

STATE OF NEW MEXICO

ENERGY AND MINERALS DEPARTMENT

OIL CONSERVATION DIVISION HOBBS DISTRICT OFFICE

GARREY CARRETHERS
GOVERNOR

Supervisor, District 1

/ed

8-28-89

POST OFFICE BUY 1980 HOBBS, NEW MEXICO 88(94), 1980 (505) 393-6161

DHC-741 OIL CONSERVATION DIVISION P. O. BOX 2088 SANTA FE, NEW MEXICO 87501 RE: Proposed: MC DHC NSL NSP SWD WFX **PMX** Gentlemen: I have examined the application for the: and my recommendations are as follows: Jerry Sexton

AMERADA HESS CORPORATION

Drawer "D"
Monument, New Mexico 88265

AUGUST 21, 1989

NEW MEXICO OIL CONSERVATION COMMISSION P.O. BOX 2088 SANTA FE, NEW MEXICO 87501

RE: E.W. WALDEN #2
REQUEST TO DOWNHOLE COMMINGLE
THE BLINEBRY AND DRINKARD GAS
ZONES

DEAR SIR;

AMERADA HESS CORPORATION IS REQUESTING APPROVAL FOR AN EXCEPTION TO RULE 303-C TO PERMIT DOWNHOLE COMMINGLING OF THE BLINEBRY AND DRINKARD GAS ZONES IN THE WELLBORE OF THE E.W. WALDEN #2. PRESENTLY THE BLINEBRY ZONE IS PRODUCING 1 BO AND 168 MCFPD AND THE DRINKARD ZONE IS CI DUE TO ZERO PRODUCTION. REPEATED SWABS IN THE DRINKARD ZONE HAVE PROVEN UNECONOMICAL TO CONTINUE DUE TO FLUID ENCROACHMENT. IF THIS APPLICATION IS APPROVED, BOTH GAS ZONES WILL BE TURNED TOGETHER AND PLACED ON SUCKER ROD PUMP SO AS TO APPLY A CONTINUOUS SWABBING ACTION IN THE WELLBORE AND PERMIT THE FLOW OF NATURAL GAS INTO THE WELLBORE FROM BOTH ZONES AT AN ECONOMICAL RATE.

IN THE WELLBORE, THE BLINEBRY ZONE IS PERFORATED FROM 5483' TO 5605' AND THE DRINKARD ZONE IS PERFORATED FROM 6262'-6376'. BOTTOM HOLE PRESSURES WERE CALCULATED WITH THE METHOD DOCUMENT-ED IN THE FOLLOWING ATTACHMENTS.
THE RESULTS OF THESE CALCULATIONS WERE:

BLINEBRY: 302 PSIA @ 5544', 24 HOUR SHUT IN DRINKARD" 356 PSIA @ 6319', 24 HOUR SHUT IN

ADJUSTED TO A COMMON DATUM

BLINEBRY: 308 PSIA @ 6319' DRINKARD: 356 PSIA @ 6319'

1 4

NO FORMATION PRECIPITATION WHICH MIGHT DAMAGE THE FORMATION IS ANTICIPATED BASED ON PREVIOUS EXPERIENCE. ASSUMING 200 MCFPD TOTAL PRODUCTION WITH 38 MCFPD ALLOCATED TO THE DRINKARD AND 162 MCFPD TO THE BLINEBRY, THE COMBINED STREAM VALUE OF \$262/DAY WOULD BE EQUAL TO THE TWO INDIVIDUAL STREAMS.

NO SECONDARY RECOVERY PROJECT INVOLVING THIS WELLBORE IS UNDER CONSIDERATION AT THIS TIME. IF FUTURE RECOVERY PROJECTS WERE TO BE CONSIDERED, NO PROBLEMS WITH THIS COMMINGLING PROSPECT JEOPARDIZING THE EFFICIENCY OF A SECONDARY RECOVERY OPERATION IS ANTICIPATED.

