

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Type Test ☒ Initial ☐ Annual ☐ Special						Test Date 4/27/82																																																																																				
Company Harvey E. Yates Co.				Connection El Paso Natural Gas																																																																																						
Pool Undesignated Austin-Miss				Formation Mississippian																																																																																						
Completion Date 2/20/82		Total Depth 13524'		Plug Back TD		Elevation 3968																																																																																				
Casing Size 5 1/2"		Wt. 17-20		Set At 4.778 13393'		Perforations: Open Hole From 13393' To 13524'																																																																																				
Tub. Size 2 3/8"		Wt. 4.7		Set At 1.995 13350'		Perforations: From - To -																																																																																				
Type Well - Single - Bradenhead - G.G. or G.O. Multiple Single						Packer Set At 13187'																																																																																				
Producing thru Tbp		Reservoir Temp. °F 193 @ 13524'		Mean Annual Temp. °F 60°		Baro. Press. - P _a 13.2" Hg																																																																																				
L 13524'		H 13524'		G _g 0.671		% CO ₂ 1.358																																																																																				
				% N ₂ 1.358		% H ₂ S Nil																																																																																				
				Prover -		Meter Run 4.026																																																																																				
				County Lea		State New Mexico																																																																																				
<table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th colspan="7">FLOW DATA</th> <th colspan="2">TUBING DATA</th> <th colspan="2">CASING DATA</th> <th rowspan="2">Duration of Flow</th> </tr> <tr> <th>NO</th> <th>Prover Line Size</th> <th>X</th> <th>Orifice Size</th> <th>Press. p.s.i.g.</th> <th>Diff. h_w</th> <th>Temp. °F</th> <th>Press. p.s.i.g. DWT</th> <th>Temp. °F</th> <th>Press. p.s.i.g.</th> <th>Temp. °F</th> </tr> <tr> <td>1</td> <td>4.026</td> <td>5/64</td> <td>1.750</td> <td>240</td> <td>2.0</td> <td>70</td> <td>3977</td> <td></td> <td>PACKER</td> <td></td> <td>72.0 hrs</td> </tr> <tr> <td>2</td> <td>4.026</td> <td>7/64</td> <td>1.750</td> <td>137</td> <td>7.0</td> <td>78</td> <td>2855</td> <td></td> <td></td> <td></td> <td>1.0 hr</td> </tr> <tr> <td>3</td> <td>4.026</td> <td>9/64</td> <td>1.750</td> <td>123</td> <td>11.0</td> <td>78</td> <td>2150</td> <td></td> <td></td> <td></td> <td>1.0 hr</td> </tr> <tr> <td>4</td> <td>4.026</td> <td>12/64</td> <td>1.750</td> <td>130</td> <td>12.0</td> <td>81</td> <td>1595</td> <td></td> <td></td> <td></td> <td>1.0 hr</td> </tr> <tr> <td>5</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td>925</td> <td></td> <td></td> <td></td> <td></td> </tr> </table>								FLOW DATA							TUBING DATA		CASING DATA		Duration of Flow	NO	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g. DWT	Temp. °F	Press. p.s.i.g.	Temp. °F	1	4.026	5/64	1.750	240	2.0	70	3977		PACKER		72.0 hrs	2	4.026	7/64	1.750	137	7.0	78	2855				1.0 hr	3	4.026	9/64	1.750	123	11.0	78	2150				1.0 hr	4	4.026	12/64	1.750	130	12.0	81	1595				1.0 hr	5							925				
FLOW DATA							TUBING DATA		CASING DATA		Duration of Flow																																																																															
NO	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g. DWT	Temp. °F	Press. p.s.i.g.	Temp. °F																																																																																
1	4.026	5/64	1.750	240	2.0	70	3977		PACKER		72.0 hrs																																																																															
2	4.026	7/64	1.750	137	7.0	78	2855				1.0 hr																																																																															
3	4.026	9/64	1.750	123	11.0	78	2150				1.0 hr																																																																															
4	4.026	12/64	1.750	130	12.0	81	1595				1.0 hr																																																																															
5							925																																																																																			
RATE OF FLOW CALCULATIONS																																																																																										
NO	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor F _L	Gravity Factor F _g	Super Compress. Factor, F _{sp}	Rate of Flow Q, Mscf/d																																																																																			
1	14.93	22.50	253.2	.9905	1.221	1.025	416																																																																																			
2	14.93	32.43	150.2	.9831	1.221	1.014	589																																																																																			
3	14.93	38.71	136.2	.9831	1.221	1.013	703																																																																																			
