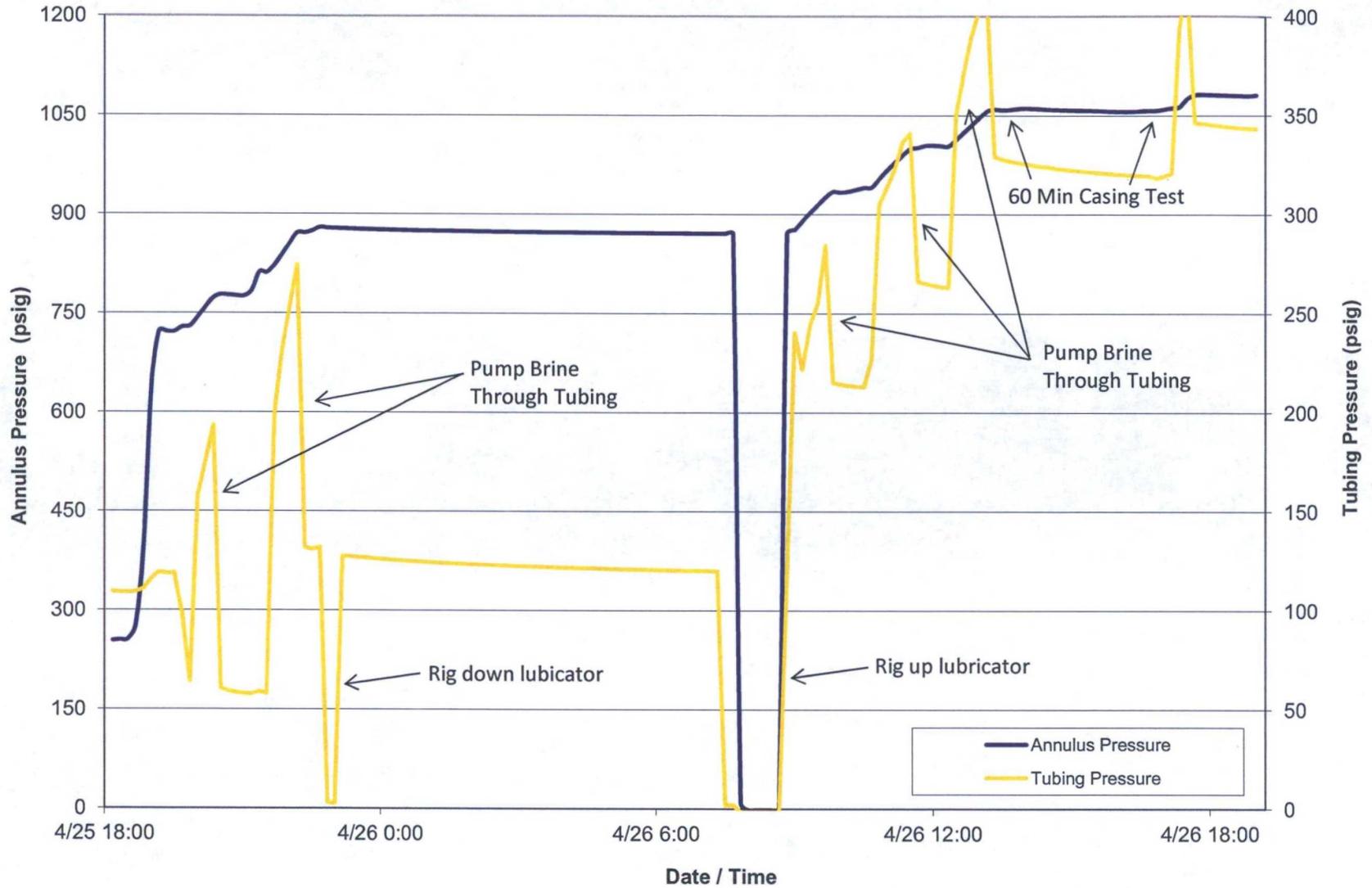
Western Refining Well No. 1 MIT - Borehole Calculations

Inf Depth	N2 Volume	N2 Pressure	Borehole Volume	Borehole Volume	Borehole Volume
Logged	Turbine	Gauge	Cumulative	Incremental Per Interval	Incremental Per Foot
ft	scf	psig	bbls	bbls	bbls/ft
1,520	53,400	1,080.83	N/A	N/A	N/A
1,522	53,850	1,081.14	128.55	1.03	0.52
1,524	54,175	1,081.43	129.29	0.74	0.37
1,526	54,600	1,081.72	130.27	0.98	0.49
1,532.5	58,200	1,080.39	139.01	8.74	1.34

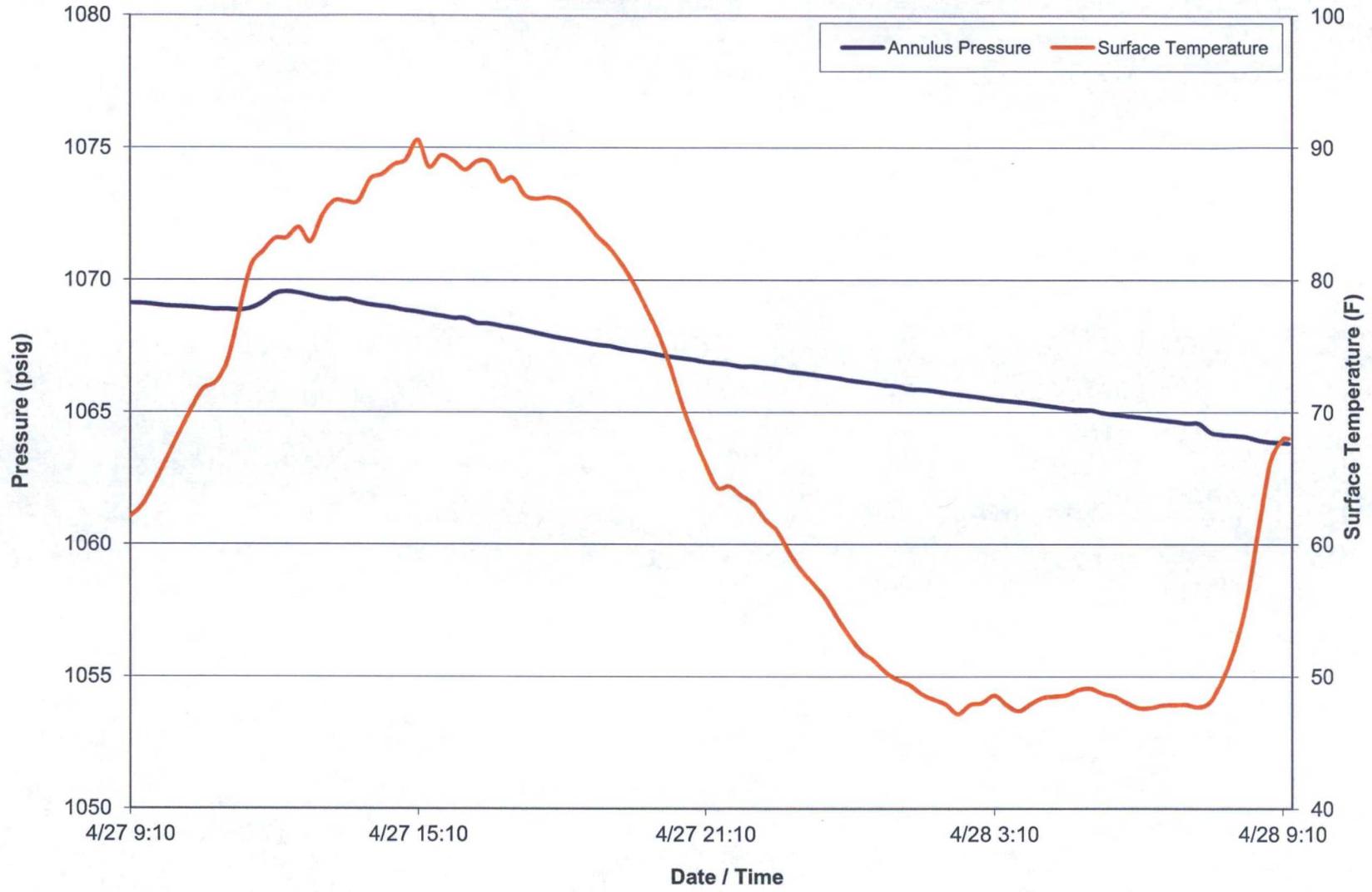
*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

Appendix E – Pressure and Temperature Graphs

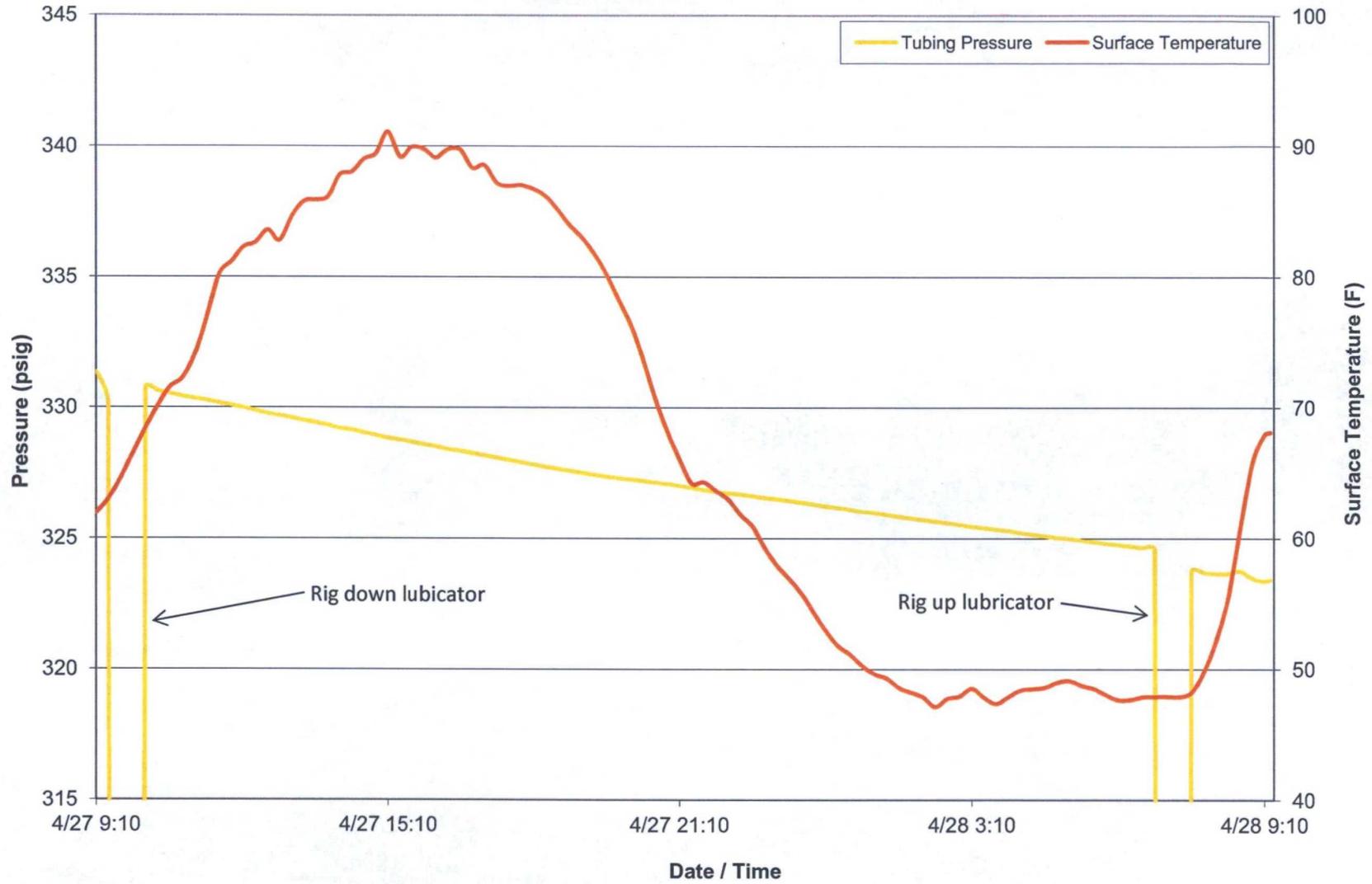
Western Refining Well No. 1 MIT Injection Pressures



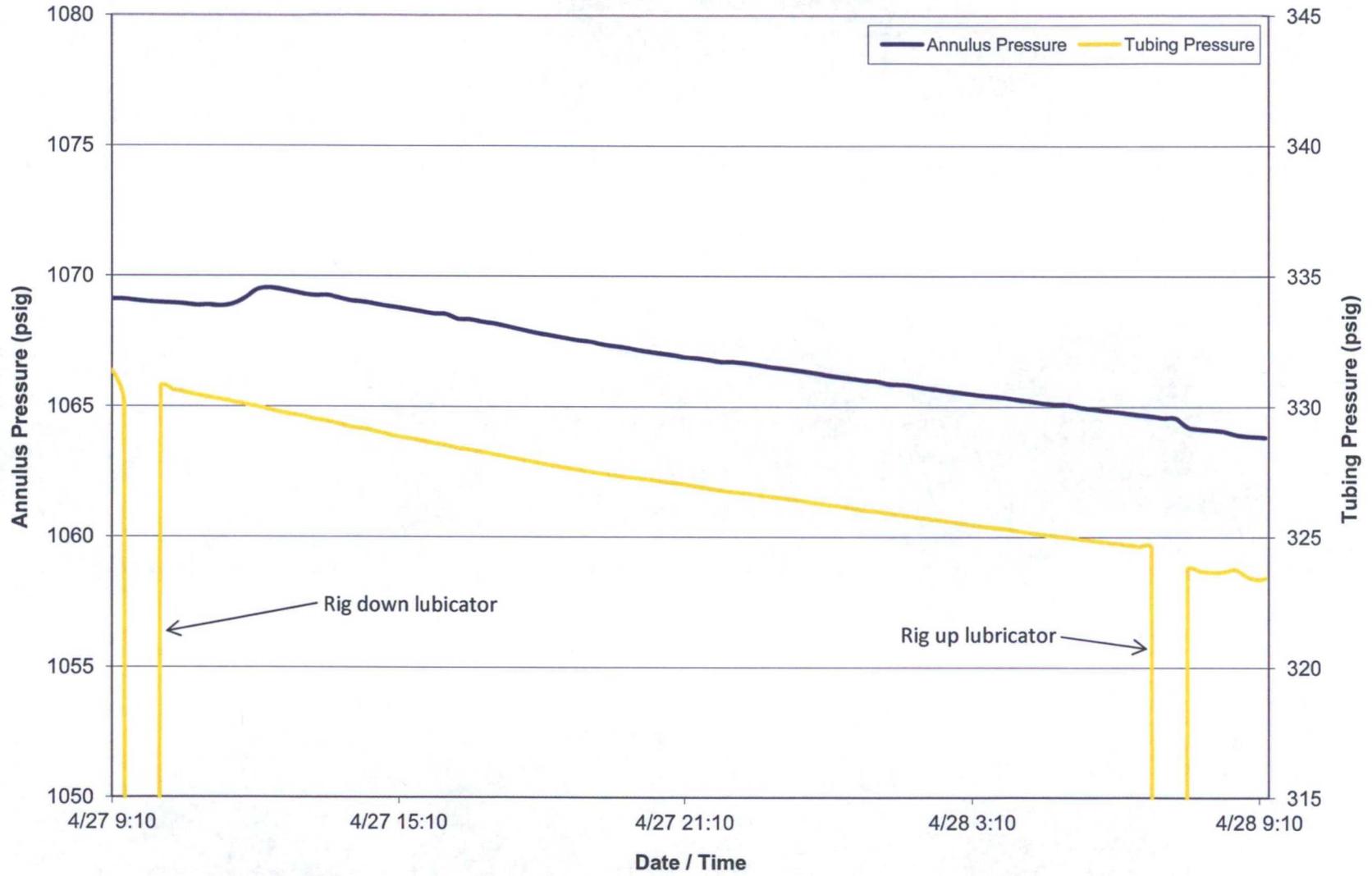
Western Refining Well No. 1 MIT Annulus Test Pressure