AMERADA HESS CORPORATION WILL BE THE OPERATOR OF THE SAID WELL ON UNIT K, 2009' FSL, 1911' FWL, SEC. 15, T-22S, R-37E, LEA COUNTY, NEW MEXICO. AMERADA HESS CORPORATION HAS COMMON OWNERSHIP OF BOTH ZONES WITH A WORKING INTEREST OF 100%, 1/8 ROYALTY AND NO OVERRIDING ROYALTY.

A PLAT OF THE AREA IS ATTACHED AT THE END OF THIS LETTER. A DIVISION FORM C-116 WHICH SHOWS THE PRODUCTION FROM THE BLINEBRY ZONE IS INCLUDED.

PRODUCTION DECLINE CURVES HAVE BEEN SUPPLIED FOR BOTH PRODUCING FORMATIONS. USING THESE RATES, A COMBINED RATE WAS CALCULATED AS 17.0%/YR.

OFFSET OPERATORS HAVE BEEN NOTIFIED OF THIS PROPOSAL BY A COPY OF THIS LETTER.

IF THERE ARE ANY QUESTIONS REGARDING THIS PROPOSAL, PLEASE CONTACT ME AT (505) 393-0087.

SINCERLY,

DENISE WARD-WANN

SENIOR PETROLEUM ENGINEER

BLINEBRY DECLINE RATE

$$qi = 2400 MCFPM$$

$$q = 2000 \text{ MCFPM}$$

 $t = 1 \text{ yr}$

$$a = \frac{1n}{2000}$$

$$a = .182$$

$$a = 18.2$$
%

DRINDARD DECLINE RATE

$$qi = 540 \text{ MCFPM}$$

 $q = 480 \text{ MCFPM}$

$$q = 480 MCFPM$$

$$t = 1 yr$$

$$a = 1n \frac{540}{480}$$

$$a = .118$$

$$a = 11.8$$
%

COMBINED DECLINE RATE

$$qi = 2940 MCFPM$$

$$q = 2480 \text{ MCFPM}$$

$$t = 1 yr$$

$$a = .170$$
 $a = 17.0%$

$$a = 17.0$$
%

ALLOCATION BASED ON DECLINE RATES

If: x = Blinebry
1-x = Drinkard

a = x(a) + (1-x)(a)c blinebry drinkard

.170 = x(.182) + 1-x(.118)

.170 = .182x + .118 - .118x

.170 - .182 = .182x - .118x

.052 = .064x

x = .052/.064

x = .812

1 - x = .188

¥ 5

Blinebry allocation = 81% Drinkard allocation = 19%

E.W. WALDEN #2

Blinebry Perfs - 5483'-5605' avg. depth $(\overline{L}) = 5544'$

Drinkard Perfs - 6262'-6376' avg. depth (\overline{L}) = 6319'

Blinebry = .694

G

Drinkard = .702

(

Assume Patm = 13.2 psia Assume temp. grad. = 0.4 F/100'

Assume avg. surface temp. = 74 degrees F

BHT = 74 F + 5544' (.4/100') = 96°F (Blinebry)

BHT = 74 F + 6319' (.4/100') = 99°F (Drinkard)

Pswh = 250 + 13.2 = 263.2 psia (Blinebry)

Pswh = 290 + 13.2 = 303.2 psia (Drinkard)

BLINEBRY ZONE

SBHP

c/:

Formula: Psfs = Pwhs e

$$Tpc = 388 R$$

$$Tr = \overline{T}_{.} = 545/388 = 1.40$$

TRIAL & ERROR METHOD

$$Pr = \overline{Ppc}$$

$$Pr = 282 psia/666 psia = 0.42$$

$$Tr = 1.40$$

$$z = .952$$

$$c/z$$
Psfs = Pwhs e .131/.952

Psfs = 263 e

Psfs = 302 psia

DRINKARD ZONE

$$\overline{T} = 74^{'} + 99^{'}$$
 $= \frac{74^{'} + 99^{'}}{2} + 460^{'} = 546^{'}R$

$$C = \frac{(.702)(6319)}{53.34(546)} = .152$$

$$Tpc = 390^{\circ} R$$

TRIAL & ERROR METHOD

$$Z = .945$$

$$c/z$$
 Psfs = Pwhs e

$$Psfs = 303 e$$

$$Psfs = 356 psia$$

BLINEBRY SBHP © 5544' = 302 psia DRINKARD SBHP © 6319' = 356 psia

Adjusted to a common datum @ 6319'
.: Blinebry zone SBHP needs to be adjusted 775'

$$\overline{T} = 96^{\circ} + 99^{\circ}$$
 $\frac{}{2} + 460^{\circ} = 557.5^{\circ} R$

