## NEW MEXICO OIL CONSERVATION COMMISSION

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tial t Annual Special Date of Test 2-27-97 pany Gities Service Oil Company Lease Closen B Well No. 11 t				MUI	TI-POINT	BACK PRE	SSURE TES	ST FOR GA	S WELLS		Revised 12-1
tial t Annual Special Date of Test 2-27-97 pany Gities Service Oil Company Lease Closeen B Well No. 11 t A H Sec. 30 Prop. 22 Rge. 36 Purchaser El Paco Metural Gas ing 51 Wt. 14 I.D. Set at 3366 Perf. To register the service of the service o	ool	Jalme	.t	1201	_Formatio	n <u> </u>	tes		County	Lea	L
t <u>4 H</u> Sec. <u>30</u> Twp. <u>22</u> Rge. <u>36</u> Purchaser <u>11</u> Pase Maturel Gas ing <u>54</u> Wt. <u>14</u> I.D. Set at <u>3346</u> Perf. <u>To</u> ing <u>2</u> Wt. <u>4.7</u> I.D. Set at <u>3340</u> Perf. <u>To</u> Pay: From <u>3366</u> to <u>3466</u> L <u>x0</u> <u>.455</u> <u>.51</u> Bar.Press. <u>13.2</u> ducing Thru: Casing <u>Tubing I rope Well Single</u> e of Completion: <u>2-14-57</u> Packer <u>None</u> Reservoir Temp. <u>Single</u> -Breacenhead-C. G. or G.O. Dual ted Through (Prover) (Camber) (Verses) <u>Type Tape</u> <u>Costerver</u> ) (Choke) Press. Diff. Temp. Press. Temp. <u>Ouration of F100</u> Size Size psig h <sub>w</sub> OP. psig OP. psig <u>27</u> . Mr. <u>1160</u> <u>1102</u> <u>72</u> <u>22</u> <u>1.250</u> <u>24</u> <u>43</u> <u>43</u> <u>43</u> <u>556</u> <u>732</u> <u>732</u> <u>322</u> <u>1.250</u> <u>544</u> <u>44</u> <u>556</u> <u>556</u> <u>752</u> <u>322</u> <u>1.250</u> <u>544</u> <u>44</u> <u>556</u> <u>556</u> <u>752</u> <u>322</u> <u>1.250</u> <u>544</u> <u>44</u> <u>556</u> <u>556</u> <u>752</u> <u>322</u> <u>1.250</u> <u>544</u> <u>44</u> <u>556</u> <u>556</u> <u>782</u> <u>752</u> <u>323</u> <u>23</u> <u>1.250</u> <u>544</u> <u>44</u> <u>556</u> <u>556</u> <u>782</u> <u>752</u> <u>323</u> <u>24</u> <u>1.250</u> <u>544</u> <u>445</u> <u>556</u> <u>556</u> <u>782</u> <u>752</u> <u>323</u> <u>25 <u>1.250</u> <u>544</u> <u>44</u> <u>556</u> <u>556</u> <u>782</u> <u>752</u> <u>323</u> <u>25 <u>1.250</u> <u>544</u> <u>44</u> <u>556</u> <u>556</u> <u>782</u> <u>752</u> <u>323</u> <u>26 1.250</u> <u>544</u> <u>44</u> <u>556</u> <u>556</u> <u>782</u> <u>752</u> <u>323</u> <u>74.2</u> <u>1.0157</u> <u>.9571</u> <u>2123</u> <u>2332</u> <u>23 1.250</u> <u>541</u> <u>442</u> <u>544</u> <u>556</u> <u>782</u> <u>752</u> <u>752</u> <u>333</u> <u>35.6738</u> <u>35.6738</u> <u>59.2</u> <u>1.0157</u> <u>.9571</u> <u>2332</u> <u>74.2</u> <u>1.0157</u> <u>.9571</u> <u>2332</u> <u>2332</u> <u>74.2</u> <u>1.0157</u> <u>.9571</u> <u>2332</u> <u>2332</u> <u>55.6738</u> <u>51.2</u> <u>56.2</u> <u>67.2</u> <u>1.0157</u> <u>.9571</u> <u>2332</u> <u>55.6738</u> <u>51.2</u> <u>55.1</u> <u>55.2</u> <u>61.4</u> <u>55.2</u> <u>55.1</u> <u>55.2</u> <u>61.4</u> <u>55.2</u> <u>55.2</u></u></u>	nit	ial <b>I</b>									
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Size       Size       psig       h_w       OF.       psig       OF.       De.       De.       De. <td>Τ</td> <td>(Prover)</td> <td>(Choke</td> <td>) Pre</td> <td>ss. Diff.</td> <td>. Temp.</td> <td></td> <td></td> <td>Press.</td> <td></td> <td>Duratio</td>	Τ	(Prover)	(Choke	) Pre	ss. Diff.	. Temp.			Press.		Duratio
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Coefficient       Pressure       Flow Temp.       Gravity       Compress.       Rate of Flow         (24-Hour) $\sqrt{h_w p_f}$ psia $F_t$ $F_g$ $F_{pv}$ @ 15.025 psi.         35.6738       39.2       1.0270       .9971       1374.         35.6738       54.2       1.0068       .9971       2125         35.6738       61.2       1.00178       .9971       2332         35.6738       67.2       1.00178       .9971       2332         35.6738       67.2       1.00178       .9971       2332         35.6738       74.2       1.00178       .9971       2332         35.6738       74.2       1.00178       .9971       2332         35.6738       74.2       1.00178       .9971       2332         35.6738       74.2       1.00178       .9971       2332         35.6738       74.2       1.00178       .9971       2332         1.00178       .9971       2332       .976       .976         .10140       Hydrocarbons       deg.       Specific Gravity Separator Gas       .976         .10140       Hydrocarbons       deg.       .972       P_c^2-P_w^2       .		2*	1.250	61		42			598		3
