Tubing Data Casing Data Duration of Flow Casing Data Casing Data Duration Casing Data Casing Data Duration Casing Data Durat								SURE TEST		•				
Company Identity Oil Compuny Lease A, B, Coates C														
Company Identity Oil Compuny Lease A, B, Coates C	Initial Annual					Special			Date of Test <u>6-3 to 6-7-57</u>					
Casing 7	Compa	ny	idew	ger 011	Company	I	ease_A	B. Coat	es "C"	Wel	1 No. 1	_ Ug	g	
Tubing 2 Mt. 1, 7 1.P. Set at 3267 Perf. To Gas Pay: From 2950 To 3300 L 2950 MG 0.65 CL 1962 Bar. Press. 13,2 Producing Thru: Casing X Tubing Type Well G G Dual Bate of Completion: 2-3-51 Packer 1600 Single-Bradenhead-G. G. or G.O. Dual Bate of Completion: 2-3-51 Packer 1600 Single-Bradenhead-G. G. or G.O. Dual Tested Through (Freese) (State) (Meter) Type Taps 1 Inng Tubing Data Casing Data Type Taps 1 Inng To Tubing Data Casing Data To Flow Data To Freese Temp. Press. Temp. Press. Temp. Of Flow of Flow Size Size Size psig hw GP. psig	Unit	F	Sec	. 24	[wp	258_Rge	· 371	Purch	aser	.PNG				
Case From 2950 To 3300 L 2950 xG 0.266 CL 1962 Bar.Press. 13.2	Casin	ig	Wt.	20	I.D	Set	at_ 29	50 Per	·f•		То			
Case From 2950 To 3300 L 2950 xG 0.266 CL 1962 Bar.Press. 13.2														
Tubing														
Total Trough Type Taps Flange Tubing Data Casing Data Duration of Flow Chine C	Producing Thru: Casing X Tubing Type Well G G Dual Single Bradenhead G G or GoO Dual													
Tested Through (French) (Meter) Type Taps Flange Flow Data Tubing Data Casing Data Of Flow Inc. (Line) (Orifice) press. Diff. Temp. Press. Temp. Press. Temp. Of Flow Size Size psig hw OF, psig OF, psig OF, Hr. SI	Date													
Flow Data Tubing Data Casing Data Casing Data	OBSERVED DATA													
No. (1)	Tested Through (Shake) (Meter) Type Taps rlange											nge		
No. (Line) Size Size psig hw OF. psig OF. psig OF. hr. Size Size psig hw OF. psig OF. psig OF. hr. Size Size psig hw OF. psig OF. psig OF. hr. Size Size psig hw OF. psig OF. psig OF. hr. Size Size psig hw OF. psig OF. hr. Size Size psig Size Size Size Size Size Size Size Size	~			Flow	Data)ata	1	D -1:	
No. Coefficient Pressure Flow Temp. Factor Fa	$\neg \top$	(574)	144)	(*****)	Press	Diff.	Temp.	Press.	Temp.	Press.	Temp.		of Flow	
SI	No.			(Orifice) Size) psig	h _w	$\circ_{\mathtt{F}}$.	psig	°F.	psig	°F∙		1	
1. 1	ST													
1	1.	4	4 0.75		247	4.00	66_				 			
Second S	2.	4	4 0.750		258	9.00	70					+		
FLOW CALCULATIONS Pressure Flow Temp. Gravity Factor F	<u>3. </u>	4				26.01					1	1		
No. Coefficient Pressure Flow Temp. Fractor Factor F	40	4		0.150	202	20,02	1					<u> </u>		
Coefficient														
No. (24-Hour) V hwpf psia Factor Factor Fg February 24-Holl		Coo	fficie	ient		ressure	Flow CAI	Temp.	Gravity	Compress.		Rate of Flow		
C24-Hour V hwpf psia Ft Fg Fpv 913-02) psia	i i		illicient _			1 obb ar o	Fact		Factor	ractor		Q-MCTD		
1. 3.435 32.25 260 .9913 .9188 1.025 107 2. 3.135 19.39 271 .9915 .9186 1.026 165 3. 3.135 63.96 269 .9905 .9188 1.025 212 4. 3.135 81.73 276 .9868 .9198 1.026 280 PRESSURE CALCULATIONS Bas Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity Flowing Fluid Fc 0.707 (1-e-S) 0.126 Pc 190.2 Pc 21083 No. Pt (psia) Pt Fc Q (FcQ) (FcQ) Pw 2 Pc-Pw Fc Pw Pw Fc Pw Pw Fc Pw Fc Pw Fc Pw Pw Fc Pw Fc Pw Fc Pw Pw Fc Pw Fc Pw Pw Fc Pw Pw Fc Pw Fc Pw Pw Pw Fc Pw	1100			$\sqrt{h_{\rm w}p_{\rm f}}$		psia	F	t	$^{\mathtt{F}}\mathtt{g}_{-}$	Fpv	Fp v		@ 15.025 psia	
3. 135 63.96 269 .9905 .9108 1.026 280 PRESSURE CALCULATIONS PRESS	7	3.1.35							•9498					
3. 135 63.96 269 .9905 .9108 1.026 280 PRESSURE CALCULATIONS PRESS	2.					271	.991	5						
PRESSURE CALCULATIONS Gas Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas	3.	3.435		6	3.96				9118	1.02				
PRESSURE CALCULATIONS Gas Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas	4.	3.435		8	4.73	276	.986	8	.91198	1.020	2	200		
No. Pt (psia) Pt Fc (Fc Q) (Fc Q) Pw Pc Pv Pc Pv Pv Pv Pv Pv	PRESSURE CALCULATIONS													