Ppc = 666 psia

Tpc = 388° R

Tr = 557 $\frac{}{388} = 1.44$

$$C = (.694)(775) = .018$$

$$(53.34)(557)$$

TRIAL & ERROR METHOD

Assume: Psfs = 307 psia $\overline{P} = 307 + 302 = 304.5$

$$\frac{P}{Pr} = \frac{Ppc}{Ppc} = 304.5 \text{ psia/666 psia} = 0.46$$

Tr = 1.44

Fig. 16-4

$$Z = .96$$
 .018/.96

Psfs = 302 e

Psfs = 308 psia close to 307 psia

.: Psfs = 308 psia Blinebry adjusted to common datum of 6319'

BLINEBRY ZONE SBHP = 308 psia DRINKARD ZONE SBHP = 356 psia

E.W. WALDEN #2

GAS STREAM VALUES

Gas Price as of AUGUST 1989

Drinkard - \$1.31 /mcf Blinebry - \$1.31 /mcf

Assuming 200 mcfpd total production:

Drinkard production - (20 mcfpd)(\$1.31 mcf) = \$ 26.20 Blinebry production - (180 mcfpd)(\$1.31 mcf) = \$235.80

\$262.00 /day

Combined stream value = (200 mcfpd)(\$1.31 /mcf) = \$262.00 /day Values are equal.

RECEIVED

AUG 2 8 1969 OCD HOBBS OFFICE Anadarko Petroleum P.O. Box 2497 Midland, Texas 79702

Conoco, Inc. P.O. Box 460 Hobbs, New Mexico 88240

Exxon
P.O. Box 1600
Midland, Texas 79701

John Hendrix 222 W. Wall Suite 525 Midland, Texas 79701

Oryx Energy Co. P.O. Box 1861 Midland, Texas 79702

Presidio Exploration 3131 Turtle Creek Blvd. Suite 400 Dallas, Texas 75219

Sohio Petroleum Co. P.O. Box 4587 Houston, Texas 77210

Chevron
P.O. Box 670
Hobbs, New Mexico 88240

Dekalb Energy Company 800 Central Odessa, Texas 79761 Two States
P.O. Box 176
Eunice, New Mexico 88231

Wagner & Brown P.O. Box 1714 Midland, Texas 79702

Warrior P.O. Box 17479 Ft. Worth, Texas 76102

Aqua P.O. Box 1976 Hobbs, New Mexico 88240

Arch
777 Taylor Street
Suite II-A
Ft. Worth, Texas 76102

Meridian 21 Desta Drive Midland, Tesas 79705

New Mexico Oil Conservation Commission P.O. Box 1980 Hobbs, New Mexico

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Submit 2 copies to Appropriate Diametel Office. DISTRICT. II P.O. Drower DD, Amesia, NM 88210 DISTRICT. III DISTRICTLI P.O. Box 1980, Hobba, NM 88240

