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appropriate district office.
See Rule 401 & Rule 1122

State of New Mexico
Energy Minerals and Natural Resources
Oil Conservation Division
2040 South Pacheco
Santa Fe, NM 87505

Form C-122
Revised October, 1999

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Operator <u>LYNX PETROLEUM</u>				Lease or Unit Name <u>LUSK 3rd FED. Com</u>			
Type Test ☒ Initial ☐ Annual ☐ Special				Test Date <u>10-17-00</u>		Well No. <u>1</u>	
Completion Date <u>10/16/00</u>		Total Depth <u>12620'</u>		Plug Back TD <u>12575'</u>		Elevation <u>3674(6R)</u>	
Csg. Size <u>5 1/2</u>		Wt. <u>17#</u>		Set At <u>12612</u>		Perforations: From: <u>12495</u> To: <u>12518</u>	
Tbg. Size <u>2 3/8</u>		Wt. <u>4.7</u>		Set At <u>12495</u>		Perforations: From: <u>12496</u> To: <u>12519</u>	
Type Well-Single-Bradenhead-G.G. or G.O. Multiple <u>SINGLE</u>				Packer Set At <u>12451</u>		Unit Ltr - Sec - TWP - Rge <u>0-31-18S-32E</u>	
Producing Thru <u>7B6</u>		Reservoir Temp. °F <u>176°</u>		Mean Annual Temp. °F <u>60</u>		Baro. Press. -P _a <u>13.2</u>	
L <u>12451</u>		H <u>12451</u>		Gg <u>.651</u>		%CO ₂ <u>14.71</u>	
				%N ₂ <u>1.534</u>		%H ₂ S <u></u>	
				Prover <u></u>		Meter Run <u>4.026</u>	
						Taps <u>FLG</u>	

FLOW DATA				TUBING DATA				CASING DATA				Duration of Flow
No.	Prover Line Size	Orifice x Size	Press p.s.i.g.	Diff. h _w	Temp. °F	Press p.s.i.g.	Temp. °F	Press p.s.i.g.	Temp. °F			
SI												
1	4 X	2.000	408	1.69	98	3920		PK12				24 NR
2	4 X	2.000	424	2.56	92	3575		"				1 NR
3	4 X	2.000	441	6.76	96	3465		"				1 NR
4	4 X	2.000	457	10.89	94	3100		"				1 NR
5						2890		"				1 NR

RATE OF FLOW CALCULATIONS

No.	COEFFICIENT (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor f _t	Gravity Factor F _g	Super Compress Factor F _{pv}	Rate of Flow Q, Mcfd
1	19.81	91.35	421.2	.9645	1.239	1.034	2,236
2	19.81	93.06	437.2	.9706	1.239	1.038	2,301
3	19.81	94.85	454.2	.9671	1.239	1.039	2,339
4	19.81	96.51	470.2	.9688	1.239	1.041	2,389
5							

No.	P _r	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio	Meq bbl.
1	.62	558	1.48	.935	77.2	
2	.65	552	1.47	.928	A.P. I. Gravity of Liquid Hydrocarbons	
3	.67	556	1.48	.927	53.0 @ 60°	Deg.
4	.70	554	1.47	.923	Specific Gravity Separator Gas	XXXXXXX
5					Specific Gravity Flowing Fluid	XXXXXX G.M.I.X = .690
					Critical Pressure	670 P.S.I.A. 669 P.S.I.A.
					Critical Temperature	375 R 388 R

P_c	39.33,2	P_{c2}	15470.1	
No.	P_t^2	P_w	P_w^2	$P_c^2 - P_w^2$
1		3617.2	13083.8	2386.3
2		3509.3	12315.5	3154.5
3		3147.4	9906.4	5563.7
4		2940.5	8646.5	6823.6
5				

$$(1) \frac{P_c^2}{P_c^2 - P_w^2} = \frac{6.482}{\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n} = \frac{2.541}{\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n}$$

$$AOF = Q \left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = \frac{79825}{\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n} = 5,683$$

Absolute Open Flow <u>5,683</u>		Meq (@ 15.025)		Angle of Slope (°): <u>63.5</u>		Slope n: <u>.499</u>	
Remarks: <u>WELL PRODUCED 510 BBLs of 53.0 CONDENSATE</u>							
Approved By Division:		Conducted By: <u>METER & TESTING</u>		Calculated By: <u>BM</u>		Checked By: <u>BM</u>	