Coefficient       Pressure       Flow Temp.       Gravity       Compress.       Rate of Flow         (24-Hour) $\sqrt{h_w p_f}$ psia $F_t$ $F_g$ $F_{pv}$ @ 15.025 psi.         35.6738       39.2       1.0270       .9971       1374.         35.6738       54.2       1.0068       .9971       2125         35.6738       61.2       1.00178       .9971       2332         35.6738       67.2       1.00178       .9971       2332         35.6738       67.2       1.00178       .9971       2332         35.6738       74.2       1.00178       .9971       2332         35.6738       74.2       1.00178       .9971       2332         35.6738       74.2       1.00178       .9971       2332         35.6738       74.2       1.00178       .9971       2332         35.6738       74.2       1.00178       .9971       2332         1.00178       .9971       2332       .976       .976         .10140       Hydrocarbons       deg.       Specific Gravity Separator Gas       .976         .10140       Hydrocarbons       deg.       .972       P_c^2-P_w^2       .			L			<u> </u>	<u> </u>	L		<u> </u>	L
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35.6736       74.2       1.0178       .957       2578         PRESSURE CALCULATIONS         Specific Gravity Separator Gas					47 2					<u> </u>	
PRESSURE CALCUIATIONS         PRESSURE CALCUIATIONS         Specific Gravity Separator Gas         ty of Liquid Hydrocarbons       Gef / bbl.       Specific Gravity Separator Gas         ty of Liquid Hydrocarbons       Gef / bbl.       Specific Gravity Separator Gas         ty of Liquid Hydrocarbons       Gef / bbl.       Specific Gravity Flowing Fluid         Pw       P_2       F_2       F_2       Image: Colspan="2">Image: Colspan="2">Cal.       Pw         Pw       P_2       F_2       F_2       Image: Colspan="2">Cal.       Pw       F_2         Pt (psia)       Pt       F_2       F_2       (F_2Q) <sup>2</sup> Pw <sup>2</sup> P <sup>2</sup> _2 - P <sup>2</sup> _w       Cal.       Pw       Fw         765.2       469.5       585.5       585.5       585.2       658.2       666.2         646.2       331.2       585.5       585.5       658.2       666.2       670.1       1         Lute Potential:       3,150       MCFPD; n       501         Lute Potential:       3,150       MCFPD; n       501         Late Servise Oil Co.       ESS	╋										
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ANY KI Paso Natural Gas Co.		the second s		I Ges (	10.	<u> </u>					

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- Q = Actual rate of flow at end of flow period at W. H. working pressure (P<sub>W</sub>). MCF/da. @ 15.025 psia and 60° F.
- P<sub>c</sub>: 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater. psia
- P<sub>w</sub>: Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- Pt Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia

Pf Meter pressure, psia.

- hw Differential meter pressure, inches water.
- $F_g$ : Gravity correction factor.

 $F_t$  Flowing temperature correction factor.

F<sub>nv</sub> Supercompressability factor.

n \_ Slope of back pressure curve.

Note: If  $P_W$  cannot be taken because of manner of completion or condition of well, then  $P_W$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_t$ .