1000 Rio Brazos Rd., Azlec, NM 87410

State of New Mexico Energy, Minerals and Natural Resources Department

Form C-116 Revised 1/1/89

OIL CONSERVATION DIVISION

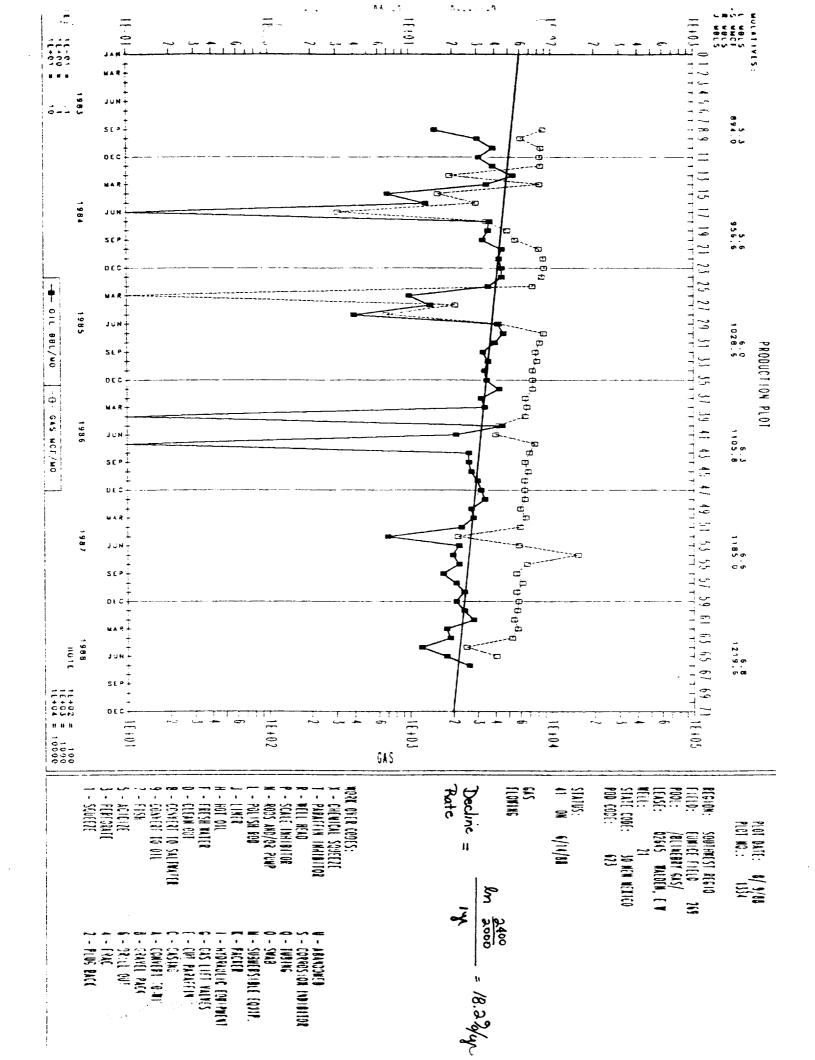
P.O. Box 2088 Santa Fe, New Mexico 87504-2088

