

NEW MEXICO OIL CONSERVATION COMMISSION
MULTIPOINT ANI NE POINT BACK PRESSURE TEST GAS WELL

Form C-122
Revised 9-1-65

Type Test ☒ Initial ☐ Annual ☐ Special					Test Date 8-19-72			
Company Tom L. Ingram				Connection				
Pool Bluitt San Andres (Gas)				Formation San Andres				Unit C
Completion Date		Total Depth 4830		Plug Back TD 4714		Elevation 4003 KB		Form or Lease Name Federal "E"
Csq. Size 4.5"	Wt. 10.5	d 4.090"	Set At 4830	Perforations: From 4618 To 4691				Well No. 1
Tbg. Size 2.375	Wt. 4.7	d 1.995"	Set At	Perforations: From XXXX' To XXXX'				Unit Sec. Twp. Rge. 24 8 37E
Type Well - Single - Bradenhead - G.G. or G.O. Multiple Single					Packer Set At 4504		County Roosevelt	
Producing Thru TBG		Reservoir Temp. °F 107 @ 4691'		Mean Annual Temp. °F 60		Baro. Press. - P _a 13.2		State New Mexico
L.	H	Gg	% CO ₂	% N ₂	% H ₂ S	Prover	Meter Run 3.068"	Taps FLG

FLOW DATA							TUBING DATA		CASING DATA		Duration of Flow
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	
SI							970	70			72
1.	3.068	X	1.25	13	36	74	940	70	(Packer Set)		1
2.	3.068	X	1.25	14	66	74	900	71			1
3.	3.068	X	2.00	15	13	74	840	75			1
4.	3.068	X	2.00	15	18	74	765	76			1
5.											

RATE OF FLOW CALCULATIONS							
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	7.84977	30.7116	26.2	.986804	1.15087	1.0000	274
2	7.90078	42.3699	27.2	.986804	1.15087	1.0000	380
3	21.98439	19.1472	28.2	.986804	1.15087	1.0000	478
4	21.99295	22.5299	28.2	.986804	1.15087	1.0000	563
5.							

NO.	P _r	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.
1	1.555	534	1.342	.737	A.P.I. Gravity of Liquid Hydrocarbons _____ Deq.
2	1.488	534	1.343	.748	Specific Gravity Separator Gas 0.755 XXXXXXXXX
3	1.387	534	1.348	.768	Specific Gravity Flowing Fluid XXXXX
4	1.263	534	1.349	.789	Critical Pressure 667 P.S.I.A. _____ P.S.I.A.
5.					Critical Temperature 409° R _____ R

P _c 1148	P _e ² 1318		
NO.	P _i ²	P _w	P _e ² - P _w ²
1	908.6	1114	1241
2	833.9	1068	1141
3	728.0	998	996
4	605.6	913	834
5			

(1) $\frac{P_c^2}{P_e^2 - P_w^2} = 17.1169$

AOF = Q $\left[\frac{P_e^2}{P_e^2 - P_w^2} \right]^h = 1.13H$

(2) $\left[\frac{P_c^2}{P_e^2 - P_w^2} \right]^h = 4.1373$

Absolute Open Flow 1,130 Mcfd @ 15.025	Angle of Slope 63.5	Slope, n
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Remarks: _____

Approved By Commission:	Conducted By: M. E. Penniger	Calculated By: Cities Service Oil Co	Checked By:
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RECEIVED

U. S. DEPT.

OIL CONSERVATION COMM.
WASHINGTON, D. C.

GASC** 09:39CDT 08/30/72

NAME FED E
STA. NO. 0 F(PV) ASSUMED TO BE 1.000

PIPE= 3.068 ORIF= 1.25 DIFF= 36 PRESS= 26.2 PB= 14.65
TEMP= 74 SPGR= 0.755

F(B)= 322.032 (FLANGE TAP)
F(R)= 1.00126
Y(2)= 1.00887
F(PB)= 1.00546
F(TF)= 0.986804
F(G)= 1.15087
F(PV)= 1

ORIFICE METER COEFFICIENT = 371.455 CU.FT./HR.
ORIFICE METER COEFFICIENT = 8.91492 MSCFD

VOLUME = 273.791 MSCFD

NAME FED E
STA. NO. 0 F(PV) ASSUMED TO BE 1.000

PIPE= 3.068 ORIF= 1.25 DIFF= 66 PRESS= 27.2 PB= 14.65
TEMP= 74 SPGR= 0.755

F(B)= 322.032 (FLANGE TAP)
F(R)= 1.00092
Y(2)= 1.01577
F(PB)= 1.00546
F(TF)= 0.986804
F(G)= 1.15087
F(PV)= 1

ORIFICE METER COEFFICIENT = 373.863 CU.FT./HR.
ORIFICE METER COEFFICIENT = 8.97272 MSCFD

VOLUME = 380.172 MSCFD

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Oct 2 1972

OIL CONSERVATION COMM.
HOOVER, N. M.

GASC** 10:53CDT 08/30/72

NAME FED E
STA. NO. 0 F(PV) ASSUMED TO BE 1.000

PIPE= 3.068 ORIF= 2 DIFF= 13 PRESS= 28.2 PB= 14.65
TEMP= 74 SPGR= 0.755

F(B)= 906.016 (FLANGE TAP)
F(R)= 1.00326
Y(2)= 1.00228
F(PB)= 1.00546
F(TF)= 0.986804
F(G)= 1.15087
F(PV)= 1

ORIFICE METER COEFFICIENT = 1040.3 CU.FT./HR.
ORIFICE METER COEFFICIENT = 24.9673 MSCFD

VOLUME = 478.043 MSCFD

NAME FED E
STA. NO. 0 F(PV) ASSUMED TO BE 1.000

PIPE= 3.068 ORIF= 2 DIFF= 18 PRESS= 28.2 PB= 14.65
TEMP= 74 SPGR= 0.755

F(B)= 906.016 (FLANGE TAP)
F(R)= 1.00277
Y(2)= 1.00316
F(PB)= 1.00546
F(TF)= 0.986804
F(G)= 1.15087
F(PV)= 1

ORIFICE METER COEFFICIENT = 1040.71 CU.FT./HR.
ORIFICE METER COEFFICIENT = 24.9771 MSCFD

VOLUME = 562.734 MSCFD

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10/1/72

OIL CONSERVATION COMM.
HOOVER, N. M.