| LOIM | U-12 |
|------|-------------|
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| | |

| | | | M117. | rt-potnr | BACK PR | ESSURE TES' | r for gas | WELLS | F | Revised 12-1-55 |
|---------------|------------------------------------|--|--------------------------------------|-------------------------------------|-------------------------|---------------------------------|---------------------------------|-----------------------|----------------------------|-------------------------------|
| Pool | BLINEBRY (| (GAS) | | | | | | | LEA | |
| Init | ialx | And the second s | Annual | | Sp | ecial | 7 1i | _Date of | Test_12 | -14-57 |
| | any N. B. H | | | | | | | | | |
| | XX G S | | | | | | | | | |
| | | | | | | | | | То | 5608 |
| m | ng 54 W | 4.7 | ō.́b.́ | 2.375 | Cat at | 579() Par | rf Tubb | Pav | To | |
| | | | | | | | | | | |
| | | | | | | | | | | ss. <u>13.2</u> |
| 'Prod Date | ucing Thru: | Casi | ng <u>X</u> 1-6-57 | Pac | Tubing, ker 5 | Sin | Type We gle-Brade Reservo | nhead-G. oir Temp. | G.G. Dua G. or G 100 | 0. Dual |
| 2200 | or compres | | ± | A Malane a process called No. 18 of | | RVED DATA | | | | |
| . | ed Through | (| -\-(\alpha\-\) | __\1 | | | | Tune Ta | ns | |
| Test | ed Inrough | | | | TY (IESI | | | Casing | | |
| \neg | (PENNE) | (KNKK | , | ss. Dif | f. Temp | Tubing Press. | | | Temp. | Duration |
| No. | (Line) Size | (Orifi Siz | · 1 | ig h | °F. | psig | o _F , | psig | [⊃] F• | of Flow Hr. |
| SI | - AAA | 0.000 | | | | | | 1780 | | 3 |
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| 4. | 11 | 11 | 12. | 0 | 81 | | | 108 | | 3 |
| 5. 1 | | | | | | | | | <u> </u> | |
| | Coeffici | ent | | Pressiii | FLOW C | CALCULATION | S Gravity | Compr | ess. | Rate of Flow Q-MCFPD |
| No. | ODELLICI | eno | | | | 40001 | 10000 | I | - 1 | - |
| | (24-Hou | r) | $/$ h _w p $_{\mathbf{f}}$ | Mercury | cx | Ft | Fg | Fpv | | @ 15.025 psia |
| 1. | 1299 | | | 10 | | 9924 | .8381 | | 000 | 1080 |
| 2. | 1692 | | | 16 | | .9840 | #1 #1 | 11 | | 1395 1676 |
| 3. 4. | 2040 2149 | | | 22 | | .9804 .9804 | 11 | 11 | | 1766 |
| 5. | | | | | | E CALCULATI | | | | 0.54 |
| as I | iquid Hydro | carbon | Ratio | | cf/bl | ol. | Spec | ific Grav | rity Sepa | arator Gas854 |
| Gravi | lty of Liqui | d Hydro | _carbons _l_e | None P | rod. de 280 | eg. | Spec: | 1793.2 | p2 P2 | ving Fluid |
| c | 1.758 | | (1_e | <u></u> | 200 | | * C | <u> </u> | ^ C | |
| No. | $P_{\mathbf{w}}$ | P _t . | F _c Q | (F _c (| 2)2 | (F _c Q) ² | F _w 2 | $P_c^2 - P_w^2$ |) Ca | al. Pw |
| 1,00 | Pt (psia) | | | | | (1-€_2) | | | I | P _w P _c |
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| 3. | 376.2 | 141.5 | | 8.67 | | 430 | 143.9 | 3071.7 | 379.3 | • |
| 4. | 121.2 | 14.7 | 3.105 | 9.64 | 2 | 699 | 17.4 | 31.98.2 | 131.9 | 7.3 |
| 5. | | <u> </u> | 1 336 | | | | 61 | | | |
| Abso | olute Potent PANY WEST 1 | cial: | 1,775 | IO OPPUS | | · - , · · · | 61 | | | |
| ADDI | RESS P.O. | Rox 2/ | 464 – MTI | MAND T | EXAS | | | | | |
| AGE | NT and TITLE | R. V | . HARRI | GTON - | Field Pe | troleum Eng | ineer | | | |
| WITT | NESSED | | | | | | | | | |

COMPANY

INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

NOMENCLATURE

- Q I Actual rate of flow at end of flow period at W. H. working pressure (P_W). MCF/da. @ 15.025 psia and 600 F.
- P_c = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater. psia
- P_{w} Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- Pt Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- Pf Meter pressure, psia.
- hw Differential meter pressure, inches water.
- F_g : Gravity correction factor.
- F_t Flowing temperature correction factor.
- Fpv Supercompressability factor.
- n I Slope of back pressure curve.

Note: If $P_{\mathbf{W}}$ cannot be taken because of manner of completion or condition of well, then $P_{\mathbf{W}}$ must be calculated by adding the pressure drop due to friction within the flow string to $P_{\mathbf{t}}$.

