

## MULTI-POINT BACK PRESSURE TEST FOR GAS WELLS

Pool Jalmat Formation Yates County Lea  
Initial X Annual \_\_\_\_\_ Special \_\_\_\_\_ Date of Test 10-25-60  
Company Olsen Oils, Inc. Lease Meyers "B" Well No. 3  
Unit C Sec. 13 Twp. 24 Rge. 36 Purchaser None  
Casing 7 Wt. 23.0 I.D. \_\_\_\_\_ Set at 3704 Perf. 3002 To 3226  
2 joints 1 1/2" bottom  
Tubing 2 Wt. 4.7 I.D. \_\_\_\_\_ Set at 3256 Perf. \_\_\_\_\_ To \_\_\_\_\_  
This well has 2 strings of tbg.  
Gas Pay: From 3002 To 3226 L \_\_\_\_\_ xG \*.665 -GL \_\_\_\_\_ Bar.Press. 13.2  
Producing Thru: Casing \_\_\_\_\_ Tubing X Type Well G. O. Dual  
Single-Bradenhead-G. G. or G.O. Dual  
Date of Completion: 10-7-60 Packer 3570 Reservoir Temp. \_\_\_\_\_

## OBSERVED DATA

Tested Through (Prover) (~~Choke~~) (~~Meter~~) Type Taps Prover

| No. | Flow Data                  |                              |                |                         |              | Tubing Data    |              | Casing Data    |              | Duration of Flow Hr. |
|-----|----------------------------|------------------------------|----------------|-------------------------|--------------|----------------|--------------|----------------|--------------|----------------------|
|     | (Prover)<br>(Line)<br>Size | (Choke)<br>(Orifice)<br>Size | Press.<br>psig | Diff.<br>h <sub>w</sub> | Temp.<br>°F. | Press.<br>psig | Temp.<br>°F. | Press.<br>psig | Temp.<br>°F. |                      |
| SI  |                            |                              |                |                         |              | <u>454</u>     |              | <u>463</u>     |              | <u>48</u>            |
| 1.  | <u>2</u>                   | <u>.250</u>                  | <u>414</u>     |                         | <u>90</u>    | <u>416</u>     |              | <u>437</u>     |              | <u>3</u>             |
| 2.  | <u>2</u>                   | <u>.375</u>                  | <u>360</u>     |                         | <u>83</u>    | <u>365</u>     |              | <u>398</u>     |              | <u>3</u>             |
| 3.  | <u>2</u>                   | <u>.500</u>                  | <u>283</u>     |                         | <u>78</u>    | <u>289</u>     |              | <u>365</u>     |              | <u>1 1/2</u>         |
| 4.  | <u>2</u>                   | <u>.625</u>                  | <u>210</u>     |                         | <u>63</u>    | <u>228</u>     |              | <u>336</u>     |              | <u>3</u>             |
| 5.  | <u>2</u>                   | <u>.500</u>                  | <u>255</u>     |                         | <u>71</u>    | <u>260</u>     |              | <u>348</u>     |              | <u>24</u>            |

## FLOW CALCULATIONS

| No. | Coefficient<br><u>Prover</u><br>(24-Hour) | $\sqrt{h_w P_f}$ | Pressure<br>psia | Flow Temp.<br>Factor<br>F <sub>t</sub> | Gravity<br>Factor<br>F <sub>g</sub> | Compress.<br>Factor<br>F <sub>pv</sub> | Rate of Flow<br>Q-MCFPD<br>@ 15.025 psia |
|-----|---|------------------|------------------|--|-------------------------------------|--|--|
| 1.  | <u>1.4030</u>                             |                  | <u>427.2</u>     | <u>.9723</u>                           | <u>.9498</u>                        | <u>1.027</u>                           | <u>571.0</u>                             |
| 2.  | <u>3.0691</u>                             |                  | <u>373.2</u>     | <u>.9786</u>                           | <u>.9498</u>                        | <u>1.033</u>                           | <u>1,099</u>                             |
| 3.  | <u>5.5233</u>                             |                  | <u>296.2</u>     | <u>.9831</u>                           | <u>.9498</u>                        | <u>1.026</u>                           | <u>1,567</u>                             |
| 4.  | <u>8.3555</u>                             |                  | <u>223.2</u>     | <u>.9971</u>                           | <u>.9498</u>                        | <u>1.023</u>                           | <u>1,807</u>                             |
| 5.  | <u>5.5233</u>                             |                  | <u>268.2</u>     | <u>.9896</u>                           | <u>.9498</u>                        | <u>1.025</u>                           | <u>1,426</u>                             |

