## MULTI-POINT BACK PRESSURE TEST FOR GAS WELLS

Revised 12-1-55

SI  1. 2 .375  2. 2 .375  3. 2 .500  4. 2 .625  5. 2 .500  Coefficient  Prover  (24-Hour)	psig hw	Lease Rge. 36 Set at: Set at: Tubing OFS	Meyer: Pu  3704  3256  X  70  ERVED DAT  Tubi Pres  1154  1116	Perf. 300 Perf. 300 Perf. GL Type Weingl -Brade Reserver A Temp. S. Temp.	Well One  Press.	To 322 To Bar.Pres O. Dual G. or G. s Prov	3 26 5s. 13.2 .0. Dual
Unit C Sec. 13 Twp.  Casing 7 Wt. 23.0 I.D 2 joints 12 Tubing 2 Wt. 1.7 I.D This well has 2 strings  Gas Pay: From 3002 Te 322  Producing Thru: Casing Date of Completion: 10-7-60  Tested Through (Prover) (Choke) Prover (Choke) Size Size In Size Size Size In Size Size Size In Size Size Size In Size Size Size Size Size Size Size Size	psig hw	Lease Rge. 36 Set at .  Set at .  Fubing OFS  Tem Cp 90 83 78 63	Meyer: Pu  3704  3256  xC *.66  X  70  ERVED DAT  154  116  365  289  228	Perf. 300 Perf. 300 Perf. GL Type Weingl -Brade Reserver A Temp. S. Temp.	Well  One  O2  ell G. Genhead-G.  oir Temp.  Type Tap    Casing D.    Press.    psig   163   137   398   365   365	To 322 To Bar.Pres O. Dual G. or G. s Prov	3 26 28. 13.2 29. O. Dual 20. Duration of Flow Hr. 20. 18. 3 3
Tubing 2 Wt. 4.7 I.D  This well has 2 strings  Gas Pay: From 3002 To 322  Producing Thru: Casing  Date of Completion: 10-7-60  Tested Through (Prover) (Choke) Prover) (Choke) Prover) (Choke) Prover) (Choke) Prover) (Choke) Size Size In 1. 2 .250 4. 2 .375 36 3. 2 .500 25 3. 2 .500 25 3. 2 .500 25 3. 2 .500 25 3. 2 .500 25 3. 3 .55233 4. 8.3555 5. 5.5233	of tbg. 26 L Pack  ORE) (Meter  a ress. Diff  psig h <sub>w</sub>	Set at  Set at  Fubing  OFS  OFS  7  90  83  78  63	3704 3256 X 70 ERVED DAT Tubi Pres Pres 154 116 365 289 228	Perf. 300 Perf	Type Tap    Casing D   Press.   psig   437   398   365	Bar.Pres  D. Dual  G. or G.  s Prov  ata  Temp.	Duration of Flow Hr.
Tubing 2 Wt. 4.7 I.D  This well has 2 strings  Gas Pay: From 3002 To 322  Producing Thru: Casing  Date of Completion: 10-7-60  Tested Through (Prover) (Choke)  No. (Line) (Orifice)  Size Size Prover  SI	of tbg. 26 L Pack ORE) (Meter a ress. Diff psig h <sub>w</sub>	Pubing  Rer 35  OES  Tem  Cp  90  83  78  63	X *.60 X 70 ERVED DAT Pres 1,16 365 289 228	Perf.  GGL  Type Weingl -Brade Reserve  A  ng Data s. Temp.	Type Tap  Casing D  Press.  psig  463  437  398  365	Bar.Pres  D. Dual  G. or G.  s Prov  ata  Temp.	Duration of Flow Hr.
Tubing 2 Wt. 4.7 I.D  This well has 2 strings  Gas Pay: From 3002 To 322  Producing Thru: Casing  Date of Completion: 10-7-60  Tested Through (Prover) (Choke)  No. (Time) (Orifice)  Size Size F  SI  1. 2 .250 41  2. 2 .375 30  3. 2 .500 28  4. 2 .625 21  5. 2 .500 25  Coefficient  No. (24-Hour)	of tbg. 26 L Pack ORE) (Meter a ress. Diff psig h <sub>w</sub>	Pubing  Rer 35  OES  Tem  Cp  90  83  78  63	X *.60 X 70 ERVED DAT Pres 1,16 365 289 228	Perf.  GGL  Type Weingl -Brade Reserve  A  ng Data s. Temp.	Type Tap  Casing D  Press.  psig  463  437  398  365	Bar.Pres  D. Dual  G. or G.  s Prov  ata  Temp.	Duration of Flow Hr.
