

## NEW MEXICO OIL CONSERVATION COMMISSION

Form C-122

## MULTI-POINT BACK PRESSURE TEST FOR GAS WELLS

Revised 12-1-55

Pool Eumont Formation Musen County Lea  
Initial X Annual \_\_\_\_\_ Special \_\_\_\_\_ Date of Test 7-8/7-9-57  
Company Continental Oil Company Lease Elliott B-20 Well No. 1  
Unit E Sec. 20 Twp. 22 Rge. 37 Purchaser El Paso Natural Gas Co.  
Casing 5 1/2 Wt. 14.0 I.D. 5.012 Set at 3649 Perf. 3462 To 3601  
Tubing 2 Wt. 4.7 I.D. 1.995 Set at 3584 Perf. \_\_\_\_\_ To \_\_\_\_\_  
Gas Pay: From 3462 To 3601 L 3584 xG .693 -GL 2444 Bar.Press. 13.2  
Producing Thru: Casing \_\_\_\_\_ Tubing X Type Well Single  
Single-Bradenhead-G. G. or G.O. Dual  
Date of Completion: 7-6-57 Packer None Reservoir Temp. 90°

## OBSERVED DATA

Tested Through ORIFICE (3.000) (Meter) Type Taps Flange

Flow Data						Tubing Data		Casing Data		Duration of Flow Hr.
No.	(Line) Size	(Orifice) Size	Press. psig	Diff. h <sub>w</sub>	Temp. °F.	Press. psig	Temp. °F.	Press. psig	Temp. °F.	
SI						780				72 hr.
1.	6"	1.500	250	9	66	680				2
2.	6"	1.500	250	25	62	628				2
3.	6"	1.500	250	45	64	599				2
4.	6"	1.500	250	83	67	424				2
5.	6"	1.500	250	90	68	462				24

## FLOW CALCULATIONS

No.	Coefficient Flange (24-Hour)	$\sqrt{h_{wPF}}$	Pressure psia	Flow Temp. Factor F <sub>t</sub>	Gravity Factor F <sub>g</sub>	Compress. Factor F <sub>pv</sub>	Rate of Flow Q-MCFPD @ 15.025 psia
1.	13.99	78.98	693.2	0.9963	.9533	1.069	1,222
2.	13.99	126.61	641.2	0.9961	.9533	1.069	1,802
3.	13.99	160.47	572.2	0.9962	.9533	1.098	2,296
4.	13.99	190.49	437.2	0.9933	.9533	1.044	2,639
5.	13.99	154.16	475.2	0.9924	.9533	1.049	2,141

## PRESSURE CALCULATIONS

Gas Liquid Hydrocarbon Ratio 89,208 cf/bbl. on 5th Rate  
Gravity of Liquid Hydrocarbons 62 deg.  
F<sub>c</sub> 9.936 (1-e<sup>-s</sup>) .157  
Specific Gravity Separator Gas .660  
Specific Gravity Flowing Fluid .693  
P<sub>c</sub> 793.2 P<sub>c</sub> 629.2

No.	P <sub>t</sub> (psia)	P <sub>c</sub> <sup>2</sup>	F <sub>c</sub> Q	(F <sub>c</sub> Q) <sup>2</sup>	(F <sub>c</sub> Q) <sup>2</sup> (1-e <sup>-s</sup> )	P <sub>w</sub> <sup>2</sup>	P <sub>c</sub> <sup>2</sup> -P <sub>w</sub> <sup>2</sup>	Cal. P <sub>w</sub>	P <sub>w</sub> P <sub>c</sub>
1.	693.2	480.3	12.142	14.74	2.31	482.6	146.4	694.9	114.14
2.	641.2	411.1	17.995	32.38	4.75	415.8	213.4	644.8	123.01
3.	572.2	327.4	22.616	50.25	7.89	335.3	293.9	579.1	136.97
4.	437.2	191.1	26.161	68.84	10.76	201.9	427.3	449.3	176.54
5.	475.2	225.8	21.273	45.25	7.10	232.9	396.3	462.4	164.35

Absolute Potential: 3,900 MCFPD; n 1.000

COMPANY Continental Oil Company  
ADDRESS Box 66, Eureka, New Mexico

AGENT and TITLE J. B. Ketchum

WITNESSED \_\_\_\_\_

COMPANY \_\_\_\_\_

## REMARKS

Stabilization on each of first four rates obtained in two hours. Points would not line up due to fluid production. Slope of 1.000 drawn thru highest rate of flow.

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## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- $Q$  = Actual rate of flow at end of flow period at W. H. working pressure ( $P_w$ ).  
MCF/da. @ 15.025 psia and 60° F.
- $P_c$  = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater.  
psia
- $P_w$  = Static wellhead working pressure as determined at the end of flow period.  
(Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- $P_t$  = Flowing wellhead pressure (tubing if flowing through tubing, casing if  
flowing through casing.) psia
- $P_f$  = Meter pressure, psia.
- $h_w$  = Differential meter pressure, inches water.
- $F_g$  = Gravity correction factor.
- $F_t$  = Flowing temperature correction factor.
- $F_{pv}$  = Supercompressability factor.
- $n$  = Slope of back pressure curve.

Note: If  $P_w$  cannot be taken because of manner of completion or condition of well, then  $P_w$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_t$ .