

## NEW MEXICO OIL CONSERVATION COMMISSION

ELVIS A. C.  
GAS ENGINEER

MAIN OFFICE OCC HOBBS OFFICE OCC

Form C-122

Revised 12-1-55

## MULTI-POINT BACK PRESSURE TEST FOR GAS WELLS

Pool Eumont Formation Queen County LeaInitial \_\_\_\_\_ Annual \_\_\_\_\_ Special I Date of Test 8-20 to 8-24-56Company El Paso Natural Gas Company Lease Shell State Well No. 5Unit L Sec. 2 Twp. 21 S Rge. 36 E Purchaser El Paso Natural Gas CompanyCasing 5 1/2 Wt. 15.5 I.D. 4.076 Set at 3420 Perf. \_\_\_\_\_ To \_\_\_\_\_Tubing 2 Wt. 4.7 I.D. 1.995 Set at 3478 Perf. \_\_\_\_\_ To \_\_\_\_\_Gas Pay: From 3420 To 3585 L 3478 xG .670 -GL \_\_\_\_\_ Bar.Press. 13.2Producing Thru: Casing \_\_\_\_\_ Tubing X Type Well SingleDate of Completion: 7-26-56 Packer None Single-Bradenhead-G. G. or G.O. Dual  
Reservoir Temp. \_\_\_\_\_

## OBSERVED DATA

Tested Through (Pressure)(Gauge)(Meter) Type Taps Flange

| No. | Flow Data                                 |  |                |                         |              | Tubing Data    |              | Casing Data    |              | Duration<br>of Flow<br>Hr. |
|-----|---|--|----------------|-------------------------|--------------|----------------|--------------|----------------|--------------|----------------------------|
|     | ( <del>Pressure</del> )<br>(Line)<br>Size | ( <del>Flow</del> )<br>(Orifice)<br>Size | Press.<br>psig | Diff.<br>h <sub>w</sub> | Temp.<br>°F. | Press.<br>psig | Temp.<br>°F. | Press.<br>psig | Temp.<br>°F. |                            |
| SI  |   |  |                |                         |              | <u>864</u>     |              | <u>864</u>     |              | <u>72</u>                  |
| 1.  | <u>4"</u>                                 | <u>1.250</u>                             | <u>971</u>     | <u>8.2"</u>             | <u>68</u>    | <u>714</u>     |              | <u>749</u>     |              | <u>24</u>                  |
| 2.  | <u>4"</u>                                 | <u>1.250</u>                             | <u>966</u>     | <u>6.9"</u>             | <u>68</u>    | <u>737</u>     |              | <u>799</u>     |              | <u>24</u>                  |
| 3.  | <u>4"</u>                                 | <u>1.250</u>                             | <u>971</u>     | <u>5.0"</u>             | <u>69</u>    | <u>778</u>     |              | <u>790</u>     |              | <u>24</u>                  |
| 4.  | <u>4"</u>                                 | <u>1.250</u>                             | <u>970</u>     | <u>3.9"</u>             | <u>77</u>    | <u>808</u>     |              | <u>804</u>     |              | <u>24</u>                  |
| 5.  |   |  |                |                         |              |                |              |                |              |                            |

## FLOW CALCULATIONS

| No. | Coefficient<br>(24-Hour) | $\sqrt{h_w p_f}$ | Pressure<br>psia | Flow Temp.<br>Factor<br>F <sub>t</sub> | Gravity<br>Factor<br>F <sub>g</sub> | Compress.<br>Factor<br>F <sub>pv</sub> | Rate of Flow<br>Q-MCFPD<br>@ 15.025 psia |
|-----|--------------------------|------------------|------------------|--|-------------------------------------|--|--|
| 1.  | <u>9.643</u>             | <u>198.16</u>    |                  | <u>.9984</u>                           | <u>.9463</u>                        | <u>1.062</u>                           | <u>1.905</u>                             |
| 2.  | <u>9.643</u>             | <u>167.23</u>    |                  | <u>.9984</u>                           | <u>.9463</u>                        | <u>1.062</u>                           | <u>1.609</u>                             |
| 3.  | <u>9.643</u>             | <u>120.83</u>    |                  | <u>.9985</u>                           | <u>.9463</u>                        | <u>1.062</u>                           | <u>1.161</u>                             |
| 4.  | <u>9.643</u>             | <u>84.91</u>     |                  | <u>.9980</u>                           | <u>.9463</u>                        | <u>1.057</u>                           | <u>808</u>                               |
| 5.  |                          |                  |                  |  |                                     |  |  |

