

## NEW MEXICO OIL CONSERVATION COMMISSION

NOBBS OFFICE 000

Form C-122

Revised 12-1-55

## MULTI-POINT BACK PRESSURE TEST FOR GAS WELLS

NOB OCT 20 AM 10:49

Pool Eumont Formation Fenrose County Lea  
Initial \_\_\_\_\_ Annual \_\_\_\_\_ Special X Date of Test 8-13 thru 8-17-56  
Company Standard Oil Co. of Texas Lease State 1-35 Well No. 1  
Unit M Sec. 35 Twp. 19-S Rge. 37-E Purchaser EPMG  
Casing 7 Wt. 23 I.D. 6.366 Set at 3640 Perf. \_\_\_\_\_ To \_\_\_\_\_  
Tubing 2 Wt. 4.7 I.D. 1.995 Set at 3657 Perf. \_\_\_\_\_ To \_\_\_\_\_  
Gas Pay: From 3660 To 3796 L 3657 xG 0.675 -GL 2468 Bar.Press. 13.2  
Producing Thru: Casing \_\_\_\_\_ Tubing X Type Well Single  
Single-Bradenhead-G. G. or G.O. Dual  
Date of Completion: 7-22-55 Packer None Reservoir Temp. \_\_\_\_\_

## OBSERVED DATA

Tested Through (Proven) (Choke) (Meter)Type Taps Flange

No.	Flow Data					Tubing Data		Casing Data		Duration of Flow Hr.
	(Proven) (Line) Size	(Choke) (Orifice) Size	Press. psig	Diff. h <sub>w</sub>	Temp. °F.	Press. psig	Temp. °F.	Press. psig	Temp. °F.	
SI						871		876		72 SIP
1.	4"	1.5"	575	7.352	71	630		722		24
2.	4"	1.5"	560	6.22	72	657		717		24
3.	4"	1.5"	567	4.72	72	702		735		24
4.	4"	1.5"	564	3.52	74	739		757		24
5.										

## FLOW CALCULATIONS

No.	Coefficient Fig. (24-Hour)	$\sqrt{h_{wPf}}$	Pressure psia	Flow Temp. Factor F <sub>t</sub>	Gravity Factor F <sub>g</sub>	Compress. Factor F <sub>pv</sub>	Rate of Flow Q-MCFPD @ 15.025 psia
1.	13.99	178.24	588.2	.9896	.9427	1.062	2,470.5
2.	13.99	148.37	573.2	.9887	.9427	1.062	2,054.5
3.	13.99	113.22	580.2	.9887	.9427	1.062	1,567.9
4.	13.99	84.10	577.2	.9868	.9427	1.060	1,160.2
5.							

## PRESSURE CALCULATIONS

Gas Liquid Hydrocarbon Ratio dry cf/bbl.  
Gravity of Liquid Hydrocarbons \_\_\_\_\_ deg.  
F<sub>c</sub> 9.936 (1-e<sup>-5</sup>) 0.222

Specific Gravity Separator Gas \_\_\_\_\_  
Specific Gravity Flowing Fluid \_\_\_\_\_  
P<sub>c</sub> 889.2 P<sub>c</sub> 790.7

No.	P <sub>w</sub> P <sub>t</sub> (psia)	P <sub>t</sub> <sup>2</sup>	F <sub>c</sub> Q	(F <sub>c</sub> Q) <sup>2</sup>	(F <sub>c</sub> Q) <sup>2</sup> (1-e <sup>-5</sup> )	P <sub>w</sub> <sup>2</sup>	P <sub>c</sub> <sup>2</sup> -P <sub>w</sub> <sup>2</sup>	Cal. P <sub>w</sub>	P <sub>w</sub> / P <sub>c</sub>
1.	735.2	413.7	24.55	602.7	133.8	540.5	250.2	740	0.8268
2.	730.2	449.2	20.41	416.6	92.5	533.2	257.5	736	0.8212
3.	748.2	511.5	15.58	242.7	53.9	559.8	230.9	752	0.8414
4.	770.2	565.8	11.53	132.9	29.5	593.2	197.5	772	0.8662
5.									

Absolute Potential: 6,250 MCFPD; n 1COMPANY Standard Oil Co. of TexasADDRESS Bin "B", Royalty, TexasAGENT and TITLE J. M. McManan, District EngineerWITNESSED Edward MabeCOMPANY El Paso Natural Gas Company

REMARKS

Back pressure curve with slope of (1) was drawn through highest flow rate in accordance with paragraph 104 (1) of back pressure manual.

See  
6-15-56  
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## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- $Q$  = Actual rate of flow at end of flow period at W. H. working pressure ( $P_w$ ).  
MCF/da. @ 15.025 psia and 60° F.
- $P_c$  = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater.  
psia
- $P_w$  = Static wellhead working pressure as determined at the end of flow period.  
(Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- $P_t$  = Flowing wellhead pressure (tubing if flowing through tubing, casing if  
flowing through casing.) psia
- $P_f$  = Meter pressure, psia.
- $h_w$  = Differential meter pressure, inches water.
- $F_g$  = Gravity correction factor.
- $F_t$  = Flowing temperature correction factor.
- $F_{pv}$  = Supercompressibility factor.
- $n$  = Slope of back pressure curve.

Note: If  $P_w$  cannot be taken because of manner of completion or condition of well, then  $P_w$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_t$ .