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State of New Mexico
Energy, Minerals and Natural Resources Department

Form C-122
Revised 4-1-91

OIL CONSERVATION DIVISION

P.O. Box 2088
Santa Fe, New Mexico 87504-2088

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Operator <i>Texaco E and P. Inc.,</i>						Lease or Unit Name <i>O.L. Coleman</i>					
Type Test ☐ Initial ☐ Annual ☐ Special						Test Date <i>11-30-94</i>		Well No. <i>7</i>			
Completion Date <i>11-20-94</i>		Total Depth <i>3875</i>		Plug Back TD <i>3823</i>		Elevation		Unit Ltr. - Sec. - TWP - Rge. <i>G 17 - 21 - 36</i>			
Csg. Size <i>5 1/2</i>	Wt. <i>15.5</i>	d <i>4.950</i>	Set At <i>3875</i>	Perforations: From: <i>3311</i> To: <i>3318</i>				County <i>Lea</i>			
Tbg. Size <i>None</i>	Wt. <i></i>	d <i></i>	Set At <i></i>	Perforations: From: <i></i> To: <i></i>				Pool <i></i>			
Type Well - Single - Bradenhead - G.G. or G.O. Multiple <i>single</i>						Packer Set At <i>None</i>		Formation <i>Vates</i>			
Producing Thru <i>CSG</i>		Reservoir Temp. °F <i>100 @ 3311</i>		Mean Annual Temp. °F <i>60</i>		Baro. Press - P <i>13.2</i>		Connection <i>sales line</i>			
L <i>3311</i>	H <i>3311</i>	Gg <i>.667</i>	% CO ₂ <i>.76</i>	% N ₂ <i>2.71</i>	% H ₂ S	Prover		Meter Run <i>2.067</i>	Taps <i>FLG</i>		

FLOW DATA					TUBING DATA		CASING DATA		Duration of Flow	
NO.	Prover Line Size	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.		Temp. °F
SI						<i>None</i>		<i>240</i>		<i>24 hrs.</i>
1.	<i>2 x 1.250</i>		<i>25</i>	<i>2.00</i>	<i>64</i>	<i>None</i>		<i>225</i>		<i>1 hr</i>
2.	<i>2 x 1.250</i>		<i>50</i>	<i>23.00</i>	<i>62</i>	<i>None</i>		<i>213</i>		<i>1 hr</i>
3.	<i>2 x 1.250</i>		<i>50</i>	<i>49.50</i>	<i>62</i>	<i>None</i>		<i>200</i>		<i>1 hr</i>
4.	<i>2 x 1.250</i>		<i>55</i>	<i>72.00</i>	<i>72</i>	<i>None</i>		<i>180</i>		<i>1 hr</i>
5.										

RATE OF FLOW CALCULATIONS							
NO.	COEFFICIENT (24 HOUR)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor Fg.	Super Compress. Factor, F _{pv}	Rate of Flow Q, Mcfd
1.	<i>8.120</i>	<i>8.74</i>	<i>38.2</i>	<i>.9962</i>	<i>1.224</i>	<i>1.004</i>	<i>87</i>
2.	<i>8.120</i>	<i>38.13</i>	<i>63.2</i>	<i>.9981</i>	<i>1.224</i>	<i>1.009</i>	<i>382</i>
3.	<i>8.120</i>	<i>55.93</i>	<i>63.2</i>	<i>.9981</i>	<i>1.224</i>	<i>1.009</i>	<i>560</i>
4.	<i>8.120</i>	<i>70.07</i>	<i>68.2</i>	<i>.9887</i>	<i>1.224</i>	<i>1.008</i>	<i>694</i>
5.							

NO.	P _r	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio	Mcf/bbl.
1.	<i>.05</i>	<i>524</i>	<i>1.40</i>	<i>.992</i>	<i>dry gas</i>	
2.	<i>.09</i>	<i>522</i>	<i>1.40</i>	<i>.982</i>	<i>dry</i>	
3.	<i>.09</i>	<i>522</i>	<i>1.40</i>	<i>.982</i>	<i>.667</i>	<i>XXXXXXXXXX</i>
4.	<i>.10</i>	<i>532</i>	<i>1.43</i>	<i>.984</i>	<i>* 667</i>	<i>XXXXXX</i>
5.					<i>* 372</i>	

NO.	P _i ²	P _w	P _w ²	P _c ² - P _w ²
1.		<i>238.2</i>	<i>56.7</i>	<i>7.4</i>
2.		<i>226.3</i>	<i>51.2</i>	<i>12.9</i>
3.		<i>213.3</i>	<i>45.5</i>	<i>18.6</i>
4.		<i>193.4</i>	<i>37.4</i>	<i>26.7</i>
5.				

1) $\frac{P_c^2}{P_c^2 - P_w^2} = \underline{2.401}$

2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = \underline{2.001}$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = \underline{1.389}$

P_c *253.2* P_c² *64.1*

Absolute Open Flow <i>1.389</i> Mcfd @ 15.025	Angle of Slope Θ <i>51.6</i>	Slope, n <i>.792</i>
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Remarks: *No fluid produced during test*

** = corrected to 2.71 % N₂*

Approved By Division <i>MARK SEXTON</i>	Conducted By: <i>Prowell testers</i>	Calculated By: <i>BM</i>	Checked By: <i>BM</i>
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