## PRESSURE CALCULATIONS

Gas Liquid Hydrocarbon Ratio \_\_\_\_\_ cf/bbl.

Gravity of Liquid Hydrocarbons \_\_\_\_\_ deg.

F<sub>c</sub> Measured (1-e<sup>-s</sup>) \_\_\_\_\_

Specific Gravity Separator Gas \_\_\_\_\_

Specific Gravity Flowing Fluid \_\_\_\_\_

P<sub>c</sub> 877.2 P<sub>c</sub><sup>2</sup> 769.5

| No. | P <sub>w</sub><br><del>P<sub>w</sub></del> (psia) | P <sub>t</sub> <sup>2</sup> | F <sub>c</sub> Q | (F <sub>c</sub> Q) <sup>2</sup> | (F <sub>c</sub> Q) <sup>2</sup><br>(1-e <sup>-s</sup> ) | P <sub>w</sub> <sup>2</sup> | P <sub>c</sub> <sup>2</sup> -P <sub>w</sub> <sup>2</sup> | Cal.<br>P <sub>w</sub> | P <sub>w</sub> /<br>P <sub>c</sub> |
|-----|---|-----------------------------|------------------|---------------------------------|---|-----------------------------|--|------------------------|------------------------------------|
| 1.  | <u>758.2</u>                                      |                             |                  |                                 |   | <u>574.9</u>                | <u>194.6</u>   |                        | <u>.83</u>                         |
| 2.  | <u>772.2</u>                                      |                             |                  |                                 |   | <u>596.3</u>                | <u>171.2</u>   |                        | <u>.85</u>                         |
| 3.  | <u>803.2</u>                                      |                             |                  |                                 |   | <u>645.1</u>                | <u>124.4</u>   |                        | <u>.90</u>                         |
| 4.  | <u>827.2</u>                                      |                             |                  |                                 |   | <u>684.9</u>                | <u>85.2</u>  |                        | <u>.94</u>                         |
| 5.  |   |                             |                  |                                 |   |                             |  |                        |                                    |

Absolute Potential: 7.000 MCFPD; n .98COMPANY El Paso Natural Gas CompanyADDRESS P. O. Box 1384, Jol., New MexicoAGENT AND TITLE R. T. Wright R. T. Wright, Petroleum EngineerWITNESSED Earl G. SmithCOMPANY El Paso Natural Gas Company

## REMARKS

Decreasing sequence used because of fluid.  
Not enough draw down because of choke size.

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

$Q$  = Actual rate of flow at end of flow period at W. H. working pressure ( $P_w$ ).  
MCF/da. @ 15.025 psia and 60° F.

$P_c$  = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater.  
psia

$P_w$  = Static wellhead working pressure as determined at the end of flow period.  
(Casing if flowing thru tubing, tubing if flowing thru casing.) psia

$P_t$  = Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia

$P_f$  = Meter pressure, psia.

$h_w$  = Differential meter pressure, inches water.

$F_g$  = Gravity correction factor.

$F_t$  = Flowing temperature correction factor.

$F_{pv}$  = Supercompressability factor.

$n$  = Slope of back pressure curve.

Note: If  $P_w$  cannot be taken because of manner of completion or condition of well, then  $P_w$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_t$ .