

NEW MEXICO OIL CONSERVATION COMMISSION
MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122
 Revised 9-1-65

Type Test ☒ Initial ☐ Annual ☐ Special					Test Date April 15, 1977				
Company Phillips Petroleum Co.				Connection El Paso Natural Gas Company					
Pcol Tubb—Gas				Formation Tubb				Unit	
Completion Date		Total Depth		Plug Back TD		Elevation		Farm or Lease Name	
		7479		7437		3326		Sims	
Csg. Size	Wt.	d	Set At	Perforations:				Well No.	
	15.5	5-1/2	7478	From 5959 To 6167				7	
Tbg. Size	Wt.	d	Set At	Perforations:				Unit Sec. Twp. Rge.	
	4.7	2-3/8	6398	From 6415 To 7421				C 24 225 37E	
Type Well — Single — Bradenhead — G.G. or G.O. Multiple					Packer Set At		County		
dual completion					6335		Lea		
Producing Thru		Reservoir Temp. °F		Mean Annual Temp. °F		Baro. Press. — P _a		State	
annulus		102 @ 6000		60°		13.2		New Mexico	
L	H	Gg	% CO ₂	% N ₂	% H ₂ S	Prover	Meter Run	Taps	
5959	5959	.701	—	—	—	—	4"	Flange	

FLOW DATA						TUBING DATA		CASING DATA		Duration of Flow	
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.		Temp. °F
SI							packer		853	60	48 hr.
1.	4 x 1.25			22.8	16.0	68	packer		769	68	1 hr.
2.	4 x 1.25			31.7	27.0	70	packer		685	68	1 hr.
3.	4 x 1.50			41.6	57.8	74	packer		484	70	1 hr.
4.	4 x 1.50			35.8	49.0	78	packer		277	72	1 hr.
5.											

RATE OF FLOW CALCULATIONS							
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor F _g	Super Compress. Factor, F _{pv}	Rate of Flow Q, Mcfd
1	7.469	24.00	36.0	.9924	1.194	1.015	216
2	7.469	34.82	44.9	.9905	1.194	1.015	312
3	10.84	56.28	54.8	.9868	1.194	1.015	730
4	10.84	49.00	49.0	.9831	1.194	1.014	632
5							

NO.	P _t	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio — Mcf/bbl.	
1.	.05	528	1.35	.971	A.P.I. Gravity of Liquid Hydrocarbons — Deg.	
2.	.07	530	1.35	.971	Specific Gravity Separator Gas .701 X X X X X X X X	
3.	.08	534	1.36	.971	Specific Gravity Flowing Fluid X X X X X	
4.	.07	538	1.37	.972	Critical Pressure 668 P.S.I.A. — P.S.I.A.	
5.					Critical Temperature 392 R — R	

NO.	P _t ²	P _w	P _w ²	P _c ² - P _w ²
1	611.8	782.2	611.9	138.1
2	487.5	698.3	487.6	262.7
3	247.2	497.5	247.5	502.8
4	78.5	280.7	78.8	671.5
5				

$$(1) \frac{P_c^2}{P_c^2 - P_w^2} = 1.117$$

$$(2) \left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1.077$$

$$AOF = Q \left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 681$$

Absolute Open Flow	681	Mcfd @ 15.025	Angle of Slope @	56	Slope, n	1672
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Remarks: Calculation made by computer.

