

NEW MEXICO OIL CONSERVATION COMMISSION
MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122
Revised 9-1-65

Type Test ☒ Initial ☐ Annual ☐ Special				Test Date 3-20-80	
Company TENNECO OIL COMPANY				Connection TO AIR	
Pool ATOKA				Unit	
Completion Date 3-16-80		Total Depth 13,190		Plug Back TD 13,070	
				Elevation 4128 GL	
Farm or Lease Name KEMNITZ DEEP UNIT LF 29				Well No. 2	
Csg. Size 5 1/2	Wt. 17.00	d 4.892	Set At 13,188	Perforations: From 12,641 To 12,661	
Tbg. Size 2 7/8	Wt. 6.40	d 2.875	Set At 12,568	Perforations: From OPEN To END	
Type Well - Single - Bradenhead - G.G. or G.O. Multiple					
Packer Set At 12,563				County LEA	
Producing Thru TUBING		Reservoir Temp. °F 200° 12,630		Mean Annual Temp. °F 60°	
				Baro. Press. - P _a 13.2	
L 12,630		H 12,630	G _g .637	% CO ₂ .221	% N ₂ 1.737
				% H ₂ S	Prover
					Meter Run 4"
					Taps FLANGE

FLOW DATA						TUBING DATA		CASING DATA		Duration of Flow
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	
SI							4781			
1.	4 X 2.250			935	3.5	118	4112	65		
2.	4 X 2.250			740	6	103	3645	68		1 HR.
3.	4 X 2.250			740	9	95	3360	72		1 HR.
4.	4 X 2.250			740	11	92	3090	72		1 HR.
5.										

RATE OF FLOW CALCULATIONS							
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor F _g	Super Compress. Factor, F _{pv}	Rate of Flow Q, Mcfd
1.	25.64	51.17	748.2	.9485	1.253	1.047	1633
2.	25.64	67.22	753.2	.9610	1.253	1.054	2187
3.	25.64	82.33	753.2	.9680	1.253	1.056	2704
4.	25.64	91.02	753.2	.9706	1.253	1.058	3003
5.							

NO.	P _t	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio
1.	1.12	578	1.58	.913	72.174 Mcf/bbl.
2.	1.13	563	1.54	.901	A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.
3.	1.13	555	1.52	.896	Specific Gravity Separator Gas .637 XXXXXXXXXX
4.	1.13	552	1.51	.893	Specific Gravity Flowing Fluid XXXXX
5.					Critical Pressure 669 P.S.I.A.
					Critical Temperature 365 R

* P_c 4871.8 P_c² 23,734.4

NO.	P _t ²	P _w	P _w ²	P _c ² - P _w ²
1	* 4231.6	17906.4	5828.0	
2	* 3827.5	14649.8	9084.6	
3	* 3514.6	12352.4	11382.0	
4	* 3263.1	10647.8	13086.6	
5				

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.814$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1.5787$

AGF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 4.741$

Absolute Open Flow	4.741 Mcfd @ 15.025	Angle of Slope θ	52.5	Slope, n	.767
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Remarks: BOTTOM HOLE PRESSURES MEASURES WITH KUSTER GAUGE. MADE 5.5 BBLS. CONDENSATE.
*CALCULATED FROM KNOWN BOTTOM HOLE PRESSURE.

Approved By Commission:	Conducted By:	Calculated By:	Checked By:
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OIL CONSERVATION DIV.

APR 3 '80

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