No. Pt (psia) Pt	Gas Liquid Hydrocarbon Ratio					CI/DDL.			Specific Gravity Flowing Fluid					
No. Pt (psia) Pt (psi	F 0.707 (1-e-8				(1-e ⁻⁵)) 0.126			P. 190.2 Pc 21.083					
No. Pt (psia) 1. 121.2 179.9 0.016 0.006 0.000 179.9 50.4 13.0 0.027 2. 399.2 159.4 0.120 0.014 0.002 159.4 80.9 12.6 0.026 3. 379.2 113.8 0.150 0.023 0.003 113.8 96.5 12.1 0.025 4. 359.2 127.6 0.200 0.010 0.005 127.6 112.7 11.3 0.023 5. Absolute Potential: 590 MCFPD; n 1.000 COMPANY Tidewater 011 Company ADDRESS Box 51.7 Hobbs, New Mexico AGENT and TITLE in P. Shackelford, Area Supt. WITNESSED Earl Smith COMPANY E1 Pago Natural Gas Co.	C VOID C													
No. Pt (psia) 1. 121.2 179.9 0.016 0.006 0.000 179.9 50.4 13.0 0.027 2. 399.2 159.4 0.120 0.014 0.002 159.4 80.9 12.6 0.026 3. 379.2 113.8 0.150 0.023 0.003 113.8 96.5 12.1 0.025 4. 359.2 127.6 0.200 0.010 0.005 127.6 112.7 11.3 0.023 5. Absolute Potential: 590 MCFPD; n 1.000 COMPANY Tidewater 011 Company ADDRESS Box 51.7 Hobbs, New Mexico AGENT and TITLE in P. Shackelford, Area Supt. WITNESSED Earl Smith COMPANY E1 Pago Natural Gas Co.	- 	F /.						. 2		-2 -2	,		D	
Pt (ps1a)	No.			$P_{\mathbf{t}}^{2}$	F_c^Q	(F _c Q) ²	· (F _c Q)~	P_{w}^{2}	Pc-Pw	i (P _C	
1. 121.2 17.5 0.120 0.011 0.002 159.1 80.9 12.6 0.026				170 0	0.076	0.006			179.9	60.4		0	0.027	
3. 379.2 113.8 0.150 0.023 0.003 113.6 90.5 124. 4. 359.2 127.6 0.200 0.010 0.005 127.6 112.7 11.3 0.023 Absolute Potential: 590 MCFPD; n 1.000 COMPANY Tidewater Oil Company ADDRESS Box 517 Hobbs, New Mexico AGENT and TITLE in P. Shackelford, Area Supt. WITNESSED Earl Smith COMPANY El Pago Natural Gas Co.	1 ± 1	300	22	159.1					159.4	80.9				
4. 359.2 127.6 0.200 0.010 0.005 127.6 112.7 11.3 5.023 Absolute Potential: 590 MCFPD; n 1.000 COMPANY Tidewater Oil Company ADDRESS Box 517 Hobbs, New Mexico AGENT and TITLE in P. Shackelford, Area Supt. WITNESSED Earl Smith COMPANY El Pago Natural Gas Co.	3.				0.150	0.023	· (
Absolute Potential: 590 MCFPD; n 1.000 COMPANY Tidewater Oil Company ADDRESS Box 517 Hobbs, New Mexico AGENT and TITLE ii. P. Shackelford, Area Supt. WITNESSED Earl Smith COMPANY El Paso Natural Gas Co.	4.					0.010		0.005	127.6	112.7		2	U.U.S	
COMPANY Tidewater Oil Company ADDRESS Box 517 Hobbs, New Mexico AGENT and TITLE ii. P. Shackelford, Area Supt. WITNESSED Earl Smith COMPANY El Pago Natural Gas Co.					<u> </u>								<u></u>	
ADDRESS Box 517 Hobbs, New Mexico AGENT and TITLE ii. P. Shackelford, Area Supt. WITNESSED Earl Smith COMPANY El Paso Natural Gas Co.	Absolute Potential: 590 MCFPD; n L.													
AGENT and TITLE ii. P. Shackelford, Area Supt. WITNESSED Earl Smith COMPANY El Pago Natural Gas Co.					Por Cl.7	HANH	Name I Park	Mexico	-					
WITNESSED <u>Earl Smith</u> COMPANY <u>El Pago Natural Gas Co.</u>			TITLE		ii. P. Si	ackelfo	rd. Area	Supt			_			
COMPANY El Pago Matural Vas Co.	MITM	NESSED			Earl Smi	th								
	COM	PANY			El Paso	Natural	Gas Co.	MARKS						

2nd test slope greater than 1.000. Good pull down, alignment and spread. 1.000 was drawn through flow point corresponding to highest rale of flow.

INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

NOMENCLATURE

- Q \equiv Actual rate of flow at end of flow period at W. H. working pressure (P_W). MCF/da. @ 15.025 psia and 600 F.
- P_c = 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater.
- PwT Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- Pt Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- Pf Meter pressure, psia.
- $h_{\mbox{\scriptsize W}}\mbox{\footnotesize I}$ Differential meter pressure, inches water.
- $F_g = Gravity$ correction factor.
- F_t Flowing temperature correction factor.
- F_{pv} Supercompressability factor.
- n I Slope of back pressure curve.

Note: If $P_{\rm W}$ cannot be taken because of manner of completion or condition of well, then $P_{\rm W}$ must be calculated by adding the pressure drop due to friction within the flow string to $P_{\rm t}$.