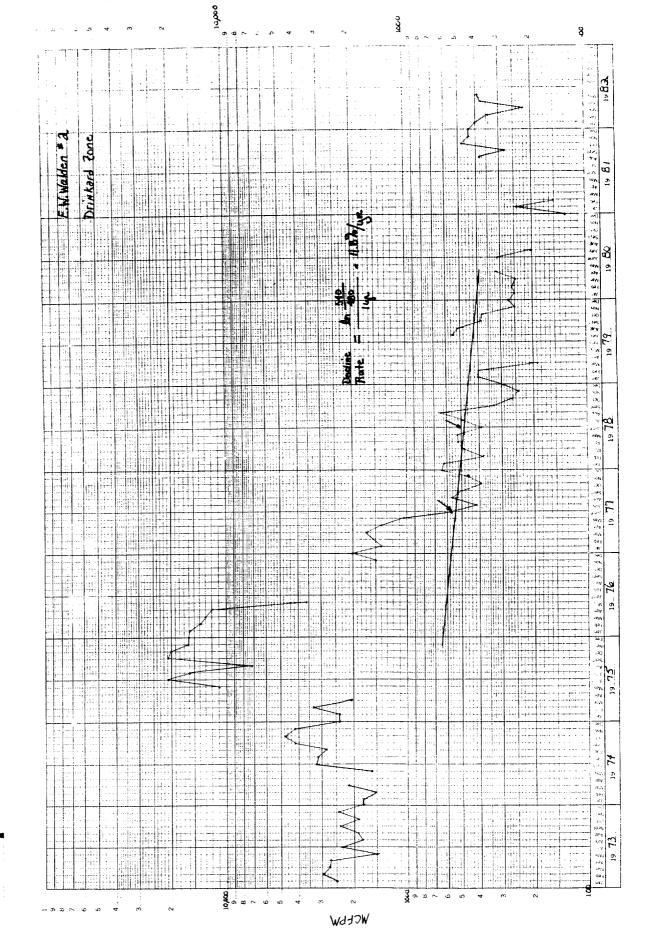
GAS - OIL RATIO TEST

		order that well can be assigned increased allowables when authorized by the Division.	During gas-oil ratio test, each well shall be produced at a rate not exceeding the top unit allowable for the	Instructions:	E.W. Walden	LEASE NAME		Address Drawer "D", Monument, NM	AMERADA HESS CORPORATION	Operator
		d allowab	I shall be p		2	8	¥E E	88265		
		ies whe	produce		~	c				
•	any w		datar		15	s	LOCATION			
•	all prod	rized b	ate not		22	4	Ş			
(ocing th	y the D	exceed to take		37	20			B1	
(rough casir	ivision.	ing the top		9-10-88	TEST	DATE OF		Blinebry Gas	Pool
(F6		unit all		'n	STA	TUS	TYPE OF TEST - (X)	as	
	•	temperati	lowable fo		2"	SIZE	CHOKE	<u>3</u> Ή		
		e of 60	or the pool in		55	PRESS.	TBG.	Scheduled		
Date		Sig		com h	GAS WELL	ABLE ALLOW-	DAILY	&		
3	Printed name and title August 23, 1989	Signature Denise Wann	JEMMJE.	ereby ce eplete to t	24	HOURS	OF OF	c		
	23, 19	Wann	, کم ایج	rtify tha	0	BBLS.	PA	Completion		0
	989	- Senior	ann	t the ab	1	OH V	PROD. DURING TEST		Lea	County
				ove info	1	BBLS.	NG TEST	(0		
Telen	(505)	Petroleum		I hereby certify that the above information complete to the best of my knowledge and belief.	194	MCF		Special		
Telephone No.) 393-2144	m Engineer		is true and f.	194,000	CU.FT/BBL	GAS-OIL			

Instructi

(See Rule 301, Rule 1116 & appropriate pool rules.)





JTHEAST NEW NEXTCO PACKER LEAD SE TEST

Cperator Amerada Hess Corp.			Lease		Well No. 2	
Location of Well	n Unit	Sec 15	Twp 22S	Rge 37E	County	Lea
DI NELL		servoir or Pool	Type of Prod (Oil or Gas)	Method of Prod Flow, Art Lift	Prod. Medium (Tbg or Csg)	
Upper Compl	Blinebry		Gas	Flow	Tbg.	2"
Lower Compl	Drinkard		Gas	Flow	Tbq.	2*

