NEW MEXICO OIL CONSERVATION COMMISSION

HOBBS OFFICE OCC

O A. UTZ

Form C-122

Revised 12-1-55

De	ol <u>By</u>		N	ULTI -	-POINT B	BACK PRE	SSURE TES	ST FOR GA	s wells Zatos		Revised 12-1-55	
In	itialAnnu		_Annual			Special		- Î	Date of	Test	3=29=35	
Cor	npany <u>Conf</u>	inenta.	011 0	omoat	33	Lease	eley.	er 8-8	We:	ll No	<i>L</i> ,	
Unit <u>D</u> Sec. 8 Twp. 22 Rge. 38 Purchaser RPNG Casing 52: Wt. 17.0 I.D. Set at 3791 Perf. 2985 To 3890												
Tubing 3" Wt. 9.3 I.D. Set at 3765 Perf. To												
Gas Pay: From 2965 To 3												
Dot	Producing Thru: Casing X Tubing Type Well G.C. Dual Single-Bradenhead-G. G. or G.O. Dual Date of Completion: Packer Reservoir Temp. 90											
Dat	e of Comptet	tion:	<u> 7-31</u> .	4.95	Packe	r		Reservo	oir Temp.	90]	
						OBSERV	ED DATA					
Tes	ted Through	(Prove	+) × (Ch	ske)	(Meter)				Type Tap	os	£1130	
Flow Data Tubing Data Casing Data											Γ	
No.	(Prover)	(Chok	re) P	ress.	Diff.		Press.	Temp.	Press.		ľ	
	Size	Siz	e :	osig	h _w	\circ_{F} .	psig	°F.	psig	∍ _F .	of Flow Hr.	
SI 1.						_			960		7/2	
2.	1.		250 250	530 587	9.0 21.2	20 69		<u> </u>	377	 	24	
3.	2		250	536		67		<u> </u>	\$02 737	 	2 <u>1</u>	
<u>4.</u> 5.	1.		250	537	59.5	76			533	 	ak	
<u> </u>		<u> </u>										
						FLOW CAL	CULATION	S				
	Coeffici	.ent		Pressure				Gravity Compre		ess. Rate of Flow		
No.			/	-		Fac	tor	Factor	Facto	r	Q-MCFPD	
	(24-Hour)		√ h _w p _f		psia	F	• 1	F _g	Fpv	@ 15.025 psia		
10	9.643 9.643		75.5		593.2	<u>0,</u>	90,72	0.9325 0.9325	1.	052 683		
3.	9.543		142.0		600,2	0,3102 0,0915 0,9933 0,9850		0.9325	l.	070	107%	
4.	9.643			189.0		279.2 0. 600.2 0.		0,932 5 0,932 5		070	1358 1790	
1. 2. 3. 4. 5.	70372 3077		3.0740	1	C 2			قور مشار البي تراع ما الماني المراع ما الماني المراع مانيا الماني المراع مانيا المانيا المانيا المانيا المانيا	لامدُ.	058	3.175	
					PRI	ESSURE C	ALCUTATIO	ONS				
Gas]	Liquid Hydro	carbon	Ratio		.yet-y	cf/bbl.		Speci	fic Gravi	tv Sena	rator Gas (5)	
Grav:	Gravity of Liquid Hydrocarbons deg. Specific Gravity Flowing Fluid											
^{t'} c	4.22(<i>i</i>		(1-	<u>-s)</u>	0.1	<u> </u>		Pc	973.2	_Pc	345.0	
	$P_{\mathbf{W}}$		T			7				T		
No.		$P_{\mathbf{t}}^{2}$	F _c Q		$(F_cQ)^2$	(F	_{cQ}) ²	P _w 2	$P_c^2 - P_w^2$	Ca	1. P.,	
-	Pt (psia)					(1.	<u>-</u> €_0)		·	P,	$\frac{P_{\mathbf{w}}}{\mathbf{P_{\mathbf{c}}}}$	
1. 2.	890.2 815.2	792.5 684.5	2.00	85	200		809	793.39	151.9	30	1 ,937	
$\frac{\tilde{3}}{3}$	750.2		564.5 4.51 562.5 5.72		20.6 32.6	2.70 4.30		\$67,20	278.3		5.2 .841	
3. 4. 5.	646.2	417.0		7.550		+ + + + + + + + + + + + + + + + + + + +	.16	566.80	378.7 521.0	75 55		
5.					5 7.0			3 2 1 14 3 2 2 2 7 C	- A A - A - A - A - A - A - A - A - A -	1 93	*/	
Abso	olute Potent			60		MCFPD;	n .					
COMPANY Corning tal Company												
	ESS_	Park.	427-ic	ò_S,	N							
AGENT and TITLE W. D. Howard Gas Parties. WITNESSED												
	PANY											

REMARKS

ILLEGIBLE

INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

NOMENCLATURE

- Q \equiv Actual rate of flow at end of flow period at W. H. working pressure (P_W). MCF/da. @ 15.025 psia and 60° F.
- P_c 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater. psia
- PwI Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- Pt Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- Pf Meter pressure, psia.
- hw Differential meter pressure, inches water.
- Fg Gravity correction factor.
- Ft Flowing temperature correction factor.
- F_{pv} Supercompressability factor.
- n I Slope of back pressure curve.

Note: If $P_{\mathbf{W}}$ cannot be taken because of manner of completion or condition of well, then $P_{\mathbf{W}}$ must be calculated by adding the pressure drop due to friction within the flow string to $P_{\mathbf{t}}$.