

OIL CONSERVATION DIVISION

P.O. Box 2088

Santa Fe, New Mexico 87504-2088

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Operator						Lease or Unit Name JACKSON Unit					
Test Type ☐ Initial ☐ Annual ☐ Special						Test Date 12-21-99			Well No. 7		
Completion Date			Total Depth 13600			Plug Back TD 13600			Elevation		
Casing Size 7.000			WT. 29.000			d 6.340			Set At 13600		
Tbg. Size 3.500			WT. 8.700			d 2.995			Set At 13210		
Type Well-Single-Bradshaw-GLG or G.O. Multiple						Packer Set At			Formation Wolfcamp		
Producing thru tubing			Reservoir Temp. F 187			Mean Annual Temp. F 38			Baro. Pressure 13.30		
I. 13600		II. 13600		Gg. .677		% CO ₂ 1.51		% N ₂ .90		% H ₂ S	
								Prover meter		Meter Run 4.026	
										Taps flange	

Flow Data				Tubing Data		Casing Data		SIP/Flow Duration (HRS.)
No.	(Prover) Line Size x Orifice Size	Press. PSIG	Diff. h _w	Temp. F	Press. PSIG	Temp. F	Press. PSIG	
Shut-in Pressure					2134	45		
1.	4.03 x 2.25	262.30	5.80	51	2026	56		1
2.	4.03 x 2.25	269.80	13.50	48	1971	53		1
3.	4.03 x 2.25	291.00	29.20	62	1816	67		1
4.	4.03 x 2.25	344.00	64.10	50	1656	56		1

RATE OF FLOW CALCULATIONS

No.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. FACTOR P _L	Gravity FACTOR P _g	Super Compress. FACTOR P _{pv}	Rate of Flow (Q) MCFD
1.	31.150	39.981	275.6	1.0088	1.2154	1.0295	1572.0
2.	31.150	61.821	283.1	1.0117	1.2154	1.0310	2441.4
3.	31.150	94.263	304.3	.9981	1.2154	1.0304	3670.2
4.	31.150	151.337	357.3	1.0098	1.2154	1.0392	6012.2

No.	P _f	TEMP.	T _f	Z
1.	.409	511	1.355	.9434
2.	.421	508	1.347	.9407
3.	.452	522	1.384	.9418
4.	.531	510	1.352	.9260

Gas-Liquid Hydrocarbon Ratio	21.0	Mc/Dbbl
API Gravity of Liquid Hydrocarbons	52.0	Deg.
Specific Gravity Separator Gas	.677	
Specific Gravity Flowing Fluid	.817	
Critical Pressure	673 PSIA	666 PSIA
Critical Temperature	377 R	421 R

P _C	2147.3	P _C ²	4610.9
No.	P _w	P _w ²	P _C ² - P _w ²
1.	2043.4	4175	435.612
2.	1993.7	3974	636.123
3.	1853.0	3433	1177.278
4.	1735.0	3010	1600.649

$$(1) \frac{P_C^2}{P_C^2 - P_W^2} = \frac{2.881}{17066}$$

$$(2) \left[\frac{P_C^2}{P_C^2 - P_W^2} \right]^n = \frac{2.839}{17066}$$

$$AOF = Q \left[\frac{P_C^2}{P_C^2 - P_W^2} \right]^n = 17066$$

Absolute Open Flow	17066	Mcf/d @ 15.025	Angle of Slope -	45.4	Slope, n	.986
Remarks						
Approved By Division:		Conducted By: LARRY RACKLEY		Calculated By: BPT System/Guardian		Checked By: <i>Larry Rackley</i>