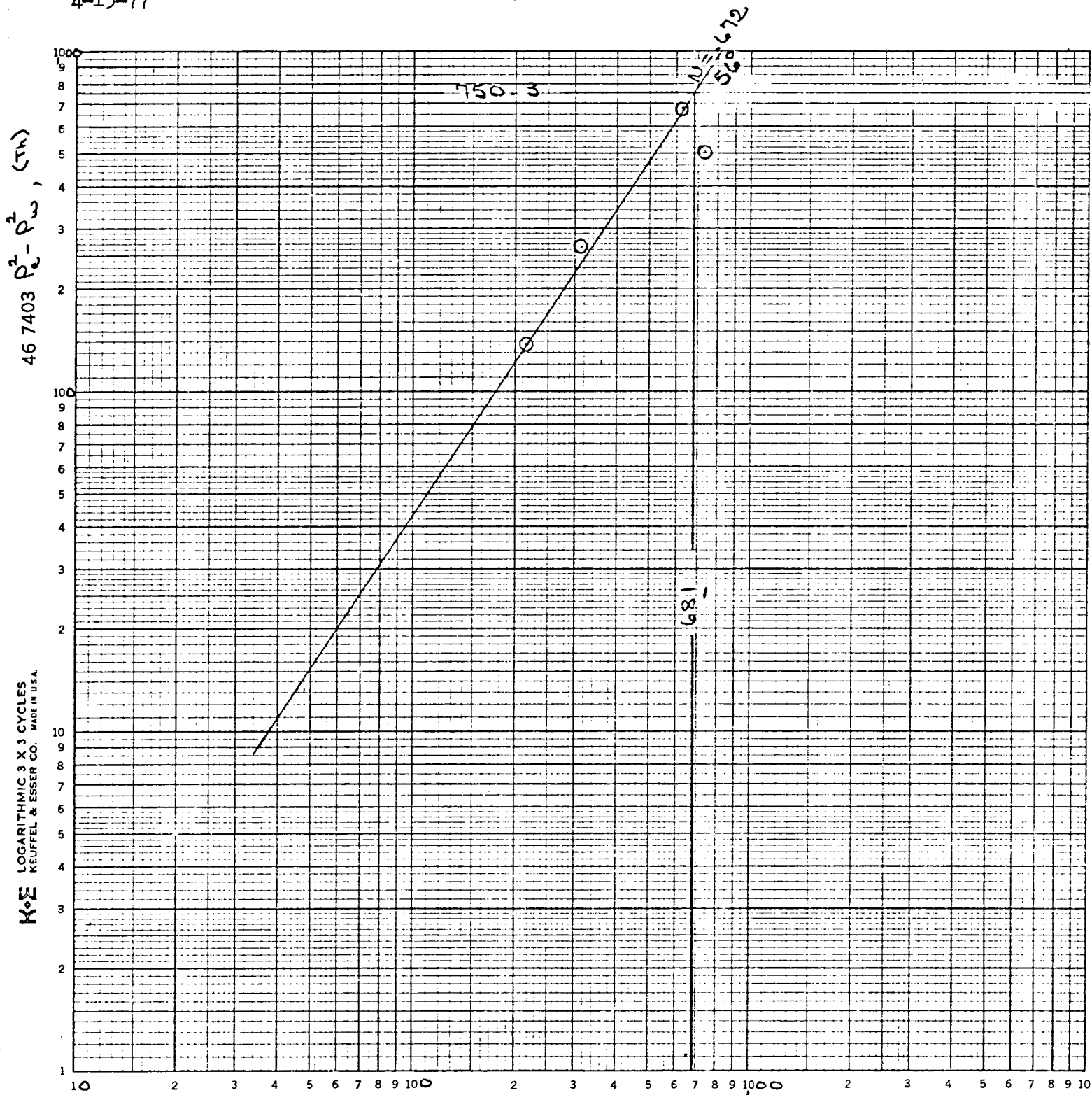
Approved By Commission:	Conducted By:	Calculated By:	Checked By:
	R. E. Lee	S. D. Justus	

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12-2-87

U.S. DEPARTMENT OF JUSTICE
FEDERAL BUREAU OF INVESTIGATION
WASHINGTON, D.C. 20535

Phillips Petroleum Company
 Sims No. 7
 Unit C, 24, 22-S, 37-E, Lea County
 Tubb-Gas
 4-15-77



Q, MCFD

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FEB 1977

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WASHINGTON, D.C. 20250