

## NEW MEXICO OIL CONSERVATION COMMISSION

HOBBBS OFFICE 000

Form C-122

## MULTI-POINT BACK-PRESSURE TEST FOR GAS WELLS

Revised 12-1-55

Pool Eumont Formation Seven Rivers County Lea  
Initial \_\_\_\_\_ Annual \_\_\_\_\_ Special x Date of Test 8-6 to 8-10-56  
Company The Superior Oil Company Lease \_\_\_\_\_ State \_\_\_\_\_ Well No. 1-12  
Unit L Sec. 12 Twp. 218 Rge. 35E Purchaser El Paso Natural Gas Company  
Casing 7 Wt. 20 I.D. 6.456 Set at 4211 Perf. 3674 To 3690  
Tubing 2 1/2 Wt. 6.5 I.D. 2.441 Set at 3973 Perf. \_\_\_\_\_ To \_\_\_\_\_  
Gas Pay: From 3674 To 3690 L 3674 xG 0.680 -GL 2498 Bar.Press. 13.2  
Producing Thru: Casing x Tubing \_\_\_\_\_ Type Well G. O. Dual  
Single-Bradenhead-G. G. or G.O. Dual  
Date of Completion: 7-6-56 Packer 3697 Reservoir Temp. \_\_\_\_\_

## OBSERVED DATA

Tested Through (Prover) (Choke) (Meter)

Type Taps \_\_\_\_\_

| No. | Flow Data   |                |             |             |           | Tubing Data |           | Casing Data |           | Duration of Flow Hr. |
|-----|-------------|----------------|-------------|-------------|-----------|-------------|-----------|-------------|-----------|----------------------|
|     | (Line) Size | (Orifice) Size | Press. psig | Diff. $h_w$ | Temp. °F. | Press. psig | Temp. °F. | Press. psig | Temp. °F. |                      |
| SI  |             |                |             |             |           |             |           |             |           |                      |
| 1.  | 1/2         | 1.250          | 560         | 10.24       | 66        |             |           | 887         |           | 72                   |
| 2.  | 1/2         | 1.250          | 559         | 20.25       | 65        |             |           | 860         |           | 24                   |
| 3.  | 1/2         | 1.250          | 562         | 30.25       | 64        |             |           | 839         |           | 24                   |
| 4.  | 1/2         | 1.250          | 568         | 40.00       | 66        |             |           | 819         |           | 24                   |
| 5.  | 1/2         | 1.250          | 585         | 49.00       | 66        |             |           | 785*        |           | 24                   |

\*Unable to get 30% drawdown because of small choke size.

| No. | Coefficient (24-Hour) | $\sqrt{h_{wpf}}$ | Pressure psia | Flow Temp. Factor $F_t$ | Gravity Factor $F_g$ | Compress. Factor $F_{pv}$ | Rate of Flow Q-MCFPD @ 15.025 psia |
|-----|-----------------------|------------------|---------------|-------------------------|----------------------|---------------------------|------------------------------------|
| 1.  | 9.643                 | 76.60            |               | .9943                   | .9393                | 1.066                     | 735                                |
| 2.  | 9.643                 | 107.63           |               | .9952                   | .9393                | 1.066                     | 1034                               |
| 3.  | 9.643                 | 131.88           |               | .9962                   | .9393                | 1.066                     | 1269                               |
| 4.  | 9.643                 | 171.2            |               | .9943                   | .9393                | 1.066                     | 1644                               |
| 5.  |                       |                  |               |                         |                      |                           |                                    |

## PRESSURE CALCULATIONS

Gas Liquid Hydrocarbon Ratio \_\_\_\_\_ cf/bbl.  
Gravity of Liquid Hydrocarbons \_\_\_\_\_ deg.  
 $F_c$  Calculated 0.823 (1-e<sup>-s</sup>) .158

Specific Gravity Separator Gas \_\_\_\_\_  
Specific Gravity Flowing Fluid \_\_\_\_\_  
 $P_c$  900  $P_c^2$  810

| No. | $P_w$ $P_t$ (psia) | $P_t^2$ | $F_c Q$ | $(F_c Q)^2$ | $(F_c Q)^2 (1-e^{-s})$ | $P_w^2$ | $P_c^2 - P_w^2$ | Cal. $P_w$ | $P_w / P_c$ |
|-----|--------------------|---------|---------|-------------|------------------------|---------|-----------------|------------|-------------|
| 1.  | 873                | 762     | .605    | .366        | .058                   | 762     | 48              | 872.95     | 97.0        |
| 2.  | 852                | 726     | .851    | .724        | .114                   | 726.1   | 89.9            | 852.12     | 94.7        |
| 3.  | 832                | 692     | 1.044   | 1.090       | .172                   | 692.2   | 117.8           | 831.96     | 92.4        |
| 4.  | 798                | 637     | 1.353   | 1.831       | .289                   | 637.3   | 172.7           | 798.93     | 88.8        |
| 5.  |                    |         |         |             |                        |         |                 |            |             |

Absolute Potential: 4,350 MCFPD; n .626COMPANY THE SUPERIOR OIL COMPANYADDRESS MIDLAND, TEXASAGENT and TITLE Jim Sullivan (Gas Engineer)

WITNESSED \_\_\_\_\_

COMPANY \_\_\_\_\_

REMARKS \_\_\_\_\_

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

$Q$  = Actual rate of flow at end of flow period at W. H. working pressure ( $P_w$ ).  
MCF/da. @ 15.025 psia and 60° F.

$P_c$  = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater.  
psia

$P_w$  = Static wellhead working pressure as determined at the end of flow period.  
(Casing if flowing thru tubing, tubing if flowing thru casing.) psia

$P_t$  = Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia

$P_f$  = Meter pressure, psia.

$h_w$  = Differential meter pressure, inches water.

$F_g$  = Gravity correction factor.

$F_t$  = Flowing temperature correction factor.

$F_{pv}$  = Supercompressibility factor.

$n$  = Slope of back pressure curve.

Note: If  $P_w$  cannot be taken because of manner of completion or condition of well, then  $P_w$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_t$ .