

## NEW MEXICO OIL CONSERVATION COMMISSION

ELVIS A. UTE  
GAS ENGINEER

Form C-122

HOBBS OFFICE OCC

MAIN OFFICE OCC

Revised 12-1-55

## MULTI-POINT BACK PRESSURE TEST FOR GAS WELLS

Pool Permian Formation Permian County 29  
1955 OCT 10 PM 3:06 1955 SEP 4Initial I Annual \_\_\_\_\_ Special \_\_\_\_\_ Date of Test 8-10-56Company Gulf Oil Corporation Lease Leahy, Fred Well No. 8Unit D Sec. 29 Twp. 19N Rge. 37E Purchaser Permian Basin PL Co.Casing 5.5 Wt. 17.0 I.D. 4.892 Set at 3704 Perf. 3432 To 3506Tubing 2.375 Wt. 4.7 I.D. 1.995 Set at 3099 Perf. \_\_\_\_\_ To \_\_\_\_\_Gas Pay: From 3432 To 3506 L 3432 xG .400 -GL 2334 Bar.Press. 13.2Producing Thru: Casing I Tubing \_\_\_\_\_ Type Well CO DualDate of Completion: 3-28-56 Packer 3740 Single-Bradenhead-G. G. or G.O. Dual  
Reservoir Temp. \_\_\_\_\_

## OBSERVED DATA

Tested Through (Prover) (Choke) (Meter) Type Taps Pipe

| No. | Flow Data                  |                              |                |                         |              | Tubing Data    |              | Casing Data    |              | Duration of Flow Hr. |
|-----|----------------------------|------------------------------|----------------|-------------------------|--------------|----------------|--------------|----------------|--------------|----------------------|
|     | (Prover)<br>(Line)<br>Size | (Choke)<br>(Orifice)<br>Size | Press.<br>psig | Diff.<br>h <sub>w</sub> | Temp.<br>°F. | Press.<br>psig | Temp.<br>°F. | Press.<br>psig | Temp.<br>°F. |                      |
| SI  |                            |                              |                |                         |              |                |              |                |              |                      |
| 1.  | 4                          | 2.75                         | 143.0          | 2.0                     | 82           |                |              | 134.5          |              | 72                   |
| 2.  | 4                          | 2.75                         | 135.0          | 10.0                    | 97           |                |              | 127.5          |              | 23                   |
| 3.  | 4                          | 2.75                         | 140.0          | 21.5                    | 84           |                |              | 118.1          |              | 24                   |
| 4.  | 4                          | 2.75                         | 170.7          | 23.9                    | 88           |                |              | 106.7          |              | 25                   |
| 5.  |                            |                              |                |                         |              |                |              | 87.3           |              | 20                   |

## FLOW CALCULATIONS

| No. | Coefficient<br>(24-Hour) | $\sqrt{h_{wpe}}$ | Pressure<br>psia | Flow Temp.<br>Factor<br>F <sub>t</sub> | Gravity<br>Factor<br>F <sub>g</sub> | Compress.<br>Factor<br>F <sub>pv</sub> | Rate of Flow<br>Q-MCFPD<br>@ 15.025 psia |
|-----|--------------------------|------------------|------------------|--|-------------------------------------|--|--|
| 1.  | 73.22                    | 30.53            | 144.2            | .9795                                  | .9993                               | 1.009                                  | 21.34                                    |
| 2.  | 73.22                    | 71.22            | 140.2            | 1.0003                                 | .9991                               | 1.009                                  | 23.37                                    |
| 3.  | 73.22                    | 142.70           | 142.2            | .9998                                  | .9993                               | 1.009                                  | 73.98                                    |
| 4.  | 73.22                    | 140.60           | 161.9            | .9994                                  | .9993                               | 1.009                                  | 77.62                                    |
| 5.  |                          |                  |                  |  |                                     |  |  |

CO<sub>2</sub> 2.045  
H<sub>2</sub> 2.342

## PRESSURE CALCULATIONS

Gas Liquid Hydrocarbon Ratio \_\_\_\_\_ cf/bbl.  
Gravity of Liquid Hydrocarbons 0.848 deg.  
F<sub>c</sub> 1.022 (1-e<sup>-s</sup>)Specific Gravity Separator Gas \_\_\_\_\_  
Specific Gravity Flowing Fluid \_\_\_\_\_  
P<sub>c</sub> 1005.7 P<sub>c</sub> 1005.7

| No. | P <sub>w</sub><br>P <sub>t</sub> (psia) | P <sub>t</sub> <sup>2</sup> | F <sub>c</sub> Q | (F <sub>c</sub> Q) <sup>2</sup> | (F <sub>c</sub> Q) <sup>2</sup><br>(1-e <sup>-s</sup> ) | P <sub>w</sub> <sup>2</sup> | P <sub>c</sub> <sup>2</sup> -P <sub>w</sub> <sup>2</sup> | Cal.<br>P <sub>w</sub> | P <sub>w</sub><br>P <sub>c</sub> |
|-----|---|-----------------------------|------------------|---------------------------------|---|-----------------------------|--|------------------------|----------------------------------|
| 1.  | 143.0                                   | 20449                       | 2.002            | 4.008                           | 11.811  | 20449                       | 20449-11.811   | 143.0                  | 143.0                            |
| 2.  | 135.0                                   | 18225                       | 5.338            | 28.50                           | 11.811  | 18225                       | 18225-11.811   | 135.0                  | 135.0                            |
| 3.  | 140.0                                   | 19600                       | 23.220           | 539.80                          | 25.870  | 19600                       | 19600-25.870   | 140.0                  | 140.0                            |
| 4.  | 170.7                                   | 29139                       | 14.020           | 196.56                          | 27.130  | 29139                       | 29139-27.130   | 170.7                  | 170.7                            |
| 5.  |   |                             |                  |                                 |   |                             |  |                        |                                  |

Absolute Potential: 11,860 MCFPD; n .70COMPANY Gulf Oil Corporation  
ADDRESS Box 2167, Hobbs, N.M.AGENT and TITLE F. L. Smith

WITNESSED \_\_\_\_\_

COMPANY \_\_\_\_\_

REMARKS \_\_\_\_\_

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

$Q$  = Actual rate of flow at end of flow period at W. H. working pressure ( $P_w$ ).  
MCF/da. @ 15.025 psia and 60° F.

$P_c$  = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater.  
psia

$P_w$  = Static wellhead working pressure as determined at the end of flow period.  
(Casing if flowing thru tubing, tubing if flowing thru casing.) psia

$P_t$  = Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia

$P_f$  = Meter pressure, psia.

$h_w$  = Differential meter pressure, inches water.

$F_g$  = Gravity correction factor.

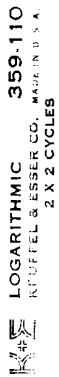
$F_t$  = Flowing temperature correction factor.

$F_{pv}$  = Supercompressibility factor.

$n$  = Slope of back pressure curve.

Note: If  $P_w$  cannot be taken because of manner of completion or condition of well, then  $P_w$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_t$ .

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**Figure 1**

1992

|         |         |         |         |
|---------|---------|---------|---------|
| 1000000 | 1000000 | 1000000 | 1000000 |
| 1000000 | 1000000 | 1000000 | 1000000 |

1. *Chlorophyll a* and *Chlorophyll b* were determined by the method of Arar and Collins (1971).