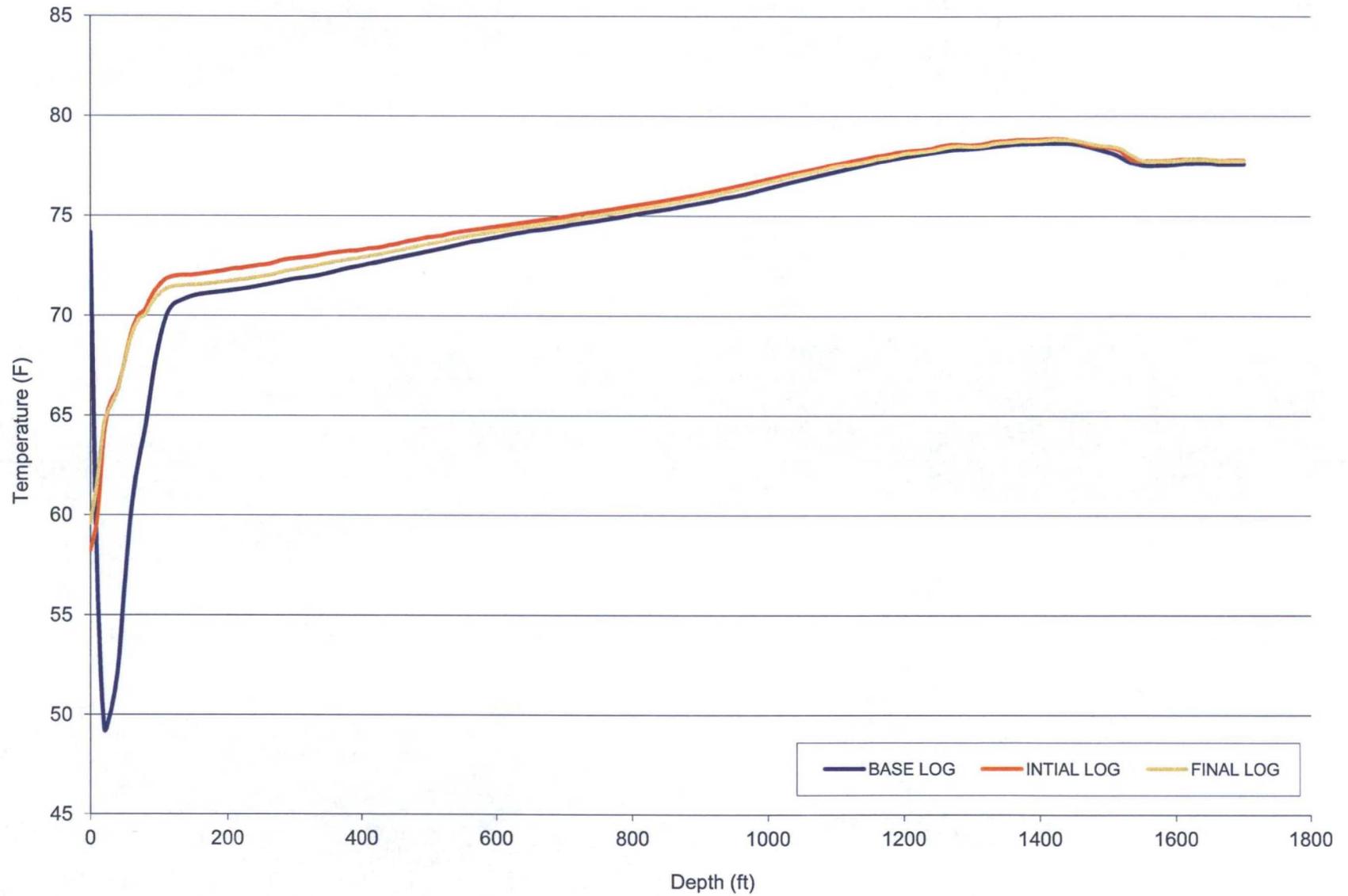
Western Refining Well No. 1 MIT Tubing Test Pressure



Western Refining Well No. 1 MIT Annulus vs. Tubing Pressure



Western Refining Well No. 1 MIT Wellbore Temperature Graph



*MIT Report – Western Refining Company, LP
State LPG Storage No. 1*

Appendix F – Well Logs



Casedhole Solutions

**MIT
DENSITY
SURVEY**

Company WESTERN REFINING COMPANY
Well STATE LPG WELL #1
Field JAL
County LEA
State NEW MEXICO

Company WESTERN REFINING COMPANY
Well STATE LPG WELL #1
Field JAL
County LEA
State NEW MEXICO

Location: API #:

Other Services

Permanent Datum SEC M-321TWP 23S RGE 37E
Log Measured From BOTTOM FLANGE Elevation 3312
Drilling Measured From K.B. D.F. G.L. 3312

Date	4-25-16						
Run Number	ONE						
Depth Driller							
Depth Logger	1750						
Bottom Logged Interval	1750						
Top Log Interval	SURFACE						
Open Hole Size	WATER						
Type Fluid							
Density / Viscosity							
Max. Recorded Temp.							
Estimated Cement Top							
Time Well Ready							
Time Logger on Bottom							
Equipment Number	0839						
Location	HUTCHINSON KS.						
Recorded By	WILL GEORGE						
Witnessed By	THOMASON						
Borehole Record		Tubing Record					
Run Number	Bit	From	To	Size	Weight	From	To
Casing Record	Size	Mgr/Ft	Top	Bottom			
Surface String	9-5/8"	36 lb/ft	Surface	259'			
Prod. String	7"	23 lb/ft	Surface	1521'			
Production String	5-1/2"	N/A	Surface	1825'			
Liner	3-1/2"	9.3 LB/FT	Surface				
Tubing							

<<< Fold Here >>>

All interpretations are opinions based on inferences from electrical or other measurements and we cannot and do not guarantee the accuracy or correctness of any interpretation, and we shall not, except in the case of gross or willful negligence on our part, be liable or responsible for any loss, costs, damages, or expenses incurred or sustained by anyone resulting from any interpretation made by any of our officers, agents or employees. These interpretations are also subject to our general terms and conditions set out in our current Price Schedule.

Comments

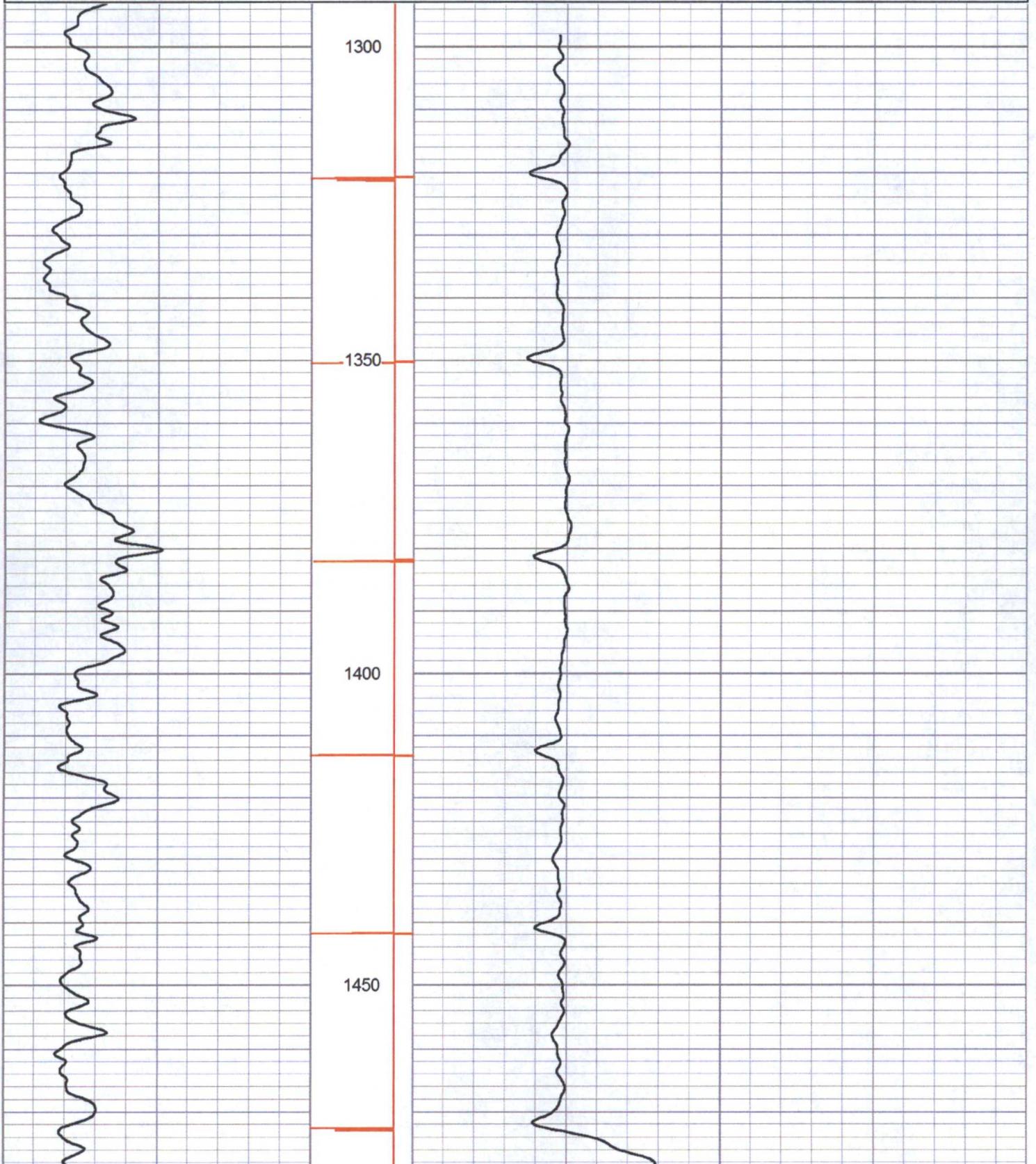
THANK YOU FOR USING CASEDHOLE SOLUTIONS
Bend in Tubing @ 1750'

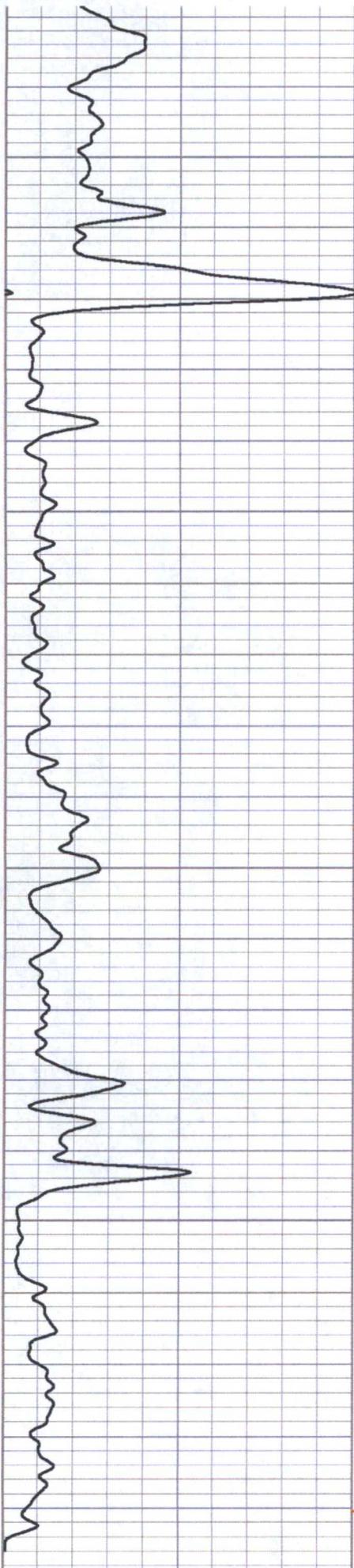


BASE DENSITY PASS

Database File: western refining #1.db
Dataset Pathname: pass4.4
Presentation Format: gr-n-ccl
Dataset Creation: Mon Apr 25 17:01:47 2016 by Calc Std Casedhole 09061
Charted by: Depth in Feet scaled 1:240

0 GR (GAPI) 150 9 CCL -2 0 DENSITY (cps) 2500





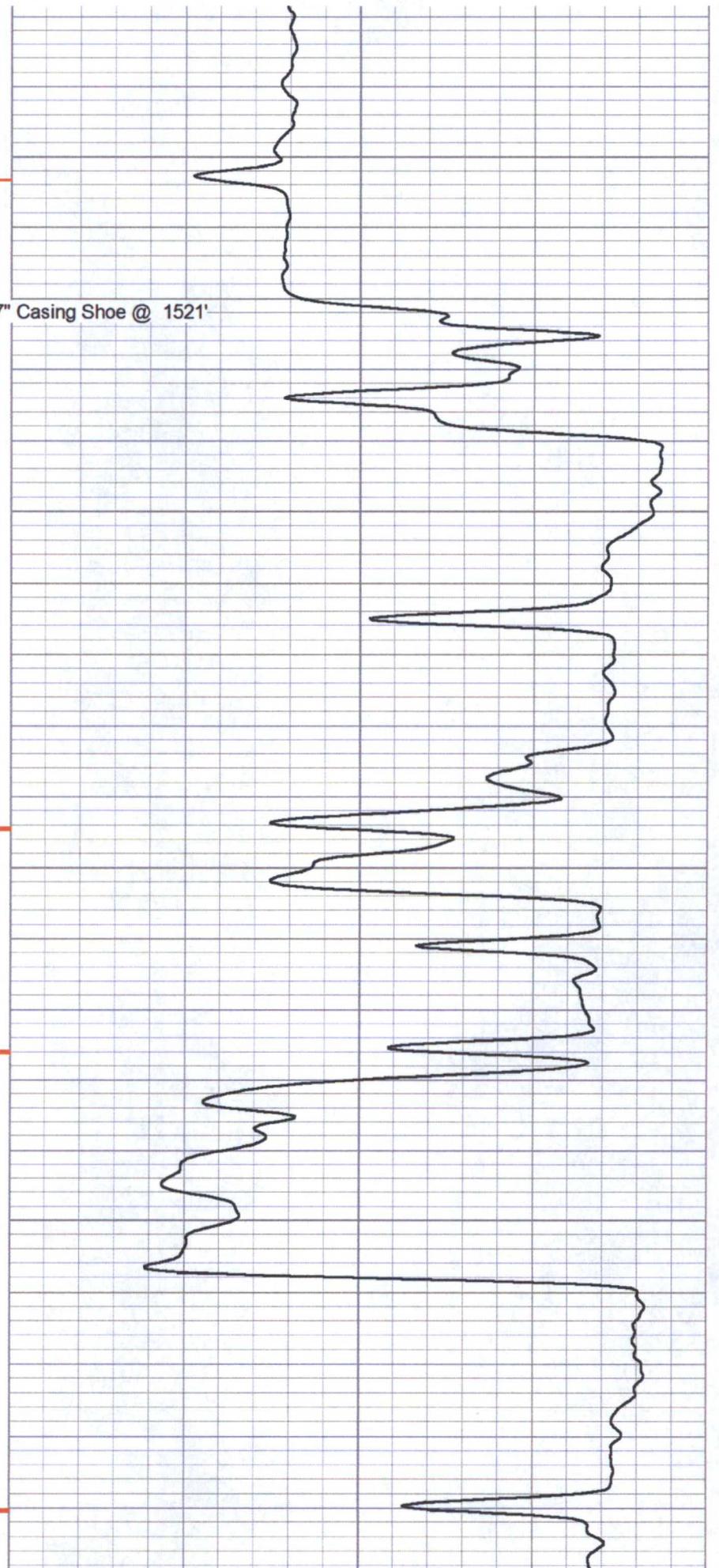
1500

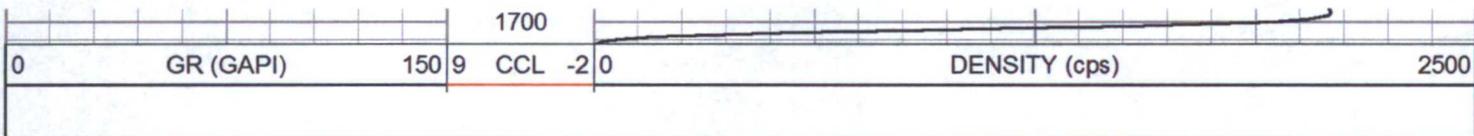
7" Casing Shoe @ 1521'

