

## NEW MEXICO OIL CONSERVATION COMMISSION

Form C-122

Revised 12-1-55

## MULTI-POINT BACK PRESSURE TEST FOR GAS WELLS

Pool Eumont Formation Queen County Lea  
Initial X Annual \_\_\_\_\_ Special \_\_\_\_\_ Date of Test 5-7-58  
Company Humble Oil & Refining Lease J. L. Greenwood Well No. 5  
Unit I Sec. 9 Twp. 22-S Rge. 37-E Purchaser El Paso Natural Gas Co.  
Casing 7 Wt. 24.0 I.D. 6.336 Set at 3630 Perf. 3453 To 3516  
Tubing 2-1/2 Wt. 6.5 I.D. 2.441 Set at 3416 Perf. - To -  
Gas Pay: From 3453 To 3516 L 3416 xG 0.695 -GL 2374 Bar.Press. 39.2  
Producing Thru: Casing \_\_\_\_\_ Tubing X Type Well Single  
Single-Bradenhead-G. G. or G.O. Dual  
Date of Completion: 4-16-58 Packer 3416 Reservoir Temp. \_\_\_\_\_

## OBSERVED DATA

Tested Through (Prover) (Choke) (Meter)

Type Taps -

No.	Flow Data					Tubing Data		Casing Data		Duration of Flow Hr.
	(Prover) (Line) Size	(Choke) (Orifice) Size	Press. psig	Diff. h <sub>w</sub>	Temp. °F.	Press. psig	Temp. °F.	Press. psig	Temp. °F.	
SI						527	80			72
1.	2	1.250	28		84	496				3
2.	2	1.250	36		70	472				3
3.	2	1.250	67		58	363				3
4.	2	1.250	84		57	244				3
5.	No 24 hr. point									

## FLOW CALCULATIONS

No.	Coefficient (24-Hour)	$\sqrt{h_{wpf}}$	Pressure psia	Flow Temp. Factor F <sub>t</sub>	Gravity Factor F <sub>g</sub>	Compress. Factor F <sub>pv</sub>	Rate of Flow Q-MCFPD @ 15.025 psia
1.	35.6%		39.2	0.9777	0.9282	1.051	1131
2.	35.6%		49.2	0.9905	0.9282	1.051	1704
3.	35.6%		80.2	1.0019	0.9282	1.046	2766
4.	35.6%		97.2	1.0029	0.9282	1.032	3338
5.	Unable to secure 24 hour point due to location being too near residence.						

## PRESSURE CALCULATIONS

Gas Liquid Hydrocarbon Ratio \_\_\_\_\_ cf/bbl.  
Gravity of Liquid Hydrocarbons \_\_\_\_\_ deg.  
F<sub>c</sub> 3.844 (1-e<sup>-s</sup>) 0.151

Specific Gravity Separator Gas .695  
Specific Gravity Flowing Fluid \_\_\_\_\_  
P<sub>c</sub> 540.2 P<sub>c</sub> 291.82  
\*0.695 Assumed

No.	P <sub>w</sub> P <sub>t</sub> (psia)	P <sub>c</sub> <sup>2</sup>	F <sub>c</sub> Q	(F <sub>c</sub> Q) <sup>2</sup>	(F <sub>c</sub> Q) <sup>2</sup> (1-e <sup>-s</sup> )	P <sub>w</sub> <sup>2</sup>	P <sub>c</sub> <sup>2</sup> -P <sub>w</sub> <sup>2</sup>	Cal. P <sub>w</sub>	P <sub>w</sub> /P <sub>c</sub>
1.	509.2	259.3	6.43	41.34	6.634	263.94	25.9	535.7	.96
2.	487.2	237.4	10.00	100.00	15.100	250.50	41.3	500.5	.93
3.	376.2	141.5	16.34	267.00	40.317	141.82	110.0	428.6	.79
4.	277.2	76.8	19.56	382.59	57.772	134.57	157.2	344.9	.64
5.									

Absolute Potential: 4510 MCFPD; n .51COMPANY Humble Oil & Refining CompanyADDRESS Box 2347, Hobbs, New MexicoAGENT AND TITLE R. G. Jorlin District SuperintendentWITNESSED L. B. SouthernCOMPANY El Paso Natural Gas Co.

## REMARKS

JRM/mcb Orig & 1 cc: O. C. C., Santa Fe, N. M.  
cc: Mr. W. E. Hubbard  
Gas Division, Houston  
Mr. R. R. McCarty, Midland  
Mr. H. L. Mensley, Midland

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

$Q$  = Actual rate of flow at end of flow period at W. H. working pressure ( $P_w$ ).  
MCF/da. @ 15.025 psia and 60° F.

$P_c$  = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater.  
psia

$P_w$  = Static wellhead working pressure as determined at the end of flow period.  
(Casing if flowing thru tubing, tubing if flowing thru casing.) psia

$P_t$  = Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia

$P_f$  = Meter pressure, psia.

$h_w$  = Differential meter pressure, inches water.

$F_g$  = Gravity correction factor.

$F_t$  = Flowing temperature correction factor.

$F_{pv}$  = Supercompressability factor.

$n$  = Slope of back pressure curve.

Note: If  $P_w$  cannot be taken because of manner of completion or condition of well, then  $P_w$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_t$ .