## PRESSURE CALCULATIONS

Gas Liquid Hydrocarbon Ratio None cf/bbl.  
Gravity of Liquid Hydrocarbons \_\_\_\_\_ deg.  
F<sub>c</sub> Measured (1-e<sup>-s</sup>) \_\_\_\_\_

Specific Gravity Separator Gas \_\_\_\_\_  
Specific Gravity Flowing Fluid \_\_\_\_\_  
P<sub>c</sub> 476.2 P<sub>c</sub><sup>2</sup> 226.8

| No. | $\frac{P_w}{P_t}$ (psia) | P <sub>t</sub> <sup>2</sup> | F <sub>c</sub> Q | (F <sub>c</sub> Q) <sup>2</sup> | (F <sub>c</sub> Q) <sup>2</sup><br>(1-e <sup>-s</sup> ) | F <sub>w</sub> <sup>2</sup> | P <sub>c</sub> <sup>2</sup> -P <sub>w</sub> <sup>2</sup> | Cal.<br>P <sub>w</sub> | $\frac{P_w}{P_c}$ |
|-----|--------------------------|-----------------------------|------------------|---------------------------------|---|-----------------------------|--|------------------------|-------------------|
| 1.  | <u>429.2</u>             | <u>184.2</u>                |                  |                                 |   | <u>202.7</u>                | <u>24.1</u>  | <u>450.2</u>           | <u>.94</u>        |
| 2.  | <u>378.2</u>             | <u>143.0</u>                |                  |                                 |   | <u>169.1</u>                | <u>57.7</u>  | <u>411.2</u>           | <u>.86</u>        |
| 3.  | <u>302.2</u>             | <u>91.3</u>                 | <u>MEASURED</u>  |                                 |   | <u>143.0</u>                | <u>83.8</u>  | <u>378.2</u>           | <u>.79</u>        |
| 4.  | <u>241.2</u>             | <u>58.2</u>                 |                  |                                 |   | <u>121.9</u>                | <u>104.9</u>   | <u>349.2</u>           | <u>.73</u>        |
| 5.  | <u>268.2</u>             | <u>71.9</u>                 |                  |                                 |   | <u>130.5</u>                | <u>96.3</u>  | <u>361.2</u>           | <u>.75</u>        |

Absolute Potential: 3,100 MCFPD; n .790

COMPANY Olsen Oils, Inc.

ADDRESS P. O. Box 691 - Jal, New Mexico

AGENT and TITLE Jack O. Whitling

WITNESSED Jack O. Whitling

COMPANY El Paso Natural Gas Company

REMARKS

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- $Q$  = Actual rate of flow at end of flow period at W. H. working pressure ( $P_w$ ).  
MCF/da. @ 15.025 psia and 60° F.
- $P_c$  = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater.  
psia
- $P_w$  = Static wellhead working pressure as determined at the end of flow period.  
(Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- $P_t$  = Flowing wellhead pressure (tubing if flowing through tubing, casing if  
flowing through casing.) psia
- $P_f$  = Meter pressure, psia.
- $h_w$  = Differential meter pressure, inches water.
- $F_g$  = Gravity correction factor.
- $F_t$  = Flowing temperature correction factor.
- $F_{pv}$  = Supercompressibility factor.
- $n$  = Slope of back pressure curve.

Note: If  $P_w$  cannot be taken because of manner of completion or condition of well, then  $P_w$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_t$ .