1550

1600

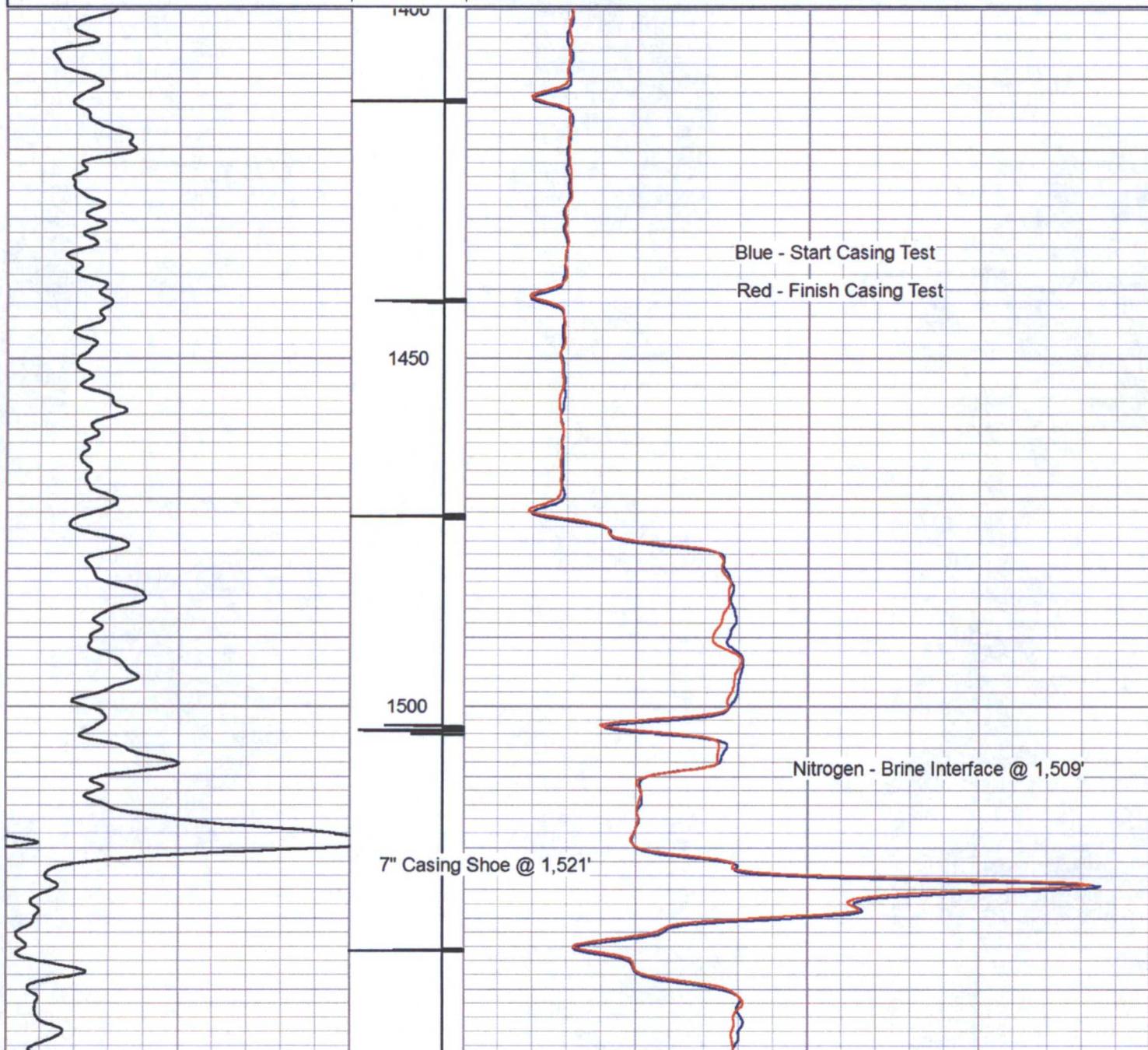
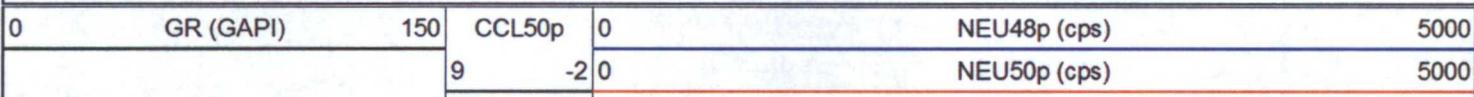
1650

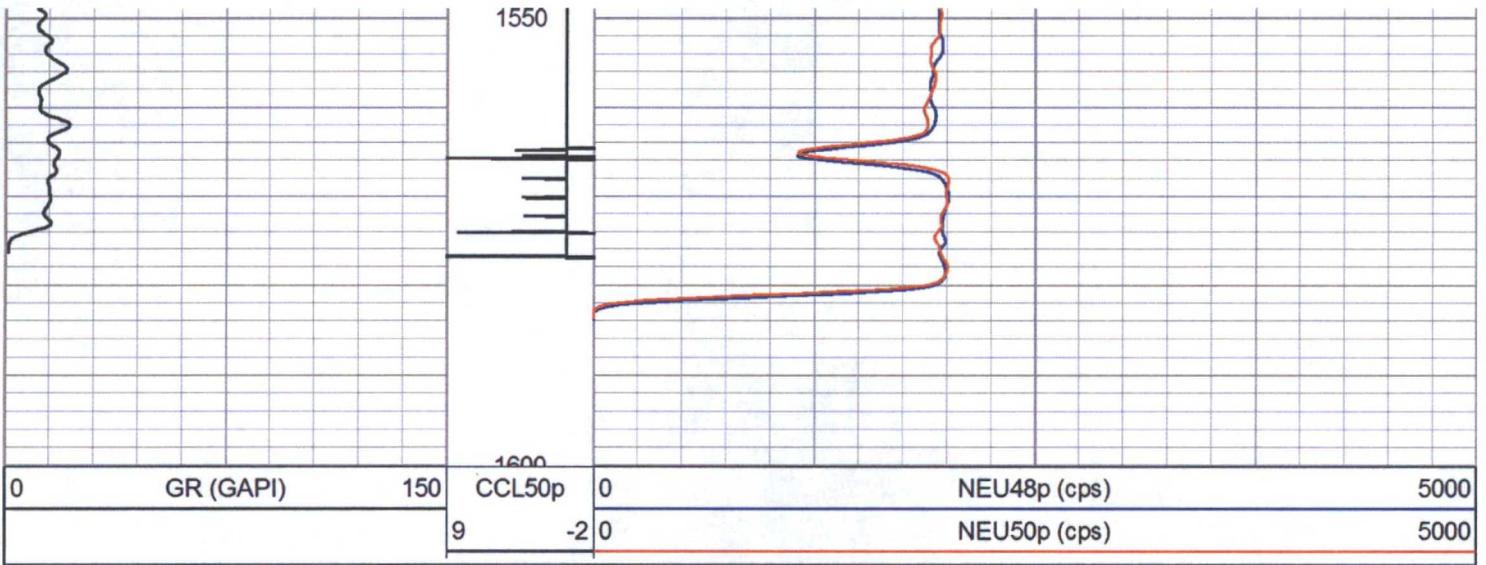




CASING TEST

Database File: western refining #1.db
 Dataset Pathname: pass48ct
 Presentation Format: gr-n-ccl
 Dataset Creation: Wed May 11 14:29:56 2016
 Charted by: Depth in Feet scaled 1:240



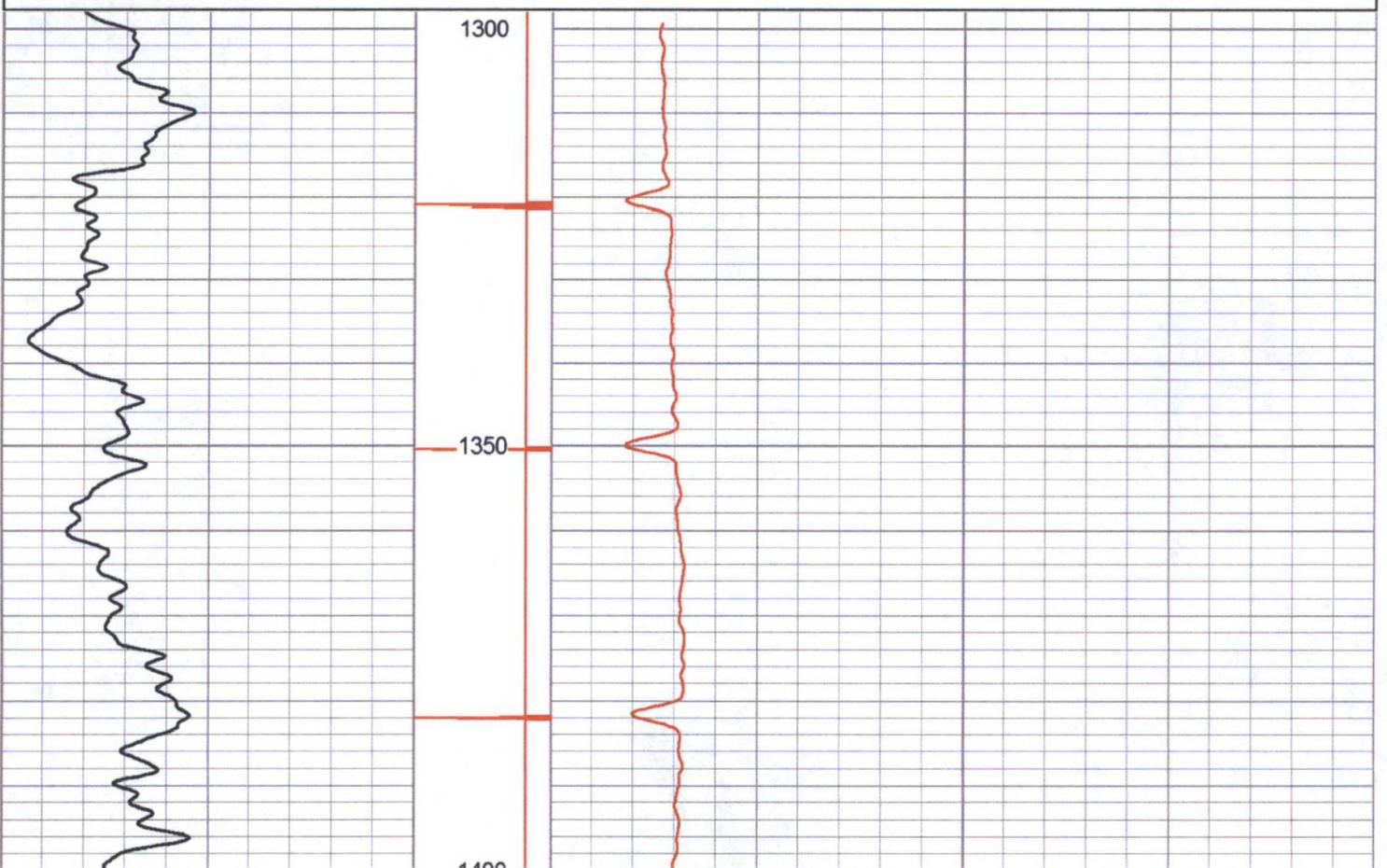


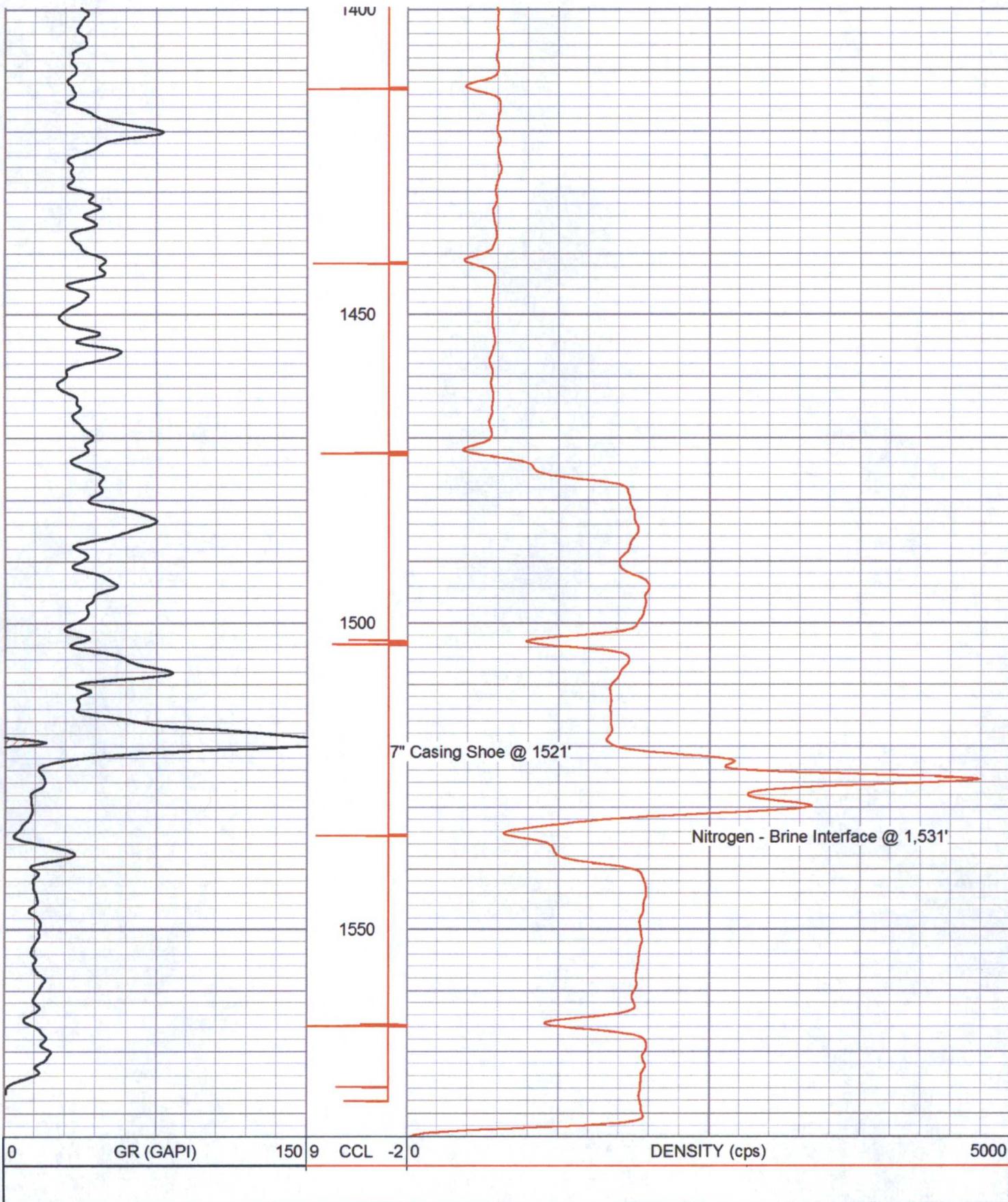
**Casedhole
Solutions**

POST INJECTION PASS

Database File: western refining #1.db
 Dataset Pathname: pass78
 Presentation Format: gr-n-ccl
 Dataset Creation: Tue Apr 26 19:24:19 2016 by Log Std Casedhole 09061
 Charted by: Depth in Feet scaled 1:240

