

NE MEXICO OIL CONSERVATION COMMISSION
MULTIPOINT / ONE POINT BACK PRESSURE TEST R GAS WELL

Form C-122
Revised 9-1-65

Type Test ☒ Initial ☐ Annual ☐ Special						Test Date 9-13/20-79	
Company Adobe Oil & Gas Corporation				Connection El Paso Natural Gas Company			
Pool Austin				Formation Mississippian		Unit F	
Completion Date 9/11/79		Total Depth 13,890		Plug Back TD 13,821		Elevation 3963 KB	
Csg. Size 5 1/2		Set At 13,821		Performances: From 13,288 To 13,373		Well No. 2	
Tub. Size 2 7/8		Set At 12,952		Performances: From open To ended		Unit Sec. Twp. Rge. F 16 14 36	
Type Well - Single - Prodenhead - G.G. or G.O. Multiple Single				Packer Set At 12,952		County Lea	
Producing Thru Tubing		Reservoir Temp. °F 225 @ 12,936		Mean Annual Temp. °F 13.2		State New Mexico	
L *12,936		H 12,936		Gg .643		% CO ₂ % N ₂ % H ₂ S Prover Meter Run Taps 4" Flange	

FLOW DATA						TUBING DATA		CASING DATA		Duration of Flow	
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	of Flow
5!							3800		Condensate	Ck. Size	72 hrs.
1.	4	x	1.500	651	7.84	110	1800		31.69 bbls.	8/64	24 hrs.
2.	4	x	1.500	672	7.84	89	1527		28.35 bbls.	10/64	24 hrs.
3.	4	x	1.500	692	7.84	106	1280		31.69 bbls.	12/64	24 hrs.
4.	4	x	1.500	643	9.00	88	1100		35.03 bbls.	14/64	24 hrs.
5.											

RATE OF FLOW CALCULATIONS							
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcd
1	7.469	72.17	664.2	.9551	1.247	1.049	673
2	7.469	73.29	685.2	.9732	1.247	1.057	702
3	7.469	74.36	705.2	.9585	1.247	1.053	699
4	7.469	76.85	656.2	.9741	1.247	1.056	736
5							

NO.	P _r	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio	22.168	Mcf/bbl.
1.	.99	570	1.53	.909	A.P.I. Gravity of Liquid Hydrocarbons	50.0 @ 60°	Deq.
2.	1.02	549	1.48	.895	Specific Gravity Separator Gas	.643	X X X X X X X X
3.	1.05	566	1.52	.902	Specific Gravity Flowing Fluid	X X X X X	
4.	.98	548	1.47	.896	Critical Pressure	670	P.S.I.A. P.S.I.A.
5.					Critical Temperature	372	R R

P _c 3813.2 P _c ² 14540.5			
NO.	P _r ²	P _w	P _w ² P _c ² - P _w ²
1		2351.3	5528.6 9011.9
2		2056.7	4230.0 10310.5
3		1502.0	2256.0 12284.5
4		1404.2	1971.8 12568.7
5			

$$(1) \frac{P_c^2}{P_c^2 - P_w^2} = 1.613$$

$$(2) \left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1.269$$

$$AOF = Q \left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = .854$$

Absolute Open Flow	854	Mcd @ 15.025	Angle of Slope @	63.5	Slope, n	.499
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Remarks: * Bottom hole instrument set at this point.
Made total 126.76 bbls. condensate during test.

Approved By Commission:	Conducted By:	Calculated By:	Checked By:
<i>John A. Murray</i>	Adobe Oil & Gas Corp.	Joe B. Murray	