GAS WELL BACK PRESSURE CURVE

WELL TESTER: LARRY RACKLEY

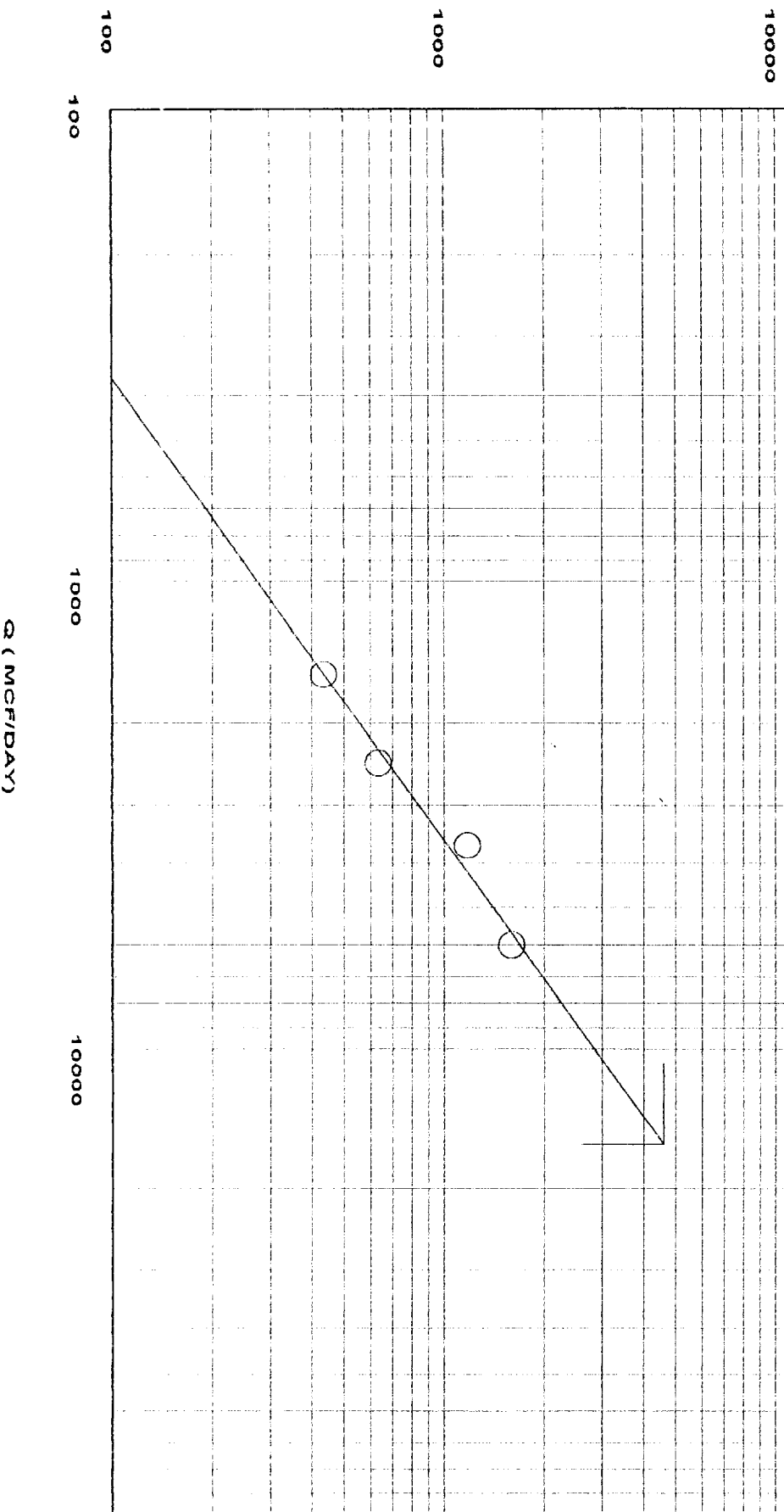
TEST DATE: 12-21-99

JACKSON 7

LEA

, NM.

Exponent n: 0.9861



MITCHELL ANALYTICAL LABORATORY

2638 Faudree
Odessa, Texas 79765-8538
561-5579

Gas Analysis

Company.... Guardian
Producer...
Lease..... **JACKSON #7**
Station #.. **MURCHISON**
Cylinder #.
Date Run... 12/23/1999
Lab Ref #.. 99-DEC-G8650

Sample Press... 566.0
Sample Temp... 45.0
Date Sampled.. 12/12/1999
Sampled by.... **LARRY RACKLEY**
Field Gravity.. 0.0000
Analyzed by... **DANIEL**
Field H2S..... 0.0000

Physical Constants per GPA 2145-93
Calculations per GPA 2172-86
@ 14.65 psia & 60.0 Deg. F.

	MOL %	GPM (Ideal)	BTU (Ideal Dry)
Nitrogen	0.902	0.098	0.0
Methane	83.234	14.033	838.0
CO2	1.515	0.254	0.0
Ethane	9.508	2.528	167.7
H2S	0.000	0.000	0.0
Propane	3.149	0.862	79.0
Iso-Butane	0.433	0.141	14.1
N-Butane	0.688	0.216	22.4
Iso-Pentane	0.161	0.059	6.4
N-Pentane	0.149	0.054	6.0
2,2-DMB	0.000	0.000	0.0
2-Me-C5	0.000	0.000	0.0
3-Me-C5	0.000	0.000	0.0
Hexanes +	0.261	0.111	12.4
TOTALS	100.000	18.355	1145.9

GROSS HEATING VALUE @ 14.65 PSIA

GASOLINE CONTENT (GPM/Real)

Dry	Wet	
1149	1130	BTU/Real Cu.Ft.
0.6771	0.6764	Specific Gravity (Real)
1146	1127	BTU/Ideal Cu.Ft.
0.6753	0.6744	Specific Gravity (Ideal)

Ethane & Heavier	3.982
Propane & Heavier ...	1.446
Butane & Heavier	0.581
Pentane & Heavier ...	0.224

Z Factor : 0.9970