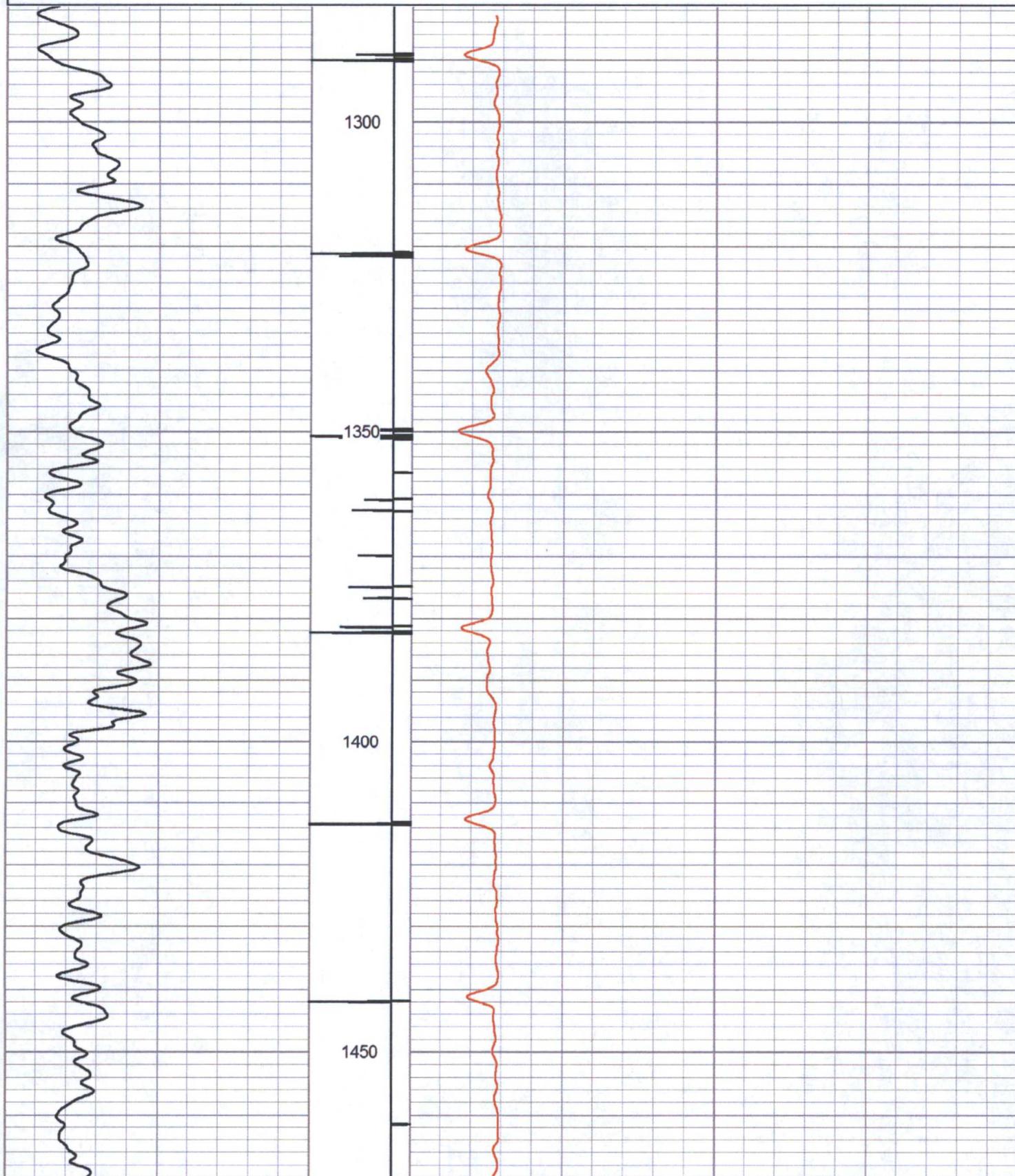
0	GR (GAPI)	150	9	CCL	-2	0	DENSITY (cps)	5000
---	-----------	-----	---	-----	----	---	---------------	------

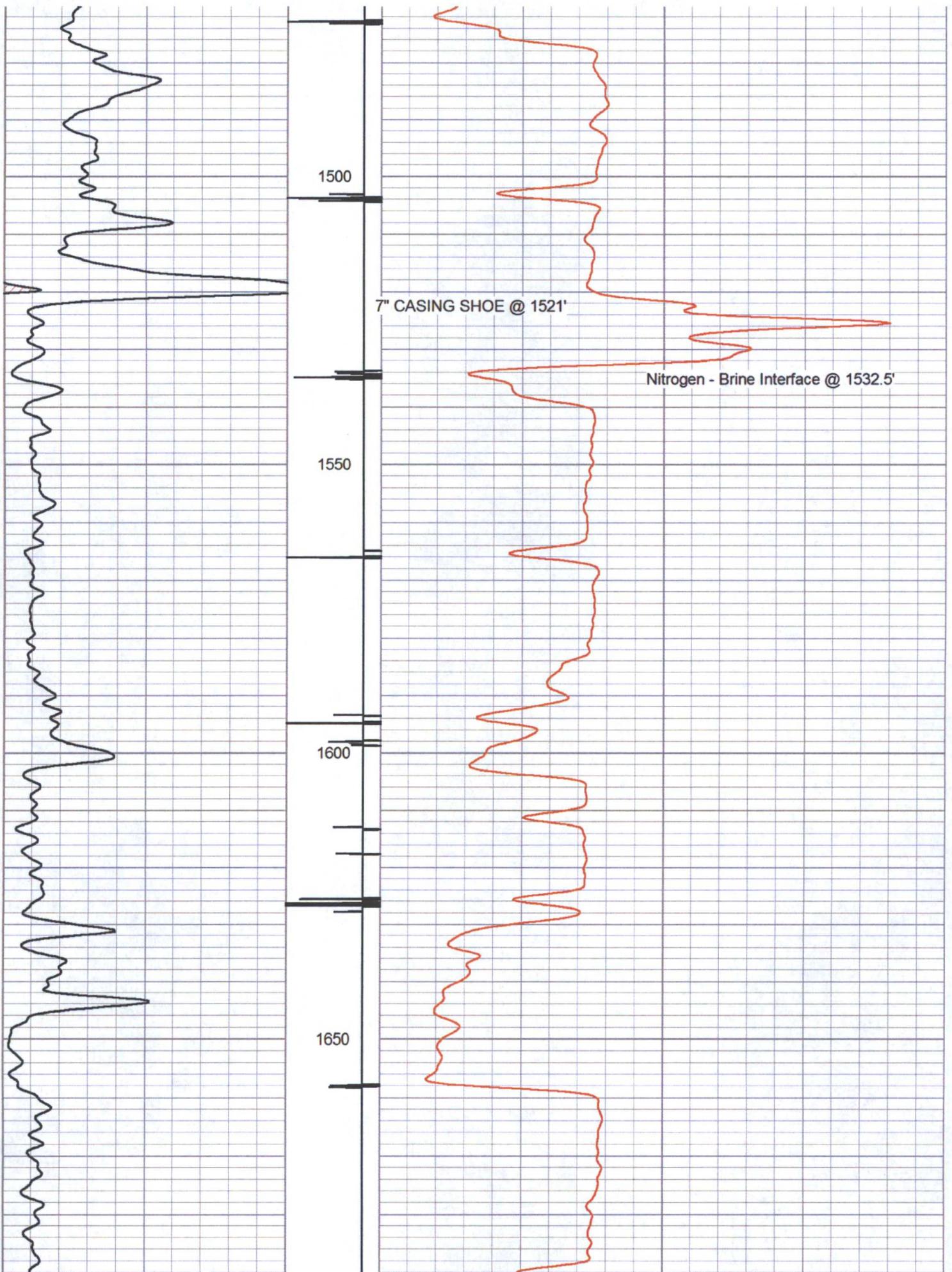


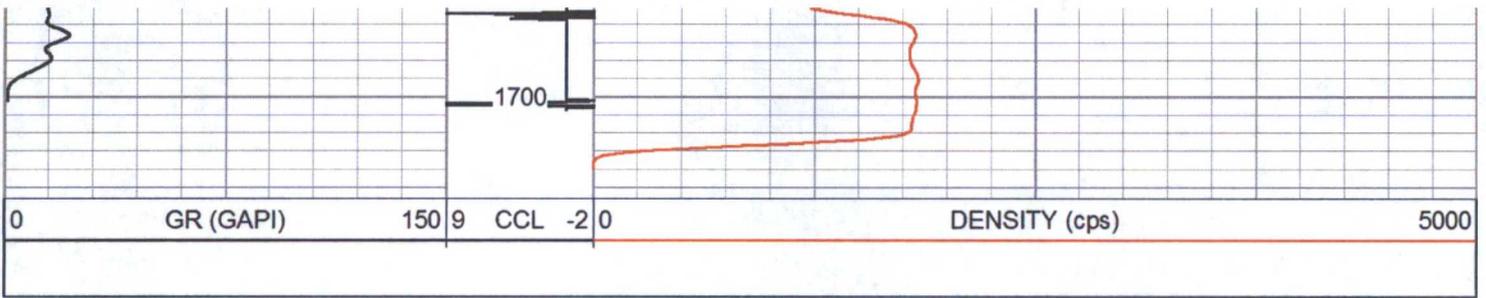


Database File: western refining #1.db
Dataset Pathname: pass80
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Dataset Creation: Wed Apr 27 08:12:17 2016 by Log Std Casedhole 09061
Charted by: Depth in Feet scaled 1:240

0 GR (GAPI) 150 9 CCL -2 0 DENSITY (cps) 5000

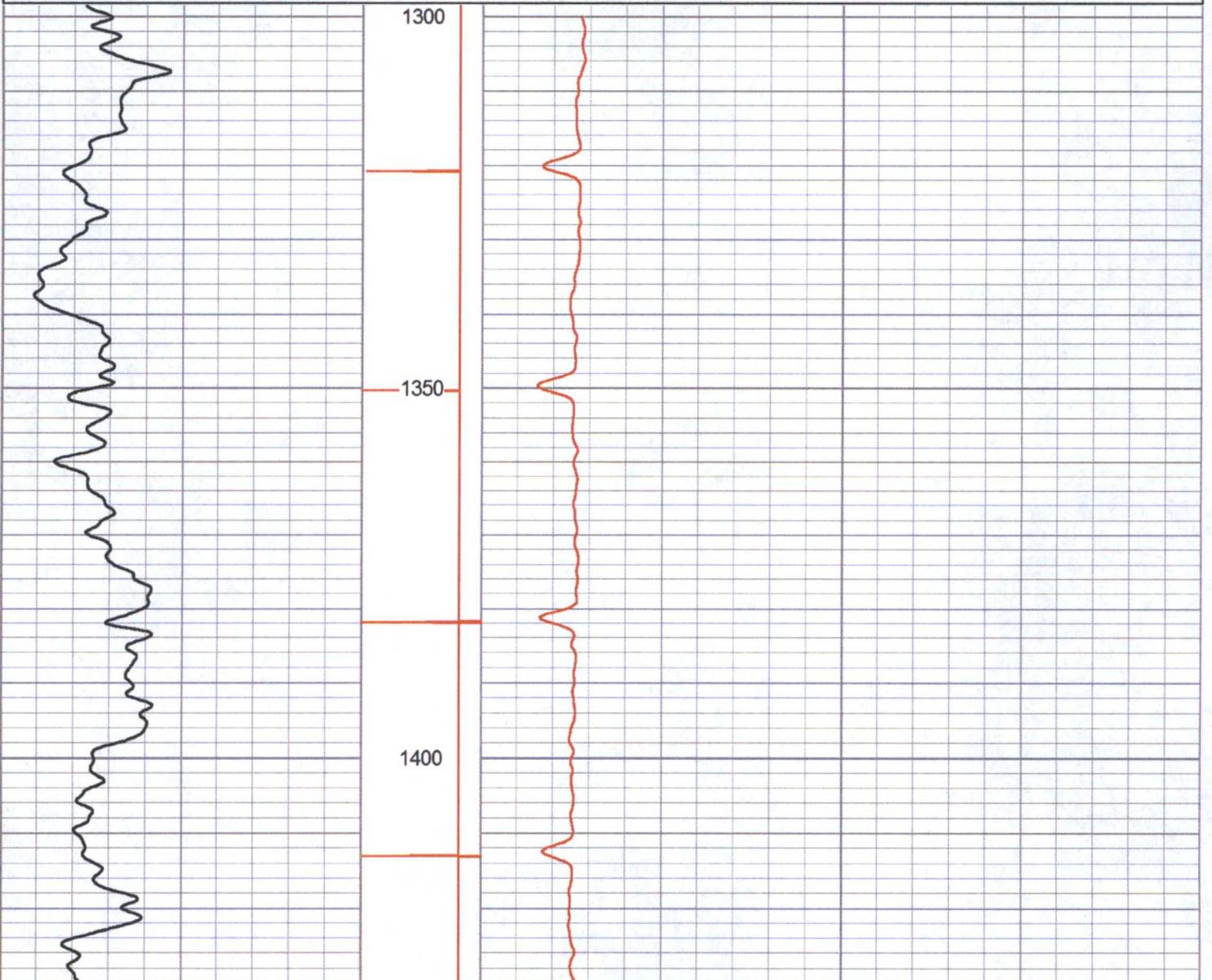
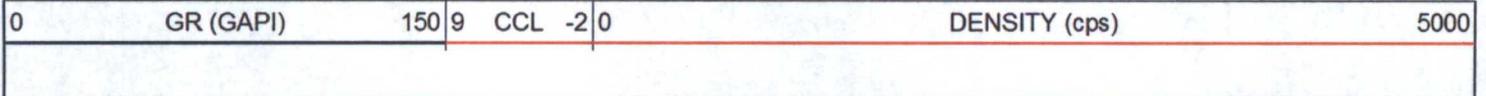


