

NEW MEXICO OIL CONSERVATION COMMISSION
MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122
Revised 9-1-63

Type Test 4 POINT ☒ Initial ☐ Annual ☐ Special				Test Date 1-28-85							
Company DALPORT OIL COMPANY				Connection TO AIR							
Pool Chaves SE Green - Assoc				Formation Green							
Completion Date 1-27-85		Total Depth 2670.		Plug Back To 2658.							
				Elevation 4019							
Casing Size 4.500		Wt. 11.0		Perforations: From 2562. To 2571.							
Tub. Size 2.375		Wt. 4.7		Perforations: From 0. To 0.							
				Well No. #1							
Type Well - Single - Blindhead - G.G. or G.O. Multiple SINGLE				Packer Set At 0.							
Producing thru TUBING		Reservoir Temp. °F 95. # 2566.		Mean Annual Temp. °F 60.0							
				Baro. Press. - P _a 13.2							
L 2566.		H 2566.		C _g 0.945							
				% CO ₂ 0.							
				% N ₂ 63.11							
				% H ₂ S 0.							
				Prover 0.							
				Motor Run 2.1							
				Type FLANGE							
FLOW DATA											
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	TUBING DATA		B.H.P. DATA		Duration of Flow
							Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	CHOKE	
51							499.	48.			72.0
1.	2.07 X 1.000			75.	2.0	50.	400.	48.		4/64	1.0
2.	2.07 X 1.000			75.	4.0	50.	320.	48.		7/64	1.0
3.	2.07 X 1.000			75.	6.0	50.	195.	49.		11/64	1.0
4.	2.07 X 1.000			70.	7.0	50.	70.	49.		16/64	1.0
5.											
RATE OF FLOW CALCULATIONS											
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor F _g	Super. Compress. Factor, F _{sp}	Rate of Flow Q, Mcfd				
1	4.95	13.28	88.2	1.0098	1.0287	1.0047	69.				
2	4.95	18.78	88.2	1.0098	1.0287	1.0047	97.				
3	4.95	23.00	88.2	1.0098	1.0287	1.0047	119.				
4	4.95	24.13	83.2	1.0098	1.0287	1.0045	125.				
5											
NO.	P _t	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio _____ 0. _____ Mcf/bbl.						
					A.P.I. Gravity of Liquid Hydrocarbons _____ 0. _____ Deg.						
1	0.16	510.	1.73	0.991	Specific Gravity Separator Gas _____ 0.945 _____ XXXXXXXXX						
2	0.16	510.	1.73	0.991	Specific Gravity Flowing Fluid _____ XXXXX _____ 0.945						
3	0.16	510.	1.73	0.991	Critical Pressure _____ 546. _____ P.S.I.A. _____ 546. _____ P.S.I.A.						
4	0.15	510.	1.73	0.991	Critical Temperature _____ 295. _____ °F _____ 295. _____ °R						
5											
P _c 512.8 P _c ² 263.											
NO.	P _t ²	P _w	P _w ²	P _c ² - P _w ²	(1) $\frac{P_c^2}{P_t^2 - P_w^2} = 1.2009$ (2) $\left[\frac{P_c^2}{P_t^2 - P_w^2} \right]^n = 1.1224$						
1	171.	414.	171.	92.							
2	111.	334.	111.	152.							
3	43.	209.	44.	219.							
4	7.	85.	7.	256.	AOI = Q $\left[\frac{P_t^2}{P_t^2 - P_w^2} \right]^n = 133.6$						
5											
Absolute Open Flow _____ 133.6 _____ Mcfd @ 15.023					Angle of Slope @ _____ 57.75 _____ Slope, n _____ .631						
Remarks: _____											
Approved By Commission: _____ Conducted By: RICHARD TOWNLEY Calculated By: BENNETT AND CATHEY INC. Checked By: _____											

6-21-85

FEB 18 1985

RECEIVED
FEDERAL OFFICE