4	14.93	41.45	143.2	.9804	1.221	1.014	751																																																																																			
5																																																																																										
<table border="1" style="width:100%; border-collapse: collapse;"> <tr> <td>NO</td> <td>R₁</td> <td>Temp. °R</td> <td>T₁</td> <td>Z</td> <td>Gas Liquid Hydrocarbon Ratio</td> <td>Mcf/ubbl.</td> </tr> <tr> <td>1</td> <td>.38</td> <td>530</td> <td>1.39</td> <td>.951</td> <td>34.153</td> <td></td> </tr> <tr> <td>2</td> <td>.22</td> <td>538</td> <td>1.41</td> <td>.972</td> <td>A.P.I. Gravity of Liquid Hydrocarbons</td> <td>50.5 @ 60 Deg.</td> </tr> <tr> <td>3</td> <td>.20</td> <td>538</td> <td>1.41</td> <td>.974</td> <td>Specific Gravity Separator Gas</td> <td>0.671 XXXXX</td> </tr> <tr> <td>4</td> <td>.21</td> <td>541</td> <td>1.42</td> <td>.973</td> <td>Specific Gravity Flowing Fluid</td> <td>XXXXX .760</td> </tr> <tr> <td>5</td> <td></td> <td></td> <td></td> <td></td> <td>Critical Pressure</td> <td>669 P.S.I.A. 667 P.S.I.A.</td> </tr> <tr> <td></td> <td></td> <td></td> <td></td> <td></td> <td>Critical Temperature</td> <td>382 R 411 R</td> </tr> </table>								NO	R ₁	Temp. °R	T ₁	Z	Gas Liquid Hydrocarbon Ratio	Mcf/ubbl.	1	.38	530	1.39	.951	34.153		2	.22	538	1.41	.972	A.P.I. Gravity of Liquid Hydrocarbons	50.5 @ 60 Deg.	3	.20	538	1.41	.974	Specific Gravity Separator Gas	0.671 XXXXX	4	.21	541	1.42	.973	Specific Gravity Flowing Fluid	XXXXX .760	5					Critical Pressure	669 P.S.I.A. 667 P.S.I.A.						Critical Temperature	382 R 411 R																																		
NO	R ₁	Temp. °R	T ₁	Z	Gas Liquid Hydrocarbon Ratio	Mcf/ubbl.																																																																																				
1	.38	530	1.39	.951	34.153																																																																																					
2	.22	538	1.41	.972	A.P.I. Gravity of Liquid Hydrocarbons	50.5 @ 60 Deg.																																																																																				
3	.20	538	1.41	.974	Specific Gravity Separator Gas	0.671 XXXXX																																																																																				
4	.21	541	1.42	.973	Specific Gravity Flowing Fluid	XXXXX .760																																																																																				
5					Critical Pressure	669 P.S.I.A. 667 P.S.I.A.																																																																																				
					Critical Temperature	382 R 411 R																																																																																				
<table border="1" style="width:100%; border-collapse: collapse;"> <tr> <td>NO</td> <td>P_i</td> <td>P_w</td> <td>P_w²</td> <td>P_i² - P_w²</td> <td>(1) $\frac{P_i^2}{P_i^2 - P_w^2} = 1.060$</td> <td>(2) $\left[\frac{P_i^2}{P_i^2 - P_w^2} \right]^n = 1.054$</td> </tr> <tr> <td>1</td> <td></td> <td>2869.4</td> <td>8233.6</td> <td>7688.1</td> <td rowspan="5">AOI = Q $\left[\frac{P_i^2}{P_i^2 - P_w^2} \right]^n = .791$</td> <td rowspan="5"></td> </tr> <tr> <td>2</td> <td></td> <td>2166.0</td> <td>4691.4</td> <td>11230.3</td> </tr> <tr> <td>3</td> <td></td> <td>1613.2</td> <td>2602.4</td> <td>13319.3</td> </tr> <tr> <td>4</td> <td></td> <td>949.8</td> <td>902.1</td> <td>15019.6</td> </tr> <tr> <td>5</td> <td></td> <td></td> <td></td> <td></td> </tr> </table>								NO	P _i	P _w	P _w ²	P _i ² - P _w ²	(1) $\frac{P_i^2}{P_i^2 - P_w^2} = 1.060$	(2) $\left[\frac{P_i^2}{P_i^2 - P_w^2} \right]^n = 1.054$	1		2869.4	8233.6	7688.1	AOI = Q $\left[\frac{P_i^2}{P_i^2 - P_w^2} \right]^n = .791$		2		2166.0	4691.4	11230.3	3		1613.2	2602.4	13319.3	4		949.8	902.1	15019.6	5																																																					
NO	P _i	P _w	P _w ²	P _i ² - P _w ²	(1) $\frac{P_i^2}{P_i^2 - P_w^2} = 1.060$	(2) $\left[\frac{P_i^2}{P_i^2 - P_w^2} \right]^n = 1.054$																																																																																				
1		2869.4	8233.6	7688.1	AOI = Q $\left[\frac{P_i^2}{P_i^2 - P_w^2} \right]^n = .791$																																																																																					
2		2166.0	4691.4	11230.3																																																																																						
3		1613.2	2602.4	13319.3																																																																																						
4		949.8	902.1	15019.6																																																																																						
5																																																																																										
Absolute Open Flow 791				Mcf/d @ 15.025		Angle of Slope 48	Slope, n .900																																																																																			
Remarks: MADE 3 BBL OIL IN 4.0 HOURS = 18.0 B O/D																																																																																										
Approved By Division		Conducted By:		Calculated By:		Checked By:																																																																																				
		JARREL WELL TESTING, INC.		R. Reston		Joe A. Coleman PE #2208																																																																																				

RECEIVED

MAY 7 1982

O.C.D.
HOBBS OFFICE