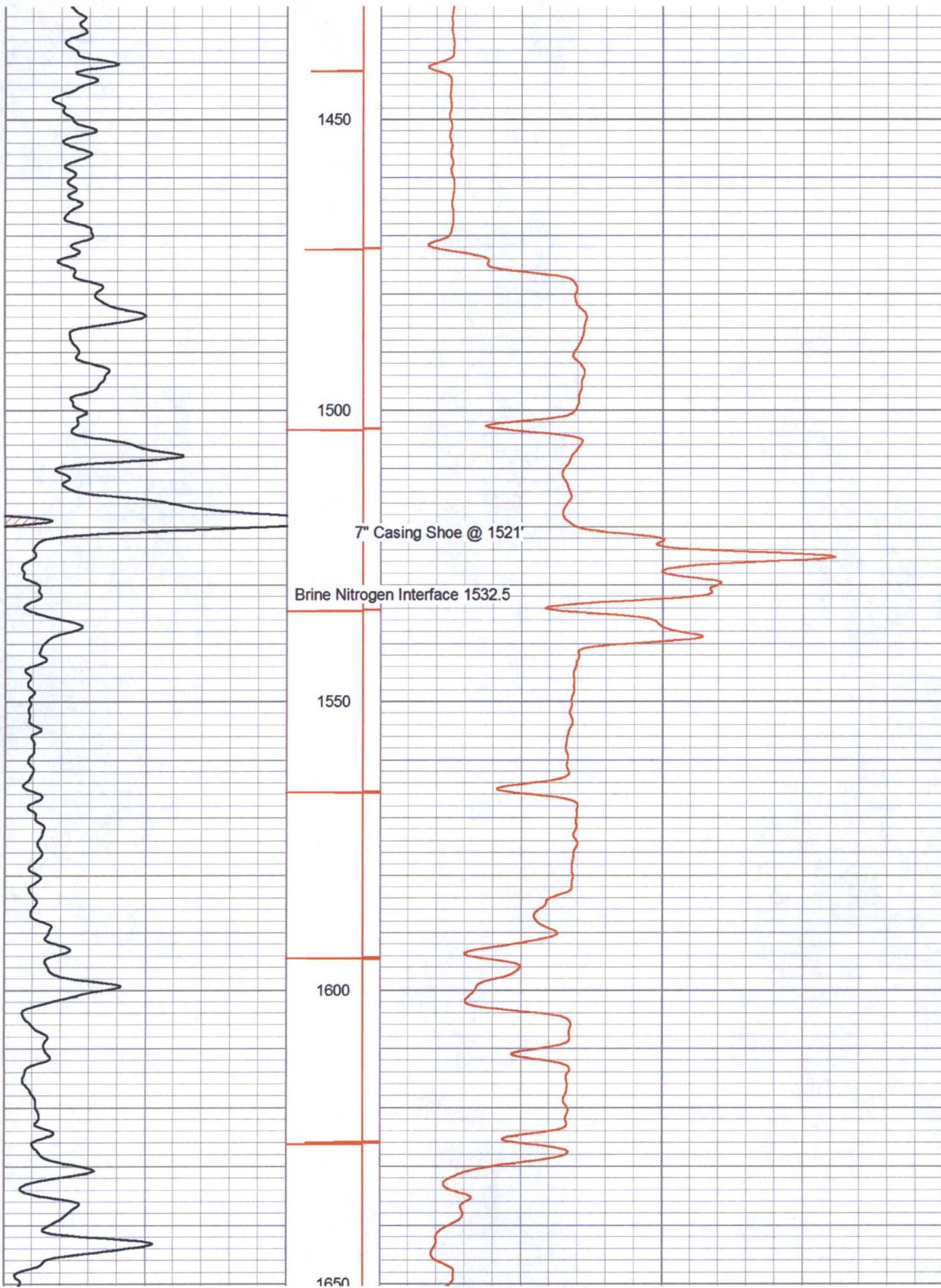


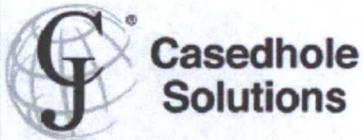
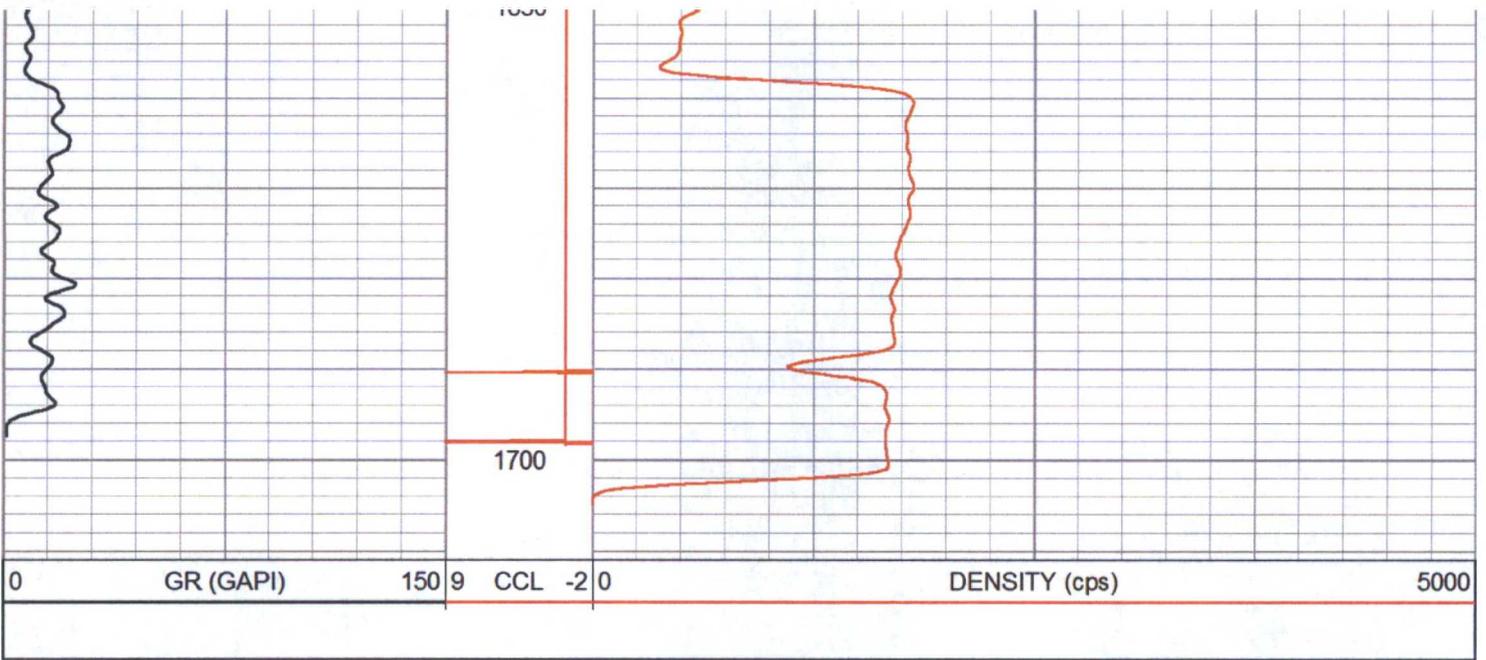



Finalization Log

Database File: western refining #1.db
 Dataset Pathname: pass83
 Presentation Format: gr-n-ccl
 Dataset Creation: Thu Apr 28 08:16:45 2016 by Log Std Casedhole 09061
 Charted by: Depth in Feet scaled 1:240