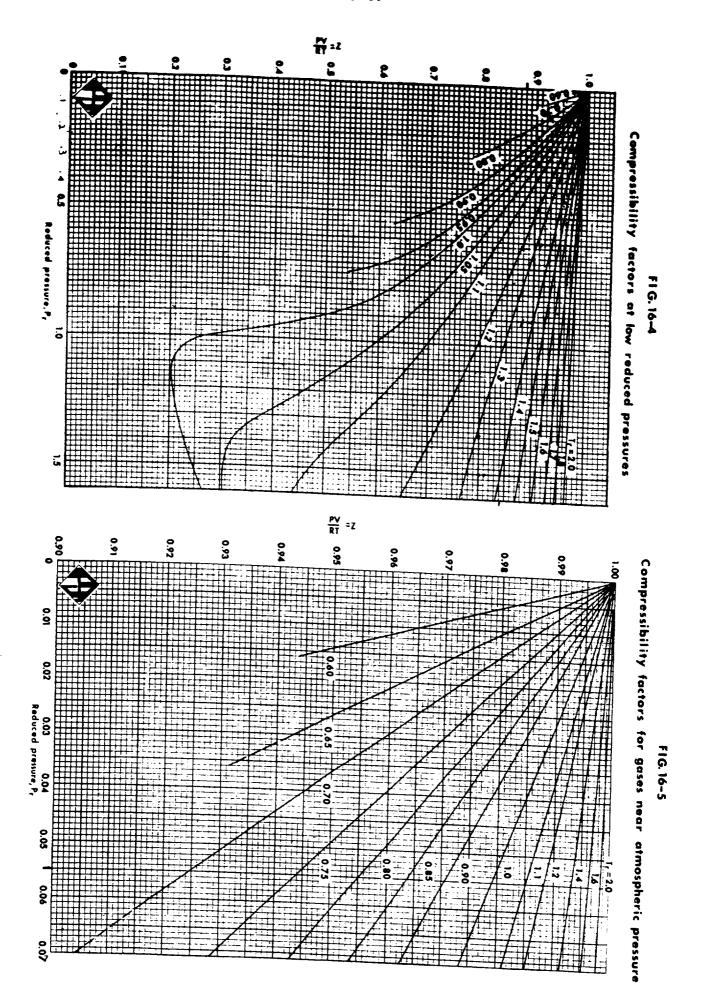
FLOW TEST NO. 1

Both zones shut-in at (hour, date): 9:00 A.M. 4-3-89 Well opened at (hour, date): 9:00 A.M. 4-4-89		Upper Completion	Lowe n Comple
Indicate by (X) the zone producing		x	_
Pressure at beginning of test			290
Stabilized? (Yes or No)			YES
Maximum pressure during test			290
Minimum pressure during test			290
Pressure at conclusion of test		E 0	290
Pressure change during test (Maximum minus Minimum)		222	
Was pressure change an increase or a decrease?			
Well closed at (hour, date): 9:00 A.M. 4-5-89	Total Time O	m	
Oil Production During Test: 1 bbls; Grav ; During Test_			
Remarks			
			••

FLOW TEST NO. 2

Unner

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vapors. For example for propane at 300 psia and 140°F., turn to the Mollier chart for propane, Fig. 17-6, locate the 300 psia and 140°F. point, and interpolate on the constant specific volume lines to obtain 0.33 cu ft/lb. Dividing this into 1 gives 3.03 lb/cu ft as the density, D_T. If the compressibility is required,

$$Z = \frac{MP}{10.73 TD_v}$$

Symbols have been defined previously. Then

$$Z = \frac{(44.09) (300)}{(10.73) (460+140) (3.03)} = 0.68$$

ACID GASES

Natural gases which contain H₂S and/or CO₂ frequently exhibit different compressibility factor behavior than do sweet gases. Wichert and Aziz (Gas Processing/Canada, pp 20-25, January February 1971; Hydrocarbon Processing, pp 119-122, May 1972) present a simple easy to use calculational procedure to account for these differences. The method uses the standard gas compressibility factor chart (Figure 16-3) and provides accurate sour gas compressibili-

ties for gas compositions that contain as much as 80% total acid gas.

Wichert and Aziz define a "Critical temperature adjustment factor" which is a function of the concentrations of CO_2 and H_2S in the sour gas. This correction factor is then used to adjust the pseudo critical temperature and pressure of the sour gases according to the equations:

$$T_c^{I} = T_c - \epsilon$$

$$P_c^{I} = \frac{P_c T_c^{I}}{[T_c + B (1-B) \epsilon]}$$

Where:

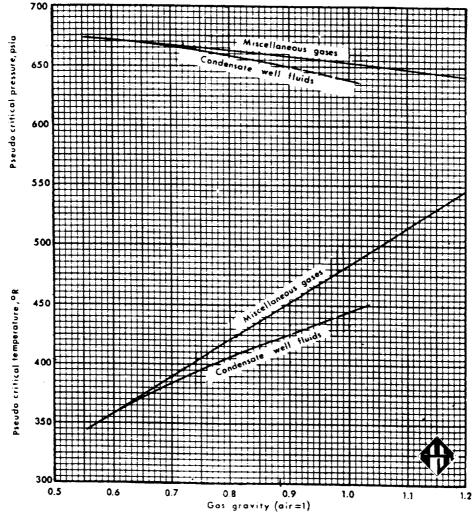
T_c = Mole Fraction average pseudo critical temperature

P_c = Mole Fraction average pseudo critical pressure

T_i = Pseudo critical temperature adjusted for acid gas composition

(Text cont'd. p. 16-15)

FIG.16-6
Pseudocritical properties of natural gases



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AUG 28 1989

OCD HOBBS OFFICE