Producing Thru:   Casing   Date of Completion:   10-7-60	Pack  OKE) (Meter  a ress. Diff  psig h <sub>w</sub> Ut  50  83	Fubing OFS  OFS  Tem  Cp  90  83  78  63	xC *.66  X  70  ERVED DAT  Tubi Pres  154 116 365 289 228	Type Weingl -Brade Reserve	Type Tap    Casing D   Press.   psig   437   398   365	Bar.Pres  D. Dual  G. or G.  s Prov  ata  Temp.	Duration of Flow Hr.
Producing Thru: Casing  Date of Completion: 10-7-60  Tested Through (Prover) (Choke)  No. (Prover) (Choke) Prover (Choke)  Size Size Size Prover (Choke)  Size Size Size Size Prover (Choke)  Size Size Size Size Size Size Size Size	Pack  OKE) (Meter  a  ress. Diff  psig h <sub>w</sub> 14  50  83	OES Tem C <sub>F</sub> 90 83 78 63	X 70 ERVED DAT Tubi p Pres poi 1454 116 365 289 228	Type Weingl -Brade Reserve  A ng Data S. Temp.	Type Tap    Casing D   Press.   psig   463   437   398   365	o. Dual G. or G. s Prov ata Temp.	Duration of Flow Hr.
Tested Through (Prover) (Choke)    No. (Prover) (Choke)   Prover) (Choke)   Prover	Packone (Meter a psig h <sub>w</sub>	OES  Tem	Tubi p Pres poll 1454 1416 265 289 228	Reserve	Type Tap    Casing D   Press.   psig   463   437   398   365	s Prov	Duration of Flow Hr.
Tested Through (Prover) (United)    No.   (Prover) (Choke)   Prover) (Orifice)   Size   Size   From Size   Size   Size   From Size   S	oke) (Meter a ress. Diff psig h <sub>w</sub>	OFS  Tem	Tubi Pres political p	ng Data s. Temp.	Type Tap Casing D Press. psig 437 398 365	s Prov	Duration of Flow Hr.
Plow Data   Prover   (Choke)   Prover   (Choke)   Prover   (Choke)   Prover   (Orifice)   Size   Prover   Pro	a ress. Diff psig h <sub>w</sub>	78 6. Tem 6. Tem 90 83 78 63	Tubi Pres . pol 454 116 365 289 228	ng Data s. Temp. S °P.	Casing D Press. psig 463 437 398 365	ata Temp.	Duration of Flow Hr.
Flow Data  (Prover) (Choke) Prover)  No. (Line) (Orifice) Size Size Prover  1. 2 .250 L1  2. 2 .375 36  3. 2 .500 28  4. 2 .625 21  5. 2 .500 25  No. Coefficient Prover  (24-Hour) \(\frac{1}{2}\) hwpf  1. 1.4030  2. 3.0691  3. 5.5233  4. 8.3555  5. 5.5233  Gas Liquid Hydrocarbon Ratio Cravity of Liquid Hydrocarbons	a ress. Diff psig h <sub>w</sub>	7. Tem  c <sub>F</sub> 90  83  78  63	p Pres . psi 454 116 365 289 228	s. Temp.	Casing D Press. psig 463 437 398 365	ata Temp.	Duration of Flow Hr.
No.   (Prover)   (Choke)   Prover   (Orifice)   Size   Size   Prover	ress. Diff psig h <sub>w</sub> LL  50  83	78 6. Tem 6 90 83 78 63	p Pres . psi 454 116 365 289 228	s. Temp.	Press.  psig 463 437 398 365	Temp.	of Flow Hr.
No. (Line) (Orifice) Size Size Size Size Size Size Size Size	psig h <sub>w</sub>	90 83 78 63	, poil l4514 l416 365 289 228	g o <sub>F</sub> ,	psig 463 437 398 365	{	of Flow Hr.