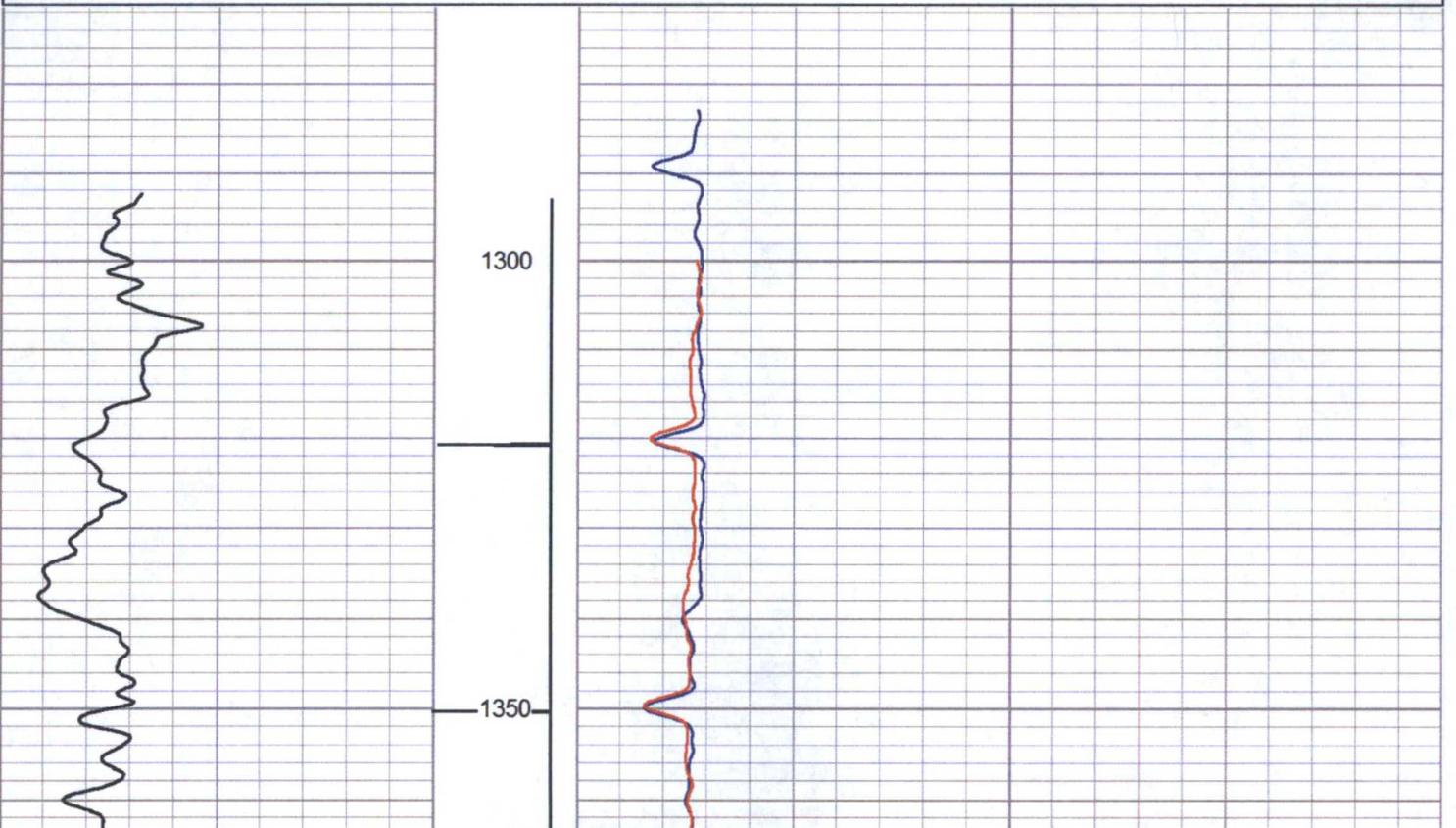


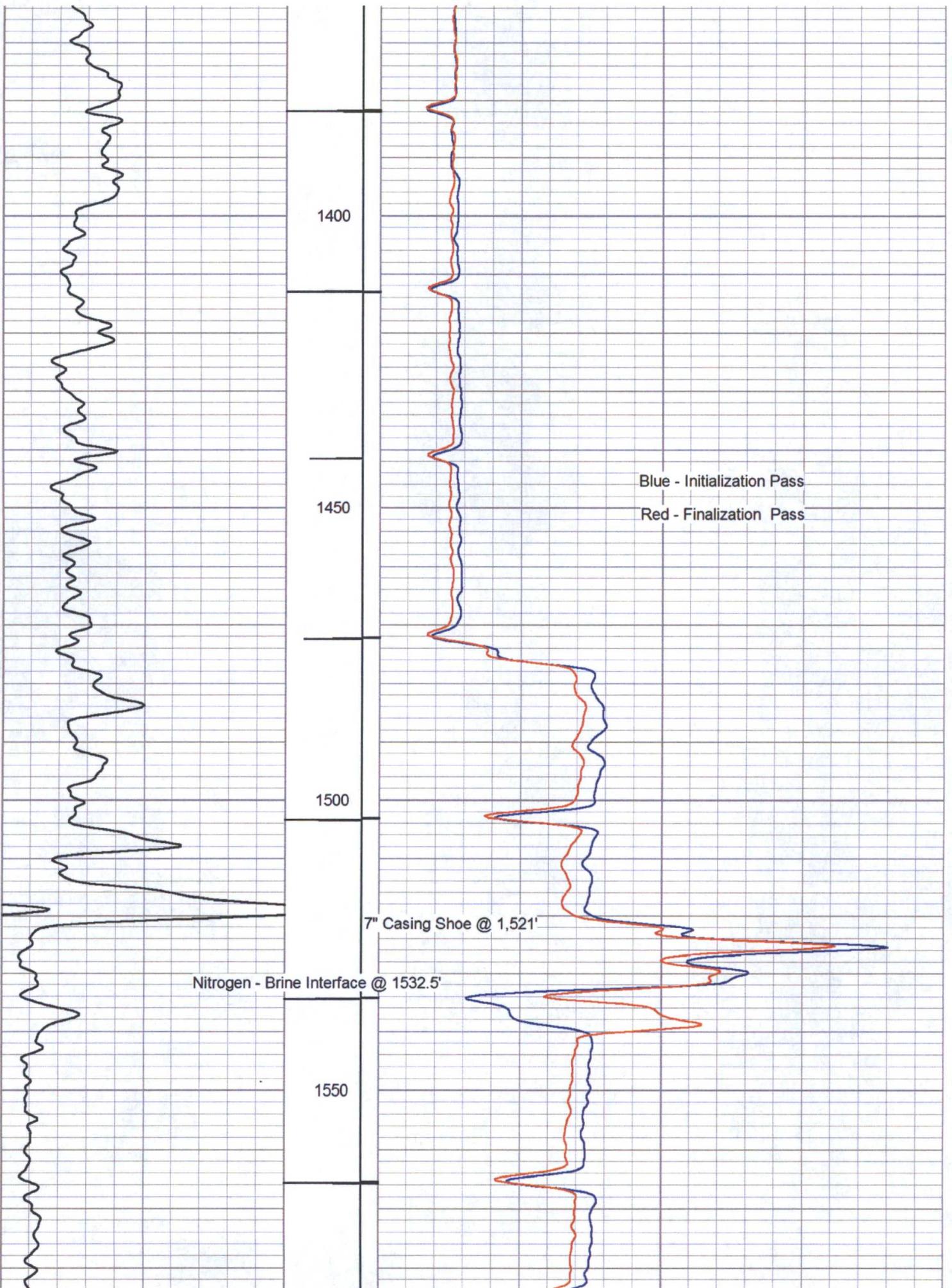


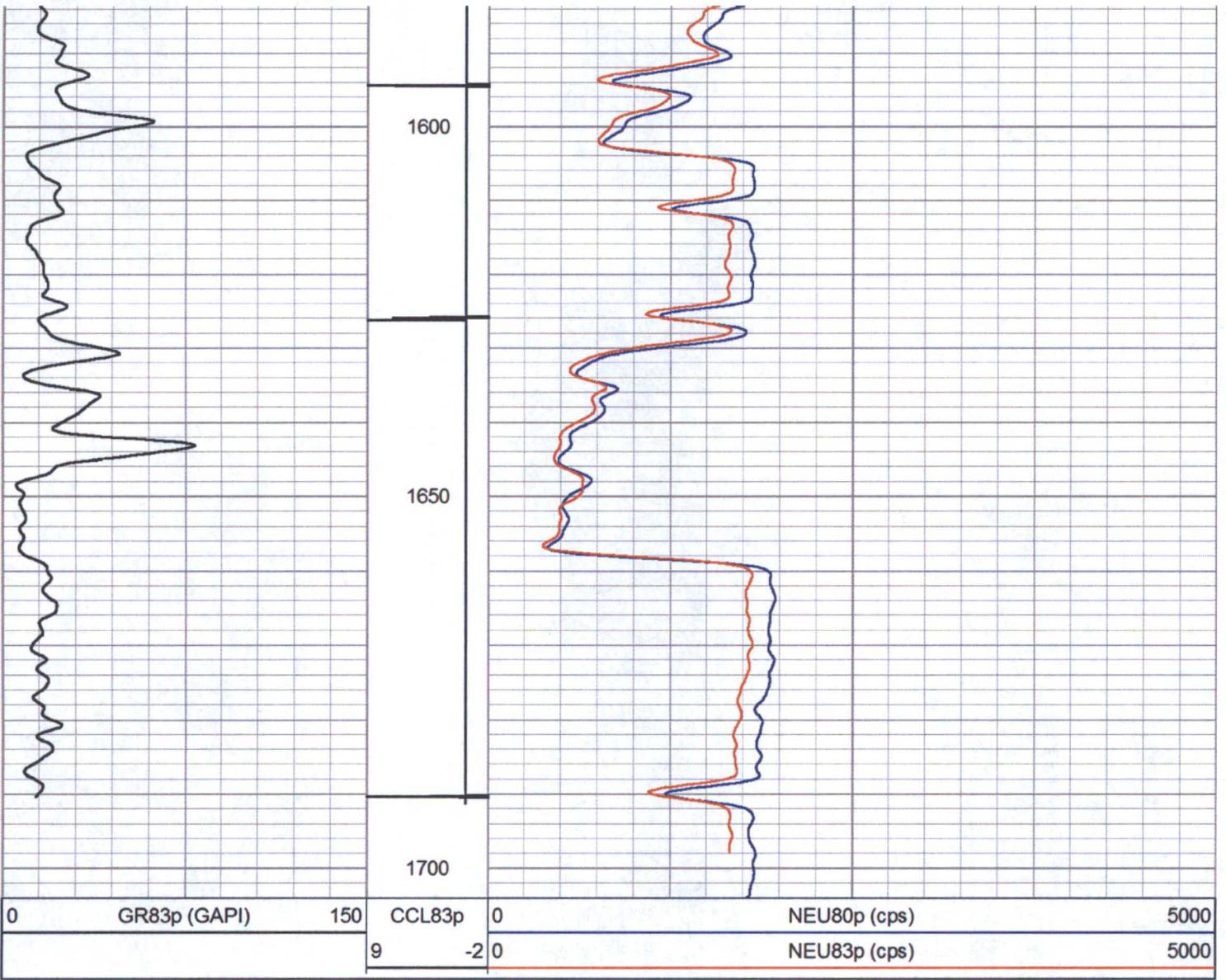
DENSITY MERGE

Database File: western refining #1.db
 Dataset Pathname: pass83m
 Presentation Format: gr-n-ccl
 Dataset Creation: Thu May 12 11:41:07 2016
 Charted by: Depth in Feet scaled 1:240

0	GR83p (GAPI)	150	CCL83p	0	NEU80p (cps)	5000
		9	-2	0	NEU83p (cps)	5000







45	TEMP3p (degF)	90
45	TEMP79p (degF)	90
45	TEMP81p (degF)	90

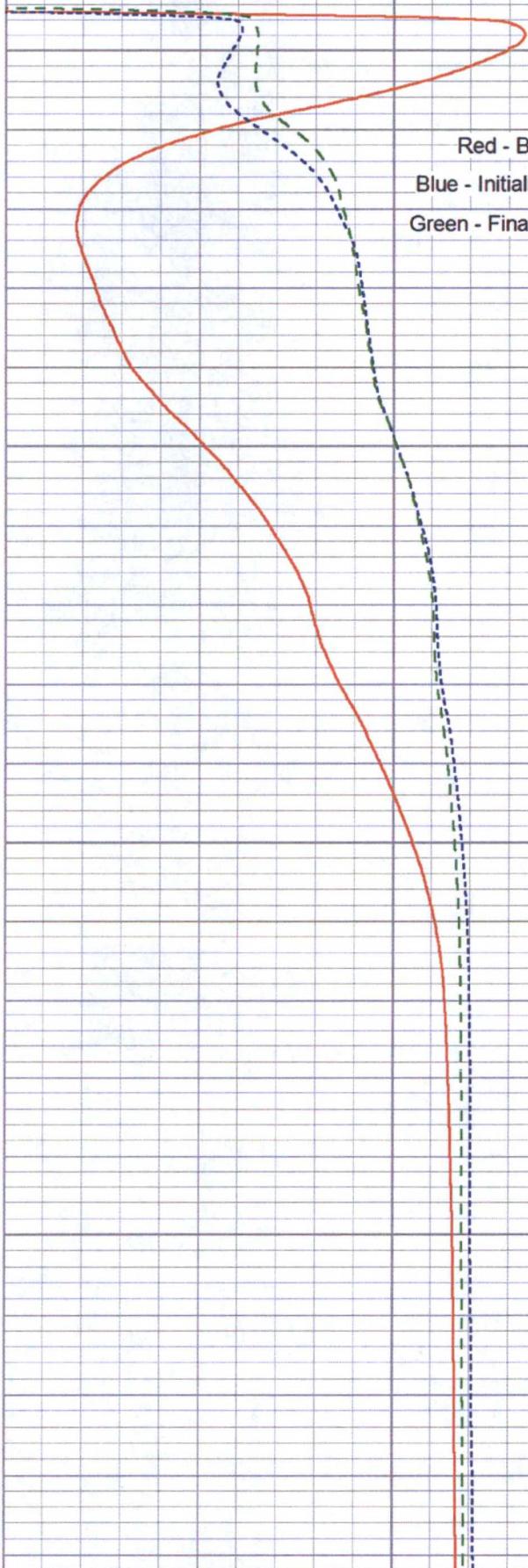
0

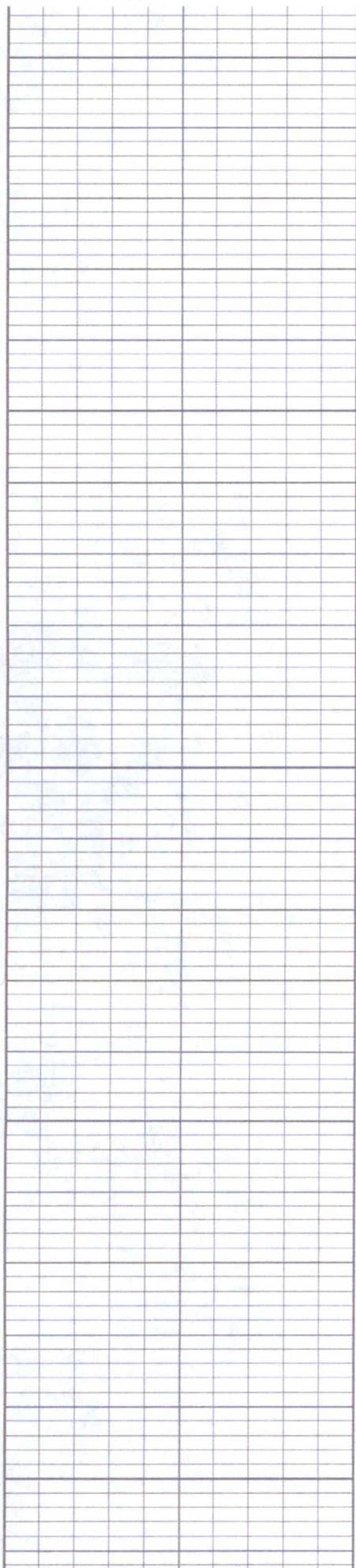
50

100

150

Red - Base Pass
Blue - Initialization Pass
Green - Finalization Pass





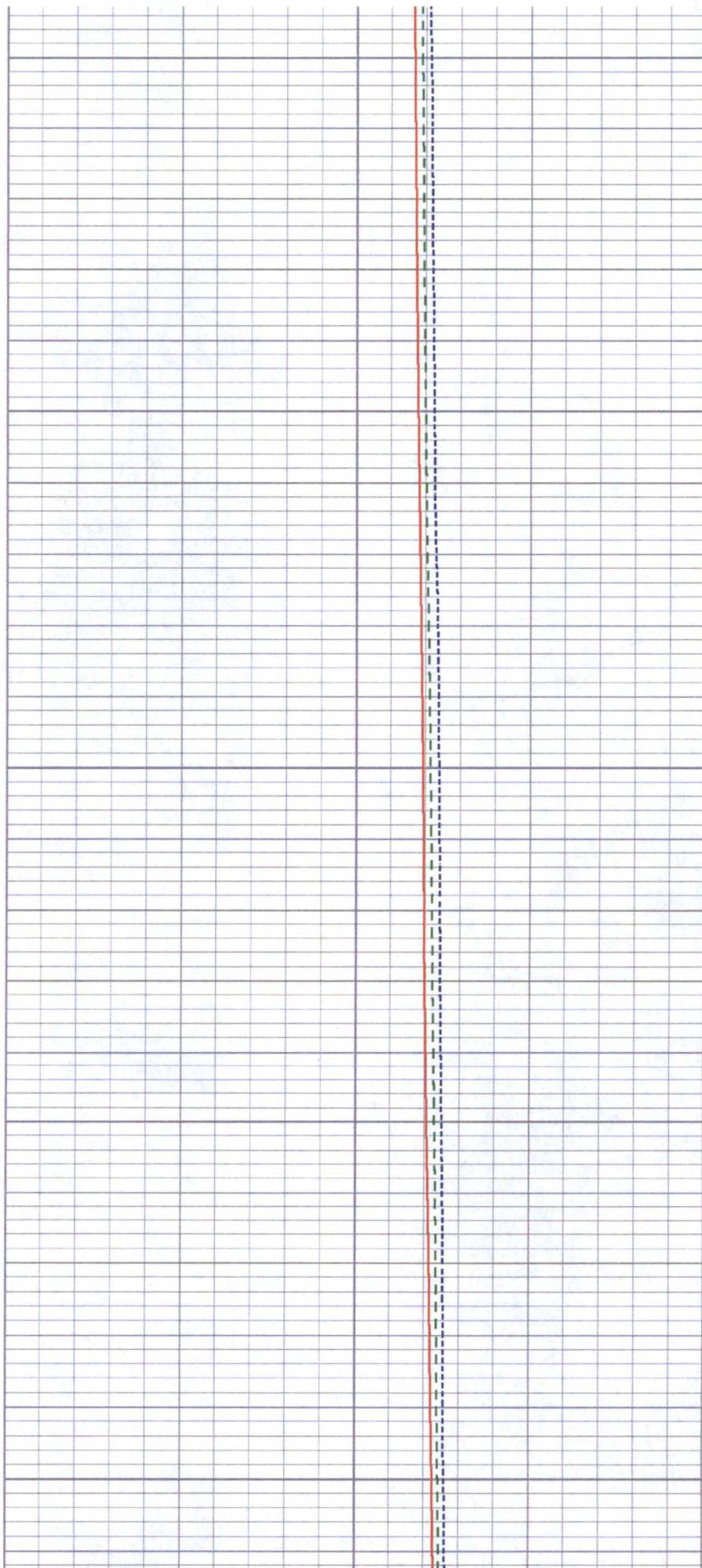
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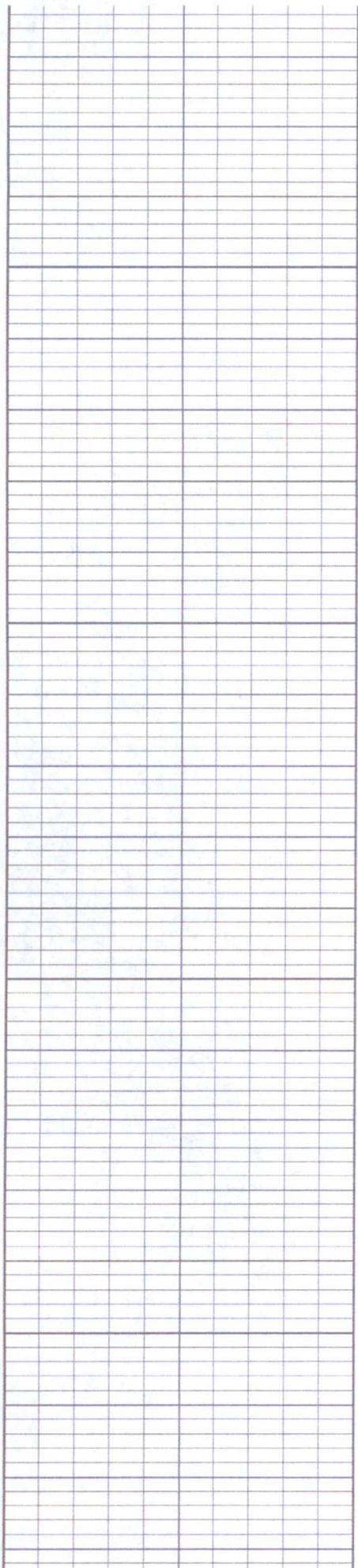
250

