

ILLEGIBLE

HOBBBS OFFICE OCC

Form C-122  
Revised 12-1-55

PRESSURE TEST FOR GAS WELLS

APR 1 PM 1:07

Pool JANET Formation Texas County Law  
Initial Annual Special X Date of Test 2-25-57  
Company Hamble Oil & Refining Co. Lease Lanshart Well No. 1  
Unit X Sec. 22 Twp. 25S Rge. 37E Purchaser Hamble  
Casing 5/8 Wt. 17 I.D. 4.092 Set at 3250 Perf. 3035 To 3100  
Tubing 2 Wt. 4.7 I.D. 1.995 Set at 3056 Perf. 3033 To 3055  
Gas Pay: From 3035 To 3100 L 3056 xG 0.465 -GL 2000 Bar. Press. 13.2  
Producing Thru: Casing Tubing Type Well Single  
Single-Bradenhead-G. or G.O. Dual  
Date of Completion: June, 1956 Packer None Reservoir Temp.

## OBSERVED DATA

Tested Through (Prover) (Choke) (Meter)

Type Taps Flange

No.	Flow Data					Tubing Data		Casing Data		Duration of Flow Hr.
	(Prover) (Line) Size	(Choke) (Orifice) Size	Press. psig	Diff. h <sub>w</sub>	Temp. °F.	Press. psig	Temp. °F.	Press. psig	Temp. °F.	
SI										72
1.		1.000	239	17.6	61	134				24
2.		1.000	225	30.9	70	145				24
3.		1.000	212	42.9	96	200				24
4.		1.000	222	56.9	60	352				24
5.		1.000								

## FLOW CALCULATIONS

No.	Coefficient (24-Hour)	$\sqrt{h_{wpf}}$	Pressure psia	Flow Temp. Factor F <sub>t</sub>	Gravity Factor F <sub>g</sub>	Compress. Factor F <sub>pv</sub>	Rate of Flow Q-MCFPD @ 15.025 psia
1.	6.139	64.42	232.2	0.9990	0.9400	1.005	397
2.	6.139	84.96	232.2	1.0029	0.9400	1.005	500
3.	6.139	97.80	232.2	1.0009	0.9400	1.004	585
4.	6.139	117.07	232.2	1.0000	0.9400	1.004	687
5.							

## PRESSURE CALCULATIONS

Gas Liquid Hydrocarbon Ratio dry cf/bbl.  
Gravity of Liquid Hydrocarbons deg.  
F<sub>c</sub> 9.936 (1-e<sup>-s</sup>) 0.130

Specific Gravity Separator Gas   
Specific Gravity Flowing Fluid   
P<sub>c</sub> 21.2 P<sub>c</sub> 261.3

No.	$\frac{P_w}{P_t}$ (psia)	P <sub>t</sub> <sup>2</sup>	F <sub>c</sub> Q	(F <sub>c</sub> Q) <sup>2</sup>	$\frac{(F_c Q)^2}{(1-e^{-s})}$	P <sub>w</sub> <sup>2</sup>	P <sub>c</sub> <sup>2</sup> -P <sub>w</sub> <sup>2</sup>	Cal. P <sub>w</sub>	$\frac{P_w}{P_c}$
1.	447.2	199.9	3.94	15.52	2.02	200.9	59.4	447.2	0.979
2.	418.2	174.9	5.09	25.90	3.32	176.2	88.1	418.2	0.980
3.	398.2	158.6	5.81	33.75	4.39	163.0	95.3	403.0	0.989
4.	365.2	133.4	6.02	36.21	6.09	139.9	121.0	373.5	0.730
5.									

Absolute Potential: 1255 MCFPD; n 0.700

COMPANY Hamble Oil & Refining Co.  
ADDRESS Box 2347, Dallas, Texas  
AGENT and TITLE W. H. H. H. H.

WITNESSED None  
COMPANY El Paso Natural Gas Co.

REMARKS

E. A. UZ  
ENGINEER

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- $Q$  = Actual rate of flow at end of flow period at W. H. working pressure ( $P_w$ ).  
MCF/da. @ 15.025 psia and 60° F.
- $P_c$  = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater.  
psia
- $P_w$  = Static wellhead working pressure as determined at the end of flow period.  
(Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- $P_t$  = Flowing wellhead pressure (tubing if flowing through tubing, casing if  
flowing through casing.) psia
- $P_f$  = Meter pressure, psia.
- $h_w$  = Differential meter pressure, inches water.
- $F_g$  = Gravity correction factor.
- $F_t$  = Flowing temperature correction factor.
- $F_{pv}$  = Supercompressibility factor.
- $n$  = Slope of back pressure curve.

Note: If  $P_w$  cannot be taken because of manner of completion or condition of well, then  $P_w$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_t$ .