SI  1. 2 .375  2. 2 .375  3. 2 .500  4. 2 .625  5. 2 .500  Coefficient  Prover  (24-Hour)	11, 50 53 10	90 83 78 63	454 416 365 289 228		463 437 398 365		48 3 3
2. 2 .375 .36 3. 2 .500 .28 4. 2 .625 .21 5. 2 .500 .25  No. Coefficient Prover (24-Hour) \( \sqrt{h_wp_f} \) 1. 1.4030 .2. 3.0691 .3. 5.5233 .4. 8.3555 .5. 5.5233  Gas Liquid Hydrocarbon Ratio_Gravity of Liquid Hydrocarbons	50 83 10	83 78 63	365 289 228		398 365		3
4. 2 .500 25  5. 2 .500 25  No. Coefficient (24-Hour) \( \sqrt{h_wp_f} \)  1. 1.4030 2. 3.0691 3. 5.5233 4. 8.3555 5. 5.5233  Gas Liquid Hydrocarbon Ratio_Gravity of Liquid Hydrocarbons	83 LO	78 63	289 228		365		
4. 2 .625 21 5. 2 .500 25  No. Coefficient	LO	63	228			<del>├</del>	
Coefficient Prover  (24-Hour) \[ \bar{h_wp_f} \]  1. \[ \bar{1.4030} \]  2. \[ \bar{3.0691} \]  3. \[ \bar{5.5233} \]  4. \[ \bar{8.3555} \]  5. \[ \bar{5.5233} \]  Gas Liquid Hydrocarbon Ratio_ Gravity of Liquid Hydrocarbons			the same of the contract of the last		330	i I	<del></del>
No. Coefficient Prover  (24-Hour) √ h <sub>w</sub> p <sub>f</sub> 1. 1.4030  2. 3.0691  3. 5.5233  4. 8.3555  5. 5.5233  das Liquid Hydrocarbon Ratio_ Fravity of Liquid Hydrocarbons			1 200		348	<del>  </del>	2),
Gas Liquid Hydrocarbon Ratio_ Gravity of Liquid Hydrocarbons	- psia		Factor Ft	Fg	Facto F <sub>pv</sub>	r	Rate of Flow Q-MCFPD 15.025 psia
as Liquid Hydrocarbon Ratio_ Fravity of Liquid Hydrocarbons	427.2		723	•9498	1.03		574.0
as Liquid Hydrocarbon Ratio_ ravity of Liquid Hydrocarbons	373.2 296.2		9786 9831	•9498 •9498	1.033		1,099 1,567
as Liquid Hydrocarbon Ratio_ Gravity of Liquid Hydrocarbons	223.2	• 3	9831 9971	•9498	1.023		1.807
as Liquid Hydrocarbon Ratio_ Fravity of Liquid Hydrocarbons	268.2		9896	9498	1.02		1 1/26 / 1/2 1
	None	PRESSUR cf/b d		Sn <b>ec</b> i Speci	fic Gravi ific Gravi <b>76.2</b>	ty_Flowi	ing Fluid
No. $P_{t}$ $P_{t}^{2}$ $F_{c}^{2}$	(F <sub>c</sub> Q)	)2	$(F_cQ)^2$ $(1-\epsilon^{-s})$	P <sub>w</sub> 2	$P_c^2 - P_w^2$	Cal P <sub>v</sub>	P <sub>C</sub>
1. 429.2 134.2				202.7	24.1	150.2	
2. 378.2 113.0 3. 302.2 91.3	30040	102 270		169.1 143.0	57.7 83.8	378.2	
4. 241.2 58.2	THAS	OWEN		121.9	101.9	31.9.2	
5. 268.2 71.9			<del> </del>	130.5	96.3	361.2	
Absolute Potential: 3,100  COMPANY Olsen Oils, Inc.  ADDRESS P. O. Box 691 - Jal  AGENT and TITLE  WITNESSED Jack 0 Whitling  COMPANY El Paso Natural G				•790			

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- Q I Actual rate of flow at end of flow period at W. H. working pressure (Pw). MCF/da. @ 15.025 psia and 600 F.
- P<sub>c</sub>= 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater. psia
- Pw. Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- Pt Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- Pf Meter pressure, psia.
- hw Differential meter pressure, inches water.
- Fg Gravity correction factor.
- $F_t$  Flowing temperature correction factor.
- $F_{nv}$  Supercompressability factor.
- n I Slope of back pressure curve.

Note: If  $P_{\mathbf{W}}$  cannot be taken because of manner of completion or condition of well, then  $P_{\mathbf{W}}$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_{+}$ .