300

350

400



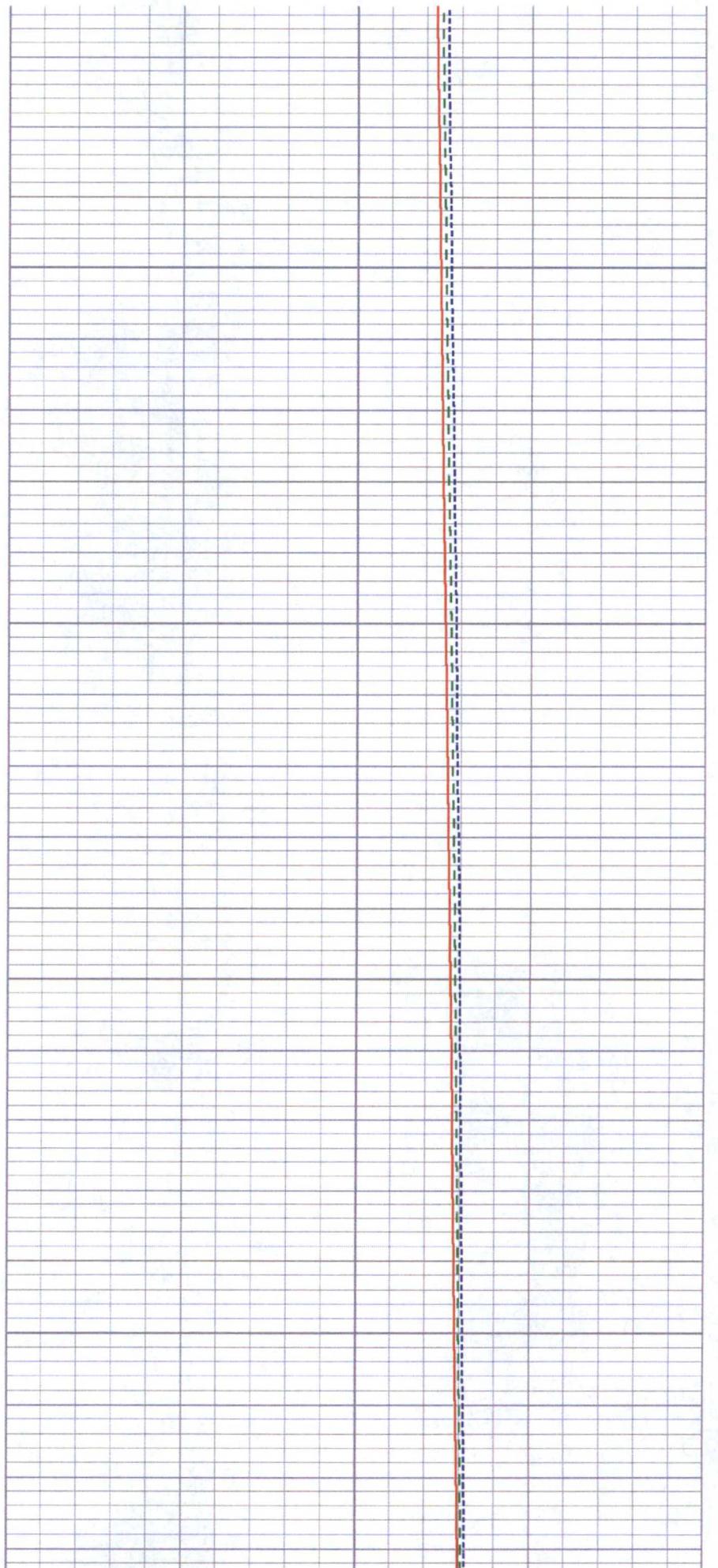


450

500

550

600

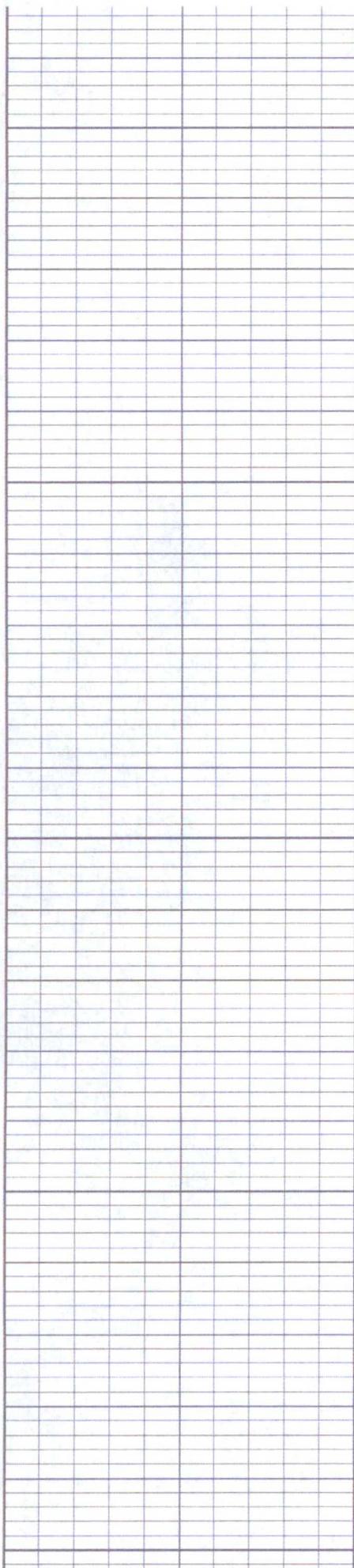


450

500

550

600



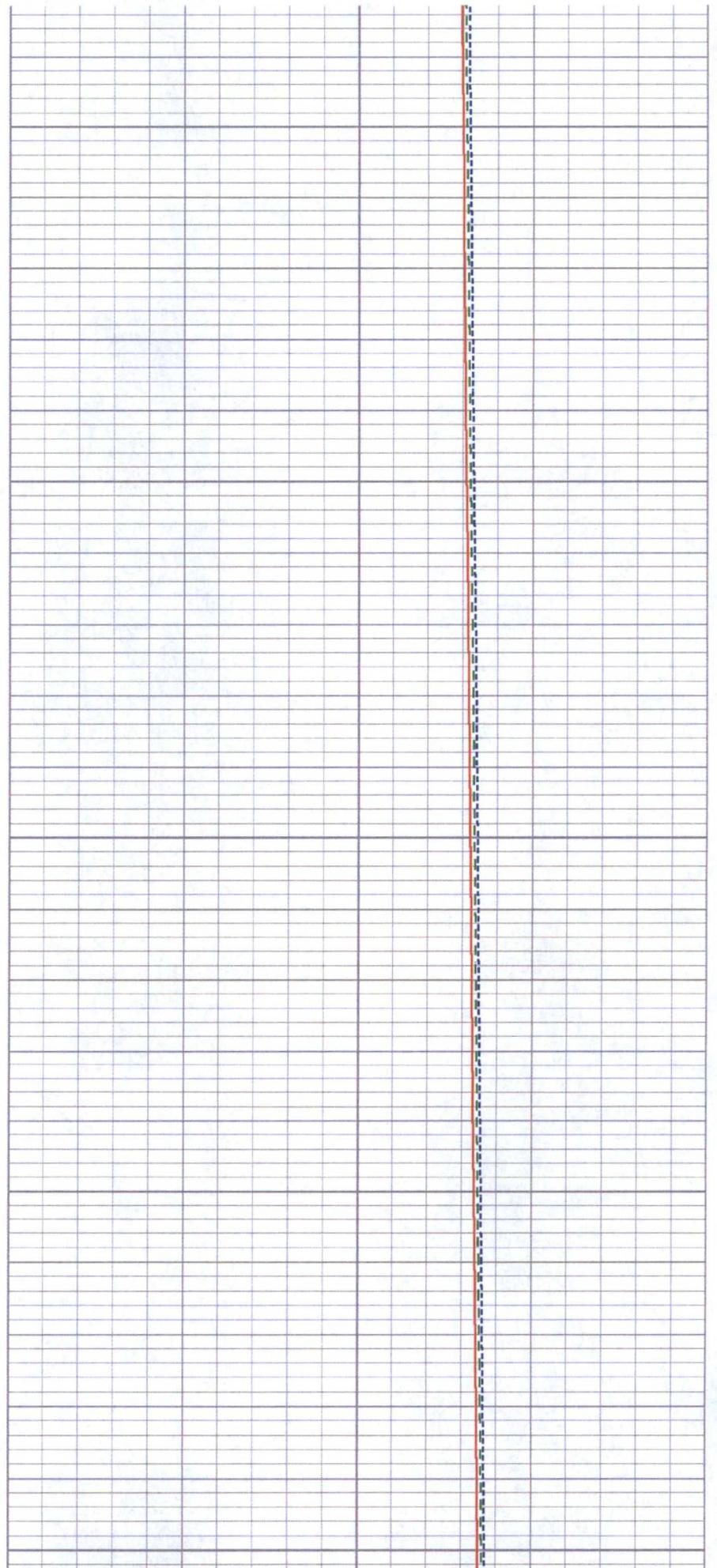
650

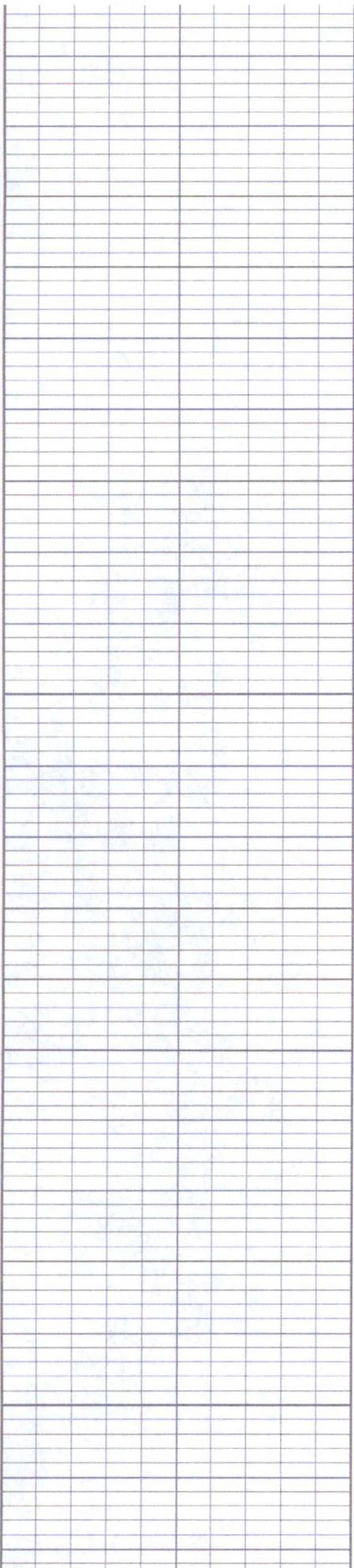
700

750

800

850



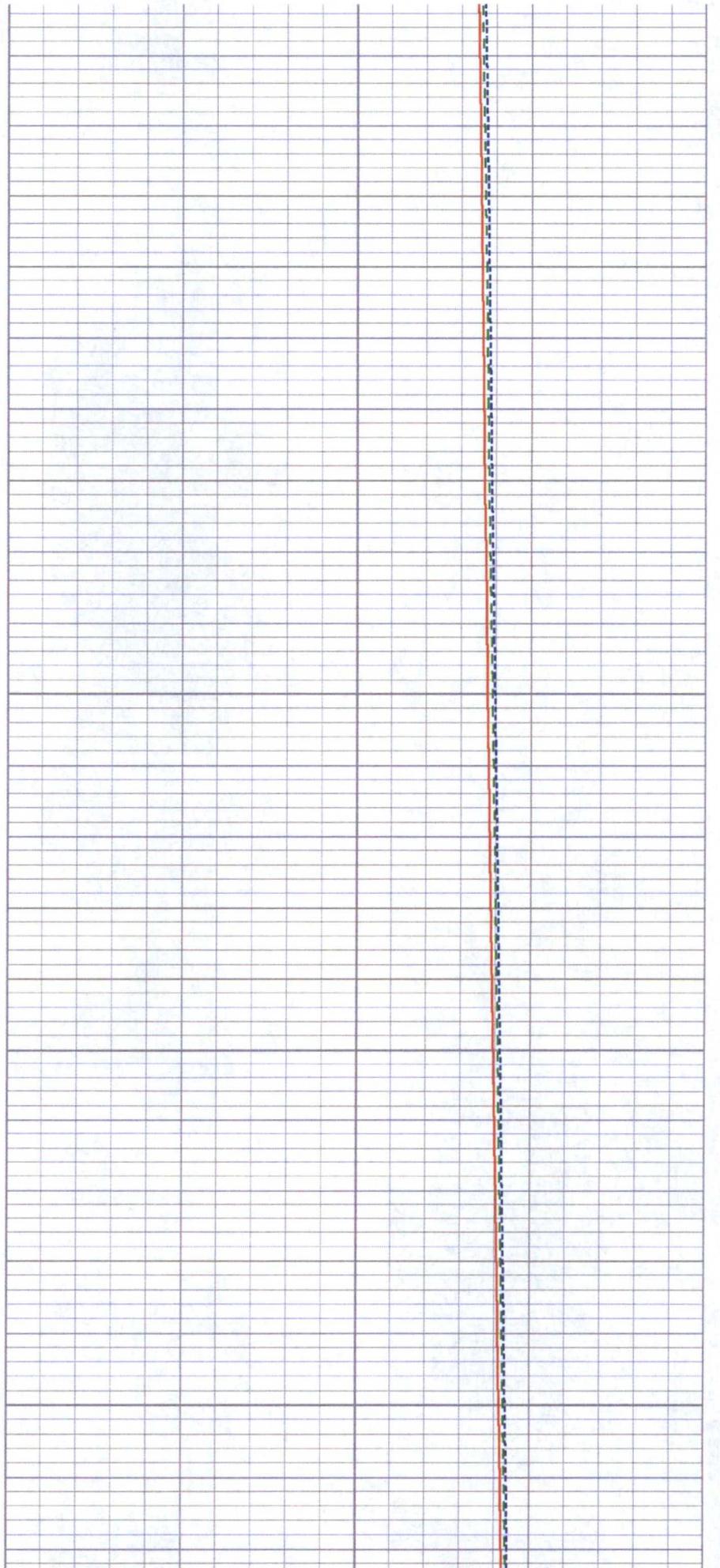


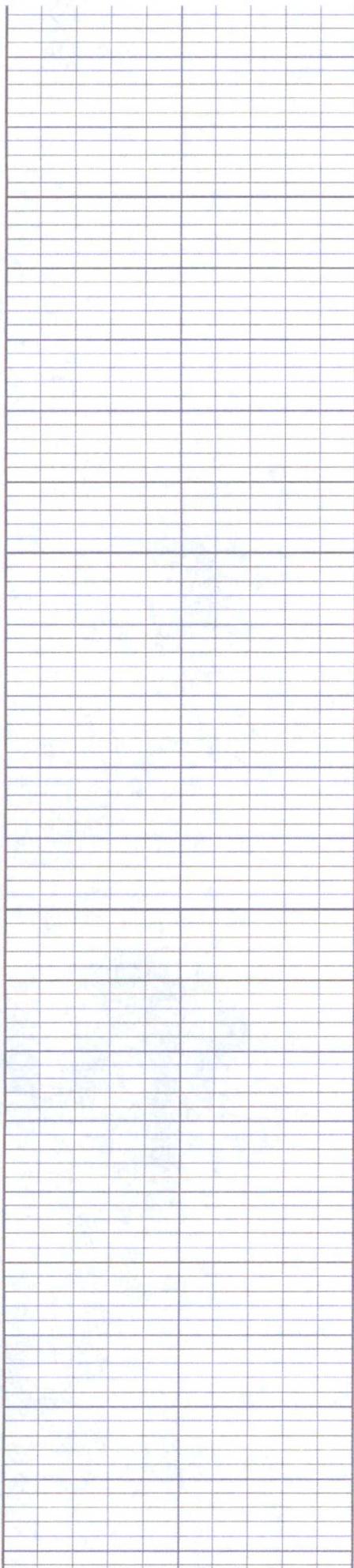
900

950

1000

1050



