Pool	Wilder	a <b>t</b> .		Tormation					T.e.s	,	
	Pool Wildest Initial X Annual										
Initial X Annual Special Date of Test 1-20-58  Company The Texas Company Lease Audie Richards Well No. 1											
Unit P Sec. 25 Twp. 20-S Rge. 32-E Purchaser None											
									To 10	016	
Casing 7" Wt. 29# I.D. 6.184 Set at 14,945 Perf. 12,909 To 12,916  Tubing 2 3/8"Wt. 4.70# I.D. 1.99 Set at 12,908 Perf. 12,908 To 12,911											
·											
Gas Pay: From 12908 To 12916 L 12908 xG 680 -GL 8777 Bar.Press. 13.2											
Producing Thru: Casing Tubing Y Type Well Single Single-Bradenhead-G. G. or G.O. Dual											
Date of Completion: 1-20-58 Packer 12.850 Reservoir Temp.											
OBSERVED DATA Orifice Well Tester											
Tested Through (Rrower) (Choke)					(Mater)			Type Taps			
	TWO	Flo	w Data		(Hg. : Margury) Tubing Data						
No.	(Prever) (Line)	(Onific	Pres	s. Diff.	Temp.			Press.	Temp.	Duration of Flow	
	Size	Size	psi	g Hg.	° <sub>F</sub> .	psig	°F.	psig	°F∙	Hr.	
SI		-				4225				91	
1. 2.		2.00		12"	52° 67°	3310 2434	54°		<del> </del>		
3.	<u> </u>	2,00		18"	500	2028	510			3	
4.	3	2,00		24*	52	1595	50		<del>  </del>	3	
5.		2.00	<u> </u>	20"	49	1681	61-		<u> </u>	2	
				FI	OW CAL	CULATIONS	3				
	Coeffici	ent MC	F/Day	Pressure	Flow	Temp.	Gravity	Compre	ss. I	ate of Flow	
No.	(24-Hour)			Ins. Hg.	rac	cor	ractor	Factor PB		Q-MCMPD Ma 15 O25 psia	
<del>_</del> _+	(24-Hour) \(\sqrt{h_p_r}\)					Fg	- Pro-	E 15.025 psis			
1. 2.	<del></del>	13		12" 1.007 14" 2993				9750		1.431	
3.		1821		18"			9427	97		1.699	
4.		21		2411	1.007		9127	97		1,993	
5.			1931	20#	1.010	7	.9427	97		1,794	
PRESSURE CALCULATIONS  Gas Liquid Hydrocarbon Ratio 37 375 cf/bbl. Specific Gravity Separator Garavity of Liquid Hydrocarbons 17 8 deg. Specific Gravity Flowing Flux Fc 5.866 (1-e-s) 604 Pc 4238.2 Pc 17.962.3									ing Fluid		
No.	P <sub>w</sub> Pt (psia)	Pt.	F <sub>c</sub> Q	$(F_cQ)^2$	(F <sub>1</sub>	cQ) <sup>2</sup> -e-s)	P <sub>w</sub> 2	$P_c^2 - P_w^2$	Cal P	P <sub>W</sub> P <sub>C</sub>	
	3323.2	1043.7	3.0	15.60 70.39	- 5	1.42	11,053	6,909	3324	6 .74	
$\overline{}$	2041-2	1366.5	9.0	98.21	50	32	1 226	12 726	2055	7 10	
	1608.2	2586.3	11.4	136.66	1	2.54	2,669	15,293	1633	7 36	
	1694.2	2870.3		2 110.67	<u>i 66</u>		2,937	15,025	1713	8 40	
	lute Potent		2,100		MCFPD;	n_1.00	00				
COMPANY THE TEXAS COMPANY ADDRESS BOX 1270 MIDLAND TRYAS											
AGENT and TITLE I. I BAKER DISTORTED CAS MAN ZULLANGE											
WITNESSED H. H. KERRY AND J. O. WHITHING											
COMPANY RI PASO NATURAL GAS COMPANY REMARKS											
die Atte allached, opposit testing											
I set alle I desconed testing											
		d	u .	un	00	inu	mer	( / Vio	4		
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## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission · at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- Q  $\equiv$  Actual rate of flow at end of flow period at W. H. working pressure (P<sub>W</sub>). MCF/da. @ 15.025 psia and 60° F.
- $P_c=72$  hour wellhead shut-in casing (or tubing) pressure whichever is greater. psia
- Pw Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.), psia
- Pt Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- $P_f$  Meter pressure, psia.
- hw Differential meter pressure, inches water.
- Fg Gravity-correction factor.
- Ft Flowing temperature correction factor.
- Fpv Supercompressability factor.
- n I Slope of back pressure curve.

Note: If Pw cannot be taken because of manner of completion or condition of well, then Pw must be calculated by adding the pressure drop due to friction within the flow string to Pt.