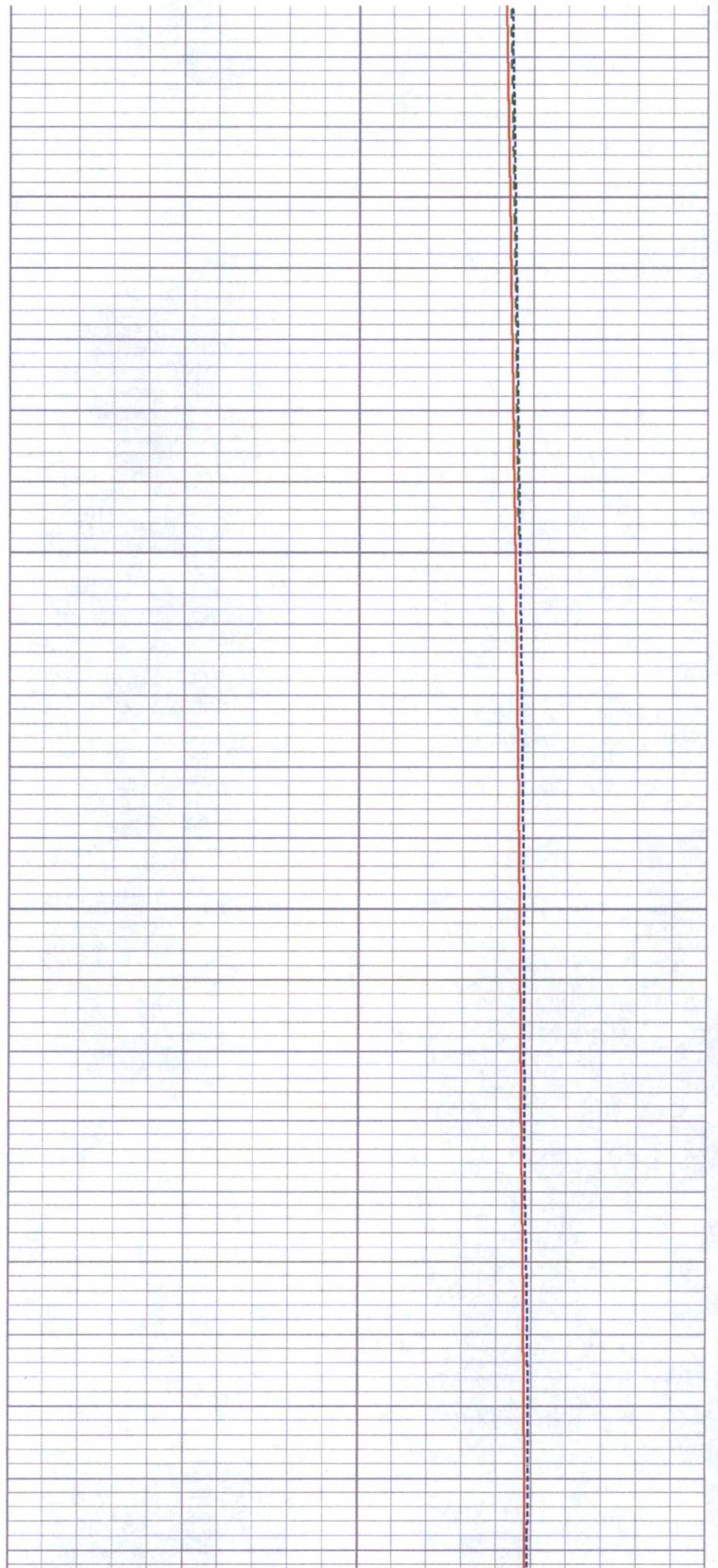


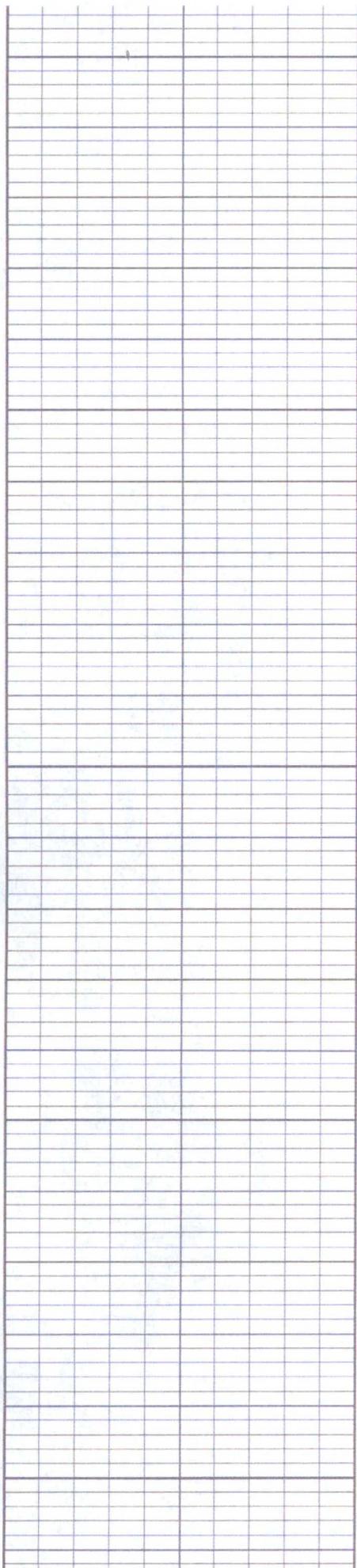
1100

1150

1200

1250





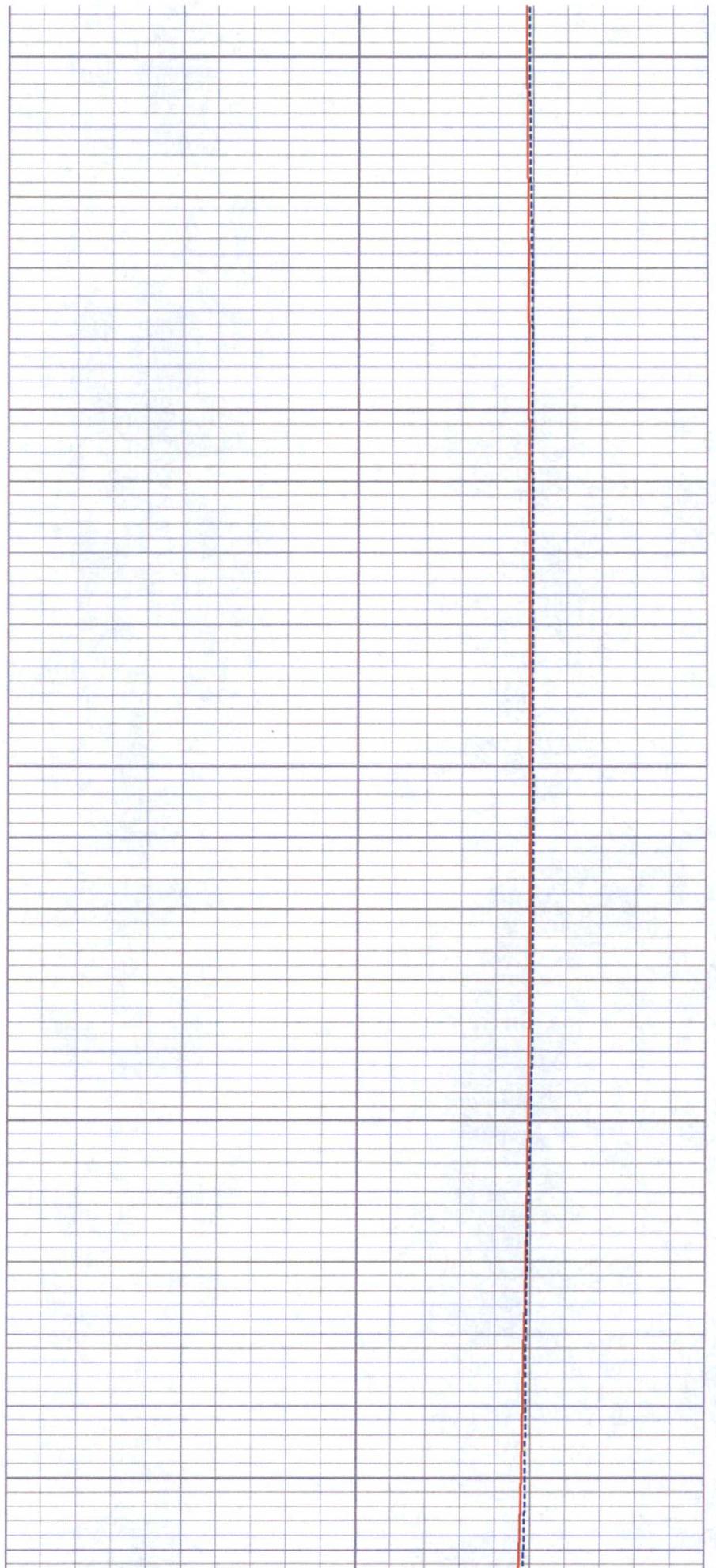
1300

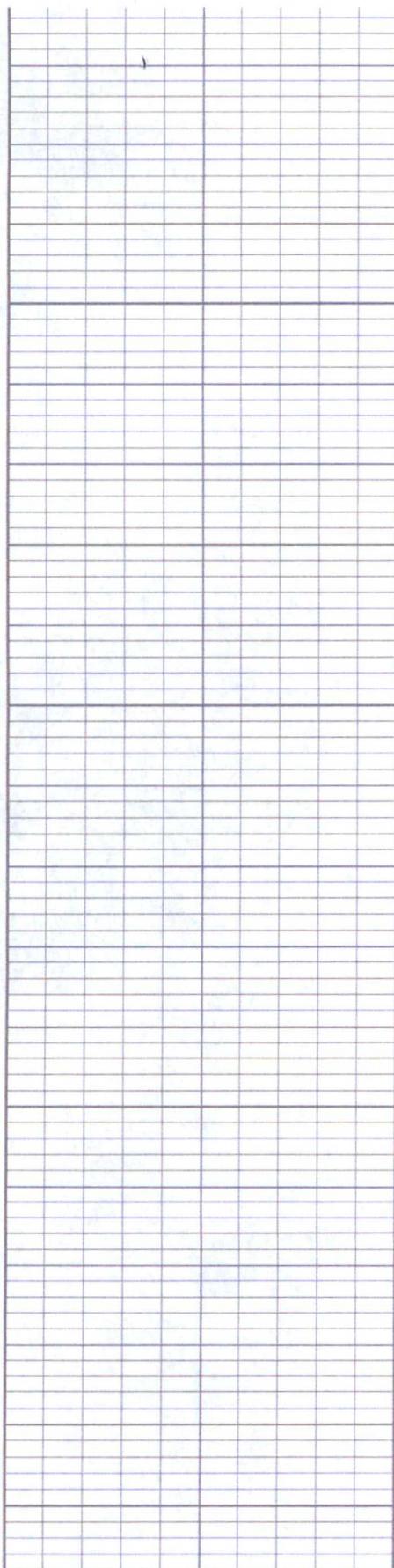
1350

1400

1450

1500



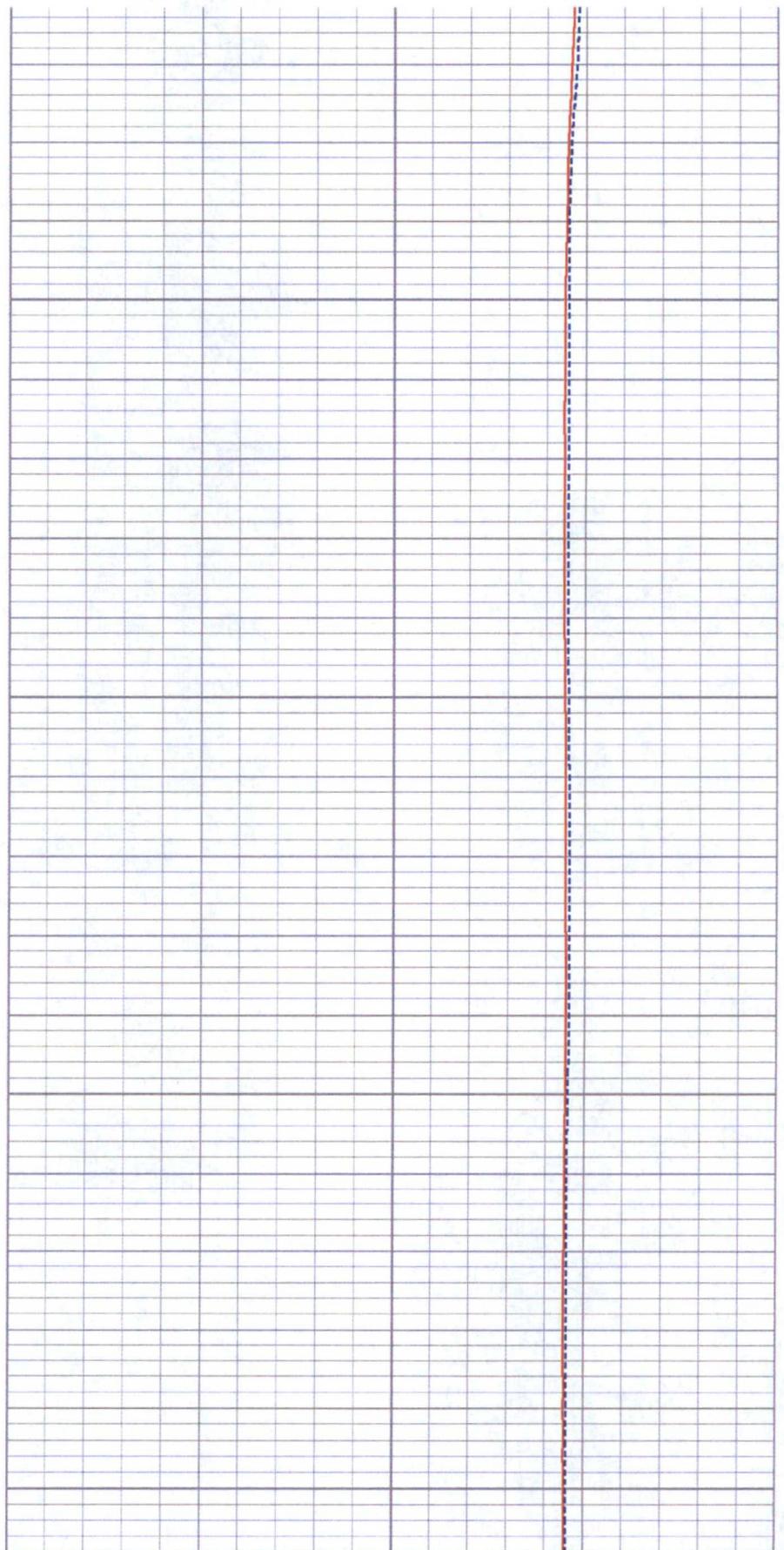


1550

1600

1650

1700



45	TEMP3p (degF)	90
45	TEMP79p (degF)	90
45	TEMP81p (degF)	90